

**AUTHORIZATION  
TO SEND TEST REPORTS  
TO EPA**

I HEREBY AUTHORIZE MYREN CONSULTING, INC. TO SEND THE APPROPRIATE COPIES OF THE TEST REPORT(S) FOR THE HEAT TECH HTP 26 STANDARD PELLET STOVE TO THE U.S. EPA.

Signature: 

Printed Name: Tom Basset

Title: Owner

Date: 1-15-16

PLEASE RETURN TO MYREN CONSULTING VIA EMAIL OR FAX AFTER SIGNING.

FAX: 509 684 3987

EMAIL: <myren.ben@gmail.com>

# Myren Consulting, Inc.

512 Williams Lake Road

Colville, WA 99114

Office: (509) 684-1154

Lab: (509) 685-9458

Fax: (509) 684-3987

email: <myren.ben@gmail.com>

---

Date: 10 January 2016

To: Tom Bassett, Heat Tech

From: Ben Myren

RE: Heat Tech HTP 26 Standard Pellet Stove Test Report

Please find enclosed your copy of the EPA test report for the HEAT TECH HTP 26 STANDARD pellet stove. Look over the info that is pertinent to your end, i.e., addresses, phone numbers, blueprints (especially), etc., to make certain that they are correct. If there are any corrections, call me and I will take care of them immediately. As soon as I receive the signed Authorization form, I will send the reports to EPA.

Remember to send in your EPA Wood Heater Certification Application to EPA ASAP. Here I am assuming the old Application still works.

If you have any questions or comments, call.

Regards, Ben

# Myren Consulting, Inc.

512 Williams Lake Road

Colville, WA 99114

Office: (509) 684-1154                      Lab: (509) 685-9458  
Fax: (509) 684-3987      email: <myren.ben@gmail.com>

PE 1.2 Sanchez Letter

26 December 2015

Dr. Rafael Sanchez, PhD.

U.S.EPA

Office of Enforcement and Compliance Assurance

Office of Compliance

William Jefferson Clinton Building, South

Room 7419D

1200 Pennsylvania Ave., N.W.

Washington, DC 20003

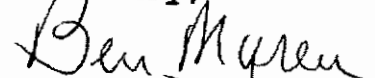
Dear Dr. Sanchez:

Please find enclosed the required two (2) copies of the certification test report for HEAT TECH HTP 26 STANDARD pellet stove. As the test results indicate, the unit's emissions are well below the EPA standard of 4.5 g/hr.

This is the first pellet stove report Myren Consulting, Inc. has submitted since the new NSPS took effect on May 15, 2015. While the report is basically organized like the reports submitted under the old NSPS, some parts of the report have been reorganized/ revised to insure compliance with the rules in the new NSPS. Thus look at the relevant pages, e.g., Individual Test Run Page Index, in the Introduction Section to find the required information.

If you or anyone else has any questions about the information or data in this test report, please contact me immediately.

Sincerely,



Alben T. Myren Jr.

President

ATM/im

# Myren Consulting, Inc.

512 Williams Lake Road  
Colville, WA 99114

Office: (509) 684-1154 Lab: (509) 685-9458  
Fax: (509) 684-3987 email: <myren.ben@gmail.com>

---

11 January 2010

EPA CBI Office  
Attn: Residential Wood Heater Compliance Program Lead  
1200 Pennsylvania Ave. NW  
Washington, D.C. 20004

Dear Dr. Sanchez:

RE: CBI INFORMATION FOR THE HEAT TECH HTP 26 STANDARD PELLET STOVE

Please find enclosed the required two (2) copies of the CBI for the test report for the HEAT TECH HTP 26 STANDARD pellet stove. The main test report has been sent under a separate cover to the following address:

Dr. Rafael Sanchez, PhD.  
U.S.EPA  
Office of Enforcement and Compliance Assurance  
Office of Compliance  
William Jefferson Clinton Building, South  
Room 7419D  
1200 Pennsylvania Ave., N.W.  
Washington, DC 20003

If you or anyone else has any questions about the CBI information in this test report, please contact me or Tom Bassett at HEAT TECH at 530 846 1985 immediately.

Sincerely,



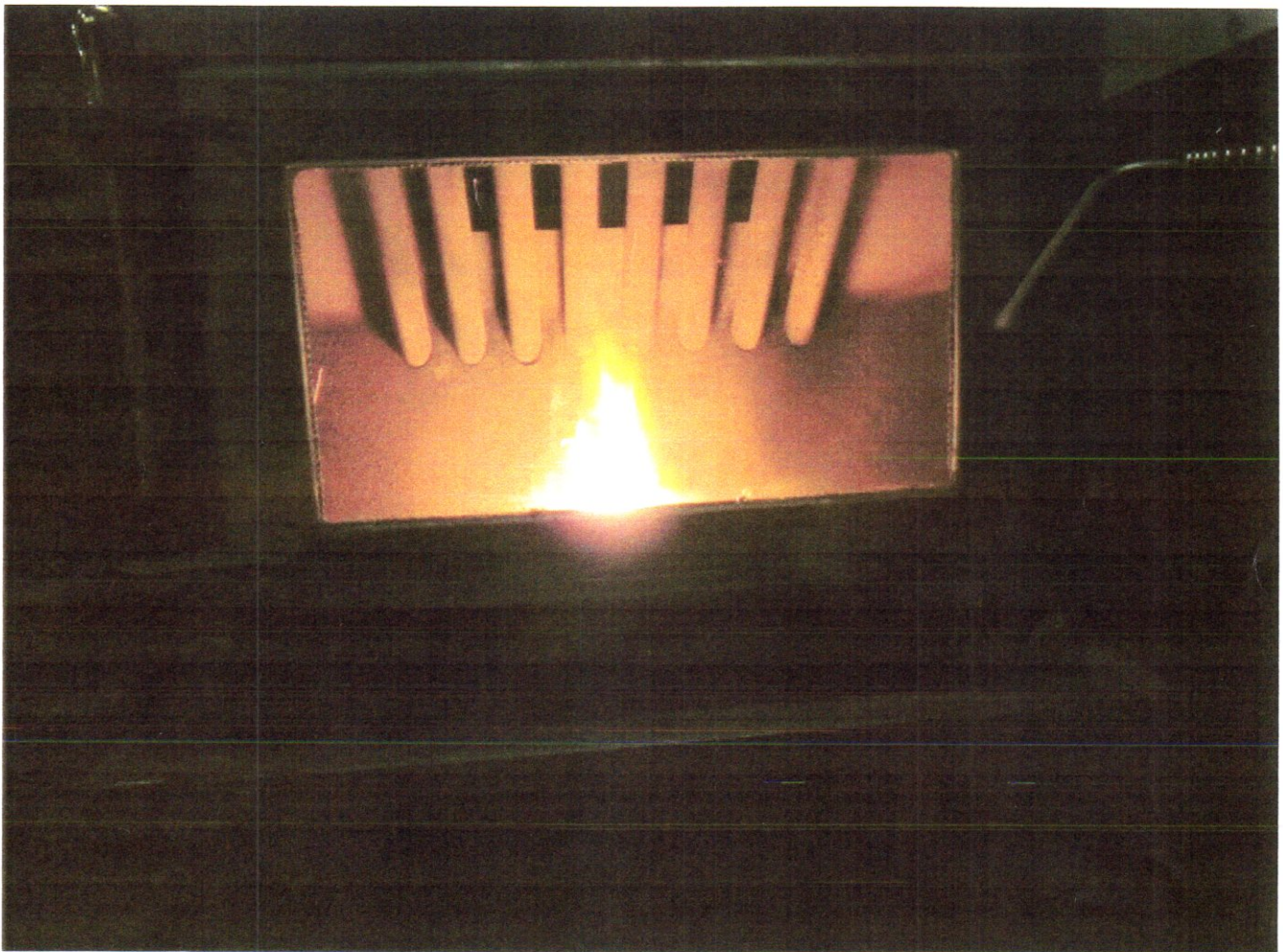
Alben T. Myren Jr.  
President  
ATM/im



**US EPA WOOD HEATER  
CERTIFICATION TEST REPORT**

**HEAT TECH  
HTP 26 STANDARD  
PELLET STOVE**

**DECEMBER 26, 2015**



**MYREN CONSULTING, INC.**

**OFFICE**

512 WILLIAMS LAKE ROAD  
COLVILLE, WA 99114  
PHONE 509-684-1154  
FAX 509-684-3987

**LABORATORY**

501 C WILLIAMS LAKE ROAD  
COLVILLE, WA 99114  
PHONE 509-685-9458  
EMAIL [myren.ben@gmail.com](mailto:myren.ben@gmail.com)

\*\*\*\*\*

**Confidential**

\*\*\*\*\*

**The data and information in this test report is confidential, proprietary information and is not to be released to and/or discussed with any party who is not authorized by the manufacturer or the testing laboratory to receive such data.**

\*\*\*\*\*

**Confidential**

\*\*\*\*\*

### Report Certification

The sampling and analysis for the appliance described in this report was carried out under my direction and supervision.

Date: 1/11/2016

Signature: Albert J. Meyer Jr.  
Title: President

I have reviewed all of the test data and test results found in this report and hereby certify that the test report is authentic and accurate.

Date: 1/11/2016

Signature: Albert J. Meyer Jr.  
Title: President

**PELLET STOVE  
TABLE OF CONTENTS**

p 1 of 1

Rev 0 12.15

<b>Introduction</b>	<b>Section(s)</b>	<b>Page (s)</b>
Title Page	Introduction	i
Confidentiality Statement		ii
Report Certification		iii
Table of Contents		iv
Testing Location and Personnel Information		v
Test Report (Data) Page Number Index		vi-vii
Individual Test Run Page Number Index		viii
Test Series Information and Discussion		ix
<b>Summary and Discussion of Results</b>		
Integrated Test Results	Data Summary	1
Particulate Sampling Train Performance		1
Test Data Summary		2-4
<b>Pellet Stove Aging Data</b>	<b>Aging</b>	<b>2</b>
<b>Individual Test Run ( Raw Data)</b>		
See Pellet Stove Test Run Page Index in the Introduction Section for a complete, sequential list of the data pages in the integrated test run.	Test Run	vari
<b>Calibration Data</b>		
See Test Report (Data) Page Number Index, Item 14, for a complete, sequential listing of the data in this section.	Cal Data	vari
<b>Stove QC</b>		
Pellet Stove Description	Stove QC	1
<b>Blueprints</b>		
Promotional (Sales) Brochure	Blueprints	vari
Laboratory verified blueprints		vari
<b>Manual</b>		
Manufacturer's Written Test Instructions	Manual	vari
Manufacturer's Owner's Manual		vari
<b>Storage</b>		
Storage Location/ Sealing Information	Storage	1
Photo of Sealed Stove		1

**TESTING LOCATION AND PERSONNEL INFORMATION**

**Unit Name: HEAT TECH HTP 26 STANDARD PELLET STOVE**

**Manufacturer Name: HEAT TECH**

**Manufacturer Address: PO BOX 727  
Biggs, CA 95917**

**Manufacturer Phone: 530 846 1985  
Fax:**

**Observers & Affiliation: None**

**SUPERVISOR: Ben Myren**

**MYREN CONSULTING'S LAB TEAM: Ilse Myren, Ben Myren, Eric Schaefer**

**LAB LOCATION: Myren Consulting's lab in Colville, WA**

**ELEVATION: ~ 1650 FEET**

**MYREN CONSULTING, INC.**

**LABORATORY  
501-C WILLIAMS LAKE ROAD  
COLVILLE, WA 99114  
509 685 9458  
509 684 3987(Fax)**

**OFFICE  
512 WILLIAMS LAKE ROAD  
COLVILLE, WA 99114  
509 684 1154  
email: <myren.ben@gmail.com>**

**Pellet Stove Test Report Page Number Index**

	<u>Section</u>	<u>Location</u>	
1. Integrated Test Results	Data Summary	Integrated Test Results	p. 1
2. Summary Table of Other Data	Data Summary	Data Summary Sheets	p. 2-4
3. Wood Heater Description	Stove QC	Wood Heater Description	p.1 (vari)
4. Manufacturer's Testing Instructions	Operators Manual	P. 1 of Section	vari
5. Test Camber Installation Description	Installation Description	Introduction	p. x
6. Pellet Stove Aging Documentation	Aging		p. 1-2
7. Pretest Burn Procedures	Individual Test Runs	Data Sheets	#9,13
8. Pretest Facility Measurements	Individual Test Runs	Data Sheets	#8, 16
9. Test Fuel Measurements			
A. Fuel Moisture	Individual Test Runs	Data Sheets	#11
10. Heater Operation and Air Supply Settings	Individual Test Run	Data Sheets	#9, 13
11. Calibrations			
A Platform Scale			
1. Semi Annual	Cal Data	P. 1	
2. Pre and Post Test	Individual Test Run	Data Sheet	#16
B. Analytical Balance			
3. Semi Annual	Cal Data	P. 3 (Variable)	
4. Pre Weighing Check	Individual Test Run	Data Sheet	#4-4
C. Temperature			
5. Thermometers	Cal Data	P. 5	
6. Thermocouple Readout(s)			
a. Semi Annual	Cal Data	P. 6	
b. Daily Check	Individual Test Run	Data Sheet	#16
D. Dry Gas Meters			
a. Semi Annual Calibration	Cal Data	P. 7 (Variable # of pp.)	
b. Post Test Audits	Cal Data	(Variable # of pp.)	
c. Transfer Meter Calibration	Cal Data	(Variable # of pp.)	
E. Miscellaneous Test Equipment			
a. Anemometer	Cal Data	P. 11	
b. Barometer	Cal Data	P. 11	
c. Draft/ Static Pressure Gauge	Cal Data	P. 11	

d. Humidity Gauge Calibration ( Sling Psychrometer)	Cal Data	P. 13
F. Combustion Gas (CO <sub>2</sub> , O <sub>2</sub> , CO) Train Response Check	Cal Data	P. 20
G. CO <sub>2</sub> Analyzer		
1. Calibration	Cal Data	P. 22
2. Pre and Post Test Zero/Span	Individual Test Run	Data Sheet #15-3
B. CO Analyzer		
1. Calibration	Cal Data	P. 24
2. Pre and Post Test Zero/Span	Individual Test Run	Data Sheet #15-1
C. Calibration Gas Certificates of Analysis		
15. Quality Checks		
A. Leak Checks		
1. Particulate Sampling Train	Individual Test Runs	P.1 of Data Sheet #2
2. Combustion Gas (CO <sub>2</sub> , O <sub>2</sub> , CO) (CEM) Train	Individual Test Runs	Data Sheet #16
B. Proportional Checks	Individual Test Runs	Table 1
16. Sample Calculations		
A. Dry Burn Rate	Individual Test Runs	Data Sheet # 8; Computer Printout
17. Raw Test Data	Individual Test Runs	Data Sheets #1-16
18. Analytical Data		
A. Filter and Beaker Tares	Individual Test Runs	Data Sheets #4-1, 4-2
B. Solvent Blanks	Individual Test Runs	Data Sheets #4-3, 5
C. Particulate Catches		
1. Gross	Individual Test Runs	Data Sheet #5
2. Blanks	Individual Test Runs	Data Sheet #5
3. Net	Individual Test Runs	Data Sheet #5
D. Constant Weight Weighings		
1. Tares	Individual Test Runs	Data Sheets # 4-1, 4-2
2. Finals	Individual Test Runs	Data Sheet #4-3
3. Analytical Balance QC Checks	Individual Test Runs	Data Sheet #4-4 (Variable pp.)



ASTM E2515/ EPA M5G-1 Individual Test Run Page Index (Pellet Stove)

The data sheets in the individual test runs are organized in the following sequence.

<u>Page Description</u>	<u># of Pages</u>
Filters photo	1
CSA B415.1-10 "Report" computer spreadsheet printout	Variable
CSA B415.1-10 "Data Input" computer spreadsheet printout	Variable
Dilution Tunnel Traverse data	1
Dilution Tunnel Gas Velocity and Volumetric Flow Rate Calculations	1
Train 1 Emission Rate/ Dilution Tunnel Calculations computer spreadsheet printout	Variable
Train 1 0-60 Minute Emission Rate/ Dilution Tunnel Calculations computer spreadsheet printout	Variable
Train 1 0-60 Minute Particulate Sampling data (Meter Box data)	Variable
Train 1 60 Minute Plus Particulate Sampling data (Meter Box data)	Variable
Filter Constant Tare Weight data	Variable
Beaker Constant Tare Weight data	Variable
Acetone Blank Beaker Constant Final Weight data	1
Train 1 0-60 Minute PM Sample Constant Final Weight data	1
Train 1 60 Minute Plus Constant Final Weight data	1
Train 1 Particulate Matter Catch Calculations	Variable
Train 2 Emission Rate/ Dilution Tunnel Calculations computer spreadsheet printout	Variable
Train 2 Particulate Sampling data (Meter Box data)	Variable
Train 2 PM Sample Constant Final Weight data	1
Train 2 Particulate Matter Catch Calculations	1
Train 3 Room Blank Sampling Rate and PM Concentration Calculations computer spreadsheet printout	Variable
Train 3 Particulate Sampling data (Meter Box data)	Variable
Train 3 PM Sample Constant Final Weight data	1
Train 3 Particulate Matter Catch Calculations	1
Analytical Balance QA/ QC data	Variable
Woodstove Data Sheet #8 Miscellaneous data	1
Woodstove Data Sheet #9 Pellet Stove Operating data	1
Woodstove Data Sheet #10 Preburn and Fuel Load Moisture Determination data	1
Woodstove Data Sheet #11 ASTM E2780 Fuel Load Calculations	1
Woodstove Data Sheet #13 Pre Burn Data	Variable
Woodstove Data Sheet #14 Burn Rate, Flue Gas and Temperature Data	Variable
Woodstove Data Sheet #15-1 CO <sub>2</sub> Pre and Post Test Zero/Span Audits	1
Woodstove Data Sheet #15-3 CO Pre and Post Test Zero/Span Audits	1
Woodstove Data Sheet #16 Quality Checks	1



## TEST SERIES INFORMATION AND DISCUSSION

MODEL LINE: HEAT TECH HTP 26 STANDARD PELLETT STOVE

TEST UNIT: HEAT TECH HTP 26 STANDARD PELLETT STOVE

Manufacturer: HEAT TECH

Date Received: 6/20/2015

Date(s) Aged: 7/1-7/3/2015, See AGING Section

Test Date(s): 7/28/2015

PM Sampling Method(s): ASTM E2515 using 4" filters (EPA M5G-1)

Operating and Fueling Protocol: EPA M28R, ASTM E2779

Number of Test Runs: 1

The Heat Tech HTP 26 Standard Pellet stove manufactured by Heat Tech located in Biggs, CA was tested by Myren Consulting, Inc. using the Environmental Protection Agency's (EPA) Test Method 28R, "Certification and Auditing of Wood Heaters", ASTM E2515-11, "Standard Test Method for Determination of Particulate Emissions Collected in a Dilution Tunnel" and ASTM E2779-10, "Standard Test Method for Determining Particulate Matter Emissions from Pellet Heaters". (See the Federal Register/ Vol.80, No.50/ Monday, March 16, 2015. [pp.13672-13753]). On March 28, 2015 Myren Consulting, Inc. requested approval from EPA to use four-inch filters when conducting all PM emission certification tests and received the approval to do so on April 7, 2015. Thus the PM sampling and PM sample processing procedures used during the certification tests found in this test report are what are found in EPA M5G-1 in the old NSPS. (See the Federal Register/ Vol.53, No.38/ Friday, February 26, 1988/ pp.5860-54926, especially in Method 5G in Appendix A on pp. 5884-5892.) The particulate matter (PM) emission data was calculated as specified in the Wood Heater New Source Performance Standard (NSPS) dated March 16, 2015. The percent overall efficiency (%OE) for the test run was calculated using the %OE algorithm found in CSA's B415.1-10.

All events and information pertinent to the test data are recorded on the data sheets for the test run, particularly on pp. 9, 13 and 14.

Any deviations made or noted from the promulgated methods other than those that were accepted and certified by EPA during the laboratory accreditation process are listed and discussed below. The Heat Tech HTP 26 Standard pellet stove was tested at Myren Consulting's lab in Colville, WA using Myren Consulting laboratory's lab accreditation. A copy of both Myren Consulting's old Lab Accreditation Certificate (#6) and new Lab Accreditation Certificate (#2) are included in the following pages because at the time the Heat Tech HTP 26 was tested, EPA had not yet been issued the new Lab Accreditation Certificate. (Myren Consulting, Inc. had formally notified EPA on February 15, 2015 that Myren Consulting, Inc. wished to continue as an accredited laboratory after the new NSPS went into effect.)

A brief note about how the four-inch (EPA M5G-1) particulate samples were processed is necessary to help the reviewer understand the net catch values. Experience has shown that the small portions of the filters that are left on the frits in the M5G-1 filter housing apparatus after the filters are removed are full of static electricity. When these small portions are removed to a plastic petri dish, they quickly adhere to the petri dish. Because trying to recapture these small pieces of filter material during weighing causes them to disintegrate into smaller and smaller pieces, which makes obtaining accurate catch weights difficult, it was decided to place this filter material in with the particulate captured with the acetone wash, where it shows up as catch. Some of the filter material was already following this pathway. Thus, there may be negative filter catch weights, particularly for the back half filters, that are used during the particulate emission rate calculation process. However, the filter material lost off the filters is accounted for in the acetone catch. The first page in the TEST RUN Section is a photo of the filters from the test run for this unit and shows this problem.

ASTM E2778-10 Equation 1 calls for a dry moisture content for the test fuel used during testing. There is no way to measure the moisture content of pellets on a dry basis. Instead one can determine the wet basis moisture content by drying a sample. This is what done and the data for this is on Data Sheet 11 in the test run. Once the wet basis moisture content is known, it is then possible to calculate the fuel burnt on a dry basis, which again is what was done. The dry burn rate (DBR) determined is the same. The revised procedures and equations used to determine the actual DBR are to be found on the page after Data Sheet 11.

The following pages contain: (1.) a discussion of test results, (2.) a diagram showing the height of the appliance and chimney used during testing (ICC EXCEL Pellet Pipe) and the location of the sampling ports in the chimney and (3.) a diagram of the EPA 6" diameter dilution tunnel used by Myren Consulting during EPA Certification testing, (4.) a copy of the letter from EPA granting Myren Consulting, Inc accreditation under the new NSPS, (5.) a copy of the old and new EPA Laboratory Accreditation Certificates for Myren Consulting's lab and (6.) a copy of the 30 day advance certification test notification sent to EPA for the week the unit was tested.

#### DISCUSSION:

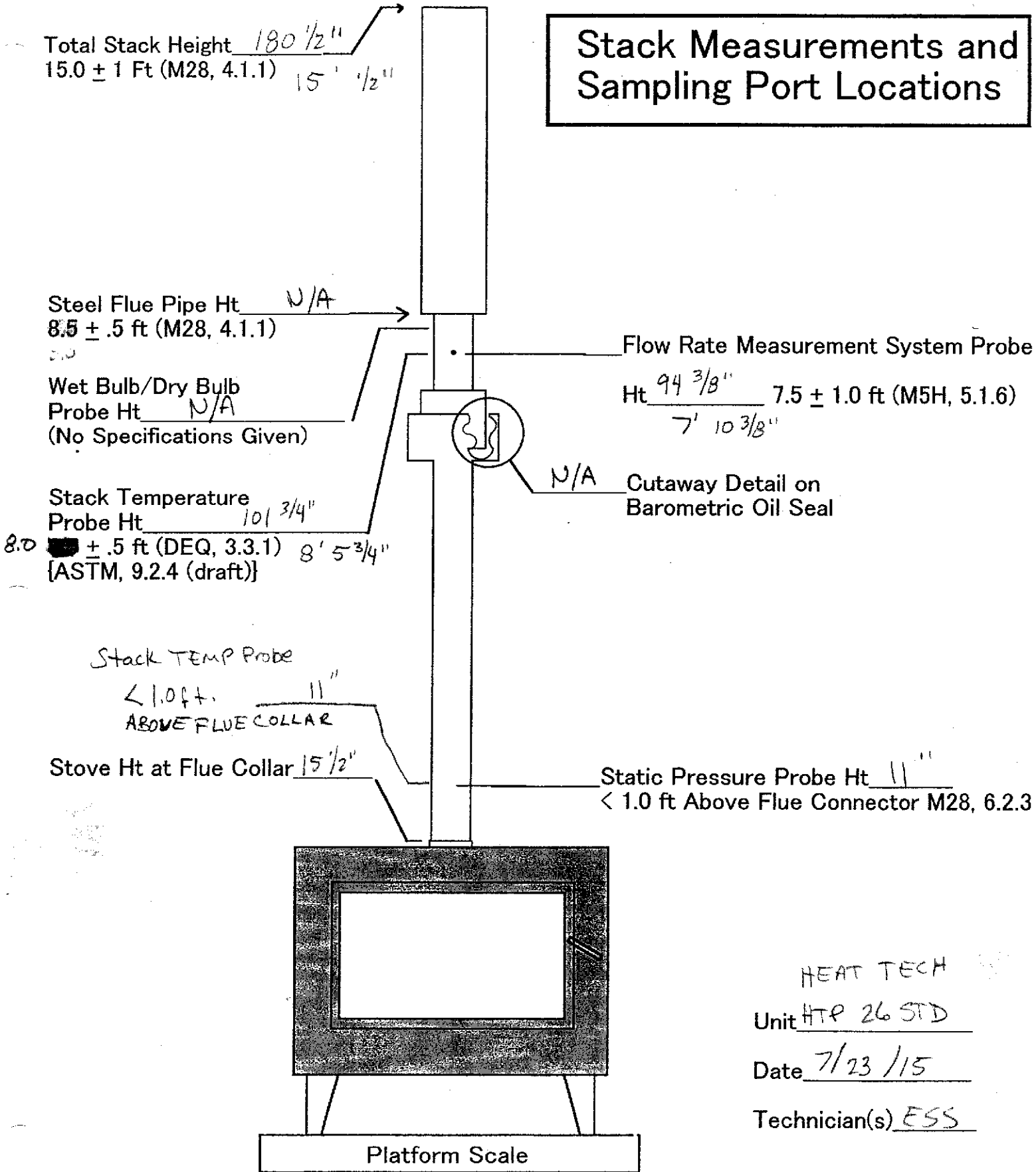
- (1.) The test series was done at Myren Consulting's lab in Colville, WA.
- (2.) The test series required 1 test run.
- (3.) As is noted in the cover letter for this report, this is the first pellet stove report Myren Consulting has submitted to EPA since the new NSPS went into effect. Thus, because the whole testing format for pellet stoves has changed, there are several revisions to the report format necessitated by the difference in rules and reporting requirements in the old NSPS versus the rules and reporting requirements in the new NSPS. Specifically the following changes have been made:
  - a. Because the pellet stove test is now an integrated sample test, there are no weighted average calculations because collecting the integrated sample "automatically" generates a "weighted average". Instead of the pages used to calculate a weighted average, there is now a single page titled *Integrated Test Results*, which reports the emission rate and overall efficiency (%OE) for the unit.
  - b. A new page has been added to the Data Summary Section (p. 2) which summarizes the PM Sampling Train Performance information and addresses the *Dual Train Comparison* criteria found in ASTM E2515 Section 11.7. The average emission rate calculated and reported on this new page using the data from the 2 PM sampling trains is then also reported on the page titled *Integrated Test Results*. Also reported on this page are the performance data for the "Room Blank" train and the PM emission rate (g/h) data for the 0-60 minute filter set from Train 1.

c. Section 60.534(d) requires that filter sets be changed (switched) at 1 h into a test run on one of the PM sampling trains. This was done on Train 1 during the test run. Thus there are additional data sheets in each test run for the 2 filter sets used in Train 1 to accomplish this requirement. There is also a photo of the filters from the test run in the section with the raw data sheets for the test run. As noted above, the PM emission rate for the first hour is reported on the computer spreadsheet for that PM sample and again in the Data Summary section itself.

d. ASTM E2515 requires 2 PM sampling trains and a third "Room Blank" train. That means there are also additional data sheets for Trains 2 and 3 in the section with the Raw Data sheets for the test run and in the Cal Data Section where the calibration and post test audit data is presented for the equipment used in all 3 of these trains.

Please look at the Table of Contents (p. iv), the Pellet Stove Test Report Page Number Index (pp. vi-vii) and the Individual Test Run Page Index (p. viii) to find any pages of interest. Or call Myren Consulting, Inc. at either 509 685 9458 or 509 684 1154 if further assistance is needed.

# Stack Measurements and Sampling Port Locations



HEAT TECH  
 Unit HTP 26 STD  
 Date 7/23/15  
 Technician(s) ESS

Stack is all 4" ICC Excel Pellet

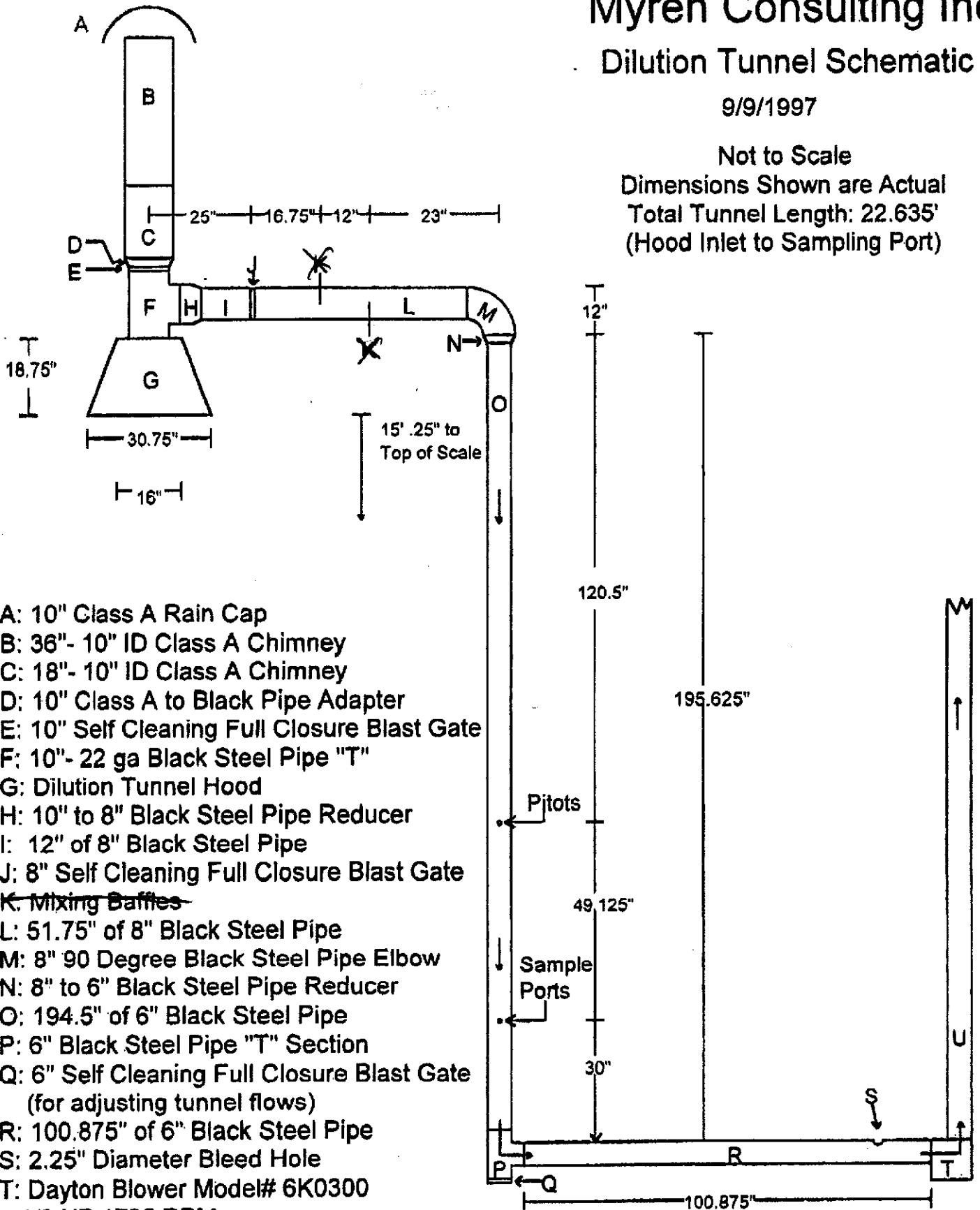
# Myren Consulting Inc

## Dilution Tunnel Schematic

9/9/1997

Not to Scale

Dimensions Shown are Actual  
Total Tunnel Length: 22.635'  
(Hood Inlet to Sampling Port)



- A: 10" Class A Rain Cap
- B: 36"- 10" ID Class A Chimney
- C: 18"- 10" ID Class A Chimney
- D: 10" Class A to Black Pipe Adapter
- E: 10" Self Cleaning Full Closure Blast Gate
- F: 10"- 22 ga Black Steel Pipe "T"
- G: Dilution Tunnel Hood
- H: 10" to 8" Black Steel Pipe Reducer
- I: 12" of 8" Black Steel Pipe
- J: 8" Self Cleaning Full Closure Blast Gate
- ~~K: Mixing Baffles~~
- L: 51.75" of 8" Black Steel Pipe
- M: 8" 90 Degree Black Steel Pipe Elbow
- N: 8" to 6" Black Steel Pipe Reducer
- O: 194.5" of 6" Black Steel Pipe
- P: 6" Black Steel Pipe "T" Section
- Q: 6" Self Cleaning Full Closure Blast Gate  
(for adjusting tunnel flows)
- R: 100.875" of 6" Black Steel Pipe
- S: 2.25" Diameter Bleed Hole
- T: Dayton Blower Model# 6K0300  
1/3 HP 1725 RPM
- U: 6" black Steel Pipe Exhaust



UNITED STATES ENVIRONMENTAL PROTECTION AGENCY  
RESEARCH TRIANGLE PARK, NC 27711

NOV 12 2015

OFFICE OF  
AIR QUALITY PLANNING  
AND STANDARDS

Ben Myren  
Myren Consulting, Inc.  
512 Williams Lake Road  
Coleville, WA 99114

Dear Mr. Myren:

Thank you for your recent inquiry regarding the United States Environmental Protection Agency (EPA) wood heater laboratory accreditation program. The review of your reaccreditation letter that you submitted November 10, 2015 is complete and acceptable. Enclosed is your current certificate of accreditation. Myren Consulting, Inc. is accredited under Subpart AAA 40 CFR Standards of Performance for New Residential Wood Heaters Sections (60.534, 60.535) and Subpart QQQQ 40 CFR Standards of Performance for New Residential Hydronic Heaters and Forced-Air Furnaces Sections (60.5476, 60.5477). Please follow the requirements for EPA Test Method 28R Certification and Auditing of Wood Heaters in Appendix A-8 to Part 60-Test Methods 26 through 30B. This approval expires on March 16, 2018, unless renewed by Myren Consulting, Inc.

As a condition of your lab accreditation, Myren Consulting, Inc. must abide by the following provisions:

- (i) Agree to participate biennially in an independently operated proficiency testing program with no direct ties to the laboratories participating;
- (ii) Agree to allow the EPA, regulatory agencies and certifying bodies access to observe certification testing;
- (iii) Agree to comply with calibration, reporting and recordkeeping requirements that affect testing laboratories; and
- (iv) Agree to perform a compliance audit test at the manufacturer's expense at the testing cost normally charged to such manufacturer if the laboratory is selected by the EPA to conduct a compliance audit test of the manufacturer's model line;
- (v) Have no conflict of interest and receive no financial benefit from the outcome of certification testing conducted pursuant to §60.5475;
- (vi) Agree to not perform initial certification tests on any models manufactured by a manufacturer for which the laboratory has conducted research and development design services within the last 5 years;
- (vii) Agree to seal any wood heater on which it performed certification tests, immediately upon completion or suspension of certification testing, by using a laboratory-specific seal.
- (viii) Agree to immediately notify the EPA of any suspended tests through email and in writing, giving the date suspended, the reason(s) why, and the projected date for restarting.

Emission test reports should be submitted to EPA's Office of Enforcement and Compliance Assurance, at one of the following addresses:



U.S. Postal Service

U.S. EPA  
Office of Enforcement and Compliance  
Assurance, Office of Compliance  
William Jefferson Clinton Building, South  
Mail Code 2227A  
1200 Pennsylvania Ave, NW  
Washington, DC 20003

Attn: Wood heater Certification Lead

Private Courier

U.S. EPA  
Office of Enforcement and Compliance  
Assurance, Office of Compliance  
William Jefferson Clinton Building, South  
Room 7419D  
1200 Pennsylvania Ave, NW  
Washington, DC 20003

Attn: Woodheater Certification Lead

I would like to thank you for your cooperation in the wood heater certification program.

Sincerely,



Steffan Johnson  
Measurement Technology Group

Enclosure (2)

cc.

Julius Banks, OECA (2227A)  
Rafael Sanchez, OECA (2227A)  
Adam Baumgart-Getz, OID (C304-05)  
Amanda Aldridge, OID (C304-05)  
David Cole, OID (C304-05)



# CERTIFICATE OF ACCREDITATION

This certifies that:



Myren Consulting, Inc

Has satisfied the requirements for laboratory accreditation for the certification of wood heaters pursuant to subpart AAA of 40 CFR Part 60, New Source Performance Standards For Residential Wood Heaters

June 5, 2012 - June 5, 2017

**EFFECTIVE DATE**

Connie Oldham  
**MEASUREMENT TECHNOLOGY GROUP  
GROUP LEADER**

Methods 5G, 28, 28A, 5H

**METHODS**

6

**CERTIFICATE NUMBER**

# Myren Consulting, Inc.

512 Williams Lake Road

Colville, WA 99114

Office: (509) 684-1154

Lab: (509) 685-9458

Fax: (509) 684-3987

email:myren.ben@gmail.com

---

DATE: 4 June 2015

TO: Dr. Rafael Sanchez, PhD., EPA

CC: Tom Bassett, Heat Tech

FROM: Ben Myren

RE: Wood Heater 30 Day Advance Certification Test Notification  
for the Heat Tech H.T.P. P 26 Standard

Section 60.534(e)(1) of the Wood Heater NSPS requires that EPA be notified at least 30 days in advance of the start or resumption of EPA Certification Testing for each specific model line. To comply with the above requirement, Myren Consulting, Inc. hereby notifies EPA that Myren Consulting, Inc., 512 Williams Lake Road, Colville, WA 99114 plans to start an EPA Certification Test series on the unit identified below.

UNIT: H.T.P. P 26 Standard pellet stove

Manufactured by:

Heat tech Industries, LLC.

PO Box 727

Biggs, CA 95917

P: 530 846 1985

Email: [sharletasgarden@gmail.com](mailto:sharletasgarden@gmail.com)

Website: [www.heattechstoves.com](http://www.heattechstoves.com)

starting sometime during the period beginning on :

Monday July 27, 2015.

The testing will be conducted at:

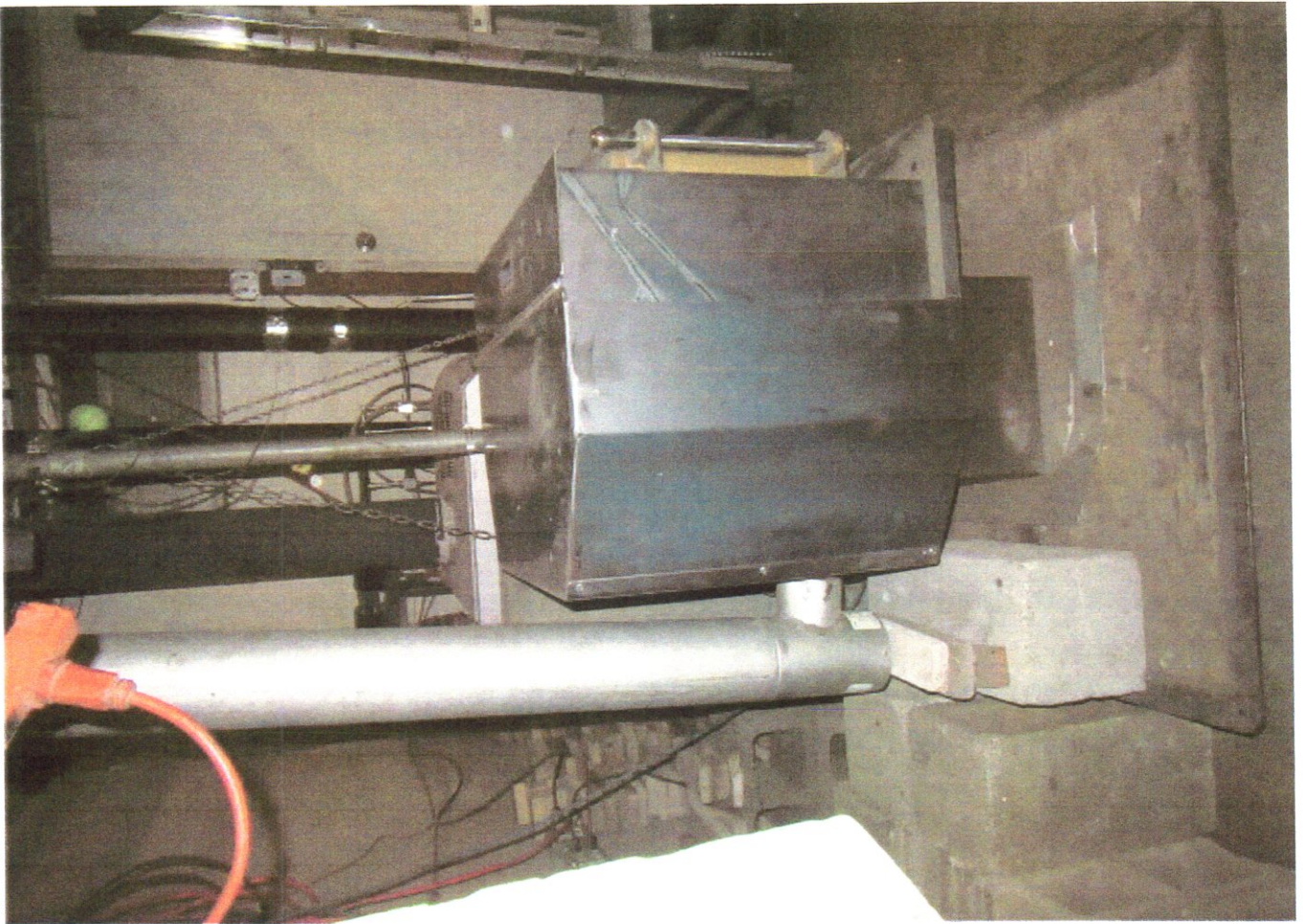
Myren Consulting, Inc's lab at 512 Williams Lake Road, Colville, WA 99114

3<sup>rd</sup> Party Certifying Entity (Probable)

PFS, 1507 Matt Pass, Cottage Grove, WI 53527 P: 608 839 1085

If you have any questions about this notification, contact me immediately.







**EPA  
PELLET STOVE  
INTEGRATED TEST RESULTS**

The integrated average particulate matter (PM)  
emission rate for the

**HEAT TECH HTP 26 STANDARD PELLET STOVE**

is

**1.9675 g/h.**

The integrated average overall HHV efficiency (%OE)  
for the

**HEAT TECH HTP 26 STANDARD PELLET STOVE**

is

**66.4%.**

The integrated average overall LHV efficiency (%OE)  
for the

**HEAT TECH HTP 26 STANDARD PELLET STOVE**

is

**71.8%.**

SUMMARY OF ASTM E2515 PARTICULATE EMISSIONS SAMPLING TRAIN PERFORMANCE

RUN #	DBR (kg/hr)	T1					T2					Avg. g/h.	% DIFF
		CATCH (mg)	SAMPLE RATE (cfm)	SAMPLE VOL (dscf)	AVG. % PROP	EMISSIONS (g/h)	CATCH (mg)	SAMPLE RATE (cfm)	SAMPLE VOL (dscf)	AVG. % PROP	EMISSIONS (g/h)		
EPA 1	0.862	19.0	.538	177.727	99.860	1.975	17.8	.539	176.892	99.875	1.960	1.9675	0.38

SUMMARY OF ASTM E2515 AMBIENT AIR  
(ROOM BLANK) SAMPLING TRAIN PERFORMANCE

RUN #	CATCH (mg)	SAMPLE RATE (cfm)	SAMPLE VOL. (dscf)	AMBIENT PM CONCENTRATION (mg/dscf)
EPA 1	1.6	.528	172.997	.009249

TRAIN 1 0-60 MINUTE  
DBR and PM EMISSIONS

Run #	DBR (kg/h)	EMISSIONS g/h
EPA 1	1.369	0.274

## Woodstove Data Summary

	Run #	1							
<b>Particulate Emissions:</b>									
Emission Rate:		<u>1.9675</u>							g/hr
Emission Factor:		<u>2.2815</u>							g/kg
(Dry fuel weight basis)									
<b>Efficiency Values: (CSA B415.10-1)</b>									
Combustion Efficiency:		<u>99.5</u>							%
Heat Transfer Efficiency: HHV:		<u>67.0</u>							%
Heat Transfer Efficiency: LHV:		<u>72.1</u>							%
Overall Efficiency: HHV:		<u>66.4</u>							%
Overall Efficiency: LHV:		<u>71.8</u>							%
<b>Heat Output:</b>									
Avg. EPA Btu/hr. for test cycle		<u>12,874</u>							Btu/hr.
Avg. B415 Btu/hr. for test cycle		<u>10,762</u>							Btu/hr.
<b>Fuel Burn Rates:</b>									
Avg. Dry Burn Rate (Wet Basis)		<u>.915</u>							kg/hr.
Avg. Dry Burn Rate (Dry Basis)		<u>.862</u>							kg/hr.
<b>PM Sampling Parameters:</b>									
Avg. Tunnel Flow(Qsd):		<u>139.060</u>							dscfm
Avg. Tunnel Velocity(Vs):		<u>812.545</u>							ft./min.
Pitot Correction Factor:		<u>.97700</u>							
Total Sample Volume:	T1	<u>177.727</u>	T2	<u>176.892</u>					dscf
Avg. Sampling Flow Rate:		<u>.538</u>		<u>.539</u>					cfm
Avg. % Proportionality:		<u>99.860</u>		<u>99.875</u>					%
Total Particulate Catch:		<u>18.0</u>		<u>17.8</u>					mg







## **AGING DATA**

**The Heat Tech HTP 26 Standard Pellet Stove was aged by Myren Consulting, Inc. The Aging installation configuration was the same as the installation used during certification testing. During Aging the stove was run on the Medium setting used during certification testing and the temperature and the (wet) burn rate data were collected using a Data Acquisition System (DAS). The Aging data was then transferred from the DAS spreadsheet to the Aging data pages in this section.**

PELLET STOVE AGING DATA  
 Woodstove Test Data Sheet #25P  
 WST5-Form 3A, Rev 12/15

Unit: HEAT Tech HTP 26 S70  
 Date(s): 7/1 - 7/3/15  
 Technicians: ATM ESS  
 Page: 1 of 2

T/C# 1

HOUR #	2015 DATE	TIME	POUNDS BURNT	STACK TEMP	COMMENTS
1	7/1	1127	2.0	299	Fire Started @ 10:27
2		1227	2.1	320	
3		1327	2.2	318	
4		1427	2.3	339	
5		1527	2.4	343	Added fuel @ 1549
6		1627	1.7	344	
7		1727	2.4	343	
8		1827	2.4	352	
9		1927	2.3	346	
10		2027	2.3	344	
11		2127	2.2	340	
12		2227	2.2	328	
13	✓	2327	2.2	339	
14	7/2	0027	2.3	329	
15		0127	2.2	307	
16		0227	2.2	327	
17		0327	2.3	327	
18		0427	2.2	318	
19		0527	2.0	280	
20		0627	2.1	303	
21		0727	2.0	298	
22		0827	2.0	290	Added Fuel @ 911
23		0927	1.7	255	
24		1027	2.2	318	
25		1127	2.3	336	
26		1227	2.3	327	
27		1327	2.5	350	
28		1427	2.6	354	Added fuel @ 1507
29	✓	1527	2.6	357	





# MYREN CONSULTING, INC

**Manufacturer:** HEAT TECH  
**Model:** TP 26 STANDARD  
**Date:** 7.28.15  
**Run:** EPA 1  
**Control #:**  
**Test Duration:** 360  
**Output Category:** VARIABLE

**Technicians:** ATMYREN  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

**Test Results in Accordance with CSA B415.1-09**

	HHV Basis	LHV Basis
Overall Efficiency	66.4%	71.8%
Combustion Efficiency	99.5%	99.5%
Heat Transfer Efficiency	67%	72.1%

Output Rate (kJ/h)	11,345	10,762	(Btu/h)
Burn Rate (kg/h)	0.86	1.90	(lb/h)
Input (kJ/h)	17,088	16,209	(Btu/h)

Test Load Weight (dry kg)	5.18	11.41	dry lb
MC wet (%)	5.73		
MC dry (%)	6.08		
Particulate (g)	4.5909		
CO (g)	106		
Test Duration (h)	6.00		

Emissions	Particulate	CO
g/MJ Output	0.07	1.56
g/kg Dry Fuel	0.89	20.53
g/h	0.77	17.71
lb/MM Btu Output	0.16	3.63

Air/Fuel Ratio (A/F)	35.66
----------------------	-------

VERSION: 2.2 12/14/2009

Manufacturer: HEAT TECH  
 Model: HTP 26 STANDARD  
 Date: 7.28.15  
 Run: EPA 1  
 Control #:  
 Test Duration: 360  
 Output Category: VARIABLE

Appliance Type: NON CAT (Cat, Non-Cat, Pellet)

Temp. Units F (F or C)  
 Weight Units lb (kg or lb)

Default Fuel Values  
 D. Fir 19,810 19,887  
 Oak  
 HHV (kJ/kg) 19,810 19,887  
 %C 48.73 50  
 %H 6.87 6.6  
 %O 43.9 42.9  
 %Ash 0.5 0.5

Wood Moisture (% wet): 5.73  
 Load Weight (lb wet): 12.10  
 Burn Rate (dry kg/h): 0.86  
 Total Particulate Emissions: 4.5909 g

Fuel Data  
 D. Fir  
 HHV 19,810 kJ/kg  
 %C 48.73  
 %H 6.87  
 %O 43.9  
 %Ash 0.5

Note 1: For other fuels, use the heating value and fuel composition determined by analysis of fuel sample in accordance with Clause 9.2.

Averages 0.05 3.38 17.53 299.30 80.49

Temp. (°F)  
 Elapsed Fuel Weight Flue Gas Composition (%) Flue Room  
 Time (min) Remaining (lb) CO CO<sub>2</sub> O<sub>2</sub> Gas Temp

Elapsed Time (min)	Fuel Weight Remaining (lb)	CO	CO <sub>2</sub>	O <sub>2</sub>	Flue Gas Temp	Room Temp
0	12.10	0.01	3.98	16.96	371.0	74.0
10	11.60	0.01	4.59	16.35	377.0	75.0
20	11.00	0.02	6.08	14.85	385.0	76.0
30	10.50	0.02	3.73	17.20	385.0	76.0
40	10.00	0.02	4.88	16.05	396.0	76.0
50	9.40	0.09	4.46	16.44	383.0	78.0
60	8.90	0.01	5.36	15.58	399.0	77.0
70	8.40	0.01	5.16	15.78	373.0	78.0
80	8.00	0.01	4.53	16.41	353.0	78.0
90	7.60	0.04	2.33	18.59	340.0	79.0
100	7.20	0.06	2.98	17.93	338.0	79.0
110	6.80	0.04	2.66	18.26	336.0	80.0
120	6.30	0.01	4.51	16.43	338.0	80.0
130	5.90	0.10	3.26	17.63	337.0	80.0
140	5.50	0.06	4.06	16.85	342.0	80.0
150	5.10	0.05	5.08	15.84	342.0	80.0
160	4.70	0.03	4.71	16.22	339.0	80.0
170	4.30	0.07	2.11	18.80	333.0	81.0
180	3.90	0.02	4.51	16.42	342.0	81.0
190	3.70	0.03	3.68	17.25	289.0	80.0
200	3.40	0.12	1.93	18.95	251.0	83.0
210	3.20	0.03	3.51	17.42	245.0	82.0
220	3.00	0.06	2.68	18.23	250.0	83.0
230	2.80	0.11	2.38	18.51	239.0	83.0
240	2.60	0.14	1.88	18.99	231.0	83.0
250	2.40	0.04	3.03	17.89	230.0	83.0
260	2.10	0.09	1.53	19.37	225.0	83.0
270	1.90	0.06	2.23	18.68	223.0	83.0
280	1.70	0.06	2.31	18.60	228.0	83.0
290	1.50	0.09	0.96	19.94	210.0	83.0
300	1.30	0.02	4.08	16.85	238.0	83.0
310	1.10	0.10	2.18	18.71	228.0	83.0
320	0.90	0.02	4.83	16.10	248.0	83.0
330	0.70	0.06	2.48	18.43	235.0	83.0
340	0.40	0.10	1.16	19.73	218.0	83.0
350	0.20	0.04	2.66	18.26	241.0	83.0
360	0.00	0.06	2.71	18.20	236.0	83.0

Note 2: In cases where the "Fuel Weight Remaining" is the same for three or more readings in a row, a "divide by zero error" will occur in the calculation sheet. In such cases, adjust the weight values by interpolation between the first occurrence and the next reading showing a decrease in weight.

# MYREN CONSULTING, INC

**Manufacturer:** HEAT TECH  
**Model:** FP 26 STANDARD  
**Date:** 7.28.15  
**Run:** EPA 1  
**Control #:**  
**Test Duration:** 60  
**Output Category:** VARIABLE

**Technicians:** ATMYREN  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

## Test Results in Accordance with CSA B415.1-09

	HHV Basis	LHV Basis
<b>Overall Efficiency</b>	64.9%	70.2%
<b>Combustion Efficiency</b>	99.5%	99.5%
<b>Heat Transfer Efficiency</b>	65%	70.5%

<b>Output Rate (kJ/h)</b>	17,606	16,701	<b>(Btu/h)</b>
<b>Burn Rate (kg/h)</b>	1.37	3.02	<b>(lb/h)</b>
<b>Input (kJ/h)</b>	27,114	25,721	<b>(Btu/h)</b>

<b>Test Load Weight (dry kg)</b>	1.37	3.02	<b>dry lb</b>
<b>MC wet (%)</b>	5.73		
<b>MC dry (%)</b>	6.08		
<b>Particulate (g)</b>	0.6392		
<b>CO (g)</b>	12		
<b>Test Duration (h)</b>	1.00		

Emissions	Particulate	CO
<b>g/MJ Output</b>	0.04	0.69
<b>g/kg Dry Fuel</b>	0.47	8.87
<b>g/h</b>	0.64	12.14
<b>lb/MM Btu Output</b>	0.08	1.60

<b>Air/Fuel Ratio (A/F)</b>	25.78
-----------------------------	-------

VERSION: 2.2

12/14/2009

Manufacturer: HEAT TECH

Appliance Type: NON CAT (Cat, Non-Cat, Pellet)

Model: HTP 26 STANDARD

Date: 7.28.15

Run: EPA 1

Control #:

Test Duration: 60

Output Category: VARIABLE

Temp. Units F (F or C)  
Weight Units lb (kg or lb)

**Default Fuel Values**

	D. Fir	Oak
HHV (kJ/kg)	19,810	19,887
%C	48.73	50
%H	6.87	6.6
%O	43.9	42.9
%Ash	0.5	0.5

Wood Moisture (% wet): 5.73  
Load Weight (lb wet): 3.20  
Burn Rate (dry kg/h): 1.37  
Total Particulate Emissions: 0.6392 g

**Fuel Data**

	D. Fir	
HHV	19,810	kJ/kg
%C	48.73	
%H	6.87	
%O	43.9	
%Ash	0.5	

Note 1: For other fuels, use the heating value and fuel composition determined by analysis of fuel sample in accordance with Clause 9.2.

Averages 0.03 4.73 16.20 385.14 76.00  
Temp. (°F)

Elapsed Time (min)	Fuel Weight Remaining (lb)	Flue Gas Composition (%)			Flue Gas Temp	Room Temp
		CO	CO <sub>2</sub>	O <sub>2</sub>		
0	3.20	0.01	3.98	16.96	371.0	74.0
10	2.70	0.01	4.59	16.35	377.0	75.0
20	2.10	0.02	6.08	14.85	385.0	76.0
30	1.60	0.02	3.73	17.20	385.0	76.0
40	1.10	0.02	4.88	16.05	396.0	76.0
50	0.50	0.09	4.46	16.44	383.0	78.0
60	0.00	0.01	5.36	15.58	399.0	77.0

Note 2: In cases where the "Fuel Weight Remaining" is the same for three or more readings in a row, a "divide by zero error" will occur in the calculation sheet. In such cases, adjust the weight values by interpolation between the first occurrence and the next reading showing a decrease in weight.



MYREN CONSULTING, INC.

Dilution Tunnel Traverse Data with 8  
Traverse Points Rev: 1.7.12

Unit: HEAT Tech HTP 26 STD

Run #: EPA 1

Date: 7/28/15

Technicians: ADM ESS

Point	Location	$\Delta p$	$\sqrt{\Delta p_{trav}}$	$\Delta p$	$\sqrt{\Delta p_{cent}}$	$T_{trav}$	$T_{cent}$	$P_g$
W-1	0.5"	<u>.035</u>	<u>.187</u> X			<u>110</u>		
2	1.5	<u>.038</u>	<u>.195</u> X			<u>111</u>		
Center	Center			<u>.040</u>	<u>.200</u> ✓		<u>111</u>	
3	4.5	<u>.041</u>	<u>.202</u> X			<u>111</u>		
4	5.5	<u>.040</u>	<u>.200</u> X			<u>112</u>		
S-1	0.5	<u>.037</u>	<u>.192</u> X			<u>112</u>		
2	1.5	<u>.040</u>	<u>.200</u> X			<u>112</u>		
Center	Center			<u>.040</u>	<u>.200</u> ✓		<u>112</u>	
3	4.5	<u>.039</u>	<u>.197</u> X			<u>112</u>		
4	5.5	<u>.036</u>	<u>.190</u> X			<u>112</u>		
	Totals		<u>1.563</u> X		<u>.400</u> X	<u>892</u> X	<u>223</u> ✓	
	Average		<u>.1954</u> X		<u>.2000</u> ✓	<u>111.5</u> X	<u>111.5</u> X	
						<u>5715</u> X	<u>5715</u> X	

$^{\circ}R = (^{\circ}F + 460)$

$BP = \underline{28.59} \text{ "Hg}$      $Ps = BP + (-Pg/13.6) = \underline{28.59} + (\underline{\quad} / 13.6) = \underline{28.59} \text{ "Hg}$

LEAK CHECKS: Manometer Level: OK ✓    Zeroed: OK ✓    Tech: ESS

Pg Leg: Pre Test: Pressure: +.250 " H<sub>2</sub>O Movement: .000 " H<sub>2</sub>O Tech: ESS 4.500/1000 AIR

Post Test: Pressure: -.180 " H<sub>2</sub>O Movement: .000 " H<sub>2</sub>O Tech: ESS 4.100/1000 AIR

Velocity Head Leg: Pre Test: Pressure: +.010 " H<sub>2</sub>O Movement: .000 " H<sub>2</sub>O Tech: ESS 3.600/1000 AIR

Post Test: Pressure: -.003 " H<sub>2</sub>O Movement: .000 " H<sub>2</sub>O Tech: ESS 3.800/1000 AIR



DILUTION TUNNEL GAS VELOCITY & VOLUMETRIC FLOW RATE CALCULATIONS Rev 1/7/12

UNIT: HEAT Tech HTP2680 DATE: 7/28/15 RUN #: LPA1 TECHNICIAN(S): ATM ESS

Average Gas Velocity in the Dilution Tunnel Vstrav (EPA M2 eqn 2-9, ASTM E 2515 EQN 7)

$$(9) V_{strav} = (85.49) \underbrace{(0.99)}_{(2)} \underbrace{cp}_{(2)} \left( \underbrace{.1954}_{(2)} \bar{X} \sqrt{\Delta P} \text{ "H}_2\text{O} \right) \sqrt{\frac{\frac{571.5}{(0)} T_s \text{ }^\circ\text{A}}{\left( \frac{28.59}{(2)} \text{ Ps "Hg} \right) \left( \frac{28.0}{78} \text{ lb./ lb. mole} \right) (2)}} = \underline{13.78259} \text{ fps}$$

$$(9A) V_s = \left( \frac{13.78259}{(2)} \text{ fps} \right) (60) = \underline{826.955} \text{ fpm}$$

EQN. 2-7 Gas Velocity in the Center of the Dilution Tunnel - Vscent (ASTM E 2515-07 EQN 7)

$$(9) V_{scent} = (85.49) \underbrace{(0.99)}_{(2)} \underbrace{cp}_{(2)} \left( \underbrace{.2000}_{(2)} \bar{X} \sqrt{\Delta P} \text{ "H}_2\text{O} \right) \sqrt{\frac{\frac{571.5}{(0)} T_s \text{ }^\circ\text{A}}{\left( \frac{28.59}{(2)} \text{ Ps "Hg} \right) \left( \frac{28.0}{78} \text{ lb./ lb. mole} \right) (2)}} = \underline{14.10704} \text{ fps}$$

$$(9A) V_s = \left( \frac{14.10704}{(2)} \text{ fps} \right) (60) = \underline{846.423} \text{ fpm}$$

ASTM E 2515-07 EQN 1 Adjustment Factor for center of Tunnel Pitot Tube Location

$$F_p = V_{strav} / V_{scent} = \underline{13.78259} \div \underline{14.10704} = \underline{.97700}$$

EQN. 2-8 Average Stack Gas Dry Volumetric Flow Rate Qstd (ASTM E 2515-07 EQN 3)

$$Q_{sd} = 3600 \left( 1 - \frac{0.0}{(2)} B_{ws} \right) \left( \frac{13.78259}{(2)} \text{ fps} \right) \left( \frac{.1963}{(3)} \text{ ft}^2 \right) \left[ (528 \text{ }^\circ\text{A}) \left( \frac{28.59}{(2)} \text{ Ps "Hg} \right) / \left( \frac{571.5}{(0)} T_s \text{ }^\circ\text{A} \right) (29.92 \text{ " Hg}) \right] = \underline{8426.551} \text{ dscfhr (or dscfh)}$$

$$(10A) \frac{8426.551}{(1)} \text{ dscfhr} \div 60 = \underline{140.443} \text{ dscfm (or dscfm)}$$

Note: Number in { } under blank lines denotes number of decimals to be used. If a blank calls for an answer already calculated, use the number of decimals previously specified for that answer.







Black Round Top

T1  
0-60

METHOD 5G-1

PARTICULATE SAMPLING DATA

Rev. 10/09

DATE: 7/28/15 PAGE 1 OF 2 UNIT: HENT Tech <sup>HTP</sup> 26570 RUN: EPA 1

METER BOX: 456-P METER Y: 1.0066 FILTER #'S: (F) 713 (R) 713

.681/.636  
PRE TEST LEAK CHECK: .005 CFM @ -15.5 IN HG FILTER SIZE: 110 mm  
.717/.7175

POST TEST LEAK CHECK: .0025 CFM @ -10.25 IN HG PROBE ID #:       
PROBE LENGTH      IN

TIME		METER READING	PITOT		TUNNEL TEMP	METER TEMP	GAS METER	VAC
CLOCK	ELAPSED	(ft <sup>3</sup> )	ΔP	Pg	(°F)	(°F)	Δh	(in Hg)
1300	00	622.900	.039		113	72	.90	-1.5
10	10	628.240	.039		113	75	.90	-1.5
20	20	633.528	.039		114	79	.90	-1.5
30	30	638.798	.039		115	83	.90	-1.5
40	40	644.164	.039		115	85	.90	-1.5
50	50	649.535	.039		116	88	.90	-1.5
1400	60	654.926	.038		117	90	.90	-1.5
	70							
	80							
	90							
	00							
	10							
	20							
	30							
	40							
	50							
	60							
	70							
	80							
	90							

BP

<u>00</u>	<u>28.59</u>	<u>    </u>	<u>    </u>
<u>60</u>	<u>28.59</u>	<u>    </u>	<u>    </u>
<u>    </u>	<u>    </u>	<u>    </u>	<u>    </u>
<u>    </u>	<u>    </u>	<u>    </u>	<u>    </u>
AVG. =		<u>28.59</u>	<u>    </u>

Pre Test Filter  
Check Weighing  
F .6510  
R .6498

End of Test Weight  
F .6528 R .6462  
.6511 .6496

1.7



white Rnd Top

T1  
60+

METHOD 5G-1

PARTICULATE SAMPLING DATA

Rev. 10/09

DATE: 7/28/15 PAGE 1 OF 2 UNIT: Heat Tech <sup>HTP</sup> 26 STD RUN: EPA 1

METER BOX: 456-P METER Y: 1.066 FILTER #'S: (F) 708 (R) 709

.554/.560

FILTER/ O-RING ID #: \_\_\_\_\_

PRE TEST LEAK CHECK: .006 CFM @ -15.5 IN HG FILTER SIZE: 110 mm

PROBE ID #: \_\_\_\_\_

POST TEST LEAK CHECK: \_\_\_\_\_ CFM @ \_\_\_\_\_ IN HG PROBE LENGTH 21.5 IN

TIME		METER READING (ft <sup>3</sup> )	PITOT		TUNNEL TEMP (°F)	METER TEMP (°F)	GAS METER Δh	VAC (in Hg)
CLOCK	ELAPSED		ΔP	Pg				
1400	00	654.926	.038		117	90	.90	-1.5
	10	660.365	.039		115	92	.90	-1.5
	20	665.739	.039		113	93	.90	-1.5
	30	671.141	.039		112	93	.90	-1.5
	40	676.547	.039		112	94	.90	-1.5
	50	681.938	.039		112	95	.90	-1.5
1500	(60)	687.328	.039		113	95	.90	-1.5
	10	692.714	.039		114	96	.90	-1.5
	20	698.091	.039		113	97	.90	-1.5
	30	703.465	.039		113	97	.90	-1.5
	40	708.832	.039		113	97	.90	-1.5
	50	714.204	.039		113	97	.90	-1.5
1600	(120)	719.575	.039		113	98	.90	-1.5
	10	724.948	.039		105	98	.90	-1.5
	20	730.316	.039		102	98	.90	-1.5
	30	735.720	.039		101	98	.90	-1.5
	40	741.120	.039		102	98	.90	-1.5
	50	746.519	.039		101	98	.90	-1.5
1700	(80)	751.923	.039		100	99	.90	-1.5
	10	757.331	.039		100	99	.90	-1.5

BP

00	28.59	<del>300</del>	28.56
60	28.59	_____	_____
120	28.58	_____	_____
180	28.57	_____	_____
240	28.56	AVG.=	28.575

Pre Test Filter  
Check Weighing  
F .6467  
R .6499

End of Test Weight  
F .6524 R .6497  
.6467 .6497

127

0

Run = 28.577



white Rnd Top

TI  
60+

METHOD 5G | PARTICULATE SAMPLING DATA

Rev. 10/09

DATE: 7/28/15 PAGE 2 OF 2 UNIT: HEAT Tech <sup>HTP</sup><sub>26</sub><sub>570</sub> RUN: EPA 1

METER BOX: 45G-P METER Y: 1.066 FILTER #'S: (F) 708 (R) 709

PRE TEST LEAK CHECK: .006 CFM @ -15.5 IN HG FILTER SIZE: 110 mm

POST TEST LEAK CHECK: .000 CFM @ -10.2 IN HG PROBE LENGTH 21.5 IN

TIME		METER READING (ft <sup>3</sup> )	PITOT		TUNNEL TEMP (°F)	METER TEMP (°F)	GAS METER Δh	VAC (in Hg)
CLOCK	ELAPSED		ΔP	Pg				
1720	200	762.734	.039		99	99	.90	-1.5
30	210	768.142	.039		98	99	.90	-1.5
40	220	773.549	.039		99	99	.90	-1.5
50	230	778.927	.039		98	99	.90	-1.5
1800	240	784.313	.039		98	99	.90	-1.5
10	250	789.697	.039		98	99	.90	-1.5
20	260	795.076	.039		99	99	.90	-1.5
30	270	800.460	.039		99	99	.90	-1.5
40	280	805.847	.039		98	99	.90	-1.5
50	290	811.232	.039		99	99	.90	-1.5
1900	300	816.624	.039		99	98	.90	-1.5
	10							
	20							
	30							
	40							
	50							
	60							
	70							
	80							
	90							

BP

00	28.59	300	28.56
60	28.59		
120	28.58		
180	28.57		
240	28.56	AVG. =	28.575

Pre Test Filter  
Check Weighing  
F .6467  
R .6499

End of Test Weight  
F .6594 R .6497  
.6467 .6497

Run = 28.577



Woodstove Data Sheet #4-1: Initial Filter Weights (Tare Weights)

Into Dessicator: Date 6/20/15 Time 1245 By ATM Front Half  Back Half

Manufacturer: PALL Size: 110 mm Lot.No.: T41116 Grade: A/E Glass 1.0µm

Balance Used: Sartorius Model: CP224S SN: 24850860

Filter #	First Wt	Date	Time	By	Second Wt	Date	Time	By	Third Wt	Date	Time	By
701	.6445	6/25	1513	ESS	.6442	7/8	11:33	ATM	.6442	7/14	1523	ESS
702	.6466		1512	ESS	.6462		11:35	ATM	.6462		1524	ESS
703	.6460		1511	ESS	.6455		11:37	ATM	.6455		1525	ESS
704	.6476		1510	ESS	.6472		11:39	ATM	.6473		1526	ESS
705	.6450		1509	ESS	.6444		11:41	ATM	.6445		1527	ESS
706	.6472		1508	ESS	.6467		11:43	ATM	.6465		1528	ESS
707	.6425		1507	ESS	.6423		11:44	ATM				
T1 708	.6470		1506	ESS	.6465		11:46	ATM	.6467		1529	ESS
T1 709	.6503		1506	ESS	.6499		11:47	ATM	.6497		1530	ESS
710	.6509		1505	ESS	.6505	9/10	13:38	ATM	.6503		1531	ESS
711	.6514		1504	ESS	.6511		13:39	ATM	.6509		1532	ESS
T1 712	.6515		1503	ESS	.6511		13:40	ATM	.6512		1533	ESS
T1 713	.6498		1502	ESS	.6496		13:41	ATM				
T2 714	.6522		1501	ESS	.6520		13:42	ATM				
T2 715	.6494		1500	ESS	.6493		13:43	ATM				
T3 716	.6480		1459	ESS	.6481		13:43	ATM				
717	.6503		1458	ESS	.6502		13:44	ATM				
718	.6539		1457	ESS	.6537		13:45	ATM				
719	.6476		1456	ESS	.6474		13:47	ATM				
720	.6539		1455	ESS	.6534		13:48	ATM	.6536		1534	ESS
721	.6455		1454	ESS	.6455		13:49	ATM				
722	.6588		1453	ESS	.6588		13:50	ATM				
723	.6564		1452	ESS	.6564		13:50	ATM				
724	.6571		1451	ESS	.6569		13:51	ATM				
725	.6601		1450	ESS	.6602		13:52	ATM				

Checked by A.T. Myron QA Reweigh

Date: 7/26/15 Time: 1500

Balance Room Environmental Conditions

Filter #	WT	Date	Time	By
716	.6481	7.26.15	1525	Jan
711	.6510	7.26.15	1526	Jan
709	.6499	7.26.15	1527	Jan
704	.6475	7.26.15	1528	Jan

WB	DB	%RH	Date	Time	By
56	69	43	6/25	839	ATM
58	72	42	7/10	1315	ATM
57	69	46	7/14	1512	ESS
57	69	47	7.26	1421	ATM

Post	Date	1 <sup>st</sup>	2 <sup>nd</sup>	3 <sup>rd</sup>	4 <sup>th</sup>	5 <sup>th</sup>
Weighing	0.0000g	0.0000	0.0000	0.0000	0.0000	
Scale Check	100.0000g	99.9995	99.9996	99.9996	99.9994	



Woodstove Data Sheet #4-2: Initial Beaker Weights ( Tare Weights)

Into Dessicator: Date 7/2/15 Time 1500 By A.T. Myren  
 Balance Used: Sartorius Model: CP224S SN:24850860

UG 150 \

Bkr #	First Wt	Date	Time	By	Second Wt	Date	Time	By	Third Wt	Date	Time	By
20	73.3173	7/5	1930	ATM	73.3180	7/6	914	ESS	73.3174	7/8	1103	ATM
21	71.0019	7/5	1929	ATM	71.0018		915	ESS				
22	71.8347	7/5	1928	ATM	71.8346		912	ESS				
23	70.7383	7/5	1932	ATM	70.7387		909	ESS	70.7386	7/8	1105	ATM
24	73.2188	7/5	1931	ATM	73.2189		910	ESS				
25	72.6533	7/5	1930	ATM	72.6532		908	ESS				
26	71.7868	7/5	1934	ATM	71.7871		906	ESS	71.7869	7/8	1107	ATM
27	72.3305	7/5	1934	ATM	72.3304		907	ESS				
28	70.5973	7/5	1933	ATM	70.5976		905	ESS	70.5971	7/8	1108	ATM
29	71.5193	7/5	1945	ATM	71.5196		920	ESS	71.5195	7/8	1110	ATM
30	70.7855	7/5	1944	ATM	70.7857		921	ESS				
31	69.6666	7/5	1943	ATM	69.6668		920	ESS				
32	53.5996	7/5	1942	ATM	53.6001		925	ESS	53.5997	7/8	1112	ATM
33	53.1491	7/5	1941	ATM	53.1494		927	ESS	53.1493	7/8	1113	ATM
34	53.2615	7/5	1941	ATM	53.2617		926	ESS				
35	53.2831	7/5	1940	ATM	53.2835		930	ESS	53.2836	7/8	1115	ATM
36	53.5742	7/5	1939	ATM	53.5743		932	ESS				
37	53.7264	7/5	1938	ATM	53.7267		929	ESS	53.7266	7/8	1116	ATM
38	53.2521	7/5	1937	ATM	53.2515		933	ESS	53.2523	7/8	1117	ATM
39	53.1505	7/5	1936	ATM	53.1504		935	ESS				
40	53.4637	7/5	1935	ATM	53.4640		936	ESS	53.4607	7/8	1118	ATM
41	52.8367	7/5	1925	ATM	52.8371		917	ESS	52.8371	7/8	1120	ATM
42	53.8693	7/5	1927	ATM	53.8696		916	ESS	53.8690	7/8	1122	ATM
43	53.2323	7/5	1926	ATM	53.2324		918	ESS	53.2322	7/8	1124	ATM

Checked by A. Timmy ren  
 QA Reweigh

Date: 7/8/15 Time: 1202  
 Balance Room Environmental Conditions

Beaker #	WT	Date	Time	By
23	70.7385	7/10	1336	ATM
29	71.5196		1338	ATM
33	53.1492		1340	ATM
43	53.2321	↓	1342	ATM

WB	DB	%RH	Date	Time	By
58	70	48	7/5	1912	ATM
57	69	46	7/6	847	ESS
57	69	46	7/8	1010	ATM
58	72	46	7/10	1315	ATM

Date 7/15/15 7/6/15 7/8/15 7/10/15 5<sup>th</sup>  
 Post Weighing 0.0000g 0.0000 0.0000 0.0000 \_\_\_\_\_  
 Scale Check 100.0000g 99.9996 99.9995 99.9995 99.9996 \_\_\_\_\_



**Woodstove Data Sheet #4-2: Initial Beaker Weights ( Tare Weights)**

Into Dessicator: Date 7/2/15 Time 1500 By ATM

Balance Used: Sartorius

Model: CP224S

SN:24850860

Bkr #	First Wt	Date	Time	By	Second Wt	Date	Time	By	Third Wt	Date	Time	By
20	73.3176	7/9	903	ESS	73.3177	7/10	1332	ATM				
28	70.5974		905	ESS	70.5976	7/10	1328	ATM				
32	53.5999		906	ESS	53.5996	7/10	1334	ATM	53.5999	7/14	1519	ESS
38	53.2526		908	ESS	53.2521	7/10	1329	ATM	53.2519	7/14	1516	ESS
40	53.4636		909	ESS	53.4630	7/10	1331	ATM	53.4630	7/14	1517	ESS
42	53.8693		910	ESS	53.8692	7/10	1327	ATM				

Checked by A. J. Myer

Date: 7/15/15 Time: 1400

Beaker #	WT	Date	Time	By

WB	DB	%RH	Date	Time	By
58	71	44	7/9/15	859	ESS
58	72	42	7/10/15	1315	ATM
57	69	46	7/14/15	1512	ESS

Date	<u>7/9/15</u>	<u>7/10/15</u>	<u>7/14/15</u>	_____	_____
Post Weighing 0.0000g	<u>0.0000</u>	<u>0.0000</u>	<u>0.0000</u>	_____	_____
Scale Check 100.0000g	<u>99.9996</u>	<u>99.9996</u>	<u>99.9996</u>	_____	_____



Woodstove Data Sheet #4-2: Initial Beaker Weights ( Tare Weights)

Into Dessicator: Date 6/17 Time 1600 By ATM

Balance Used: Sartorius

Model: CP224S

SN:24850860

Bkr #	First Wt	Date	Time	By	Second Wt	Date	Time	By	Third Wt	Date	Time	By
20												
21												
22									Acetone Blank			
23												
24												
25	72.6528	6/23	1315	AM								
26	71.7864	6/20	1443	J	71.7869	6/22	1437	ESS	71.7869	6/23	1321	ATM
27												
28	70.5910	6/20	1649	J	70.5972	6/22	1438	ESS				
29												
30												
31												
32												
33	53.1485	6/20	1639	J	53.1490	6/22	1440	ESS	53.1490	6/23	1323	ATM
34												
35												
36	53.5737	6/20	1651	J	53.5734	6/22	1442	ESS	53.5743	6/23	1300	ATM
37												
38												
39												
40	53.1650	6/23	1317	AM								
41												
42												
43												

Checked by \_\_\_\_\_ Date: \_\_\_\_\_ Time: \_\_\_\_\_

QA Reweigh

Beaker #	WT	Date	Time	By

Balance Room Environmental Conditions

WB	DB	%RH	Date	Time	By
56	68	46	6/20	1549	ATM
55	67	45	6/22	1432	ESS
55	68	42	6/23	1213	ATM

Date	1 <sup>st</sup>	2 <sup>nd</sup>	3 <sup>rd</sup>	4 <sup>th</sup>	5 <sup>th</sup>
Post Weighing	0.0000g	0.0000	0.0000	_____	_____
Scale Check	100.0000g	99.9996	99.9996	99.9996	_____

Woodstove Data Sheet #4-3: Constant Final Weights

50 ml

TI  
0-60

Unit HEAT TECH HTG 20  
Run # EPA 1 STD  
Date: 7/28/15  
WST5-Form 9, Pg 1, Rev 10/10

Final Beaker Weights

Beaker	Into	Date	Time	Bv	First	Date	Time	Bv	Second	Date	Time	Bv	Third	Date	Time	Bv
40	53.4638	7/29	1651	ATM	53.4673	7/30	1325	ATM	53.4680	7/31	1515	ESS	53.4678	8/1	1605	ATM

Final Filter Weights

Filter #	Into Dessic	Date	Time	By	First	Date	Time	By	Second	Date	Time	By	Third	Date	Time	By
F 712	.6523	7/28	2305	ATM	.6525	7/29	1336	ESS	.6523	7/30	1011	ATM				
R 713	.6462	7/28	2305	ATM	.6464	7/29	1335	ESS	.6463	7/30	1007	ATM				

QA Reweigh: Final Weight

Date	Beaker #	Final Wt	By
Date	Filter #	Final Wt	By

Scale Room Environmental Conditions

Weighing Session	2015 Date	Time	By	WB	DB	%RH

Scale Room Environmental Conditions



Comment 7/30 7/31 8/1  
7/29 0.0000 0.0000 0.0000  
0.0000 99.9995 99.9995 99.9996  
99.9995

Woodstove Data Sheet #4-3: Constant Final Weights

T1  
60T

Unit HEAT TECH MTD 26 STD  
Run # EP1-1  
Date: 7/28/15  
WST5-Form 9, Pg 1, Rev 10/10

60 ml

Final Beaker Weights

Beaker	Into	Date	Time	Bv	First	Date	Time	Bv	Second	Date	Time	Bv	Third	Date	Time	Bv
38	53.2514	7/29	1649	ATM	53.2556	7/30	1334	ATM	53.2562	7/31	1451	ESS	53.2556	8/1	1603	ATM
					53.2556	8/2	1848	Sm								

Final Filter Weights

Filter #	Into Dessic	Date	Time	By	First	Date	Time	By	Second	Date	Time	By	Third	Date	Time	By
F 708	.6594	7/28	2305	ATM	.6591	7/29	1329	ESS	.6591	7/30	1016	ATM				
R 709	.6497	7/28	2305	ATM	.6489	7/29	1328	ESS	.6490	7/30	1015	ATM				

> 1.3081

QA Reweigh: Final Weight

Date	Beaker #	Final Wt	By
Date	Filter #	Final Wt	By

Scale Room Environmental Conditions

Weighing Session	2015 Date	Time	By	WB	DB	%RH	8	9	10	11	12
1	7/29	1325	ESS	56	68	46					
2	7/30	949	ATM	55	66	49					
3	7/31	1413	ESS	58	70	47					
4	8/1	1547	ATM	54	66	45					
5	8/2	1913	ATM	57	69	45					
6											
7											

Comment 7/30 7/31 8/1 8/2  
7/29 0.0000 0.0000 0.0000 0.0000  
0.0000 99.9996 99.9995 99.9996 99.9996  
99.9995

Train 1 Woodstove Particulate  
 Catch Processing Sheet  
 Woodstove Data Sheet #5  
 ASTM E 2515/ EPA M5G-1

Unit: HEAT TECH HTP 26 STU.  
 Run: EPA 1 Train 1  
 Date: 7/28/15  
 Technicians: ATMYAN  
 Revised 11/15 - Data Sheet #5

**0-60 Minutes:**

**Filters:**

Filter # (Front): 712 Beaker #: 40 Final Wt.: 53.4678 g  
 Tare Wt.: .6512 g ml 50 Tare Wt.: 53.4630 g  
 Filter # (Rear): 713 Desiccant: Acetone Net Wt.: .0048 g  
 Tare Wt.: .6496 g Beaker Tare Wt. Check: 53.4630 g

0-60 Minute Combined Filter Final Weight: 1.2986 g  
 0-60 Minute Combined Filter Tare Weight: 1.3008 g  
 0-60 Minute Combined Net Catch Weight: -.0022 g

**60 Minutes Plus:**

Filter # (Front): 708 Beaker #: 38 Final Wt.: 53.2556 g  
 Tare Wt.: .6467 g ml 60 Tare Wt.: 53.2519 g  
 Filter # (Rear): 709 Desiccant: Acetone Net Wt.: .0037 g  
 Tare Wt.: .6497 g Beaker Tare Wt. Check: 53.2518 g

60 Minute Plus Combined Filter Final Weight: 1.3081 g  
 60 Minute Plus Combined Filter Tare Weight: 1.2964 g  
 60 Minute Plus Combined Net Catch Weight: .0117 g

**Acetone Blank Calculation:** Blank Date: 6/23/15 Blank Beaker #: 26 Desiccant: 50 ml Acetone

Final Wt.: 71.7869 g - Tare Wt.: 71.7869 g = Net Catch Wt.: .0000 g

Net Catch Weight: .0000 g / 50 ml Acetone = .0000 g/ml Acetone Blank Residual Value

**0-60 Minute Acetone Residue Value Calculation:**

(.0000 g/ml Acetone)(50 ml Acetone) = .0000 g Residue Value

**60 Minute Plus Acetone Residue Value Calculation:**

(.0000 g/ml Acetone)(60 ml Acetone) = .0000 g Residue Value

**Total Particulate Catch Calculations:**

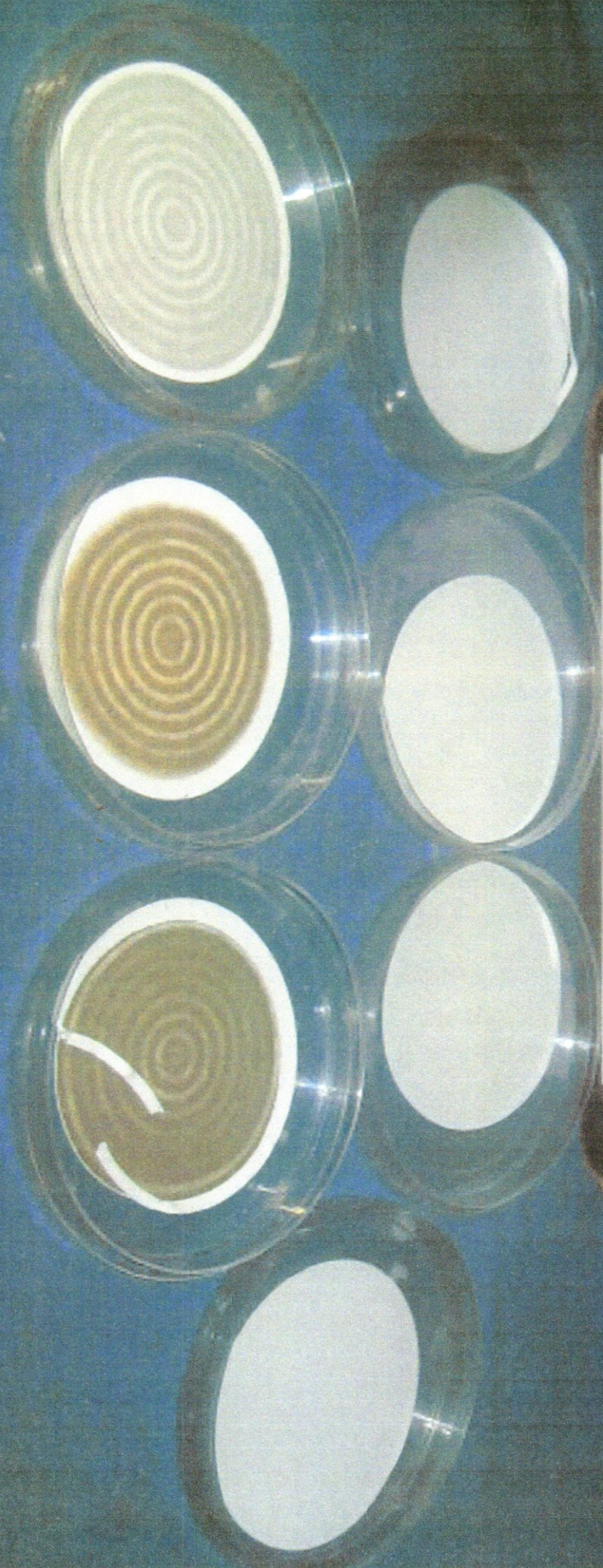
	<u>0-60 Minute</u>	<u>60 Minute Plus</u>
Combined Filter Net Catch Weight:	<u>-.0022</u> g	<u>.0117</u> g
Acetone Wash Catch Weight:	<u>.0048</u> g	<u>.0037</u> g
Less Acetone Residual Value:	<u>-.0000</u> g	<u>-.0000</u> g
Equals Net Acetone Wash Catch:	<u>.0048</u> g	<u>.0037</u> g
Total Net Catch (Combined Filter + Acetone Catch):	<u>.0026</u> g	<u>.0154</u> g
	<u>26</u> mg	<u>15.4</u> mg
<b>Total Train 1 Net Catch (0-60 Minute + 60 Minute Plus Catches):</b>		<u>18.0</u> mg







HEAT TECH HTP 26 STD EPA 1 7.28.15  
T1 0-60 T1 60+ T2 RB





Sq. Top #3

T2

METHOD 5G-1

PARTICULATE SAMPLING DATA

Rev. 10/0

DATE: 7/28/15 PAGE 1 OF 2 UNIT: HEAT Tech <sup>HTR</sup> <sub>STD</sub> RUN: EPA 1

METER BOX: 511-M METER Y: 0.9685 FILTER #'S: (F) 714 (R) 715

.783 / .786 FILTER/ O-RING ID #:           

PRE TEST LEAK CHECK: .003 CFM @ -16.0 IN HG FILTER SIZE: 110 mm

.522 / .523 PROBE ID #:           

POST TEST LEAK CHECK: .000 CFM @ -12.0 IN HG PROBE LENGTH 24 IN

TIME		METER READING	PITOT		TUNNEL TEMP	METER TEMP	GAS METER	VAC
CLOCK	ELAPSED	(ft <sup>3</sup> )	ΔP	Pg	(°F)	(°F)	Δh	(in Hg)
1300	(00)	115.300	.039		113	63.5	.75	-1.0
10	10	120.642	.039		113	67	.75	-1.0
20	20	126.012	.039		114	68.5	.75	-1.0
30	30	131.383	.039		115	70.5	.75	-1.0
40	40	136.750	.039		115	71.5	.75	-1.0
50	50	142.131	.039		116	73.5	.75	-1.0
1400	(60)	147.516	.038		117	74	.75	-1.0
10	70	152.904	.039		115	75	.75	-1.0
20	80	158.235	.039		113	75.5	.75	-1.0
30	90	163.613	.039		112	76	.75	-1.0
40	100	168.985	.039		112	76	.75	-1.0
50	110	174.370	.039		112	77	.75	-1.0
1500	(120)	179.736	.039		113	77	.75	-1.0
10	130	185.131	.039		114	78	.75	-1.0
20	140	190.513	.039		113	78	.75	-1.0
30	150	195.920	.039		113	78	.75	-1.0
40	160	201.303	.039		113	78	.75	-1.0
50	170	206.701	.039		113	78	.75	-1.0
1600	(180)	212.110	.039		113	79	.75	-1.0
10	190	217.519	.039		105	80	.75	-1.0

BP

00	28.59	300	28.56
60	28.59	360	28.56
120	28.59		
180	28.58		
240	28.57		
AVG. =		28.577	

Pre Test Filter  
Check Weighing  
F .6522  
R .6491

End of Test Weight  
F .6672 R .6494  
.6520 .6493  
0153



Sq. Top #3

T2

METHOD 5G -1

PARTICULATE SAMPLING DATA

Rev. 10/0

DATE: 7/28/15 PAGE 2 OF 2 UNIT: HEAT Tech 26570 HTP RUN: EPA 1

METER BOX: 511-M METER Y: 0.9685 FILTER #'S: (F) 714 (R) 715

.783 / .786 FILTER/ O-RING ID #: \_\_\_\_\_

PRE TEST LEAK CHECK: .003 CFM @ -16.0 IN HG FILTER SIZE: 110 mm

.522 / .523 PROBE ID #: \_\_\_\_\_

POST TEST LEAK CHECK: .000 CFM @ -12.0 IN HG PROBE LENGTH 24 IN

TIME		METER READING (ft <sup>3</sup> )	PITOT		TUNNEL TEMP (°F)	METER TEMP (°F)	GAS METER Δh	VAC (in Hg)
CLOCK	ELAPSED		ΔP	Pg				
1620	200	222.890	.039		102	79	.75	-1.0
30	210	228.303	.039		101	79.5	.75	-1.0
40	220	233.848	.039		102	79	.75	-1.0
50	230	239.119	.039		101	80	.75	-1.0
1700	<u>240</u>	244.525	.039		100	80	.75	-1.0
10	250	249.926	.039		100	80	.75	-1.0
20	260	255.352	.039		99	80	.75	-1.0
30	270	260.773	.039		98	80	.75	-1.0
40	280	266.181	.039		99	80	.75	-1.0
50	290	271.611	.039		98	80.5	.75	-1.0
1800	<u>300</u>	277.005	.039		98	80	.75	-1.0
10	310	282.415	.039		98	80.5	.75	-1.0
20	320	287.822	.039		99	80	.75	-1.0
30	330	293.233	.039		99	81	.75	-1.0
40	340	298.655	.039		98	80.5	.75	-1.0
50	350	304.060	.039		99	80	.75	-1.0
1900	<u>360</u>	309.471	.039		99	80.5	.75	-1.0
	70							
	80							
	90							

BP

00	<u>28.59</u>	300	<u>28.56</u>
60	<u>28.59</u>	360	<u>28.56</u>
120	<u>28.59</u>		
180	<u>28.58</u>		
240	<u>28.57</u>	AVG. =	<u>28.577</u>

Pre Test Filter  
Check Weighing  
F .6522  
R .6491

End of Test Weight  
F \_\_\_\_\_ R \_\_\_\_\_  
.6520 .6493

Woodstove Data Sheet #4-3: Constant Final Weights

T2

Unit HEAT TECH HTP 26 STD  
 Run # EP01  
 Date: 7/28/15  
 WST5-Form 9, Pg 1, Rev 10/10

SO MI

Final Beaker Weights

Beaker	Into	Date	Time	Bv	First	Date	Time	Bv	Second	Date	Time	Bv	Third	Date	Time	Bv
42	53.8695	7/29	1655	ATM	53.8721	7/30	1326	ATM	53.8722	7/31	1510	ESS				

Final Filter Weights

Filter #	Into Dessic	Date	Time	By	First	Date	Time	By	Second	Date	Time	By	Third	Date	Time	By
F 714	.6673	7/28	2305	ATM	.6671	7/29	1341	ESS	.6668	7/30	1014	ATM	.6671	7/31	1512	ESS
					.6669	8/1	1622	ATM								
R 715	.6494	7/28	2305	ATM	.6497	7/29	1338	ESS	.6490	7/30	1012	ATM	.6494	7/31	1511	ESS
					.6492	8/1	1621	ATM								

QA Reweigh: Final Weight

Date	Beaker #	Final Wt	By
Date	Filter #	Final Wt	By

Scale Room Environmental Conditions

Weighing Session	Date	Time	By	WB	DB	%RH
	2015					
1	7/29	1325	ESS	56	68	46
2	7/30	949	ATM	55	66	49
3	7/31	1413	ESS	58	70	47
4	8/1	1547	ATM	54	66	45
5						
6						
7						

Scale Room Environmental Conditions

8	9	10	11	12
Comment	7/30	7/31	8/1	
	0.0000	0.0000	0.0000	
	99.9996	99.9995	99.9995	
	99.9995			

Train 2/ Room Blank Woodstove  
Particulate Catch Processing Sheet  
Woodstove Data Sheet #5  
ASTM E 2515/ EPA M5G-1

Unit: HEAT Tech HTP 26 STD  
Run: EPA 1 Train 2  
Date: 7/25/15  
Technicians: A.S. Muren  
Revised 11/15 - Data Sheet #5A

Filters:

Filter # (Front): 714 ✓ Beaker #: 42 Final Wt.: 53.8722 g ✓  
Tare Wt.: .6520 g ✓ ml 50 Tare Wt.: 53.8692 g ✓  
Filter # (Rear): 715 ✓ Desiccant: Acetone Net Wt.: .0030 g ✓  
Tare Wt.: .6493 g ✓ Beaker Tare Wt., Check: 53.8691 g ✓  
Combined Filter Final Weight: 1.3161 g ✓  
Combined Filter Tare Weight: 1.3013 g ✓  
Combined Net Catch Weight: .0148 g ✓

Acetone Blank Calculation: Blank Date: 6/23/15 Blank Beaker #: 26 Desiccant: 50 ml Acetone

Final Wt.: 71.7869 g - Tare Wt.: 71.7869 g = Net Catch Wt.: .0000 g

Net Catch Weight: .0000 g / 50 ml Acetone = .0000 g/ml Acetone Blank Residual Value

Acetone Residue Value Calculation:

(.0000 g/ml Acetone)(50 ml Acetone) = .0000 g Residue Value

Total Particulate Catch Calculations:

Combined Filter Net Catch Weight: .0148 g ✓  
Acetone Wash Catch Weight: .0030 g ✓  
Less Acetone Residual Value: -.0000 g ✓  
Equals Net Acetone Wash Catch: .0030 g ✓  
Total Net Catch (Combined Filter + Acetone Catch): .0178 g ✓  
17.8 mg ✓

EPA 1 T 3 ROOM BLANK

ROOM BLANK SAMPLE FLOW PROPORTIONALITY

MYREN CONSULTING CERTIFICATION TEST DATA

5/1/2008

File Name:	EPA 1 T 3	RUN TIME (min)	GAS	INTERVAL	SAMPLING	INTERVAL	DRY GAS	DRY GAS	DRY GAS
Manufacturer:	HEAT TECH		METER	SAMPLE	RATE	SAMPLING	METER	METER	TEMP
Model Number:	HTP 26 STD		READING	VOLUME	%	RATE	READING	Δh	F
Lab Name:	MYREN		(Cu, Ft,)	(Cu. Ft.)	DIFFERENCE	(cfm)	(M3)		
Test Date:	7.28.15	0	4672.4483				132.30900	0.115	66.0
Run Number:	EPA 1 T 3	10	4677.8161	5.3678	0.0000	0.53678	132.46100	0.115	69.0
Initial Meter Reading (cf):	4672.4483	20	4683.1451	5.3290	-0.7237	0.53290	132.61190	0.115	72.0
Final Meter Reading (cf):	4862.5118	30	4688.4564	5.3113	-1.0526	0.53113	132.76230	0.115	73.5
Test Time (Min):	360.0	40	4693.7713	5.3149	-0.9868	0.53149	132.91280	0.115	75.0
Average Sample Rate (cfm):	0.5280	50	4699.0649	5.2937	-1.3816	0.52937	133.06270	0.115	76.0
Preliminary Results:		60	4704.3692	5.3043	-1.1842	0.53043	133.21290	0.115	77.0
Final results:	X	70	4709.6841	5.3149	-0.9868	0.53149	133.36340	0.115	78.0
BP:	28.577	80	4714.9883	5.3043	-1.1842	0.53043	133.51360	0.115	78.0
Average Δh:	0.115	90	4720.3208	5.3325	-0.6579	0.53325	133.66460	0.115	78.5
Dry Gas Meter Temp (F):	79.3	100	4725.6251	5.3043	-1.1842	0.53043	133.81480	0.115	79.0
Sample Volume (dscf):	172.997	110	4730.9647	5.3396	-0.5263	0.53396	133.9660	0.115	79.0
Dry Gas Meter Y:	0.9734	120	4736.2619	5.2972	-1.3158	0.52972	134.1160	0.115	80.0
Initial Room Blank Catch (mg):	1.6	130	4741.6297	5.3678	0.0000	0.53678	134.2680	0.115	80.0
Room Blank mg/dscf	0.009249	140	4746.9128	5.2831	-1.5789	0.52831	134.4176	0.115	80.5
Avg. Sampling Rate Δh:(s):	-1.645	150	4752.0369	5.1242	-4.5395	0.51242	134.5627	0.115	80.5
		160	4757.3977	5.3608	-0.1316	0.53608	134.7145	0.115	80.5
		170	4762.5996	5.2019	-3.0921	0.52019	134.8618	0.115	80.5
		180	4767.8614	5.2619	-1.9737	0.52619	135.0108	0.115	80.5
		190	4773.1127	5.2513	-2.1711	0.52513	135.1595	0.115	81.0
		200	4778.3640	5.2513	-2.1711	0.52513	135.3082	0.115	81.0
		210	4783.5977	5.2336	-2.5000	0.52336	135.4564	0.115	81.5
		220	4788.7359	5.1383	-4.2763	0.51383	135.6019	0.115	82.0
		230	4794.1214	5.3855	0.3289	0.53855	135.7544	0.115	82.0
		240	4799.3833	5.2619	-1.9737	0.52619	135.9034	0.115	82.5
		250	4804.6523	5.2689	-1.8421	0.52689	136.0526	0.115	82.5
		260	4809.9071	5.2548	-2.1053	0.52548	136.2014	0.115	81.5
		270	4815.1584	5.2513	-2.1711	0.52513	136.3501	0.115	81.5
		280	4820.4309	5.2725	-1.7763	0.52725	136.4994	0.115	81.5
		290	4825.6786	5.2478	-2.2368	0.52478	136.6480	0.115	81.5
		300	4830.9405	5.2619	-1.9737	0.52619	136.7970	0.115	81.5
		310	4836.1883	5.2478	-2.2368	0.52478	136.9456	0.115	81.5
		320	4841.4749	5.2866	-1.5132	0.52866	137.0953	0.115	81.5
		330	4846.7403	5.2654	-1.9079	0.52654	137.2444	0.115	81.5
		340	4852.0092	5.2689	-1.8421	0.52689	137.3936	0.115	82.0
		350	4857.2429	5.2336	-2.5000	0.52336	137.5418	0.115	81.0
		360	4862.5118	5.2689	-1.8421	0.52689	137.6910	0.115	81.5
		370							
		380							

NOTE: THE SAMPLED VOLUME FOR EACH SAMPLING INTERVAL MUST BE WITHIN 20% OF THE SAMPLE VOLUME FOR THE FIRST SAMPLING INTERVAL SEE ASTM E2515 SECTION 9.8.1



RB

METHOD 5G-1

PARTICULATE SAMPLING DATA

Rev. 10/09

DATE: 7/28/15 PAGE 1 OF 2 UNIT: Heavy Tech <sup>HTP</sup> <sub>26</sub> <sub>STD</sub> RUN: EPA 1

METER BOX: RBT METER Y: 0.9734 FILTER #'S: (F) 716 (R)     

.3011/.3015 .00005 cmm FILTER/ O-RING ID #:     

PRE TEST LEAK CHECK: .000 CFM @ -16.5 IN HG FILTER SIZE: 110 mm

.6928/.6928 .0000 cmm PROBE ID #:     

POST TEST LEAK CHECK: .000 CFM @ -16.25 IN HG PROBE LENGTH      IN

TIME		METER READING (ft <sup>3</sup> )	PITOT		TUNNEL TEMP (°F)	METER TEMP (°F)	GAS METER Δh	VAC (in Hg)
CLOCK	ELAPSED		ΔP	Pg				
1300	00	132.3090				66	.115	-1.75
	10	132.4610				69	.115	-1.75
	20	132.6119				72	.115	-1.75
	30	132.7623				73.5	.115	-1.75
	40	132.9128				75	.115	-1.75
	50	133.0627				76	.115	-1.75
1400	60	133.2129				77	.115	-1.75
	70	133.3634				78	.115	-1.75
	80	133.5136				78	.115	-1.75
	90	133.6646				78.5	.115	-1.80
	100	133.8148				79	.115	-1.80
	110	133.9660				79	.115	-1.80
1500	120	134.1160				80	.115	-1.80
	130	134.2680				80	.115	-1.80
	140	134.4176				80.5	.115	-1.80
	150	134.5627				80.5	.115	-1.80
	160	134.7145				80.5	.115	-1.80
	170	134.8618				80.5	.115	-1.80
1600	180	135.0108				80.5	.115	-1.80
	190	135.1595				81	.115	-1.80

BP

00	28.59	300	28.56
60	28.59	360	28.56
120	28.59		
180	28.58		
240	28.57		
		AVG. =	28.574

Pre Test Filter  
Check Weighing  
F .6480  
R     

End of Test Weight  
F .6476 R       
.6481



RB

METHOD 5G - 1

PARTICULATE SAMPLING DATA

Rev. 10/09

DATE: 7/28/15 PAGE 2 OF 2 UNIT: HEAT Tech <sup>HTR 26</sup> <sub>STD</sub> RUN: EPA 1

METER BOX: RBT METER Y: 0.9734 FILTER #'S: (F) 716 (R) —

13011/30115 .00005 cmm FILTER/ O-RING ID #: —

PRE TEST LEAK CHECK: — CFM @ -16.5 IN HG FILTER SIZE: 110 mm

.6928/1.6928 .0000 cmm PROBE ID #: —

POST TEST LEAK CHECK: .000 CFM @ -16.25 IN HG PROBE LENGTH — IN

TIME		METER READING (m <sup>3</sup> )	PITOT		TUNNEL TEMP (°F)	METER TEMP (°F)	GAS METER Δh	VAC (in Hg)
CLOCK	ELAPSED		ΔP	Pg				
1620	200	135.3082				81	.115	-1.50
30	210	135.4564				81.5	.115	-1.50
40	220	135.6019				82	.115	-1.50
50	230	135.7544				82	.115	-1.50
1700	(240)	135.9034				82.5	.115	-1.50
10	250	136.0526				82.5	.115	-1.50
20	260	136.2014				81.5	.115	-1.50
30	270	136.3501				81.5	.115	-1.50
40	280	136.4994				81.5	.115	-1.50
50	290	136.6487				81.5	.115	-1.50
1800	(300)	136.7970				81.5	.115	-1.50
10	310	136.9456				81.5	.115	-1.50
20	320	137.0953				81.5	.115	-1.50
30	330	137.2444				81.5	.115	-1.50
40	340	137.3936				82	.115	-1.50
50	350	137.5418				81	.115	-1.50
1900	(360)	137.6910				81.5	.115	-1.50
	70							
	80							
	90							

BP  
 00 28.59 300 28.56  
 60 28.59 360 28.56  
 120 28.59 — —  
 180 28.58 — —  
 240 28.57 AVG. = 28.577

Pre Test Filter  
 Check Weighing  
 F —  
 R —

End of Test Weight  
 F .6476 R —  
.6481  
.0005



Train 2/ Room Blank Woodstove  
Particulate Catch Processing Sheet  
Woodstove Data Sheet #5  
ASTM E 2515/ EPA M5G-1

Unit: HTP 26 STO  
Run: EPA 1 Train 5  
Date: 7/28/15  
Technicians: A.T. Murray  
Revised 11/15 - Data Sheet #5A

**Filters:**

Filter # (Front): 716 Beaker #: 43 Final Wt.: 53.2340 g ✓  
Tare Wt.: .6481 g ml 80 Tare Wt.: 53.2322 g ✓  
Filter # (Rear): — Desiccant: Acetone Net Wt.: .0018 g  
Tare Wt.: — g Beaker Tare Wt., Check: 53.2322 g  
Combined Filter Final Weight: .6478 g ✓  
Combined Filter Tare Weight: .6480 g ✓  
Combined Net Catch Weight: -.0002 g ✓

**Acetone Blank Calculation:** Blank Date: 6/23/15 Blank Beaker #: 26 Desiccant: 50 ml Acetone

Final Wt.: 71.7869 g - Tare Wt.: 71.7869 g = Net Catch Wt.: .0000 g

Net Catch Weight: .0000 g / 50 ml Acetone = .0000 g/ml Acetone Blank Residual Value

**Acetone Residue Value Calculation:**

(.0000 g/ml Acetone)(30 ml Acetone) = .0000 g Residue Value

**Total Particulate Catch Calculations:**

Combined Filter Net Catch Weight: -.0002 g ✓  
Acetone Wash Catch Weight: .0018 g ✓  
Less Acetone Residual Value: -.0000 g ✓  
Equals Net Acetone Wash Catch: .0018 g ✓  
Total Net Catch (Combined Filter + Acetone Catch): .0016 g ✓  
1.6 mg ✓

MT# 26 ST0

### Miscellaneous Test Data Woodstove Data Sheet #8

Unit: HEAT TECH  
Run # EPA 1  
Date: 7/1/15  
Technician: ATM ESS  
WST6-Form1, Rev 6/11

Useable Firebox Dimensions: See QC Section Useable Volume: N/A ft<sup>3</sup>  
Dilution Tunnel Draft (If Applicable): Start: .000 Stop: .000 Avg: .000 in. H<sub>2</sub>O  
Test Chamber Air Velocity: Start: 70, < 5 Stop: 75, < 10 Avg: 5.0 ft./m.  
Wet Bulb/ Start: WB: 59 °F DB: 72 °F % Amb Moisture: 1.25 %RH: 45  
Dry Bulb Stop: WB: 67 °F DB: 82 °F % Amb Moisture: 1.45 %RH: 47  
X Ambient Moisture(%Vol.) = 1.35 % X Relative Humidity (%RH) = 46 %

Empty Stove Wt: 222.2 lbs.  
Empty Stove Wt with Stack (~~inc oil seal~~) Wet: N/A lbs. Dry: N/A lbs.  
Empty Stove Wt with Stack and Ash Ash: — lbs. Total: — lbs.  
Kindling Wt. Paper: N/A lbs. Wood: N/A lbs. Total: — lbs.  
Pre Burn Fuel Wt. 2.9 + 2.9 Total: 5.8 lbs.  
Total Kindling and Pre Burn Fuel Wt. 5.8 lbs.  
Coal Bed Wt.: Range( N/A - N/A ) lbs. Actual: N/A lbs.

Allowable Amount of Charcoal That Can Be Removed:  
Coal Bed Wt. Range  $\left[ \frac{\text{Upper Wt.} + \text{Lower Wt.}}{2} \right] .25 = \text{N/A}$  lbs.  
Test Fuel Wt.: Ideal N/A lbs. Range: N/A lbs. Actual: 12.1 lbs.  
Test Fuel Size (pcs.) (.75 x 1.5 x 5" Spacers): N/A Pcs. N/A lbs.  
2 x 4's x N/A " N/A Pcs. N/A lbs. N/A %  
4 x 4's x N/A " N/A Pcs. N/A lbs. N/A %

5.1740 dkg  
Est. Dry Burn Rate(Kg/Hr.)  $12.1 - (12.1 \times .0573) \times \frac{60}{360} = 0.862$   
2.2046 Dry Burn Rate (Kg/Hr)

Est EPA Heat Output (HO<sub>E</sub>)(Avg BTU's/Hr)(19,140) X 78 x 0.862 = 12,874  
100 EPA Heat Output (HO<sub>E</sub>)BTU's/Hr

## STOVE OPERATION

The after cleaning out the stove and stack before the start of the certification, the hopper was filled with pellets and stove was started with the controls set at "Manual". After the stove went thru its "Start" cycle (approximately 10 minutes), the controls were turned to "HIGH" and it ran for about 1 hour as we finished preparing for the test. Then Preburn was started, which lasted another hour. After 60 minutes of preburn, the stove's controls were left on "High" for the first hour of the test. At 60 minutes the stove's controls were set to "Medium". At 180 minutes the stove's controls was turned down to "Low".

**Wood Density Determination  
Woodstove Test Data Sheet #11**

Unit: HEAT Tech HTP 26 STD  
Run#: EPA 1  
Date: 7/28/15  
Technician: ATM ESS

Rev 5/10

Wood Piece: Nominal Dimensions: \_\_\_\_\_ X \_\_\_\_\_ X \_\_\_\_\_  
Depth (D): \_\_\_\_\_ cm  
Width (W): \_\_\_\_\_ cm  
Length(L): \_\_\_\_\_ cm  
\_\_\_\_\_ cm      Length  $\bar{X}$  = \_\_\_\_\_ cm  
\_\_\_\_\_ cm  
\_\_\_\_\_ cm      Volume: \_\_\_\_\_ cm<sup>3</sup>  
(D x W x L)

Room Temperature: \_\_\_\_\_ °F Correction Factor: \_\_\_\_\_

Meter Readings Corrected for temperature: Yes \_\_\_\_\_ No \_\_\_\_\_

Note: Record Moisture Meter readings to the nearest 0.5% or 0.1%

	Uncor	Cor	Avg % Moisture (Dry) _____ %
Top:		%	
Bottom:		%	Avg % Moisture (Wet) _____ %
Side:		%	Scale: Leveled In _____ Out _____
$\bar{X}$ :		%	Zeroed: In _____ Out _____

Wet Weight: \_\_\_\_\_ g Dry Weight: \_\_\_\_\_ g

% Moisture Dried Basis: \_\_\_\_\_ %

$$([1 - (\text{Dry Wt}/\text{Wet Wt})] \times 100)$$

Density = \_\_\_\_\_ g / \_\_\_\_\_ cm<sup>3</sup> = \_\_\_\_\_ g/cm<sup>3</sup>  
(dry wt) (volume)

	Date	Time	Temp
Into Dryer	<u>7/28/15</u>	<u>1500</u>	<u>220</u> °F
Out of Dryer	<u>8/6/15</u>	<u>942</u>	<u>218</u> °F

(Minimum Time in Dryer: 24 hrs.)

Blk # 46

Pellet Fuel Moisture Content Determination

Tare Beaker Wt. 68.3658 g

Pellet Name: Bear Mountain

Pellet Manufacturer: Bear Mountain

Pellet Grade: Premium Plus

Wet Wt: 158.9236 g - 68.3658 g = 90.5578 g -

Gross Wet Wt. Tare Beaker Wt. Net Wet Wt.  
Dry Wt: 153.7346 g - 68.3658 g = 85.3688 g

Gross Dry Wt. Tare Beaker Wt. Net Dry Wt.

% Moisture Wet Basis: 5.730 %

$$[1 - (\text{Net Dry Wt.}/\text{Net Wet Wt.})] \times 100$$



**ASTM 2779 EQN 1: Pounds of Dry Fuel Burnt, db. (Revised)**

$$M_{Bdb} = ((M_{Swb} - M_{Ewb}) - ((M_{Swb} - M_{Ewb})(FM_{wb}/100)))$$

Full Test

$FM_{wb}$  = average fuel moisture of test fuel, % wet basis.

$M_{Sdb}$  = Weight of the test fuel in the hopper at the start of the test run, wet basis, kg (lb).

$M_{Ewb}$  = Weight of the test fuel in the hopper at the start of the test run, wet basis, kg (lb), and

$M_{Bdb}$  = Weight of the fuel burnt during the test run, dry basis, kg(lb).

2.2046 = lbs/ kg

$$M_{Bdb} = ((306.0 - 292.9) - ((306.0 - 292.9)(5.730/100))) = 11.407 \text{ lbs.} / 2.2046 = 5.174 \text{ kg}$$

**ASTM 2779 EQN 2: Pounds of Dry Fuel Burnt During a Test Segment ( $S_i$ ), db. (Revised)**

0-60 mins

$$M_{Bdb} = ((M_{SSiwb} - M_{ESiwb}) - ((M_{SSiwb} - M_{ESiwb})FM_{wb}))$$

$FM_{wb}$  = average fuel moisture of test fuel, % wet basis.

$M_{SSiwb}$  = Weight of the test fuel in the hopper at the start of the test run, wet basis, kg (lb).

$M_{ESiwb}$  = Weight of the test fuel in the hopper at the start of the test run, wet basis, kg (lb), and

$M_{BSiwb}$  = Weight of the fuel burnt during the test run, dry basis, kg(lb).

2.2046 = lbs/ kg

$$M_{BSiwb} = ((306.0 - 302.8) - ((306.0 - 302.8)(5.730/100))) = 3.017 \text{ lbs.} / 2.2046 = 1.368 \text{ kg}$$

**ASTM 2779 EQN 3: Average Dry Burn Rate (DBR)**

Full Test

$$BR(DBR) = (60 (M_{Bdb}))/\theta = (60(5.174))/360 = 0.8623 \text{ kg/h}$$

BR (DBR) = average dry burn rate over the full integrated test run, kg/h (lb/h), and  
 $\theta$  = total length of the full integrated test run, min.

**ASTM 2779 EQN 4: Average Dry Burn Rate (DBR) During a Test Run Segment ( $S_i$ )**

$$BR(DBR) = 60 (M_{BSiwb})/\theta = (60(1.368))/60 = 1.368 \text{ kg/h}$$

0-60 mins

BR (DBR) = average dry burn rate over the test run segment  $i$ , kg/h (lb/h), and  
 $\theta$  = total length of test run segment  $i$ , min.





















Pre and Post Test Zero/Span Check

Woodstove Data Sheet # 15-1

Site: Myren Consulting, Colville, WA Date: 7/28/15 Analyte: CO<sub>2</sub>

Source: Heat Tech HTD2-10 Run #: EPA 1

Zero Cyl #: 1TMB803/11 Conc. 0.0 % CO<sub>2</sub> Cyl Press: 230 psi

Certified By: Oxarc Date: 6/11/12

Span Cyl #: EB-0019810 Conc. 12.4 % CO<sub>2</sub> Cyl Press: 220 psi

Certified By: Liquid Technology Corp. Date: 4/25/12

Analyzer: Make: Horiba Model: PIR-2000 SN: 607024

Range: 0 - 25.0% CO<sub>2</sub> Analyzer Output: 0 - 1.0 v.

Flow: 1.5 SCFH Measured By: Rotameter: X Flowmeter: \_\_\_\_\_

EPA Span Values = 25.0% CO<sub>2</sub>

EPA Control Limits =  $\pm 2.5\%$  of 25.0% CO<sub>2</sub> =  $\pm 0.625\%$  CO<sub>2</sub>

Pre Run Audit: By: A.T. Myren Time: 1205 Temp: 74 °F

Audit Results

Point #	Expected Response			Actual Response			± Conc. Difference	Δ %
	Meter	DVM	%	Meter	DVM	%		
Zero	00.0	00.0	00.0	00.0	00.0	00.0	+0.03162	+0.13
Span	49.6	49.6	12.4	48.75	49.6	12.4280	+0.0280	+0.23

Comments:

Post Run Audit: By: A.T. Myren Time: 1925 Temp: 75 °F

Audit Results

Point #	Expected Response			Actual Response			± Conc. Difference	Δ %
	Meter	DVM	%	Meter	DVM	%		
Zero	00.0	00.0	00.0	00.0	00.2	00.160	+0.03160	+0.23
Span	49.6	49.6		50.0	50.4	12.6279	+0.2279	+1.84

Comments:

$\pm \text{CONC. Difference} = \text{Act \%} - \text{Exp (Std) \%}$

$\text{Zero \% Difference } (\Delta\%) = \frac{\text{Act \% (ppm)} - \text{Exp \% (ppm)}}{\text{Full Scale Value}} \times 100$

$\text{Span \% Difference } (\Delta\%) = \frac{\text{Act \% (ppm)} - \text{Exp \% (ppm)}}{\text{Exp \% (ppm)}} \times 100$

Pre and Post Test Zero/Span Check

Woodstove Data Sheet #15-3

Site: Myren Consulting, Colville, WA Date: 7/28/15 Analyte: CO

Source: HEAT Tech HTP 26570 Run #: EPA 1

Zero Cyl #: 1 TM 8903 / II Conc. 00.0 % CO

Cyl Press: 230 psi

Certified By: Oxarc

Date: 6/11/12

Span Cyl #: EB -0019810 Conc. 2.57 % CO

Cyl Press: 220 psi

Certified By: Liquid Technology Corp

Date: 4/25/12

Analyzer: Make: Horiba Model: Mexa 311 GE SN: GE-30075

Range: 0 - 10.0% CO (0 - 5.0% CO) Analyzer Output: 0 - 1.0 v.

Flow: 1.5 SCFH Measured By: Rotameter: X Flowmeter: \_\_\_\_\_

EPA Span Values= 5.0% CO

EPA Control Limits = ±2.5% of 5.0% CO = ±0.125% CO

Pre Run Audit: By: A.T. Myren Time: 1205 Temp: 74 °F

**Audit Results**

Point #	Expected Response			Actual Response			± Conc. Difference	Δ %
	Meter	DVM	%	Meter	DVM	%		
Zero	00.0	.000	00.0	-	.002	.0726	.0726	+0.25
Span	-	.257	2.57	-	.257	2.5570	-0.0131	-0.50

Comments: meter on front panel is broken

Post Run Audit: By: A.T. Myren Time: 1925 Temp: 75 °F

**Audit Results**

Point #	Expected Response			Actual Response			± Conc. Difference	Δ %
	Meter	DVM	%	Meter	DVM	%		
Zero	00.0	.000	00.0	-	.001	0.104	.0104	0.21
Span	-	.257	2.57	-	.263	2.6101	+0.04012	1.56

Comments:

±CONC. Difference= Act % - Exp (Std) %

Zero % Difference(Δ%) =  $\frac{\text{Act \% (ppm)} - \text{Exp \% (ppm)}}{\text{Full Scale Value}} \times 100$

Span % Difference (Δ%) =  $\frac{\text{Act \% (ppm)} - \text{Exp \% (ppm)}}{\text{Exp \% (ppm)}} \times 100$



**FIREPLACE DATA SHEET #10**  
 Quality Checks (Revised 1/10)

Unit: HEAT Tech HTP 2650  
 Run #: EPB 1  
 Date: 7/28/15

Ambient Blank Probe Inlet Location 38 1/2 " from the bottom of the hood (Spec =  $\leq 6.6'$ ) and 31 3/4 " from the chimney centerline (Spec =  $\leq 3.3'$ ).

Dilution Tunnel Draft: Start: .000 Stop: 1.000 Avg.: .000 "H<sub>2</sub>O

Test Chamber Air Velocity: Start: >0, <5 Stop: >5, <10 Avg.: 5.0 ft/min

Test Chamber Ambient Moisture (AM) / Relative Humidity (%RH)

Start: Wet Bulb 59 Dry Bulb 72 =%RH 45, %AM (%By Vol) 1.25  
 Stop: Wet Bulb 62 Dry Bulb 75 =%RH 47, %AM (% by Vol) 1.45  
 Avg. %RH 46, %AM (% by Vol) 1.35

Minimum Tunnel Flow For 100% Smoke Capture: Pitot Reading (Ap): .04  
 ~ Tunnel Flow: 140.00 dscfm

Fireplace Back Wall Temperature Immediately Prior to Test Start: N/A °F

Scale Check: Pre (Wt., #): 272.4 - 267.4 = 5.0 lbs. / 5.0 lbs. OK ✓  
 Post (Wt., #): 298.3 - 293.3 = 5.0 lbs. / 5.0 lbs. OK ✓

Scale Zero Drift: Pre: N/A lbs. Post: N/A lbs. Drift: N/A lbs.

(Note: To avoid having the heat from the bottom of the unit affect the load cells, the fireplace is set on a large steel plate which is supported by 4-2x4's. There also is a piece of insulation directly over the electronics in the scale deck. When the steel plate and fireplace were lifted off the scale deck, the 2X4's and insulation are still on the deck. Thus, the weight shown rather than zero.)

Combustion Gas (CO<sub>2</sub>, O<sub>2</sub> & CO) Train Leak Checks: Pre: OK ✓ Post: OK ✓  
 Draft (Static [P<sub>g</sub>]) Gauge Level and Zero Check: Pre: OK ✓ Post: OK ✓

THERMOCOUPLE CHECK (@ Ambient):

T/C #1:	<u>66</u>	T/C #2:	<u>61</u>
T/C #3:	<u>63</u>	T/C #5:	<u>—</u>
T/C #4:	<u>—</u>	T/C #6:	<u>—</u>
T/C #7:	<u>—</u>	T/C #9:	<u>62</u>
T/C #8:	<u>—</u>	T/C #10:	<u>71</u>
T/C #11:	<u>63</u>	T/C #12:	<u>32</u>
T/C #13:	<u>63</u>	T/C #14:	<u>55</u>
T/C #15:	<u>64</u>	T/C #16:	<u>55</u>
T/C #17:	<u>66</u>	T/C #18:	<u>64</u>
T/C #19:	<u>63</u>	T/C #20:	<u>—</u>
T/C #21:	<u>—</u>	T/C #22:	<u>—</u>

Thermocouple Readout:

Pretest Zero & Span Check and Calibration      Post Test Zero & Span Check  
 Zero (0° F): -1.0 ° F Adj to: 0 ° F      0° F 1      Δ%: -0.22  
 Span (2000° F): 2000 ° F Adj to: — ° F      Span(2000° F): 2003 Δ%: -0.12

Pretest Thermocouple Readout Linearity Check:

0 °F = 0      200 °F = 202      400 °F = 399      600 °F = 601  
 800 °F = 801      1000 °F = 1000      1200 °F = 1198      1400 °F = 1399  
 1600 °F = 1600      1800 °F = 1800      2000 °F = 2000

Becherini Scale Center, Inc.  
 317 E. Sprague  
 Spokane, WA 99202

# SCALE CALIBRATION RECORD

Customer: MYREN CONSULTING Date: 3/26/15

Work Order Number: 48656 PO Number:

Equipment Mfg.	Serial Number	Specifications	Weight used	Initial Readings	Final Readings
1. PANTHER	4466459	1000 x .1	Ø	/	/
	Pass...Fail		50		
Notes: NOT WORKING, TOOK BACK TO SHOP			100		
			300		
			500		
			Ø		

Equipment Mfg.	Serial Number	Specifications	Weight used	Initial Readings	Final Readings
2. PANTHER	0015555604	5K x 1		/	/
	Pass...Fail				
Notes: NOT USING					

Equipment Mfg.	Serial Number	Specifications	Weight used	Initial Readings	Final Readings
3. PANTHER	00025736A5	1000 x .1	Ø	/	Ø
	Pass...Fail		50		50.0
Notes: 1 x SMALL - CALIBRATED			100		100.0
			300		300.0
			500		500.2
			Ø	Ø	

Equipment Mfg.	Serial Number	Specifications	Weight used	Initial Readings	Final Readings
4. PANTHER	00926576KL	1000 x .1	Ø	Ø	Ø
	Pass...Fail		50	50.0	50.0
Notes: 3 x 5 DECK, CALIBRATED			100	100.0	100.0
			300	300.1	300.0
			500	500.2	500.0
			Ø	Ø	Ø

Additional Comments:

Last Checked: 9/14 Next Check Due: 9/15  
 Weights Certified: 10/14 Technician: ICC/BB

## DENSITY STANDARD USED FOR TROEMNER PRECISION WEIGHTS

Troemner Inc. adjusts all new weights and all weights received for recalibration on the basis of apparent mass versus material of density  $8.0\text{g}/\text{cm}^3$  at  $20^\circ\text{C}$ . This action is in accordance with the recommendations of the American Society for Testing and Materials specification ANSI/ASTM E 617 and the International Organization of Legal Metrology (OIML) International Recommendation No. 20.

Previously, all weights had usually been adjusted on the basis of apparent mass versus "brass," a hypothetical material of defined density  $8.4\text{g}/\text{cm}^3$  at  $0^\circ\text{C}$  and  $8.3909\text{g}/\text{cm}^3$  at  $20^\circ\text{C}$ . This practice originated in the early 1800's and was adopted in all of the English speaking countries as well as a number of other countries. Now most mass standards and test weights are made from stainless steel (density ranges from  $7.77\text{g}/\text{cm}^3$  to  $8.0\text{g}/\text{cm}^3$ ). A number of countries have adopted the recommendations of OIML and the foremost balance manufacturers are adjusting the built-in weights in their balances on the basis of apparent mass versus  $8.0\text{g}/\text{cm}^3$ . In order to smooth the transition in this country, the Reports of Calibration of the National Bureau of Standards are reporting the corrections to calibrated mass standards on both bases.

In terms of normal weighing procedures the change is very small. For a given weight, the mass value assigned on the basis of apparent mass versus density  $8.0\text{g}/\text{cm}^3$  material will be 7 parts per million higher than the value assigned on the basis of apparent mass versus "density  $8.4\text{g}/\text{cm}^3$ " material. In many cases the allowed weight adjustment tolerances are so

large that this change is immaterial although closely adjusted weights often have a smaller tolerance than the correction change. For example at the 1 kilogram level the change is 7 mg. For comparison the ANSI/ASTM E 617 Class 6 tolerance for 1 kilogram is 100 mg while the Class 3 tolerance is 25 mg. A detailed discussion of mass and mass values is given in Reference 3.

Precision Weights manufactured by Troemner Inc. to ASTM Class 1, 1.1, 2, 3, 4, 5, and 6 tolerances and the equivalent OIML and NBS tolerances are of the following materials:

Designation	Base Material	Density	Weight Range
Stainless Steel	18-8	$7.84\text{g}/\text{cm}^3$ at $20^\circ\text{C}$	1 g & larger
Stainless Steel	18-8	$8.0\text{g}/\text{cm}^3$ at $20^\circ\text{C}$	50 mg to 500 mg
Aluminum	1100	$2.7\text{g}/\text{cm}^3$ at $20^\circ\text{C}$	30 mg & smaller

### References:

1. ANSI/ASTM E 617  
Available from: Troemner Inc. 6825 Greenway Ave., Phila. Pa. 19142  
215-724-0800 or American Society for Testing and Materials, 1916 Race Street, Phila., Pa. 19103
2. OIML INTERNATIONAL RECOMMENDATION No. 20  
Available from: Organisation Internationale De Metrologie Legale  
11 Rue Trugot - 75009 Paris, France
3. NBS MONOGRAPH 133, MASS AND MASS VALUES  
Available from: Superintendent of Documents, U.S. Government  
Printing Office  
Washington, D.C. 20402  
Order by SD Catalog No. C13,44:1331 Stock Number  
0303-01178



**TROEMNER INC.**

Manufacturers of Precision Weights...  
Mass Standards • Balances • Laboratory Apparatus  
6825 Greenway Avenue - Philadelphia, Pa. 19142  
215/724-0800

Wts. used for Scale QC Checks, P. 4-4.





# QUALITY CONTROL SERVICES

LABORATORY EQUIPMENT • SALES • SERVICE • CALIBRATION • REPAIRS  
 2340 SE 11<sup>TH</sup> Ave. Portland, Oregon 97214 • Box 14831 Portland, Oregon 97293  
 (503) 236-2712 • FAX (503) 235-2535 • www.qc-services.com



Myren Consulting  
 512 Williams Lake Road  
 Colville, WA 99114

Report Number: MYRC0224850860150415

## A2LA ACCREDITED CERTIFICATE OF CALIBRATION WITH DATA

### INSTRUMENT INFORMATION

Item	Make	Model	Serial Number	Customer ID	Location
Balance	Sartorius	CPA224S	24850860	N/A	Lab
Units	Readability	SOP	Cal Date	Last Cal Date	Cal Due Date
g	0.0001	QC012	4/15/15	11/12/14	10/2015

### FUNCTIONAL CHECKS

ECCENTRICITY		LINEARITY		STANDARD DEVIATION		ENVIRONMENTAL CONDITIONS	
Test Wt:	Tol:	Test Wt:	Tol:	Test Wt:	Tol:		
100	0.0003	50 x 4	0.0002	100	0.0001	<input type="checkbox"/> Good <input checked="" type="checkbox"/> Fair <input type="checkbox"/> Poor Temperature: 21.3°C	
As-Found:		As-Found:		1. 100.0000	5. 99.9999		9. 99.9999
Pass: <input checked="" type="checkbox"/>	Fail: <input type="checkbox"/>	Pass: <input checked="" type="checkbox"/>	Fail: <input type="checkbox"/>	2. 100.0000	6. 100.0000		10. 100.0000
As-Left:		As-Left:		3. 100.0000	7. 100.0000		<b>Result</b>
Pass: <input checked="" type="checkbox"/>	Fail: <input type="checkbox"/>	Pass: <input checked="" type="checkbox"/>	Fail: <input type="checkbox"/>	4. 100.0000	8. 100.0000	0.00004	

### A2LA ACCREDITED SECTION OF REPORT

Standard	As-Found	As-Left	Expanded Uncertainty
200	199.9992	200.0002	0.00014
100	99.9995	100.0000	0.00014
50	49.9997	50.0000	0.00014
10	9.9999	10.0000	0.00014
1	1.0000	1.0000	0.00014
0.1	0.1000	0.1000	0.00014

### CALIBRATION STANDARDS

Item	Make	Model	Serial Number	Cal Date	Cal Due Date	NIST ID
Weight Set	Rice Lake	30 kg-1mg	S751	12/2/14	12/2015	OR-13-314-C

Permanent Information Concerning this Equipment:

Comments/Info Concerning this Calibration:

4/15 Performed internal calibration overwrite.

Report prepared/reviewed by:

Date: 4-15-2015

Technician: R. Hintz  
 Signature:

THIS CERTIFICATE SHALL NOT BE REPRODUCED WITHOUT THE APPROVAL OF QUALITY CONTROL SERVICES, INC.

The uncertainty is calculated according to the ISO Guide to the Expression of Uncertainty in Measurement and includes the uncertainty of standards used combined with the observed standard deviation and readability of the unit under test. The uncertainty is expanded with a k factor of 2 for an approximate 95% level of confidence. Instruments listed above were calibrated using standards traceable to the National Institute of Standards and Technology (NIST). Calibration data reflect results at the time and location of calibration. Calibration data should be reviewed to insure that the instrument is performing to its required accuracy. Calibrations comply with ISO/IEC 17025 and ANSI/Z540-1-1994 quality standards.



K&M Company  
TORRANCE, CA 90503

**ALTEK**

**CERTIFICATE OF CALIBRATION**

This is to Certify that your Altek Unit has been calibrated using standards whose accuracies are traceable to the National Institute of Standards and Technology (formerly NBS) within the limits of the NIST Calibration Services. Actual records pertaining to these standards are on file and are available for examination.

Certified by: Altek Industries Corp.  
Recommend Recalibration: Annually

In service date 4/11/96

Model K2100F Serial No. **Serial # 177533**

T. Kuech  
Calibration Technician

31 AUG 95  
Factory Calibration Date

**ALTEK INDUSTRIES CORP**  
210 Commerce Drive, Redwood City, CA 94063  
(716) 334-3720 FAX (716) 334-6676  
800-322-ALTEK  
800-322-ALTEK  
Anywhere in USA

MYREN CONSULTING, INC.  
512 Williams Lake Road  
Colville, WA 99114  
Office: 509 684 1154  
Lab: 509 685 9458

Calibration Data Sheet # 65  
Revision 1 3/3/04

THERMOCOUPLE READOUT CALIBRATION

DATE: 5/20/15  
TECHNICIAN: ESS

Thermocouple Readout Manufacturer: OMEGA

Model #: 115 KF Serial #: 00114871KF Type: K Range: 0-1900° F

Location: 45 G-P METER BOX

Calibrated with: ALTEK SERIES 22 TC SOURCE

As found: 0° F = -1 Adjusted to: 0  
1900° F = 1901 Adjusted to: 1900

	% Dif		% Dif		% Dif
0 = <u>0</u>	<u>0</u>	800 = <u>799</u>	<u>.0008</u>	1600 = <u>1600</u>	<u>0</u>
100 = <u>95</u>	<u>.0089</u>	900 = <u>896</u>	<u>.0029</u>	1700 = <u>1699</u>	<u>.0005</u>
200 = <u>202</u>	<u>-.0030</u>	1000 = <u>1000</u>	<u>0</u>	1800 = <u>1800</u>	<u>0</u>
300 = <u>299</u>	<u>.0013</u>	1100 = <u>1098</u>	<u>.0013</u>	1900 = <u>1900</u>	<u>0</u>
400 = <u>400</u>	<u>0</u>	1200 = <u>1198</u>	<u>.0012</u>	2000 = <u>—</u>	<u>—</u>
500 = <u>498</u>	<u>.0021</u>	1300 = <u>1296</u>	<u>.0023</u>		
600 = <u>600</u>	<u>0</u>	1400 = <u>1399</u>	<u>.0005</u>		
700 = <u>695</u>	<u>.0043</u>	1500 = <u>1498</u>	<u>.0010</u>		

$$\% \text{ Dif} = \frac{(\text{Reference Temperature } ^\circ\text{F} + 460) - (\text{Readout Temperature } ^\circ\text{F} + 460)}{\text{Reference Temperature } ^\circ\text{F} + 460}$$

Or

$$\% \text{ Dif} = \frac{(\text{Reference Temperature } ^\circ\text{C} + 273) - (\text{Readout Temperature } ^\circ\text{C} + 273)}{\text{Reference Temperature } ^\circ\text{C} + 273}$$

MYREN CONSULTING, INC.  
512 Williams Lake Road  
Colville, WA 99114  
Office: 509 684 1154  
Lab: 509 685 9458

Calibration Data Sheet # 65  
Revision 1 3/3/04

THERMOCOUPLE READOUT CALIBRATION

DATE: 5/20/15  
TECHNICIAN: ESS

Thermocouple Readout Manufacturer: JENCO

Model #: 768-KF.02 Serial #: 900167 Type: K Range: 0-1999°F

Location: 511-M METER BOX

Calibrated with: ALTEK SERIES 22 TC SOURCE

As found: 0° F = -3 Adjusted to: 0  
1900° F = 1896 Adjusted to: 1900

	% Dif		% Dif		% Dif
0 = <u>0</u>	<u>0</u>	800 = <u>800</u>	<u>0</u>	1600 = <u>1614</u>	<u>-1.0068</u>
100 = <u>94</u>	<u>.0107</u>	900 = <u>900</u>	<u>0</u>	1700 = <u>1710</u>	<u>-1.0046</u>
200 = <u>199</u>	<u>.0015</u>	1000 = <u>1006</u>	<u>-.0041</u>	1800 = <u>1807</u>	<u>-1.0031</u>
300 = <u>295</u>	<u>.0066</u>	1100 = <u>1107</u>	<u>-.0045</u>	1900 = <u>1900</u>	<u>0</u>
400 = <u>394</u>	<u>.0070</u>	1200 = <u>1210</u>	<u>-.0060</u>	2000 = <u>—</u>	<u>—</u>
500 = <u>490</u>	<u>.0104</u>	1300 = <u>1313</u>	<u>-.0074</u>	_____ = _____	_____
600 = <u>595</u>	<u>.0047</u>	1400 = <u>1415</u>	<u>-.0081</u>		
700 = <u>693</u>	<u>.0060</u>	1500 = <u>1514</u>	<u>-.0071</u>		

$$\% \text{ Dif} = \frac{(\text{Reference Temperature } ^\circ\text{F} + 460) - (\text{Readout Temperature } ^\circ\text{F} + 460)}{\text{Reference Temperature } ^\circ\text{F} + 460}$$

Or

$$\% \text{ Dif} = \frac{(\text{Reference Temperature } ^\circ\text{C} + 273) - (\text{Readout Temperature } ^\circ\text{C} + 273)}{\text{Reference Temperature } ^\circ\text{C} + 273}$$

MYREN CONSULTING, INC.  
 512 Williams Lake Road  
 Colville, WA 99114  
 Office: 509 684 1154  
 Lab: 509 685 9458

Calibration Data Sheet # 65  
 Revision 1 3/3/04

THERMOCOUPLE READOUT CALIBRATION

DATE: 5/20/15  
 TECHNICIAN: ESS

Thermocouple Readout Manufacturer: Omega

Model #: 46081K Serial #: 99110582 Type: K Range: 0-2000°F

Location: SOUTH STAND T/C Dial Readout - Dial #1

Calibrated with: ALTEK SERIES 22 TC SOURCE

As found: 0° F = .8 Adjusted to: 0  
 2000° F = 1999.3 Adjusted to: 2000

Temp (°F)	% Dif	Temp (°F)	% Dif	Temp (°F)	% Dif
0 = <u>0</u>	<u>0</u>	800 = <u>801.1</u>	<u>-.0009</u>	1600 = <u>1599.5</u>	<u>.0002</u>
100 = <u>97.1</u>	<u>.0052</u>	900 = <u>897.6</u>	<u>.0018</u>	1700 = <u>1698.6</u>	<u>.0006</u>
200 = <u>201.4</u>	<u>-.0021</u>	1000 = <u>1000.3</u>	<u>-.0002</u>	1800 = <u>1799.8</u>	<u>.00009</u>
300 = <u>297.0</u>	<u>.0013</u>	1100 = <u>1098.0</u>	<u>.0013</u>	1900 = <u>1898.6</u>	<u>.0006</u>
400 = <u>398.9</u>	<u>.0012</u>	1200 = <u>1198.0</u>	<u>.0012</u>	2000 = <u>2000.0</u>	<u>0</u>
500 = <u>497.0</u>	<u>.0031</u>	1300 = <u>1298.2</u>	<u>.0010</u>	2100 = <u>2098.7</u>	<u>.0005</u>
600 = <u>601.0</u>	<u>-.0009</u>	1400 = <u>1399.0</u>	<u>.0005</u>		
700 = <u>697.4</u>	<u>.0022</u>	1500 = <u>1498.6</u>	<u>.0007</u>		

$$\% \text{ Dif} = \frac{(\text{Reference Temperature } ^\circ\text{F} + 460) - (\text{Readout Temperature } ^\circ\text{F} + 460)}{\text{Reference Temperature } ^\circ\text{F} + 460}$$

Or

$$\% \text{ Dif} = \frac{(\text{Reference Temperature } ^\circ\text{C} + 273) - (\text{Readout Temperature } ^\circ\text{C} + 273)}{\text{Reference Temperature } ^\circ\text{C} + 273}$$



THERMOMETER CALIBRATION

DATE: 6/5/15 TECHNICIAN: A.T. Myren

MANUFACTURER:	<u>ERTCO</u>	<u>ERTCO</u>	<u>Fisher</u>	<u>Taylor</u>	<u>Taylor</u>	<u>Premium</u>
CAT #.	<u>1005-3FC</u>	<u>E17</u>	<u>ASTM 59F</u>	<u>1330 N/A</u>	<u>1330 N/A</u>	<u>—</u>
SERIAL NO.	<u>1697</u>	<u>K35473</u>	<u>AD4544</u>	<u>—</u>	<u>—</u>	<u>—</u>
RANGE:	<u>-1 to 100°C</u>	<u>0-260°C</u>	<u>0-180°F</u>	<u>20-120°F</u>	<u>20-120°F</u>	<u>0-220°F</u>
GRADUATIONS:	<u>0.1°C</u>	<u>1°C</u>	<u>1°F</u>	<u>1°F</u>	<u>1°F</u>	<u>2°F</u>
TYPE:	<u>Tube</u>	<u>Tube</u>	<u>Tube</u>	<u>Tube</u>	<u>Tube</u>	<u>Dial</u>
TEMP. POINT						
1	<u>1.9</u>	<u>1</u>	<u>34</u>	<u>35</u>	<u>35</u>	<u>36</u>
2	<u>8.9</u>	<u>9.0</u>	<u>48</u>	<u>48</u>	<u>49</u>	<u>50</u>
3	<u>20.1</u>	<u>21</u>	<u>69</u>	<u>70</u>	<u>70</u>	<u>72</u>
4	<u>31.5</u>	<u>32</u>	<u>89</u>	<u>90</u>	<u>91</u>	<u>92</u>

COMMENTS:

°F = (°C X 9/5) + 32  
°C = (5/9) (°F - 32)

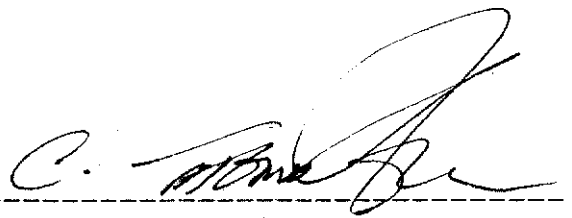
Note: The 2 Taylor Thermometers are in the Sling Psychrometer

R E P O R T O F C A L I B R A T I O N  
L I Q U I D - I N - G L A S S - T H E R M O M E T E R

THE THERMOMETER WAS TESTED IN A LARGE, CLOSED-TOP, ELECTRICALLY HEATED, LIQUID BATH, BEING "IMMERSED" 76MM. THE TEMPERATURE OF THE ROOM WAS ABOUT 25 DEGREES C (77 DEGREES F). IF THE THERMOMETER IS USED UNDER CONDITIONS WHICH WOULD CAUSE THE AVERAGE TEMPERATURE OF THE EMERGENT LIQUID COLUMN TO DIFFER MARKEDLY FROM THAT PREVAILING IN THE TEST, APPRECIABLE DIFFERENCES IN THE INDICATIONS OF THE THERMOMETER WOULD RESULT.

THE TABULATED CORRECTIONS APPLY PROVIDED THE ICE-POINT READING, TAKEN AFTER EXPOSURE FOR NOT LESS THAN 3 DAYS TO A TEMPERATURE OF ABOUT 20 DEGREES C (70 DEGREES F) IS 0.00 DEGREES C. IF THE ICE-POINT READING IS FOUND TO BE HIGHER (OR LOWER) THAN STATED, ALL OTHER READINGS WILL BE HIGHER (OR LOWER) TO THE SAME EXTENT. IF THE THERMOMETER IS USED AT A GIVEN TEMPERATURE SHORTLY AFTER BEING HEATED TO A HIGHER TEMPERATURE. AN ERROR OF 0.01 DEGREES OR LESS, FOR EACH 10 DEGREE DIFFERENCE BETWEEN THE TWO TEMPERATURES, MAY BE INTRODUCED. THE TABULATED CORRECTIONS APPLY IF THE THERMOMETER IS USED IN THE UPRIGHT POSITION; IF USED IN A HORIZONTAL POSITION, THE INDICATIONS MAY BE A FEW HUNDREDTHS OF A DEGREE HIGHER.

TEST NUMBER: 152439  
DATE: 07/16/96  
STANDARD SERIAL NO. 128239  
NIST IDENTIFICATION NO. 88024



---

Charles Tang-Nian  
QUALITY CONTROL MANAGER

EVER READY THERMOMETER CO., INC.  
228 LACKAWANNA AVENUE  
WEST PATTERSON, NJ 07424  
(201) 812-7474

PAGE 1 OF 2

R E P O R T O F C A L I B R A T I O N  
LIQUID-IN-GLASS-THERMOMETER

CALIBRATED BY EVER READY THERMOMETER CO.

MARKED: ERTCO CAT 1005-3FC S/N-1697  
RANGE: -1 TO +101 DEGREES C IN 0.1 DEGREE GRADUATIONS.

THERMOMETER READING	CORRECTION (ITS-90)**
0.00 C	0.00 C
10.00	0.00
20.00	0.00
30.00	0.00
37.00	0.00
40.00	0.00
50.00	0.00
56.00	0.00
60.00	0.02
70.00	0.00
80.00	0.00
90.00	0.00
100.00	0.00

\*\* ALL TEMPERATURES IN THIS REPORT ARE BASED ON THE INTERNATIONAL TEMPERATURE SCALE OF 1990 (ITS-90) PUBLISHED IN THE METROLOGIA 27, NO. 1, 3/10/90.

THIS THERMOMETER WAS CALIBRATED AGAINST A STANDARD CALIBRATED AT THE NATIONAL INSTITUTE OF STANDARDS AND TECHNOLOGY (NIST) FORMERLY THE NATIONAL BUREAU OF STANDARDS (NBS) IN ACCORDANCE WITH ASTM METHOD E 77, AND NBS MONOGRAPH 174.

FOR A DISCUSSION OF ACCURACIES ATTAINABLE WITH SUCH THERMOMETERS SEE NBS MONOGRAPH 250-23.

IF NO SIGN IS GIVEN ON THE CORRECTION, THE TRUE TEMPERATURE IS HIGHER THAN THE INDICATED TEMPERATURE; IF THE SIGN GIVEN IS NEGATIVE, THE TRUE TEMPERATURE IS LOWER THAN THE INDICATED TEMPERATURE. TO USE THE CORRECTIONS PROPERLY, REFERENCE SHOULD BE MADE TO THE NOTES GIVEN BELOW.

CONTINUED

TEST NUMBER: 152439  
DATE: 07/16/96  
STANDARD SERIAL NO. 128239  
NIST IDENTIFICATION NO. 88024

Dry Gas Meter Calibration Data

Date: 5/11/15 Technician: A. T. Myrum  
 Calibration Meter Mfr: Rockwell SN: 1052202 Y: 0.9963  
 Meter Box ID 45G-P Meter Mfr: Rockwell SN: 3039270  
 Electrical Check ok Pitot Leak Check N/A  
 Leak Check Front Half ok Back Half ok *See back of page*  
 BP = 28.32 in. Hg

Orifice (Δh) in. H <sub>2</sub> O	Gas Volume			Temperature				Time (Θ), Min.	VAC
		Cal. Meter (Vc), (cu.ft.)	Dry Gas Meter (Vm), (m <sup>3</sup> )(ft <sup>3</sup> )		Cal. Meter (Tc), °F	Dry Gas Meter			
						Inlet (Tmi), (°F)(°C)	Outlet (Tmo), (°F)(°C)		
.80	initial	289.827	940.300	initial	72	74	74	14.100.34	-0.5
	.80	296.640	947.060	mid	69.5	77	77	14.006	-0.5
				final	69.5	76	76		-0.5
	total	6.812	6.760	avg.	70.3	75.7	75.7	75.7	
					530.3	535.7	535.7	535.7	
.90	initial	297.291	947.700	initial	69.5	77	77	10.154.75	-0.5
	.90	303.220	953.632	mid	68	79	79	10.996	-0.5
				final	67.5	81	81		-0.5
	total	5.929	5.932	avg.	68.3	79	79	79	
					528.3	539	539	539	
1.00	initial	303.878	954.300	initial	68	80	80	9.954.91	-0.5
	1.00	309.613	960.075	mid	67.5	83	83	9.915	-0.5
				final	67.5	84	84		-0.5
	total	5.785	5.775	avg.	67.7	82.3	82.3	82.3	
					527.7	542.3	542.3	542.3	
	initial			initial					
	final			mid					
				final					
	total			avg.					
	initial			initial					
	final			mid					
				final					
	total			avg.					

$$Y = \frac{(Y)(Vc)(Pb)(Tm + 460)}{(Vm)(Pb + \Delta h/13.6)(Tc + 460)}$$

$$\Delta h@ = \frac{(0.0317)(\Delta h)}{Pb(Tmo + 460)} \left[ \frac{[(Tc + 460)(\Theta)]}{[(Vc)(Yc)]^2} \right]$$



Meter Box Calibration Page 2

$$Y = \frac{(Y_c)(V_c)(BP)(T_m + 460)}{(V_m)(BP + \Delta H/13.6)(T_c + 460)} =$$

$$Y = \frac{(.9963)(6.813)(28.32)(\overset{530.3}{703 + 460})}{(6.760)(28.32 + .80/13.6)(\overset{535.7}{75.7 + 460})} = \frac{101,939.710}{102,769.142} = 0.99193$$

$$Y = \frac{(.9963)(5.929)(28.32)(\overset{539}{79 + 460})}{(5.932)(28.32 + .90/13.6)(\overset{528.3}{68.3 + 460})} = \frac{90,168.240}{88,958.746} = 1.01360$$

$$Y = \frac{(.9963)(5.735)(28.32)(\overset{541.3}{82.3 + 460})}{(5.775)(28.32 + 1.00/13.6)(\overset{527.7}{67.7 + 460})} = \frac{87,751.875}{86,528.358} = 1.01414$$

$$Y = \frac{(\quad)(\quad)(\quad)(\quad + 460)}{(\quad)(\quad + \quad/13.6)(\quad + 460)} = \quad = \quad$$

$$Y = \frac{(\quad)(\quad)(\quad)(\quad + 460)}{(\quad)(\quad + \quad/13.6)(\quad + 460)} = \quad = \quad$$

Y Factor                      Variation      (± 0.02 Allowed From Average Y)

0.99193                      -0.0146 ✓

1.01360                      +0.0070 ✓

1.01414                      +0.0076

\_\_\_\_\_ ✓                      \_\_\_\_\_

\_\_\_\_\_ ✓                      \_\_\_\_\_

o/k

AM

Avg Y 1.00656 ✓

3.01967 ✓

METER BOX 45G-P

DATE 5/11/15

Page 3 of 3

$$\Delta H\theta = \frac{(0.0317) (\Delta H)}{(P_b) (T_{mo} + 460)} \cdot \left[ \frac{(T_w + 460) (\Theta)}{(Y_c) (V_c)} \right]^2 =$$
$$\Delta H\theta = \frac{(0.0317) (1.80)}{(28.32) (757 + 460)} \cdot \left[ \frac{(70.3 + 460) (14.006)}{(.9963) (6.813)} \right]^2 = 2.0015$$
$$\Delta H\theta = \frac{(0.0317) (1.90)}{(28.32) (79 + 460)} \cdot \left[ \frac{(68.3 + 460) (10.996)}{(.9963) (5.929)} \right]^2 = 1.8076$$
$$\Delta H\theta = \frac{(0.0317) (1.00)}{(28.32) (823 + 460)} \cdot \left[ \frac{(67.7 + 460) (9.915)}{(.9963) (5.735)} \right]^2 = 1.7308$$
$$\Delta H\theta = \frac{(0.0317) ( )}{( ) ( + 460)} \cdot \left[ \frac{( + 460) ( )}{( ) ( )} \right]^2 = \underline{\hspace{2cm}}$$
$$\Delta H\theta = \frac{(0.0317) ( )}{( ) ( + 460)} \cdot \left[ \frac{( + 460) ( )}{( ) ( )} \right]^2 = \underline{\hspace{2cm}}$$

<u><math>\Delta H\theta</math></u>	<u>VARIATION (<math>\pm 0.20</math> ALLOWED)</u>
<u>2.0015</u>	<u>+0.1549</u> ✓
<u>1.8076</u>	<u>-0.0390</u> ✓
<u>1.7308</u>	<u>-0.1158</u> ✓
_____	_____
_____	_____
AVG $\Delta H\theta$ <u>1.8466</u> ✓	

5.5399 ✓

OK  
AMM

Post Test  
**Meter Box Audit**  
 Woodstove Data Sheet #32

Unit: HEAT TECH HTP 26 S  
 Date: 7/29/15  
 Technician: ATM  
 WST9-Form2, Rev 6/11

45G-P (T1)

**Meter Box Calibration Audit**  
**Test Data**

Run #	1	2	3	4	5	6	7	8	9	10
Avg. Δh	.90									
Max Vac	-1.5									

Avg. Test Series Δh: .90 in H<sub>2</sub>O. Test Series Max Vac: -1.5 in Hg

Audit Dry Gas Meter Mfr: Rockwell SN: 1052202 Correction Factor (Y): .9963  
 Test Dry Gas Meter Mfr: Rockwell SN: 3039270 Correction Factor (Y): 1.0066

Audit Data

		Audit #1	Audit #2	Audit #3
BP ("Hg):		<u>28.62</u>	<u>28.62</u>	<u>28.61</u>
Vac ("Hg):		<u>-1.5</u>	<u>-1.5</u>	<u>-1.5</u>
Audit Meter:	Final Vol	<u>361.393</u>	<u>371.745</u>	<u>378.561</u>
	Initial Vol	<u>356.352</u>	<u>362.336</u>	<u>372.741</u>
	Vol (V <sub>e</sub> , Ft <sup>3</sup> )	<u>5.041</u> ✓	<u>9.409</u> ✓	<u>5.820</u> ✓
Audit Meter	Temp (°F) (T <sub>c</sub> )			
	Initial	<u>62.5</u>	<u>64.5</u>	<u>64.5</u>
	Mid	<u>62.5</u>	<u>63.5</u>	<u>65</u>
	Final	<u>62.5</u>	<u>63.5</u> ✓	<u>65</u>
	Avg (°F/°A)	<u>62.5 (522.5)</u> ✓	<u>63.8 (523.8)</u>	<u>64.8 (524.8)</u> ✓
Δh ("H <sub>2</sub> O)	Initial	<u>.90</u>	<u>.90</u>	<u>.90</u>
	Mid	<u>.90</u>	<u>.90</u>	<u>.90</u>
	Final	<u>.90</u>	<u>.90</u>	<u>.90</u>
	Avg	<u>.90</u> ✓	<u>.90</u> ✓	<u>.90</u> ✓
Dry Gas Meter:	Final Vol	<u>844.026</u>	<u>854.776</u>	<u>861.868</u>
	Initial Vol	<u>838.800</u>	<u>845.000</u>	<u>855.800</u>
	Vol (V <sub>d</sub> ) (ft <sup>3</sup> ) (m <sup>3</sup> )	<u>5.226</u> ✓	<u>9.776</u> ✓	<u>6.068</u> ✓
Dry Gas Meter	Temp (°F) : Inlet (T <sub>m</sub> )			
	Initial	<u>78</u>	<u>78</u>	<u>81</u>
	Mid	<u>81</u>	<u>81</u>	<u>84</u>
	Final	<u>81</u>	<u>84</u>	<u>86</u> ✓
	Avg (°F/°A)	<u>80 (540)</u>	<u>81 (541)</u> ✓	<u>83.7 (543.7)</u>
Dry Gas Meter	Temp (°F) : Outlet (T <sub>m</sub> )			
	Initial	<u>78</u>	<u>78</u>	<u>81</u>
	Mid	<u>81</u>	<u>81</u>	<u>84</u>
	Final	<u>81</u>	<u>84</u> ✓	<u>86</u> ✓
	Avg (°F/°A)	<u>80 (540)</u>	<u>81 (541)</u> ✓	<u>83.7 (543.7)</u>
Avg Dry Gas	Meter Temp (T <sub>m</sub> - °F/°A)	<u>80 (540)</u>	<u>81 (541)</u> ✓	<u>83.7 (543.7)</u>
	Time (minutes)	<u>9:33.37</u>	<u>18:13.03</u>	<u>11:19.00</u>

Note: If volume is in m<sup>3</sup>, multiply by 35.314667 to obtain ft<sup>3</sup>.  
 Note: Add 460° to all temperatures for degrees Absolute.

$$Y = \frac{(V_c)(MCF)(BP)(T_m)}{(V_a)(BP + \Delta h/13.6)(T_c)}$$

$$Y \text{ Factor \% Difference} = \frac{\text{Act} - \text{Exp}}{\text{Exp}} \times 100$$

HEAT TECH  
HTP 26 STD

Note: MCF = Meter Correction Factor (Y) for Dry Gas Meter used as a Transfer Standard

Run 1

$$Y = \frac{(5.041)(.9963)(28.62)(540)}{(5.226)(28.62 + .90/13.6)(522.5)} = \frac{77,619.389}{78,330.043} = .99093$$

$$\Delta\% = \frac{(.99093 - 1.01360)}{1.01360} \times 100 = -2.237\%$$

Run 2

$$Y = \frac{(9.409)(.9963)(28.62)(541)}{(9.776)(28.62 + .90/13.6)(523.8)} = \frac{145,144,470}{146,892.409} = .98810$$

$$\Delta\% = \frac{(.98810 - 1.01360)}{1.01360} \times 100 = -2.516\%$$

Run 3

$$Y = \frac{(5.820)(.9963)(28.61)(543.7)}{(6.068)(28.61 + .90/13.6)(524.8)} = \frac{90,196.629}{91,318.894} = .98771$$

$$\Delta\% = \frac{(.98771 - 1.01360)}{1.01360} \times 100 = -2.554\%$$

Note: The Y Factor % Difference must be  $\leq \pm 5.0\%$  to be acceptable. Avg.  $\Delta\% = -2.436$

Determination of Interpolated Y Factor for Average Certification Test Series  $\Delta H$  from Dry Gas Meter Calibration Data:

0.90 inch H<sub>2</sub>O  $\Delta h =$  1.01360 Calculated Calibration Y Factor cal on 5/11/15  
 (A) (C) (from Calibration)  
         inch H<sub>2</sub>O  $\Delta h =$           Calculated Calibration Y Factor  
 (B) (D) (from Calibration)

$$\frac{(B) - (A)}{(B) + (A)} \times 100 = \frac{(E) - (D)}{(E) + (D)} \times 100 = \frac{(F) - (C)}{(F) + (C)} \times 100$$

$$\text{Avg } \Delta h \text{ (A)} = \frac{(B) - (A)}{(B) + (A)} \times 100 = \text{(G)}$$

$$\left[ \frac{(F) - (C)}{(F) + (C)} \right] + \frac{\text{Avg } \Delta h \text{ (A)}}{C} = \text{Interpolated Y Factor For Avg. Test Series } \Delta h$$

Dry Gas Meter Back Half Leak Check:         , 000 inch H<sub>2</sub>O in One Minute  
 Front Half Leak Check          Meter Reading          Leak Rate

Meter	Vac In. Hg	Start	Stop	cmm	cfm
DGM	-17.0	.543	.543		.000
TM	-17.0	.050	.050		.000



Dry Gas Meter Calibration Data

Date: 5/14/15 Technician: JT. Myra  
 Calibration Meter Mfr: Rockwell SN: 1052202 Y: 0.9963  
 Meter Box ID Apex 511-M Meter Mfr: Rockwell SN: 322914  
 Electrical Check OK Pitot Leak Check N/A  
 Leak Check Front Half OK Back Half OK See Back of Page  
 BP = 28.32 in. Hg

Orifice (Δh) in. H <sub>2</sub> O	Gas Volume			Temperature				Time (Θ), Min.
		Cal. Meter (Vc), (cu.ft.)	Dry Gas Meter (Vm), (m <sup>3</sup> )(ft <sup>3</sup> )		Cal. Meter (Tc), °F	Dry Gas Meter		
						Inlet (Tmi), (°F)(°C)	Outlet (Tmo), (°F)(°C)	
.80	initial	267.368	886.002	initial	70	68	68	16:01.04
	final	275.436	894.3045	mid	68.5	70	68	16:017
				final	68	71	68	
	total	8.068	8.3045	avg.	68.8	69.7	68	68.83
.80					528.8	529.7	528	528.8
.90	initial	276.021	894.900	initial	68	70	68	11:37.53
	final	282.252	901.304	mid	67	71	68	11:626
				final	67	71	69	
	total	6.231	6.404	avg.	67.3	70.7	68.3	69.5
.90					527.3	530.7	528.3	529.5
.75	initial	282.926	902.000	initial	67	69	69	11:17.56
	final	288.424	907.672	mid	67	70	69	11:293
				final	67	71	69	
	total	5.498	5.672	avg.	67	70	69	69.5
.75					527	530	529	529.5
	initial			initial				
	final			mid				
				final				
	total			avg.				
	initial			initial				
	final			mid				
				final				
	total			avg.				

Vmc  
0  
0  
0  
-  
0  
0  
0  
-  
0  
0  
0

$$Y = \frac{(Y)(Vc)(Pb)(Tm + 460)}{(Vm)(Pb + \Delta h / 13.6)(Tc + 460)}$$

$$\Delta h @ = \frac{(0.0317)(\Delta h)}{Pb(Tmo + 460)} \quad [ (Tc + 460)(\Theta) ] / [ (Vc)(Yc) ]^2$$

# Back Half Leak Check

side 1      mano  
 Start      +9.10 " H<sub>2</sub>O  
 Stop      +9.10 " H<sub>2</sub>O  
             0.00 Leak Rate

side 2      mano  
 Start      +8.00 " H<sub>2</sub>O  
 Stop      +8.00 " H<sub>2</sub>O  
             0.00 Leak Rate

# 2" Manometer System

side 1      start      mano  
             +0.94 " H<sub>2</sub>O  
 Stop      +0.94 " H<sub>2</sub>O

side 2      Start      1.52 " H<sub>2</sub>O  
             Stop      1.52 " H<sub>2</sub>O  
             0.00 Leak Rate

# Front Half Leak Check

	"VAC	MIR	BDG	Leak Rate
DGM	-165 "Hg	Start 303	Stop 303	.000 cfm
Tm	-165 "Hg	685	686	.001 cfm

Had a leak on the pump outlet.  
 Tightened swag fittings, all OK.

Meter Box: 511-M  
 Date: 8/11/15  
 Page: 2 of 3

Rev 6-10

Meter Box Calibration Page 2

A. Timyren

$$Y = \frac{(Y_c)(V_c)(BP)(T_m + 460)}{(V_m)(BP + \Delta H/13.6)(T_c + 460)} =$$

$$Y = \frac{(1.9963)(8.068)(28.32)(68.8 + 460)}{(8.3045)(28.32 + 1.80/13.6)(68.8 + 460)} = \frac{120,376.224}{124,623.322} = 0.96592$$

528.8

$$Y = \frac{(1.9963)(6.231)(28.32)(69.5 + 460)}{(6.404)(28.32 + .90/13.6)(67.3 + 460)} = \frac{93,090.871}{95,855.270} = 0.97116$$

529.5

$$Y = \frac{(1.9963)(5.498)(28.32)(69.5 + 460)}{(5.672)(28.32 + .75/13.6)(67 + 460)} = \frac{82,139.883}{84,817.401} = 0.96843$$

529.5

$$Y = \frac{(\quad)(\quad)(\quad)(+460)}{(\quad)(\quad + \quad/13.6)(\quad + 460)} = \quad = \quad$$

$$Y = \frac{(\quad)(\quad)(\quad)(+460)}{(\quad)(\quad + \quad/13.6)(\quad + 460)} = \quad = \quad$$

Y Factor                      Variation      (± 0.02 Allowed From Average Y)

0.96592                      -0.0026      -

0.97116                      +0.0027      -

0.96843                      -0.0001      -

ok  
 (ASTM)

Avg Y 0.96850 -

2.90551 -

$$\Delta H\theta = \frac{(0.0317)(\Delta H)}{(P_b)(T_{mo} + 460)} \cdot \left[ \frac{(T_w + 460)(\theta)}{(Y_c)(V_c)} \right]^2 =$$

$$\Delta H\theta = \frac{(0.0317)(.80)}{(28.32)(68 + 460)} \cdot \left[ \frac{(68.8 + 460)(16.017)}{(.9963)(8.068)} \right]^2 = 1.8830$$

$$\Delta H\theta = \frac{(0.0317)(.90)}{(28.32)(68.3 + 460)} \cdot \left[ \frac{(67.3 + 460)(11.626)}{(.9963)(6.231)} \right]^2 = 1.8595$$

$$\Delta H\theta = \frac{(0.0317)(.75)}{(28.32)(69 + 460)} \cdot \left[ \frac{(67 + 460)(11.293)}{(.9963)(5.498)} \right]^2 = 1.8734$$

$$\Delta H\theta = \frac{(0.0317)(\quad)}{(\quad)(\quad + 460)} \cdot \left[ \frac{(\quad + 460)(\quad)}{(\quad)(\quad)} \right]^2 = \underline{\quad}$$

$$\Delta H\theta = \frac{(0.0317)(\quad)}{(\quad)(\quad + 460)} \cdot \left[ \frac{(\quad + 460)(\quad)}{(\quad)(\quad)} \right]^2 = \underline{\quad}$$

<u><math>\Delta H\theta</math></u>	<u>VARIATION (<math>\pm 0.20</math> ALLOWED)</u>
<u>1.8830</u>	<u>+0.0110</u> -
<u>1.8595</u>	<u>-0.0125</u>
<u>1.8734</u>	<u>+0.0143</u> -
<u>AVG <math>\Delta H\theta</math></u>	<u>1.8720</u> -

5.6159 -

ok  
 AM



**Post Test  
Meter Box Audit  
Woodstove Data Sheet #32**

Unit: HEAT TECH HP26 570  
 Date: 7/20/15  
 Technician: ATM  
 WST9-Form2, Rev 6/11

511-M (T2)

**Meter Box Calibration Audit  
Test Data**

Run #	1	2	3	4	5	6	7	8	9	10
Avg. Δh	<u>.75</u>									
Max Vac	<u>-1.0</u>									

Avg. Test Series Δh: .750 in H<sub>2</sub>O. Test Series Max Vac: -1.0 in Hg

Audit Dry Gas Meter Mfr: Rockwell SN: 1052202 Correction Factor (Y): .9963  
 Test Dry Gas Meter Mfr: Rockwell SN: 322914 Correction Factor (Y): .9685

Audit Data

		Audit #1	Audit #2	Audit #3
BP ("Hg):		<u>28.58</u>	<u>28.58</u>	<u>28.58</u>
Vac ("Hg):		<u>-1.0</u>	<u>-1.0</u>	<u>-1.0</u>
Audit Meter:	Final Vol	<u>412.005</u>	<u>417.503</u>	<u>423.374</u>
	Initial Vol	<u>406.738</u>	<u>412.408</u>	<u>418.289</u>
	Vol (V <sub>c</sub> , Ft <sup>3</sup> )	<u>45.267</u> ✓	<u>5.095</u> ✓	<u>5.085</u> ✓
Audit Meter				
Temp (°F) (T <sub>c</sub> )	Initial	<u>70</u>	<u>70</u>	<u>71</u>
	Mid	<u>70</u>	<u>70.5</u>	<u>71</u>
	Final	<u>70.5</u>	<u>71</u>	<u>71</u>
	Avg (°F/°A)	<u>70.2</u> (530.2) ✓	<u>70.5</u> (530.5) ✓	<u>71</u> (531) ✓
Δh ("H <sub>2</sub> O)	Initial	<u>.75</u>	<u>.75</u>	<u>.75</u>
	Mid	<u>.75</u>	<u>.75</u>	<u>.75</u>
	Final	<u>.75</u>	<u>.75</u>	<u>.75</u>
	Avg	<u>.75</u> ✓	<u>.75</u> ✓	<u>.75</u> ✓
Dry Gas Meter:	Final Vol	<u>343.599</u>	<u>349.203</u>	<u>355.201</u>
	Initial Vol	<u>338.200</u>	<u>344.000</u>	<u>350.000</u>
	Vol (V <sub>d</sub> ) (ft <sup>3</sup> ) (m <sup>3</sup> )	<u>5.399</u> ✓	<u>5.203</u> ✓	<u>5.201</u> ✓
Dry Gas Meter	Initial	<u>72</u>	<u>73</u>	<u>74</u>
Temp (°F) : Inlet	Mid	<u>73</u>	<u>73</u>	<u>74</u>
(T <sub>m</sub> )	Final	<u>72</u>	<u>73</u>	<u>74</u>
	Avg (°F/°A)	<u>72.3</u> (532.3) ✓	<u>73</u> (533) ✓	<u>74</u> (534) ✓
Dry Gas Meter	Initial	<u>71</u>	<u>72</u>	<u>72</u>
Temp (°F) : Outlet	Mid	<u>71</u>	<u>71</u>	<u>72</u>
(T <sub>m</sub> )	Final	<u>71</u>	<u>72</u>	<u>73</u>
	Avg (°F/°A)	<u>71</u> (531) ✓	<u>71.7</u> (531.7) ✓	<u>72.3</u> (532.3) ✓
Avg Dry Gas				
Meter Temp (T <sub>m</sub> - °F/°A)		<u>71.7</u> (531.7) ✓	<u>72.3</u> (532.3) ✓	<u>73.2</u> (533.2) ✓
Time (minutes)		<u>10:01.24</u>	<u>9:36.53</u>	<u>9:35.90</u>

Note: If volume is in m<sup>3</sup>, multiply by 35.314667 to obtain ft<sup>3</sup>.  
 Note: Add 460° to all temperatures for degrees Absolute.

$$Y = \frac{(V_d)(MCF)(BP)(T_m)}{(V_a)(BP + \Delta h/13.6)(T_c)}$$

$$Y \text{ Factor \% Difference} = \frac{\text{Act} - \text{Exp}}{\text{Exp}} \times 100$$

*HERP Tech*  
*HTP 265th*  
*511-11*

Note: MCF = Meter Correction Factor (Y) for Dry Gas Meter used as a Transfer Standard

**Run 1**

$$Y = \frac{(5.267)(.9963)(28.58)(531.7)}{(5.399)(28.58 + .75/13.6)(530.2)} = \frac{79,741.120}{81,969.534} = .9728$$

$$\Delta\% = \frac{.9728 - .9685}{.9685} \times 100 = +0.444\%$$

**Run 2**

$$Y = \frac{(5.095)(.9963)(28.58)(532.3)}{(5.203)(28.58 + .75/13.6)(530.5)} = \frac{77,224.127}{79,038.490} = .9770$$

$$\Delta\% = \frac{.9770 - .9685}{.9685} \times 100 = +0.878\%$$

**Run 3**

$$Y = \frac{(5.085)(.9963)(28.58)(533.2)}{(5.201)(28.58 + .75/13.6)(531)} = \frac{77,202.871}{79,082.573} = .9762$$

$$\Delta\% = \frac{.9762 - .9685}{.9685} \times 100 = +0.795\%$$

Note: The Y Factor % Difference must be < ±5.0% to be acceptable. Avg. Δ% = +0.706%

**Determination of Interpolated Y Factor for Average Certification Test Series Δ H from Dry Gas Meter Calibration Data:**

0.75 inch H<sub>2</sub>O Δh = 0.96843 Calculated Calibration Y Factor  
(A) (C) (from Calibration)

*from cal done on*  
*5/11/15*

inch H<sub>2</sub>O Δh = Calculated Calibration Y Factor  
(B) (D) (from Calibration)

$$\frac{(B) - (A)}{(B) + (A)} \times 100 = \frac{(D) - (C)}{(D) + (C)} \times 100 =$$

$$\text{Avg } \Delta h \text{ (A)} = \text{X 100} = \text{(G)}$$

Leg 1	Leg 2
+8.10	+7.60
+8.10	+7.60
<u>Δ 0.00</u>	<u>Δ 0.00</u>

$$\left[ \frac{(F) \times (G)}{(D) + (C)} \right] + \frac{(C)}{(D) + (C)} = \text{Interpolated Y Factor For Avg. Test Series } \Delta h$$

Dry Gas Meter Back Half Leak Check: .000 inch H<sub>2</sub>O in One Minute

Front Half Leak Check Meter Reading Leak Rate

Meter	Vac In. Hg	Start	Stop	cmm	cfm
DGM	-16.5	337.990	337.992		.002
TM	-16.5	405.487	405.487		.000

RB

Dry Gas Meter Calibration Data

Date: 5/12/15

Technician: A.T. Myrum

Calibration Meter Mfr: Rockwell SN: 1052002 Y: 0.9963

Meter Box ID Room Blank Meter Mfr: Kimmom SN: 8000571

Electrical Check ok Pitot Leak Check N/A

Leak Check Front Half ok Back Half ok over

BP = 28.34 in. Hg

Orifice (Δh) in. H <sub>2</sub> O	Gas Volume			Temperature				Time (Θ), Min.
		Cal. Meter (Vc), (cu.ft.)	Dry Gas Meter (Vm), (m <sup>3</sup> )(ft <sup>3</sup> )		Cal. Meter (Tc), °F	Dry Gas Meter		
						Inlet (Tmi), (°F)(°C)	Outlet (Tmo), (°F)(°C)	
.115	initial	315.769	127.3690	initial	73	70	70	9:58.54
	final	320.996	127.5209	mid	72	73	71	9:57.6
				final	72	75	72	
	total	5.227	11519	avg.	72.3	72.7	71	71.83
.115			5.3643		532.3	532.7	531	531.8
.100	initial	322.240	127.5570	initial	72	74	72	12:11.75
	final	328.115	127.72755	mid	72	75	73	12:19.6
				final	72	76	73	
	total	5.875	117055	avg.	72	75	72.7	73.8
.100			6.0229		532	535	532.7	533.8
.130	initial	329.235	127.7600	initial	71.5	75	73	9:19.31
	final	334.505	127.9132	mid	72	77	73	9:32.2
				final	71.5	77	74	
	total	5.270	11532	avg.	71.7	76.3	73.3	74.8
.133			5.4102		531.7	536.3	533.3	534.8
	initial			initial				
	final			mid				
				final				
	total			avg.				
	initial			initial				
	final			mid				
				final				
	total			avg.				

$$Y = \frac{(Y)(Vc)(Pb)(Tm + 460)}{(Vm)(Pb + \Delta h/13.6)(Tc + 460)}$$

$$\Delta h @ = \frac{(0.0317)(\Delta h)}{Pb(Tmo + 460)} \left[ \frac{(Tc + 460)(\Theta)}{[(Vc)(Yc)]^2} \right]$$

Back Half Leak Check

Start - 7.52" H<sub>2</sub>O

Stop - 7.52" H<sub>2</sub>O

0.00 Leak Rate

Front Half Leak Check

mtr

Vac  
"Hg

mtr Rdg

Start Stop

Leak Rate

cmm cfm

DGM

-20.5

.22635

.22645

.0001

TM

-20.5

.740

.751

.011

.400

1.2



Room: Blank  
 Meter Box: Blank  
 Date: 5/12/15  
 Page: 2 of 3

Rev 6-10

Meter Box Calibration Page 2

AT Myren

$$Y = \frac{(Y_c)(V_c)(BP)(T_m + 460)}{(V_m)(BP + \Delta H/13.6)(T_c + 460)} =$$

$$Y = \frac{(.9963)(5.227)(28.34)(71.8 + 460)}{(5.3643)(28.34 + .115/13.6)(72.3 + 460)} = \frac{78,485.749}{80,946.660} = .96960$$

$$Y = \frac{(.9963)(5.875)(28.34)(73.8 + 460)}{(6.0229)(28.34 + .100/13.6)(72 + 460)} = \frac{88,547.523}{90,830.101} = .97487$$

$$Y = \frac{(.9963)(5.270)(28.34)(74.8 + 460)}{(5.4102)(28.34 + .133/13.6)(71.7 + 460)} = \frac{79,577.811}{81,551.070} = .97580$$

$$Y = \frac{(\quad)(\quad)(\quad)(\quad + 460)}{(\quad)(\quad + \quad/13.6)(\quad + 460)} = \quad = \quad$$

$$Y = \frac{(\quad)(\quad)(\quad)(\quad + 460)}{(\quad)(\quad + \quad/13.6)(\quad + 460)} = \quad = \quad$$

Y Factor                      Variation      (± 0.02 Allowed From Average Y)

<u>0.96960</u>	<u>-0.00382</u>
<u>0.97487</u>	<u>+0.00145</u>
<u>0.97580</u>	<u>+0.00238</u>
_____	_____
_____	_____

Avg Y 0.97342

2.92027

$$\Delta H\theta = \frac{(0.0317) (\Delta H)}{(Pb) (T_{mo} + 460)} \cdot \left[ \frac{(T_w + 460) (\Theta)}{(Y_c) (V_c)} \right]^2 =$$

$$\Delta H\theta = \frac{(0.0317) (.115)}{(2834) (71 + 460)} \cdot \left[ \frac{(723 + 460) (9.976)}{(.9963) (5.227)} \right]^2 = .25189$$

$$\Delta H\theta = \frac{(0.0317) (.100)}{(2834) (727 + 460)} \cdot \left[ \frac{(72 + 460) (12196)}{(.9963) (5.875)} \right]^2 = .25801$$

$$\Delta H\theta = \frac{(0.0317) (.133)}{(2834) (733 + 460)} \cdot \left[ \frac{(717 + 460) (9.323)}{(.9963) (5.270)} \right]^2 = .24859$$

$$\Delta H\theta = \frac{(0.0317) ( )}{( ) ( + 460)} \cdot \left[ \frac{( + 460) ( )}{( ) ( )} \right]^2 = \underline{\hspace{2cm}}$$

$$\Delta H\theta = \frac{(0.0317) ( )}{( ) ( + 460)} \cdot \left[ \frac{( + 460) ( )}{( ) ( )} \right]^2 = \underline{\hspace{2cm}}$$

<u>ΔHθ</u>	<u>VARIATION (± 0.20 ALLOWED)</u>
<u>.25189</u>	<u>-.00094</u>
<u>.25801</u>	<u>+ .00518</u>
<u>.24859</u>	<u>-.00424</u>
<u>          </u>	<u>          </u>
<u>          </u>	<u>          </u>
AVG ΔHθ <u>0.25283</u>	

.75849 /

**Post Test  
Meter Box Audit  
Woodstove Data Sheet #32**

*RB  
T. RUM*

Unit: HEAT Tech HTP 26 STD  
Date: 7/29/15  
Technician: ATM  
WST9-Form2, Rev 6/11

**Meter Box Calibration Audit  
Test Data**

Run #	1	2	3	4	5	6	7	8	9	10
Avg. Δh	.115									
Max Vac	-1.75									

Avg. Test Series Δh: .115 in H<sub>2</sub>O. Test Series Max Vac: -1.75 in Hg

Audit Dry Gas Meter Mfr: Rockwell SN: 1052202 Correction Factor (Y): 0.9963  
Test Dry Gas Meter Mfr: Kimmon SN: 8000571 Correction Factor (Y): 0.9734

Audit Data

		Audit #1	Audit #2	Audit #3
BP ("Hg):		<u>28.51</u>	<u>28.52</u>	<u>28.52</u>
Vac ("Hg):		<u>-2.0</u>	<u>-2.0</u>	<u>-2.0</u>
Audit Meter:	Final Vol	<u>463.363</u>	<u>469.030</u>	<u>475.923</u>
	Initial Vol	<u>457.235</u>	<u>463.592</u>	<u>469.358</u>
	Vol (V <sub>c</sub> , Ft <sup>3</sup> )	<u>6.128</u>	<u>5.348</u>	<u>6.565</u>
Audit Meter	Temp (°F) (T <sub>c</sub> )			
	Initial	<u>75</u>	<u>75.5</u>	<u>76</u>
	Mid	<u>75</u>	<u>75.5</u>	<u>76</u>
	Final	<u>75.5</u>	<u>76.0</u>	<u>76</u>
	Avg (°F/°A)	<u>75.2 (535.2)</u>	<u>75.7 (535.7)</u>	<u>76 (536)</u>
Δh ("H <sub>2</sub> O)	Initial	<u>.115</u>	<u>.115</u>	<u>.115</u>
	Mid	<u>.115</u>	<u>.115</u>	<u>.115</u>
	Final	<u>.115</u>	<u>.115</u>	<u>.115</u>
	Avg	<u>.115</u>	<u>.115</u>	<u>.115</u>
Dry Gas Meter:	Final Vol	<u>138,8636</u>	<u>139.0274</u>	<u>139.2271</u>
	Initial Vol	<u>138,6860</u>	<u>138,8700</u>	<u>139.0370</u>
	Vol(V <sub>d</sub> )(ft <sup>3</sup> )(m <sup>3</sup> )	<u>1776 612719</u>	<u>1574 5.5585</u>	<u>1901 67133</u>
Dry Gas Meter	Temp (°F) : Inlet (T <sub>m</sub> )			
	Initial	<u>80</u>	<u>81</u>	<u>81</u>
	Mid	<u>82</u>	<u>82</u>	<u>83</u>
	Final	<u>83</u>	<u>83</u>	<u>83</u>
	Avg(°F/°A)	<u>81.7 (541.7)</u>	<u>82 (542)</u>	<u>82.3 (542.3)</u>
Dry Gas Meter	Temp (°F) : Outlet (T <sub>m</sub> )			
	Initial	<u>79</u>	<u>80</u>	<u>80</u>
	Mid	<u>79</u>	<u>80</u>	<u>80</u>
	Final	<u>80</u>	<u>80</u>	<u>80</u>
	Avg(°F/°A)	<u>79.3 (539.3)</u>	<u>80 (540)</u>	<u>80 (540)</u>
Avg Dry Gas	Meter Temp (T <sub>m</sub> - °F/°A)	<u>80.5 540.5</u>	<u>81 (541)</u>	<u>81.2 541.1</u>
	Time (minutes)	<u>11:40.88</u>	<u>10:18.60</u>	<u>12:38.31</u>

Note: If volume is in m<sup>3</sup>, multiply by 35.314667 to obtain ft<sup>3</sup>.  
Note: Add 460° to all temperatures for degrees Absolute.

$$Y = \frac{(V_d)(MCF)(BP)(T_m)}{(V_d)(BP + \Delta h/13.6)(T_c)}$$

Y Factor % Difference =  $\frac{\text{Act} - \text{Exp}}{\text{Exp}} \times 100$  *Heat Tech*  
*RB*  
*inval 3* *HTP 26 STD*  
*7/29/15*

Note: MCF = Meter Correction Factor (Y) for Dry Gas Meter used as a Transfer Standard

**Run 1**

$$Y = \frac{(6.128)(.9963)(28.51)(540.5)}{(6.2719)(28.51 + .115/13.6)(536.2)} = \frac{94,090.973}{95,728.496} = 0.98279$$

$$\Delta\% = \left( \frac{.98279 - .96960}{.96960} \right) \times 100 = +1.360\%$$

**Run 2**

$$Y = \frac{(5.348)(.9963)(28.52)(541)}{(5.5585)(28.52 + .115/13.6)(535.7)} = \frac{82,210.694}{84,948.854} = 0.96777$$

$$\Delta\% = \left( \frac{0.96777 - .96960}{.96960} \right) \times 100 = -0.189\%$$

**Run 3**

$$Y = \frac{(6.565)(.9963)(28.52)(541.1)}{(6.7133)(28.52 + .115/13.6)(536)} = \frac{100,937.354}{102,654.764} = 0.98327$$

$$\Delta\% = \left( \frac{.98327 - .96960}{.96960} \right) \times 100 = +1.410\%$$

Note: The Y Factor % Difference must be < ±5.0% to be acceptable. Avg. Δ% = +0.8603

**Determination of Interpolated Y Factor for Average Certification Test Series Δ H from Dry Gas Meter Calibration Data:**

.115 inch H<sub>2</sub>O Δh = .96960 Calculated Calibration Y Factor  
 (A) (C) (from Calibration)

\_\_\_\_\_ inch H<sub>2</sub>O Δh = \_\_\_\_\_ Calculated Calibration Y Factor  
 (B) (D) (from Calibration)

\_\_\_\_\_ - \_\_\_\_\_ = \_\_\_\_\_ X 100 = \_\_\_\_\_  
 (B) (A) (E) (D) (C) (E) (F)

\_\_\_\_\_ - \_\_\_\_\_ = \_\_\_\_\_ X 100 = \_\_\_\_\_  
 Avg Δh (A) (G)

*Start + 8.72*  
*END + 8.72*  
*Δ 0.00*

$\left( \frac{F}{G} \times \frac{C}{D} \right) + \frac{E}{H} = \text{Interpolated Y Factor For Avg. Test Series } \Delta h$

Dry Gas Meter Back Half Leak Check: .000 inch H<sub>2</sub>O in One Minute  
 Front Half Leak Check \_\_\_\_\_ Meter Reading \_\_\_\_\_ Leak Rate

Meter	Vac In. Hg	Start	Stop	cmm	cfm
DGM	-15.0	138.6523	138.6523	.0000	.000
TM	-15.0	457.005	457.005	-	.000



**APEX INSTRUMENTS REFERENCE METER VERIFICATION  
USING WET-TEST METER #11AE6  
2-POINT ENGLISH UNITS**

Calibration Meter Information	
WTM Model #	AL20
WTM Serial #	11AE6
WTM Gamma	0.9999
Original 15Pt Gamma	0.9963

Calibration Conditions			
Date	Time	13-Mar-15	2:00
Barometric Pressure		30.05	in Hg
Calibration Tech		EW	
DGM Serial Number		S-110-1052202	

Factors/Conversions		
Std Temp	528	°R
Std Press	29.92	in Hg
K <sub>1</sub>	17.647	°R/in Hg

Run Time	Calibration Data										Results			
	Metering Console					Calibration Meter					Dry Gas Meter			
	DGM Input Pressure	Volume Initial	Volume Final	Volume Sample	Outlet Temp		Volume Initial	Volume Final	Volume Sample	Outlet Temp		Calibration Factor		Flowrate
Elapsed (⊖)	(P <sub>m</sub> )	(V <sub>m</sub> )	(V <sub>m</sub> )	(V <sub>m</sub> )	Initial (t <sub>m</sub> )	Final (t <sub>m</sub> )	(V <sub>m</sub> )	(V <sub>m</sub> )	(V <sub>m</sub> )	Initial (t <sub>m</sub> )	Final (t <sub>m</sub> )	Previous (Y)	Current (Y)	Std & Corr (Q <sub>meas</sub> /Q <sub>corr</sub> )
min	in H <sub>2</sub> O	cubic feet	cubic feet	cubic feet	°F	°F	cubic feet	cubic feet	cubic feet	°F	°F			cfm
6.00	-3.7	253.732	259.811	6:079	73.4	73.4	731.750	737.710	5.960	71	71	0.9963	0.9939	0.992
												Variation	0.25%	must be less than 1.5%
10.00	-2.2	259.811	265.431	5:620	73.4	73.4	737.710	743.240	5.530	71	71	0.9964	0.9938	0.552
												Variation	0.26%	must be less than 1.5%

I certify that the above Dry Gas Meter was calibrated in accordance with USEPA Methods, CFR 40 Part 60, App A, Method 5, Paragraph 7.1.2.2, using the Precision Wet Test Meter # 11AE6, which in turn was calibrated using the American Bell Prover # 3785, certificate # F107, which is traceable to the National Bureau of Standards (N.I.S.T.).

Signature



Date

3/13/15

**APEX INSTRUMENTS REFERENCE METER CALIBRATION**  
**USING WET-TEST METER #11AE6**  
**15-POINT ENGLISH UNITS**

Calibration Meter Information	
WTM Model #	AL-20
WTM Serial #	11AE6
WTM Gamma	0.9999

Calibration Conditions			
Date	Time	18-Feb-14	9:15
Barometric Pressure		29.8	in Hg
Calibration Technician		EW	
DGM Serial Number		S-110-1052202	

Factors/Conversions		
Std Temp	526	°R
Std Press	29.92	in Hg
K <sub>t</sub>	17.647	°R/in Hg

Run Time	Calibration Data											Results		
	Dry Gas Meter					Calibration Meter						Dry Gas Meter		
	Elapsed	Meter Pressure	Volume Initial	Volume Final	Sample Volume	Outlet Temp Initial	Outlet Temp Final	Volume Initial	Volume Final	Sample Volume	Outlet Temp Initial	Outlet Temp Final	Calibration Factor Value	Variation
(@)	(P <sub>m</sub> )	(V <sub>m1</sub> )	(V <sub>m2</sub> )	(V <sub>m</sub> )	(t <sub>m1</sub> )	(t <sub>m2</sub> )	(V <sub>w1</sub> )	(V <sub>w2</sub> )	(V <sub>w</sub> )	(t <sub>w1</sub> )	(t <sub>w2</sub> )	(Y)	(ΔY)	(Q <sub>massflow</sub> )
min	in H <sub>2</sub> O	cubic feet	cubic feet	cubic feet	°F	°F	cubic feet	cubic feet	cubic feet	°F	°F			cfm
5	-5.1	657.117	663.335	6.218	73.4	73.4	677.080	683.140	6.060	68.0	68.0	0.9970	0.00149	1.21
5	-5.1	663.335	669.550	6.215	73.4	73.4	683.140	689.180	6.040	68.0	68.0	0.9942	-0.00133	1.20
5	-5.1	669.550	675.768	6.218	73.4	73.4	689.180	695.230	6.050	68.0	68.0	0.9954	-0.00016	1.21
Passed Calibration Factor												0.9955	Averages	1.21

6	-3.7	694.023	699.987	5.964	75.2	75.2	713.145	718.970	5.825	68.0	68.0	0.9990	0.00269	0.97
6	-3.7	699.987	705.997	6.010	75.2	75.2	718.970	724.820	5.850	68.0	68.0	0.9956	-0.00071	0.97
6	-3.7	705.997	712.025	6.028	75.2	75.2	724.820	730.680	5.860	68.0	68.0	0.9944	-0.00198	0.97
Passed Calibration Factor												0.9963	Averages	0.97

7	-2.8	712.025	717.674	5.649	75.2	75.2	730.680	736.190	5.510	68.0	68.0	0.9955	0.00082	0.78
7	-2.8	717.674	723.317	5.643	75.2	75.2	736.190	741.690	5.500	68.0	68.0	0.9947	0.00007	0.78
7	-2.8	723.317	728.975	5.658	75.2	77.0	741.690	747.190	5.500	68.0	68.0	0.9938	-0.00090	0.78
Passed Calibration Factor												0.9947	Averages	0.78

10	-2.0	728.975	734.645	5.670	77.0	77.0	747.190	752.730	5.540	68.0	68.0	0.9986	0.00215	0.55
10	-2.0	734.645	740.312	5.667	77.0	77.0	752.730	758.260	5.530	68.0	68.0	0.9973	0.00088	0.55
10	-2.0	740.312	745.991	5.679	77.0	77.0	758.260	763.780	5.520	68.0	68.0	0.9934	-0.00303	0.55
Passed Calibration Factor												0.9964	Averages	0.55

15	-1.9	675.768	681.868	6.100	73.4	75.2	695.230	701.215	5.985	68.0	68.0	0.9974	-0.00135	0.40
15	-1.9	681.868	687.947	6.079	75.2	75.2	701.215	707.180	5.965	68.0	68.0	0.9992	0.00043	0.40
15	-1.9	687.947	694.023	6.076	75.2	75.2	707.180	713.145	5.965	68.0	68.0	0.9997	0.00092	0.40
Passed Calibration Factor												0.9988	Averages	0.40

Overall Average Y **0.9963**

Note: For Calibration Factor Y, the ratio of the reading of the calibration meter to the dry gas meter, acceptable tolerance of individual values from the average is ±0.02.

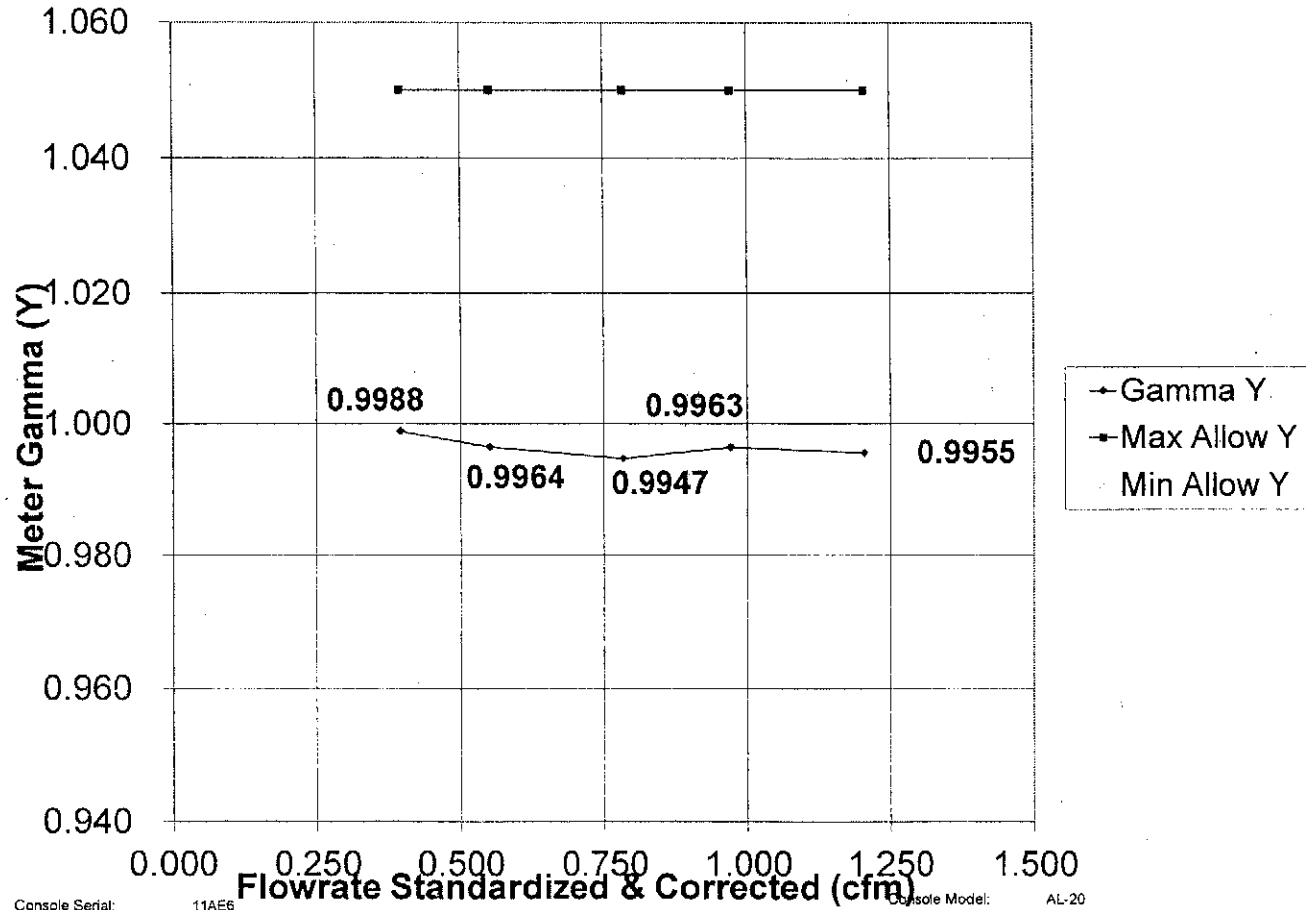
I certify that the above Dry Gas Meter was calibrated in accordance with USEPA Methods, CFR 40 Part 60, using the Precision Wet Test Meter # 11AE6, which in turn was calibrated using the American Bell Prover # 3785, certificate # F107, which is traceable to the National Bureau of Standards (N.I.S.T.).

Signature *Ed Web* Date *2/18/14*

Calibration Date: 2-18-2014

Calibration Technician: EW

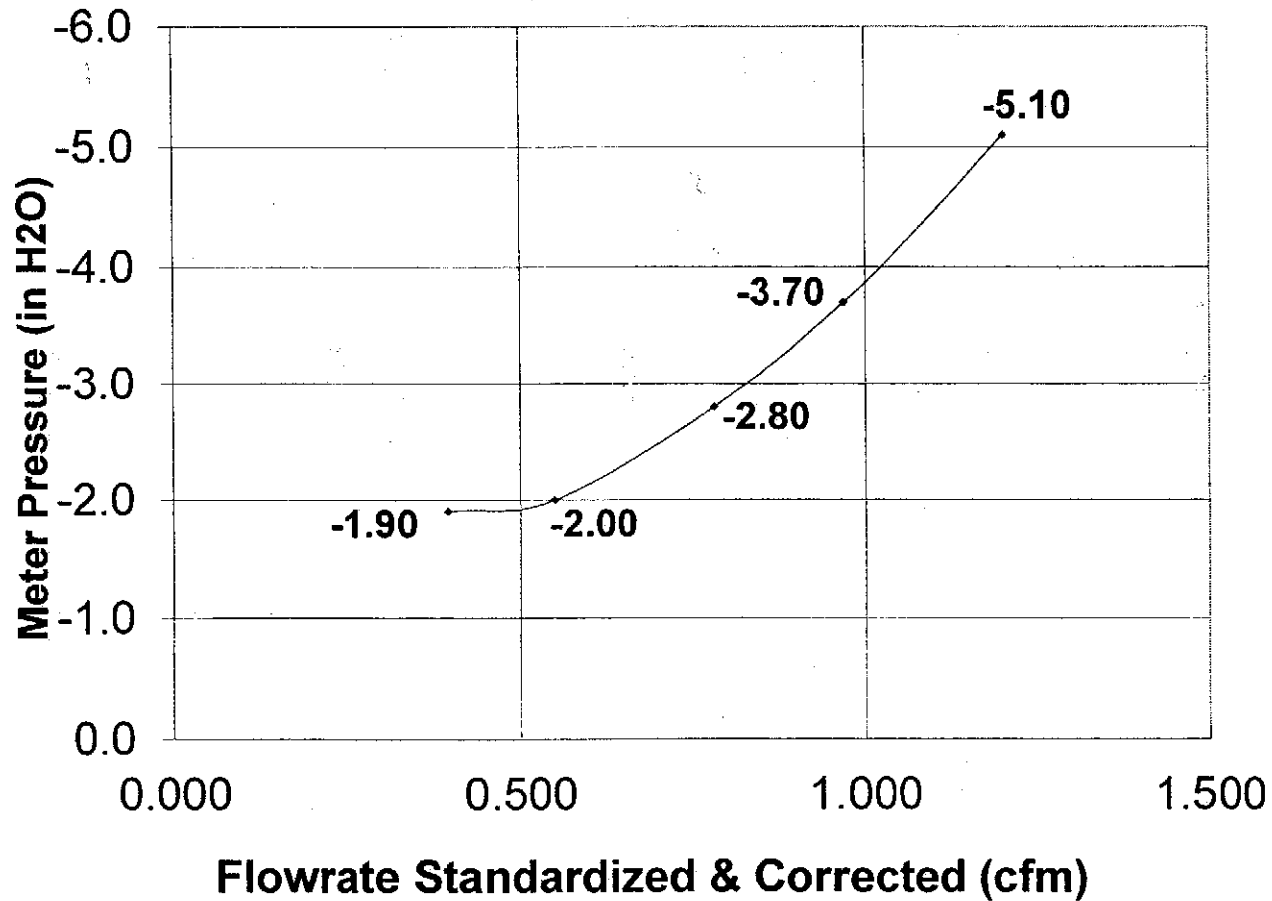
### Meter Gamma vs Flowrate



Calibration Date: 2-18-2014

Calibration Technician:

### Meter Pressure vs Flowrate



Console Serial: 11AE6

Console Model: AL-20



### VANEOMETER CALIBRATION

Myren Consulting used a Dwyer Model 3480 Vaneometer to measure test chamber air velocity. The manufacturer's specifications for accuracy are  $\pm 5.0\%$  from 0 to 100 fpm and  $\pm 10\%$  from 100 to the top of the scale. Myren Consulting insures that the instrument is level and clean prior taking each reading. According to EPA personnel (Westlin, RTP) no further calibration is necessary.

### DRAFT GUAGE CALIBRATION

Myren Consulting used a Dwyer Model 115 AV, a  $-0.05 - 0.0 - 0.25$ " inclined red oil manometer (readability resolution  $\pm 0.001$ " H<sub>2</sub>O) to measure the static pressure in the stack. Once leveled and zeroed as per the manufacturer's written operating instructions, the Dwyer manometer is a primary standard and needs no further calibration.

The manometer is leveled and zeroed at the start of each test, checked as necessary during a run to verify that the settings have not changed and again at the end of each test run. The results of these checks are recorded on Woodstove Data Sheet #16 in each individual test.

### BAROMETER CALIBRATION

Myren Consulting used a Princo Model 453 SN W14275 Mercury barometer and a Weems and Plath aneroid barometer to measure the barometric pressure (BP). The Weems and Plath barometer was calibrated daily by comparing it to the Princo and adjusting it as necessary. The Princo when calibrated following the manufacturer's instructions is a primary standard and needs no further calibration.

### MOISTURE METER CALIBRATION

Myren Consulting uses a Delmhorst J-2000 which was calibrated daily using the "Check" feature. Then the operation of the moisture meter was checked with a Delmhorst Moisture Content Standard Model MCS-1 at 12.6 and 23.8%. The results of these checks are recorded on Data Sheet #10.

The readings obtained with the moisture meter are then corrected as per the manufacturer's written instructions for temperature. If Delmhorst #496 insulated pins are used, the meter is set at 222 using the Set Pin Calibration instructions. The meter is set at 1 for the Species correction. 1 is the setting for D. Fir

WOODSTOVE DATA SHEET #26-A  
 CEM GAS TRAIN RESPONSE TIME  
 PRE CERTIFICATION TEST SERIES CHECK

Date	5/13/15										
Technicians	ATM										
Elapsed Time	CO <sub>2</sub> Conc. (V)	CO <sub>2</sub> Conc. (V)	CO <sub>2</sub> Conc. (V)	CO Conc. (V)	CO Conc. (V)	CO Conc. (V)	O <sub>2</sub> Conc. (V)	O <sub>2</sub> Conc. (V)	O <sub>2</sub> Conc. (V)	Conc. (V)	Conc. (V)
0 Seconds	.486	.484	.480	.156	.158	.159					
15	.486	.485	.480	.155	.158	.159					
30	.291	.290	.288	.149	.150	.151					
45	.106	.102	.101	.060	.061	.061					
60	.046	.048	.047	.043	.043	.044					
75	.008	.009	.008	.032	.031	.031					
90	.004	.006	.004	.005	.005	.006					
105	.003	.004	.002	.002	.002	.003					
120	.001	.001	.001	.001	.001	.001					
135	.001	.001	.001	.001	.001	.001					
150	.000	.001	.000	.000	.001	.001					
165	.000	.000	.000	.000	.000	.001					
180	.000	.000	.000	.000	.000	.000					
Initial Response Time (Seconds)	> 280	N 295	N 295	> 280, < 45	780, < 45	780, < 45					
95% Response Time (Seconds)	> 60	> 60	> 60	> 75, < 90	> 75, < 90	> 75, < 90					
Analyzer Flow Rate	1.50 ft <sup>3</sup> /min										

Comments

95% drop  
 .024    .024    .024    .008    .008    .008

Pne Heat Tech  
HTP 26 STD

CO<sub>2</sub> Analyzer

Multipoint Calibration Report Form

Site: Myren Lab, Colville, WA Date: 7/28/15

Analyzer: Make: Horiba Model: PIR 2000 SN: 607204

Calibration by: A.T. Myren

Cal Gas Flow: 1.5 scfh Measured by: Rotameter: X Mass Flowmeter: \_\_\_\_\_

BP: 28.60 "Hg Instrument ID: Princo

Temp: 66 °F Instrument ID: Omega Digicator

Analyzer Last Calibrated: 7/16/15 By: A.T. Myren

Cylinders:

1. # ITM8803/11 Concentration: 0.00 %CO<sub>2</sub> Cyl. Press.: 230 psi.

Certified By: Oxarc Date: 6/11/12

2. # FB-0019810 Concentration: 12.4 %CO<sub>2</sub> Cyl. Press.: 220 psi.

Certified by: Liquid Technology Corp Date: 4/25/12

3. # 250-1175 Concentration: 21.0 %CO<sub>2</sub> Cyl. Press.: 300 psi.

Certified by: Oxarc Date: 8/22/97

4. # SX-40585 Concentration: 6.04 %CO<sub>2</sub> Cyl. Press.: 1320 psi.

Certified by: Matheson Tri Gas Date: 4/12/10

Analyzer: Calibrated Range: 0-25 % Output: 0-1.0 v.

Flow: 1.5 scfh Measured by: Rotameter: X Mass Flowmeter: \_\_\_\_\_

Calibration Results

Point #	Cyl. #	% CO <sub>2</sub>	Expected		Actual		Adj.		% Dif.	Curve Conc.	Potentiometer	
			Meter	DVM	Meter	DVM	Meter	DVM			Unadj.	Adj.
1	1	0.00	.000	.000	00.0	.000	-	-	+0.17		4.90	-
2	2	12.4	49.6	.496	50.0	.504	48.75	.496	+0.23		7.25	6.82
3	3	21.0	84.0	.840	82.35	.839			+0.02			
4	4	6.04	2.42	.242	23.75	.238			-1.00			
5	1	0.00	00.0	.000	00.0	.001			+0.23			

Comments:

0.000 V = 0.0316170  
 0.496 V = 12.4280009  
 0.839 V = 21.0005002  
 0.238 V = 5.9798819  
 0.001 V = 0.0566097  
 0.500 V = 12.5279717

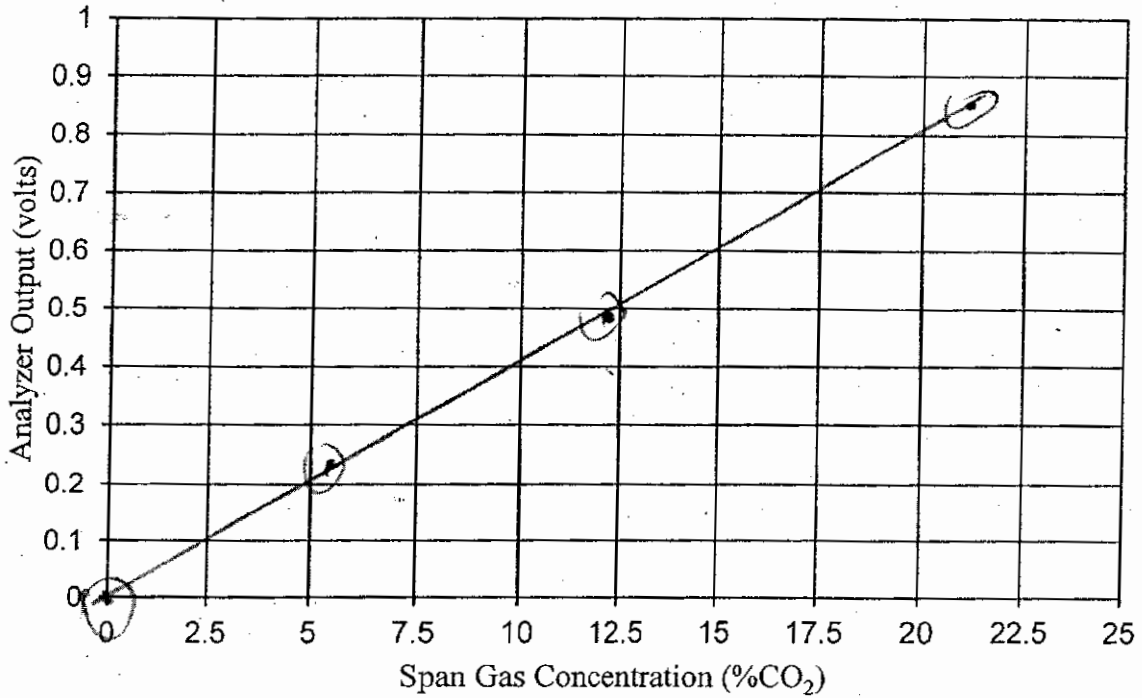
# Linear Regression Results

$Y = MX + B$   
Slope M = 0.0400108  
Y Intercept (B) = -0.0012563  
Correlation Coefficient (r) 0.9999889

Analyzer: Horiba PIR 2000

SN: 607204

Date: 7/28/15



**Comments:**



Pre HMT Tech  
HTP 26 STD

CO Analyzer

Multipoint Calibration Report Form

Site: EPA Lab, Colville, WA

Date: 7/28/15

Analyzer: Make: Horiba

Model: MEXA 311-GE

SN: GE-30075

Calibration by: A.T. Myren

Cal Gas Flow: 1.5scfh Measured by: Rotameter: X Mass Flowmeter: \_\_\_\_\_

BP: 28.60 "Hg Instrument ID: Princo

Temp: 66 °F Instrument ID: Omega Digicator

Analyzer Last Calibrated: 7/16/15

By: A.T. Myren

Cylinders: 17M8803/11

1. # \_\_\_\_\_ Concentration: 0.00 %CO Cyl. Press.: 230 psi.

Certified By: Oxarc Date: 6/11/12

2. # 128-0019810 Concentration: 2.57 %CO Cyl. Press.: 220 psi.

Certified by: Liquid Technology Corp Date: 4/25/12

3. # 250-1175 Concentration: 4.03 %CO Cyl. Press.: 800 psi.

Certified by: Oxarc Date: 8/22/97

4. # SX40585 Concentration: 1.29 %CO Cyl. Press.: 1320 psi.

Certified by: Matheson Tri Gas Date: 4/12/10

Analyzer: Calibrated Range: 0 - 5.0 % Output: 0 - 1.0 v.

Flow: 1.50 CFH Measured by: Rotameter: X Mass Flowmeter: \_\_\_\_\_

Calibration Results

Point #	Cyl. #	% CO	Expected		Actual		Adj.		Curve Conc.	% Dif.	Potentiometer	
			Meter	DVM	Meter	DVM	Meter	DVM			Unadj.	Adj.
1	1	0.00	-	1.000	-	1.002	-	-		+0.25	-	-
2	2	2.57	-	2.57	-	2.65	-	2.57		-0.51	-	-
3	3	4.03	-	4.03	-	4.09	-			+0.50		
4	4	1.29	-	1.29	-	1.27	-			-0.78		
5	1	0.00	-	1.000	-	1.000	-			+0.65		

Comments: The meter on the instrument is broken and unreparable. Horiba no longer makes the part

-0.002 V = .0127264  
 .257 V = 2.5569939  
 .409 V = 4.0501547  
 .127 V = 1.2799484  
 1.000 V = 0.0323732

Pre HERT Tech HTP 26 STD

### Linear Regression Results

$$Y = MX + B$$

Slope M = 0.1017612

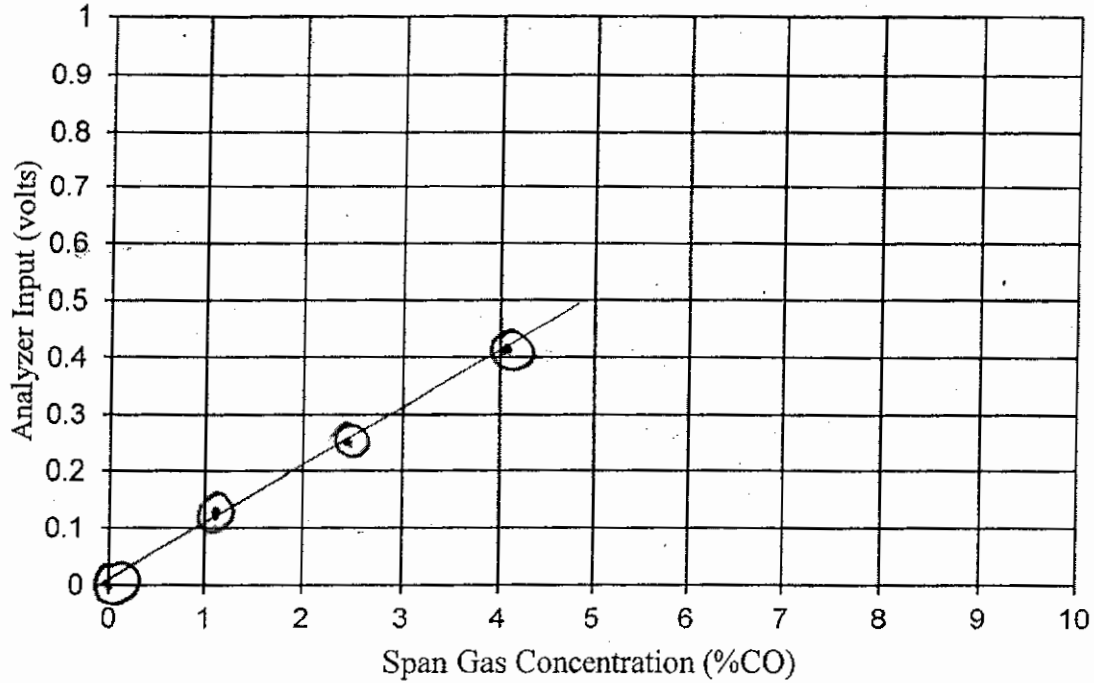
Y Intercept (B) = -0.0032240

Correlation Coefficient (r) 0.9998220

Analyzer: Horiba Mexa 311-GE

SN: GE - 30075

Date: 7/28/15



Comments:



# LIQUID TECHNOLOGY CORPORATION

"INDUSTRY LEADER IN SPECIALTY GASES"

## Certificate of Analysis - EPA PROTOCOL GAS -

Customer OXARC (Colville, WA)  
Date April 25, 2012  
Delivery Receipt DR-42051  
Gas Standard 2.50% CO, 12.5% Carbon Dioxide/Nitrogen - EPA PROTOCOL  
Final Analysis Date April 25, 2012  
Expiration Date April 25, 2015

**DO NOT USE BELOW 150 psig**

Cylinder Data  
Cylinder Serial Number: EB-0019810      Cylinder Outlet: CGA 350  
Cylinder Volume: 133 Cubic Feet      Cylinder Pressure: 1900 psig, 70°F  
Expiration Date: April 25, 2015

Analytical Data  
EPA Protocol, Section No. 2.2, Procedure G-1

Replicate Concentrations  
**Carbon Monoxide: 2.57% +/- 0.02%**  
**Carbon Dioxide: 12.4% +/- 0.12%**  
**Nitrogen: Balance**

Reference Standard(s):

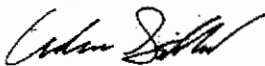
SRM/GMIS:	GMIS	GMIS
Cylinder Number:	CC-166392	CC-125534
Concentration:	2.48% CO/Nitrogen	13.32% CO2/Nitrogen
Expiration Date:	04/18/14	10/14/12

Certification Instrumentation

Component:	Carbon Monoxide	Carbon Dioxide
Make/Model:	Horiba - VIA 510	Horiba - VIA 510
Serial Number:	4344482008	SN075GSF
Principal of Measurement:	NDIR	NDIR
Last Calibration:	April 06, 2012	April 06, 2012

Analytical uncertainty and NIST Traceability are in compliance with EPA-600/R-97/121.

Certified by:

  
Adam Strickland

PGVP Vendor ID: E12012

"UNMATCHED EXCELLENCE"



# MATHESON TRI-GAS

ask...The Gas Professionals™

## Certificate of Analysis - EPA Protocol Mixtures

1650 Enterprise Parkway  
Twinsburg, Ohio 44087  
215-648-4000

Customer: OXARC INC  
Cylinder Number: SX-40586  
Cylinder pressure: 1600 psig  
Last Analysis date: 4/9/2010  
Expiration Date: 3/18/2013

Protocol: Reference # Lot #  
G1 519323 109-96-17643

**DO NOT USE THIS CYLINDER WHEN THE PRESSURE FALLS BELOW 150 PSIG**

### REPLICATE RESPONSES

Component	Certified Conc	Date	Response 1	Response 2	Response 3	Date	Response 4
Oxygen	5.98% ± 1% REL	3/18/2010	5.98%	5.98%	5.99%		
Carbon Dioxide	6.04% ± 1% REL	3/18/2010	6.03%	6.07%	6.01%		
Carbon Monoxide	1.29% ± 1% REL	4/2/2010	1.30%	1.30%	1.30%	4/9/2010	1.29% 1.28% 1.29%

ANCE GAS: Nitrogen

### REFERENCE STANDARDS

Component	SRM #	Sample #	Cylinder #	Concentration
Oxygen	NTRM-82658	01110212	SX-20658	10.09%
Carbon Dioxide	SRM-1674b	7-F-05	CAL-014611	6.876 %
Carbon Monoxide	SRM-2639a	54-D-51	CAL-013889	0.991 %

### CERTIFICATION INSTRUMENTS

Component	Make/Model	Serial Number	Measurement Principle	Last Calibration
Oxygen	Rosemount 755	2002832	Paramagnetic	2/26/2010
Carbon Dioxide	Varian 3800 GC	LR-92489	TC, FID	3/16/2010
Carbon Monoxide	Varian 3800 GC	LR-92489	TC, FID	4/2/2010

Notes: T134744

This certification was performed according to EPA Traceability Protocol for Assay & Certification of Gaseous Calibration Standards September 1997, using procedure G1 and/or G2.

Analyst

*Phil D. Monti*

Date 4/12/2010



WELDING PRODUCTS  
INDUSTRIAL SUPPLIES  
INDUSTRIAL GASES  
MEDICAL GASES



SPECIALTY GASES  
BEVERAGE SYSTEMS  
SAFETY PRODUCTS  
FIRE EQUIPMENT

WWW.OXARC.COM

**MAIN OFFICE**

SPOKANE, WA 99220  
4003 E. BROADWAY  
P.O. BOX 2805  
(509) 535-7794  
FAX (509) 535-0368

BOISE, ID 83709  
7615 W. LEMHI ST.  
(208) 376-0377  
FAX (208) 376-1133

COEUR D'ALENE, ID 83814  
3530 RAMSEY RD.  
(208) 765-3311  
FAX (208) 667-5974

COLVILLE, WA 99114  
328 W. 1ST.  
(509) 684-3776  
FAX (509) 684-6742

ELLENSBURG, WA 98926  
704 N. WENAS  
(509) 925-1518  
FAX (509) 925-1136

HERMISTON, OR 97838  
HERMISTON-  
McNARY HIWAY  
(503) 567-7377  
FAX (503) 567-2265

KENNEWICK, WA 99336  
800 W. COLUMBIA DR.  
(509) 582-4202  
FAX (509) 586-9859

LEWISTON, ID 83501  
2513 3RD. AVE., NORTH  
(208) 743-6571  
FAX (208) 746-8374

MOSES LAKE, WA 98837  
1401 WHEELER ROAD  
(509) 765-9247  
FAX (509) 766-9958

OKANOGAN, WA 98840  
2258 ELMWAY  
(509) 826-3205  
FAX (509) 826-3905

PASCO, WA 99302  
716 SOUTH OREGON  
(509) 547-2494  
FAX (509) 547-3103

TWIN FALLS, ID 83303  
729 COMMERCIAL AVE.  
(208) 734-9711  
FAX (208) 734-7923

HATCHEE, WA 98801  
IME GARDENS RD.  
(509) 662-8417  
FAX (509) 662-1229

YAKIMA, WA 98903  
1004 EAST MEAD  
(509) 248-0827  
FAX (509) 452-8704

**Primary Standard Certificate of Analysis**

Method of Analysis Micro GC / Gravimetric

Customer: Myren Consulting Reference # PM7234-2

P.O.# Cylinder # 250-1175

**Results of Investigation**

<u>Component</u>	<u>Requested</u>	<u>Concentration</u>
Air	N/A	N/A
Argon	N/A	N/A
Carbon Dioxide	21.0%	21.0%
Carbon Monoxide	4.00%	4.03%
Helium	N/A	N/A
Hydrogen	N/A	N/A
Methane	N/A	N/A
Nitrogen	Balance	Balance
Oxygen	21.0%	21.0%

Hazard Class UN 1956  
DOT Shipping Name Compressed Gas NOS  
Shipping Volume (scf approximate) 160 scf @ ntp  
Cylinder Pressure 1500 psig  
CGA Valve Connection 350

Oxarc Primary Standard mixtures are prepared with gravimetric techniques using weights traceable to NIST. Mixture blended to +/- 1% relative to minor component and certified to +/- 1% analytical accuracy.

Authorized Signature Travis Auger Date 8/25/97  
Travis Auger

Comments:

## STOVE DESCRIPTION/ QC

The HEAT TECH HTP 26 STANDARD pellet stove basically looks like a wood stove. It uses a top feed auger system to drop pellets down a chute into the burn pot. The operating controls are located on the side and are easy to use.

## CBI

The information in this Section of this test report is considered Confidential Business Information (CBI) and has been redacted and sent under a separate cover to the following address:

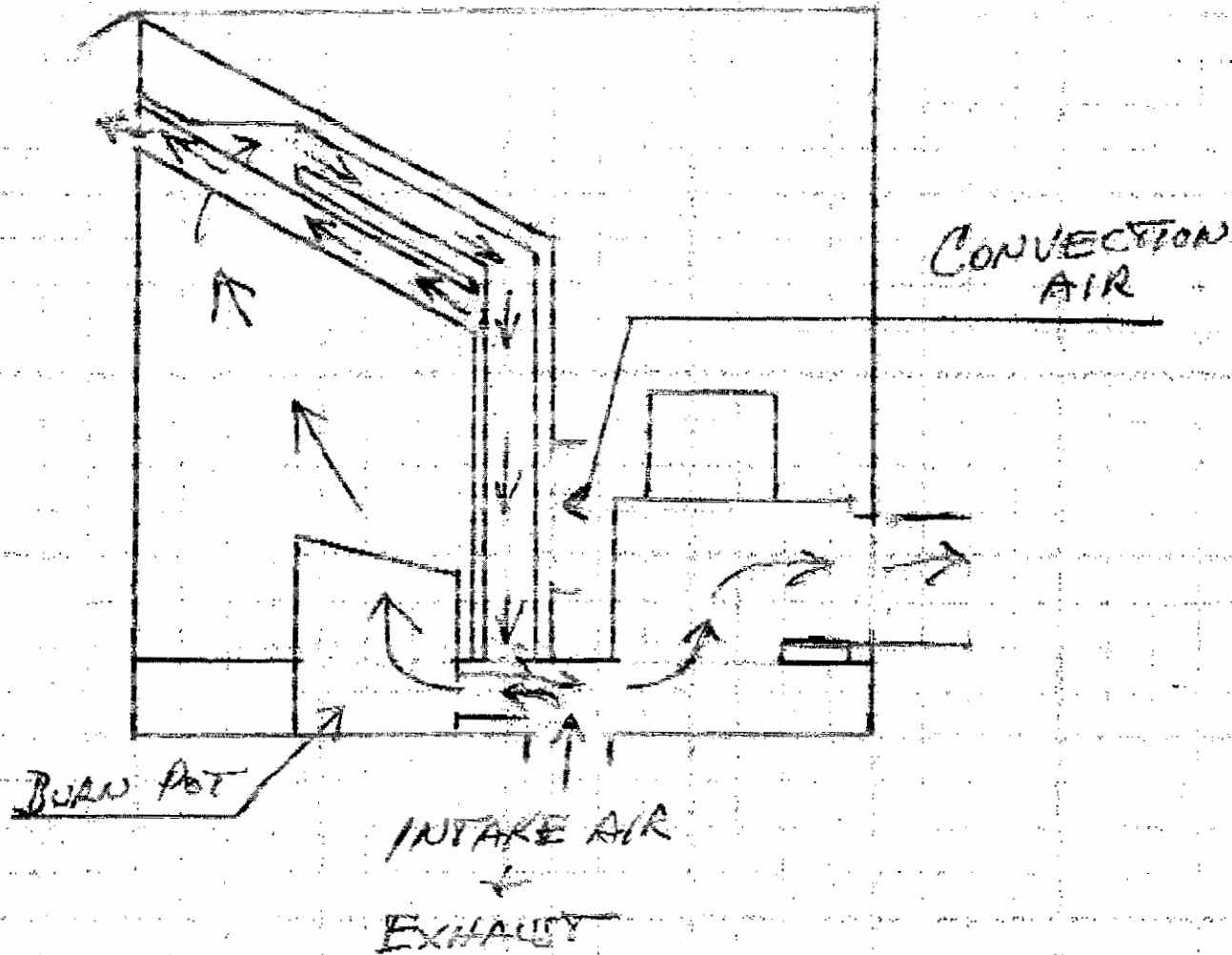
EPA CBI Office

Attn: Residential Wood Heater Compliance Program Lead

1200 Pennsylvania Ave. NW

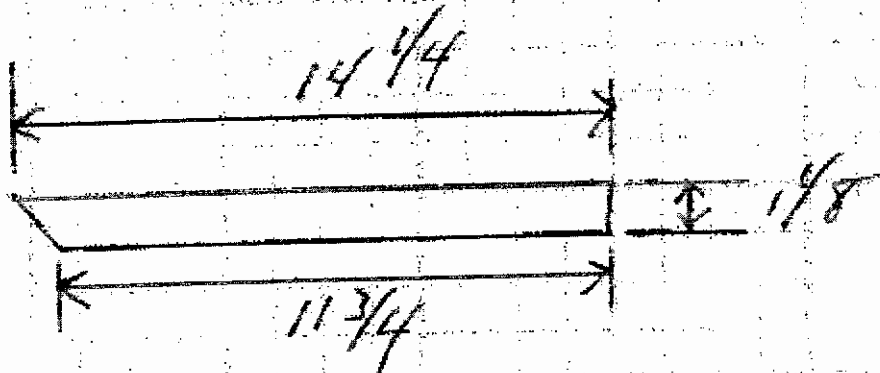
Washington, D.C. 20004

CMP 26 STANDARD ~~PLAN~~



HEAT TEST  
CMP 26 STANDARD  
AIR FLOW (SIDE VIEW)  
10-25-15  
NOT TO SCALE

QMP 26 STANDARD ~~PIPE~~

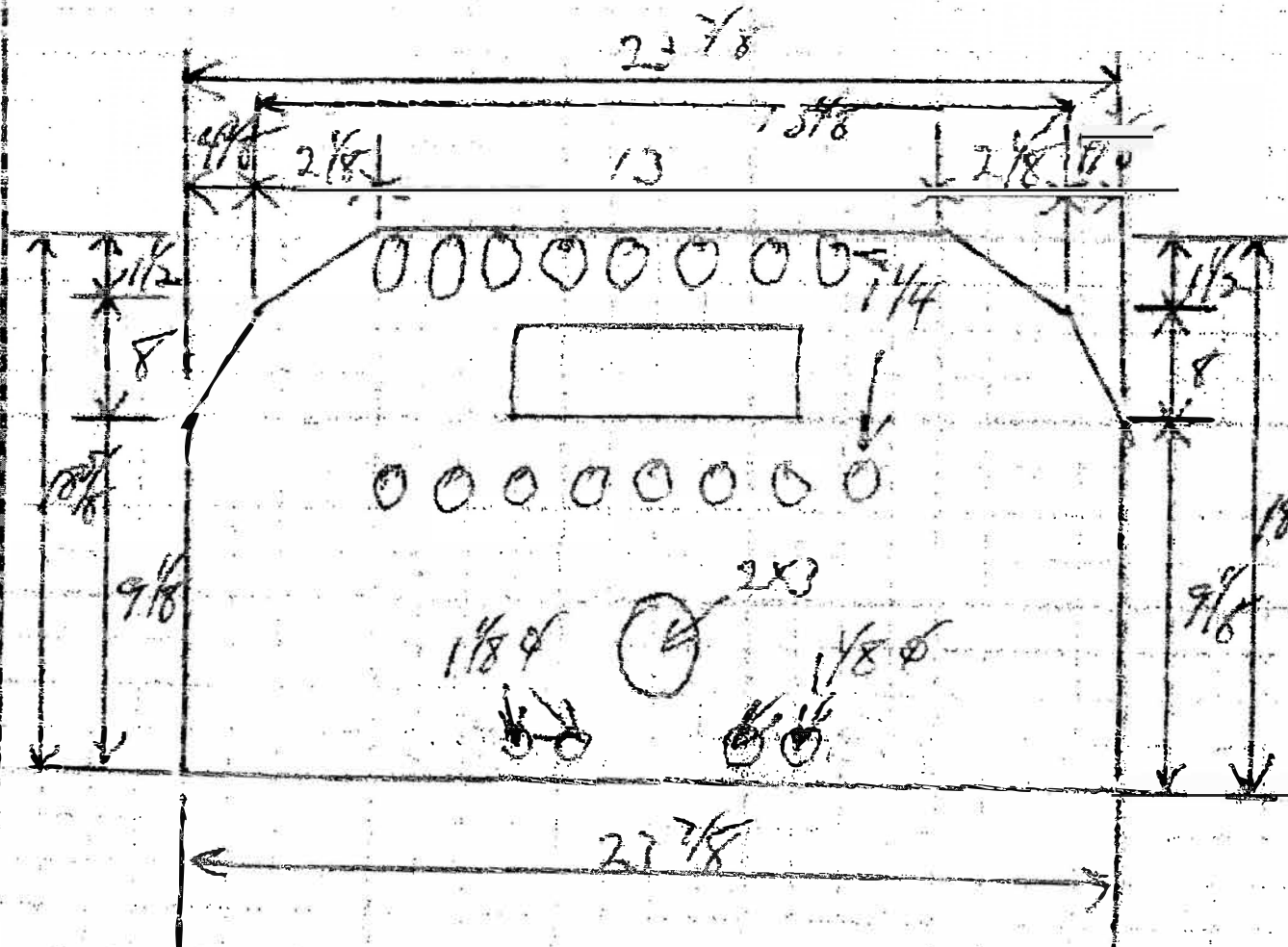


EXHAUST TUBE  
 $1 \frac{1}{8}$   $\phi$  .049 WALL

HEAT TECH  
QMP 26 STANDARD  
EXHAUST TUBE  
10-25-15  
NOT TO SCALE



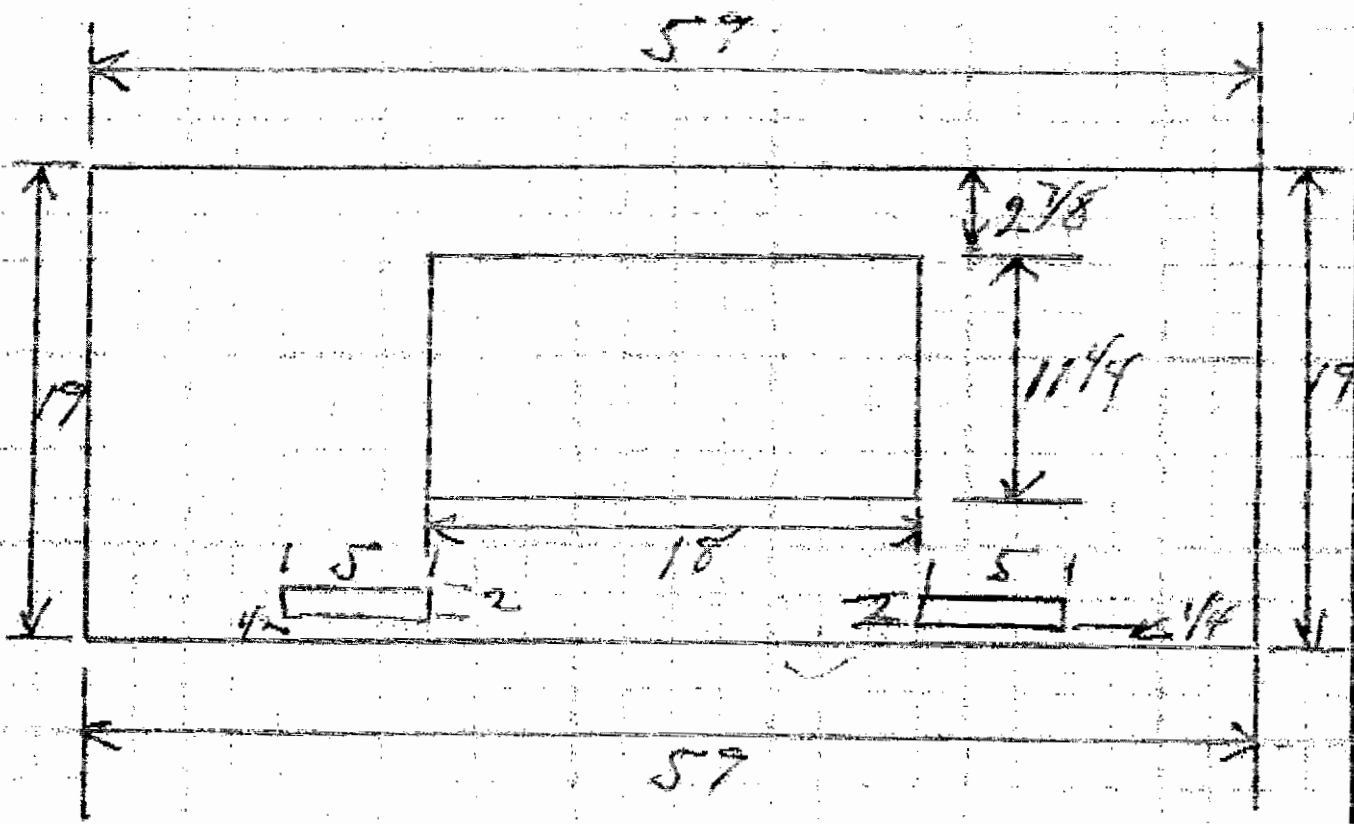
COMP 26 STANDARD PECKER



FIRE BOX  
12 GA STEEL

HEAT TREAT  
COMP 26 STANDARD  
10-25-15  
FIRE BOX  
NOT TO SCALE

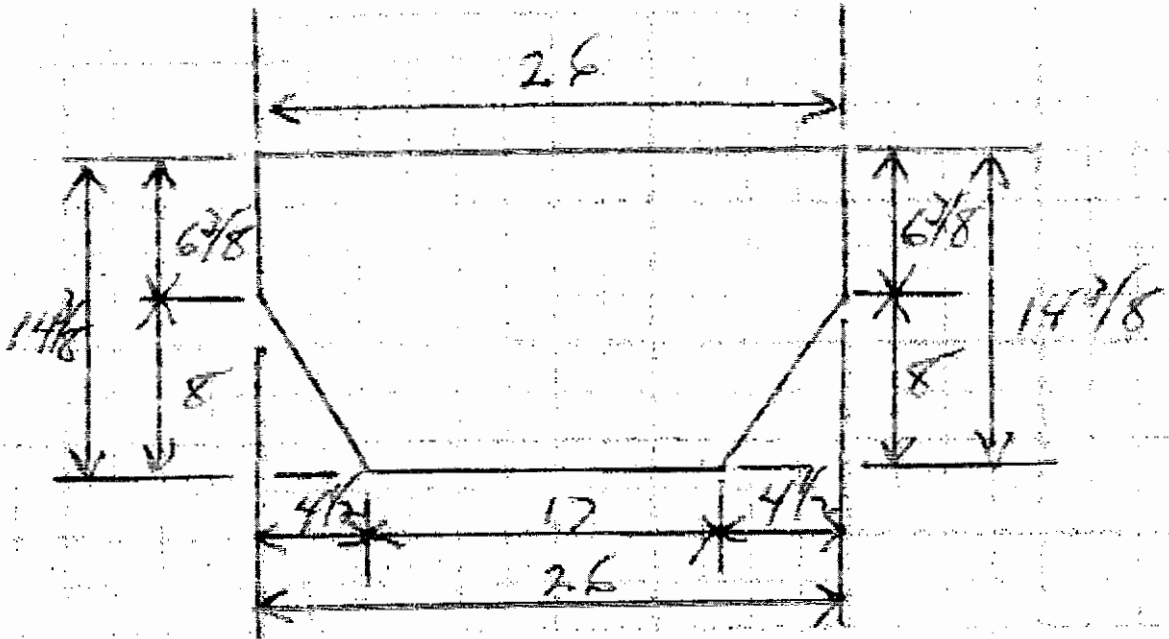
COMP 25 STANDARD PAPER



Body  
1064

NEAT TEST  
COMP 25 STANDARD  
BODY  
10-25-15  
NOT TO SCALE

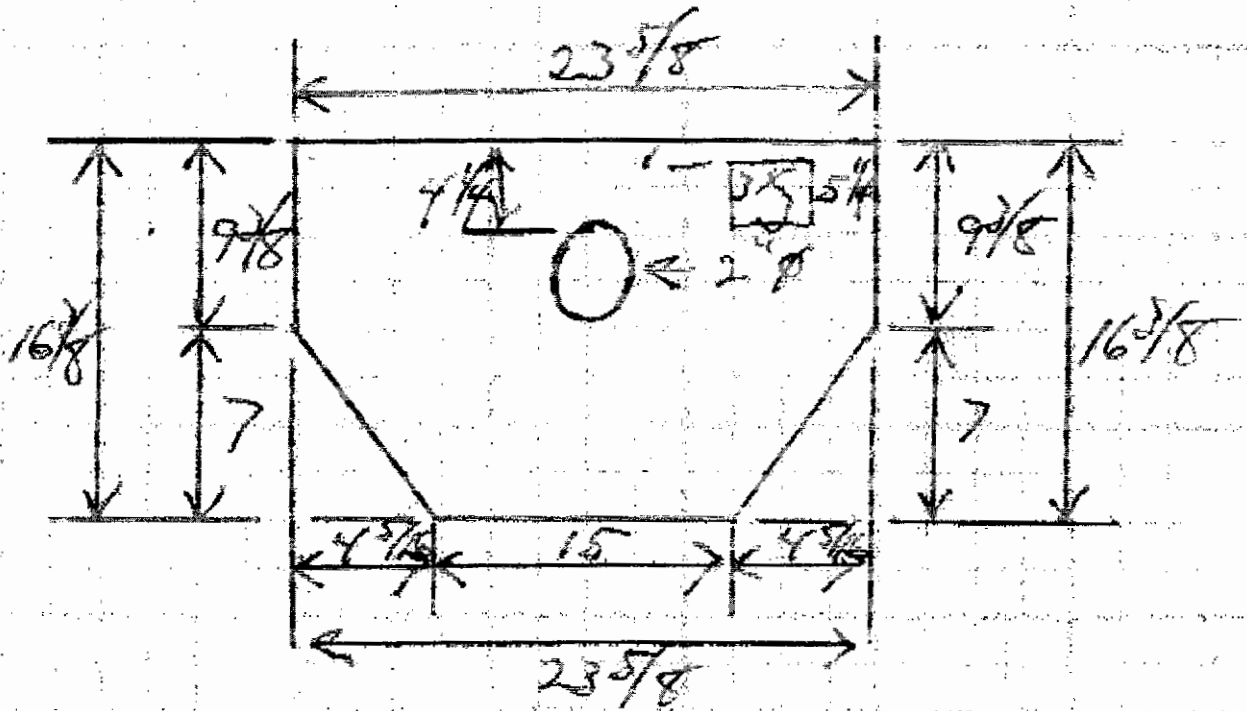
GMP 26 STANDARD PANEL



FALSE TOP  
12 GA.

HEAT TREAT  
GMP 26 STANDARD  
FALSE TOP  
10-25-15  
NOTE: SCALE

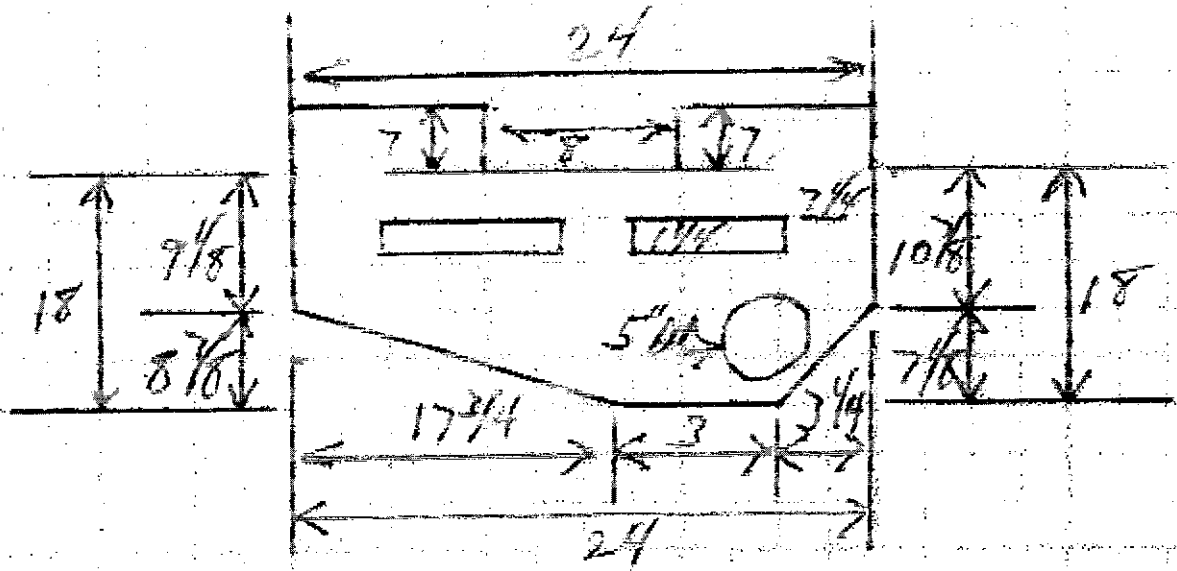
COMP 26 STANDARD SHEET



AIR CHAMBER  
12 GA.

HEAT TECH  
COMP 26 STANDARD  
AIR CHAMBER  
10-25-15  
NOT TO SCALE

COMP 26 STANDARD PLATE

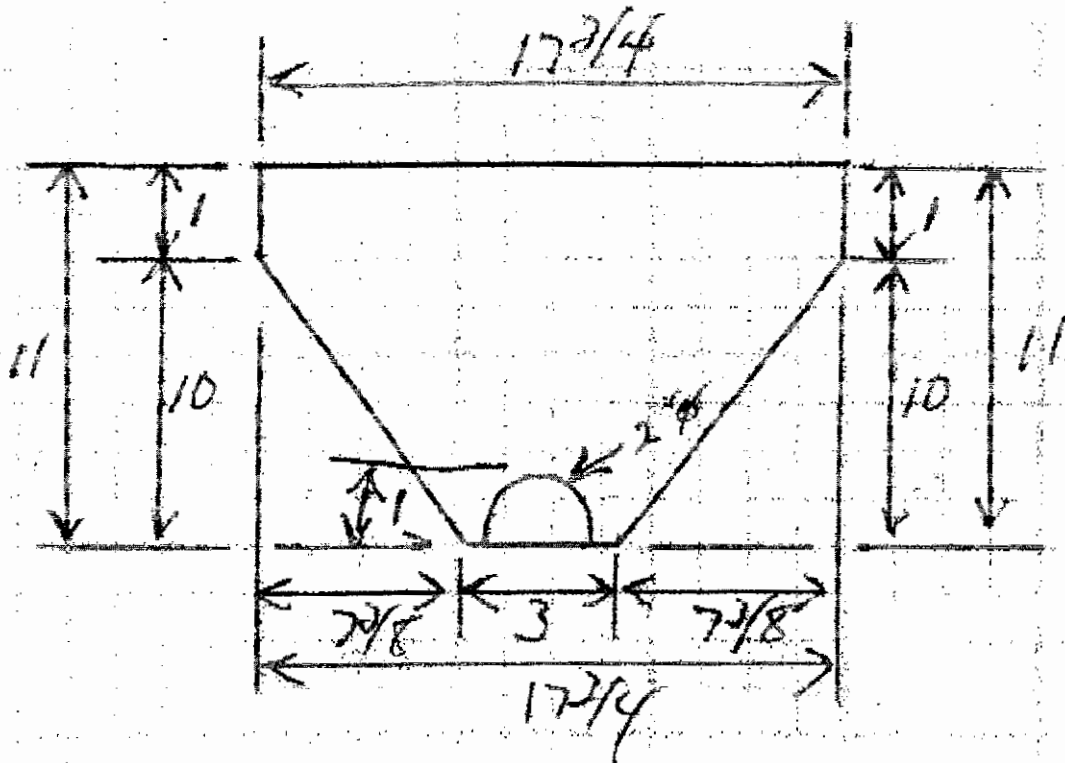


FALSE BOTTOM  
17 GA PLT

HEAT TECH  
COMP 26 STANDARD  
FALSE BOTTOM  
10-25-15  
NOT TO SCALE



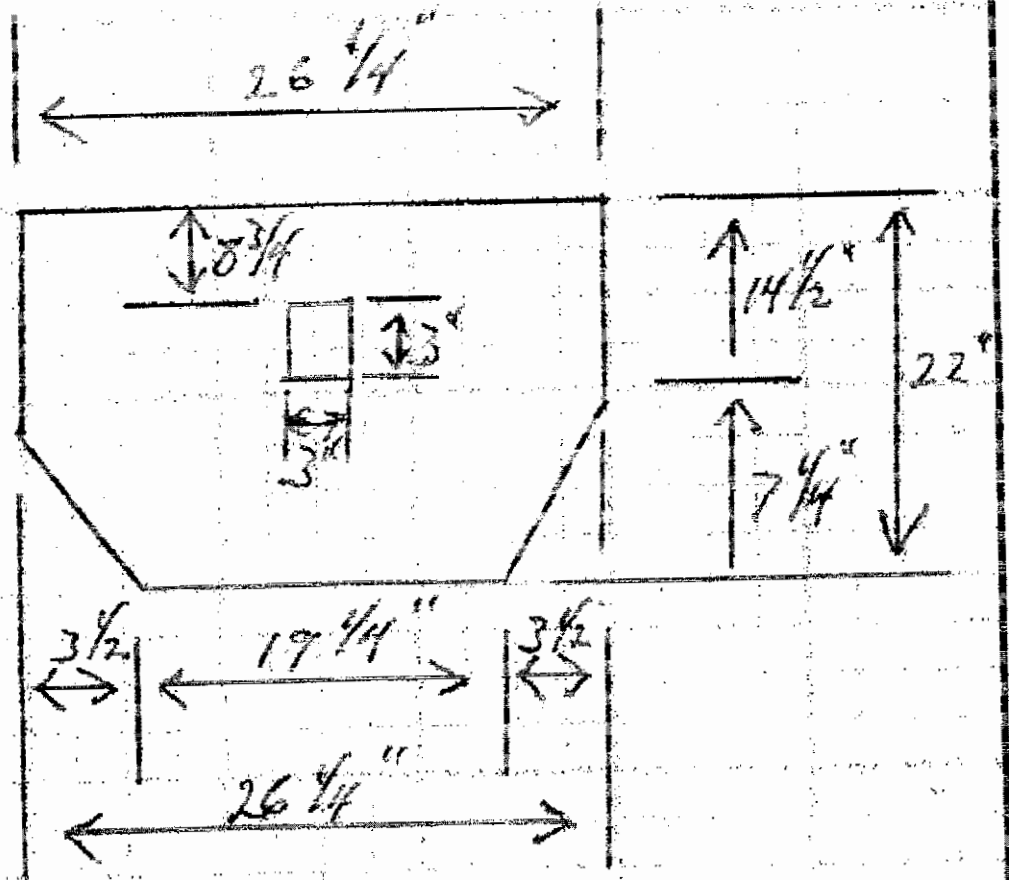
COMP 26 STANDARD PECE



HOPPED BACK  
16 GA.

HEAT TECH  
COMP 26 STANDARD  
HOPPED BACK  
10-25-15  
NO. 80 SCALE

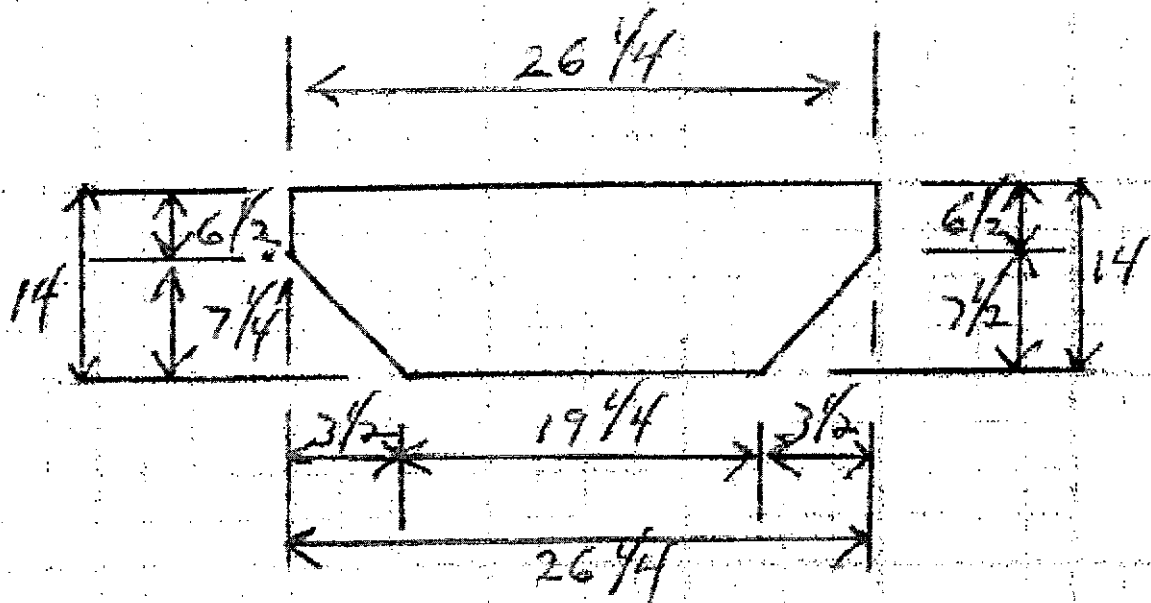
CMP 26 STANDARD DUCT



BOTTOM PLT  
3/16 PLT.

HEAT TECH  
CMP 26 STANDARD  
BOTTOM PLT.  
10-25-15  
NOT TO SCALE

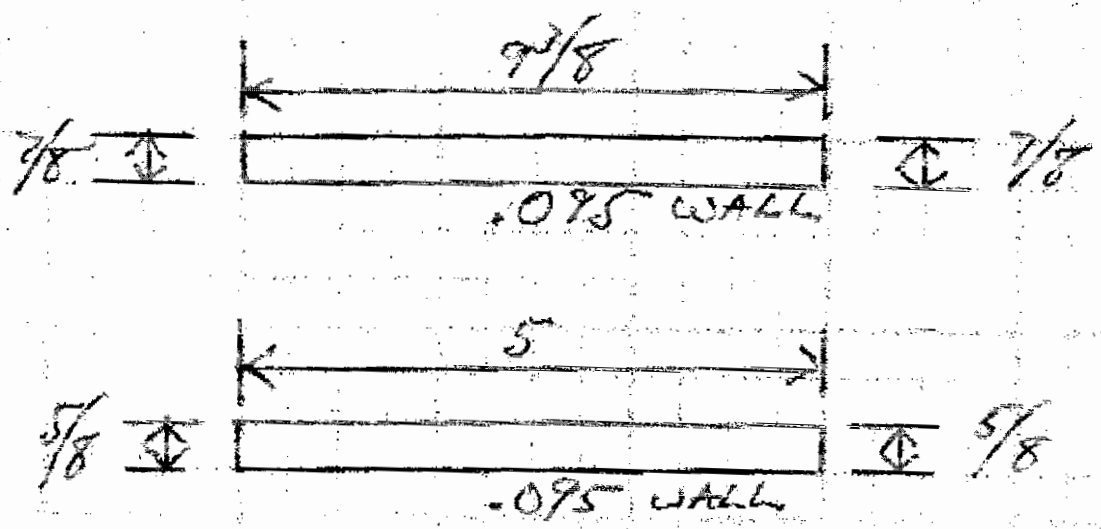
# BMP 26 STANDARD PELLET



REAR TOP  
12 GA.  
ALL DIMENSIONS IN INCH

HEAT TECH  
BMP 26 STANDARD  
REAR TOP  
10-25-15  
NOT TO SCALE

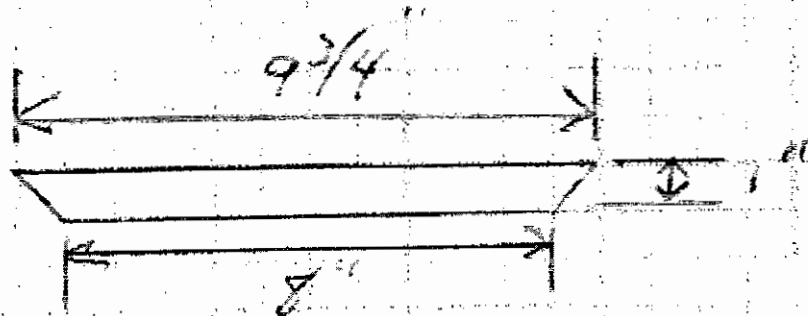
COMP 26 STANDARD PELLET



IGNITOR TUBE (OUTER)  
IGNITOR TUBE (INNER)

HEAT TUBE  
COMP 26 STANDARD  
IGNITOR TUBE  
10-25-15  
NOT TO SCALE

COMP 26 STANDARD ~~HEAT EXCH~~

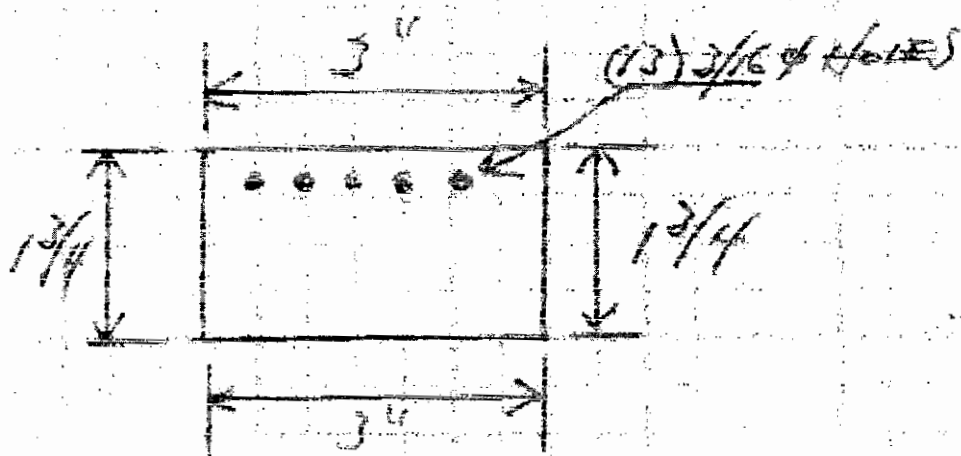
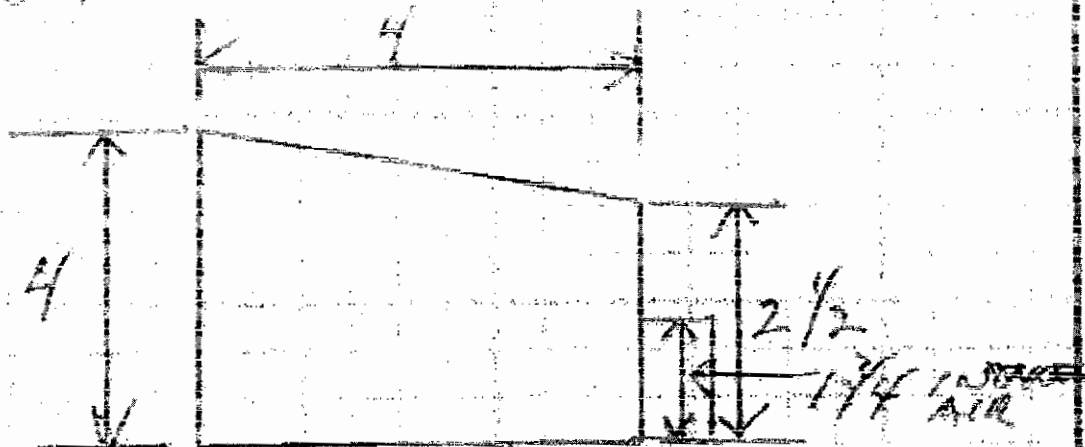


HEAT EXCHANGE TUBE  
1"  $\phi$ . 065 WALL

10-25-15  
HEAT TECH  
COMP 26 STANDARD  
HEAT EXCHANGE  
TUBE  
NOT TO SCALE



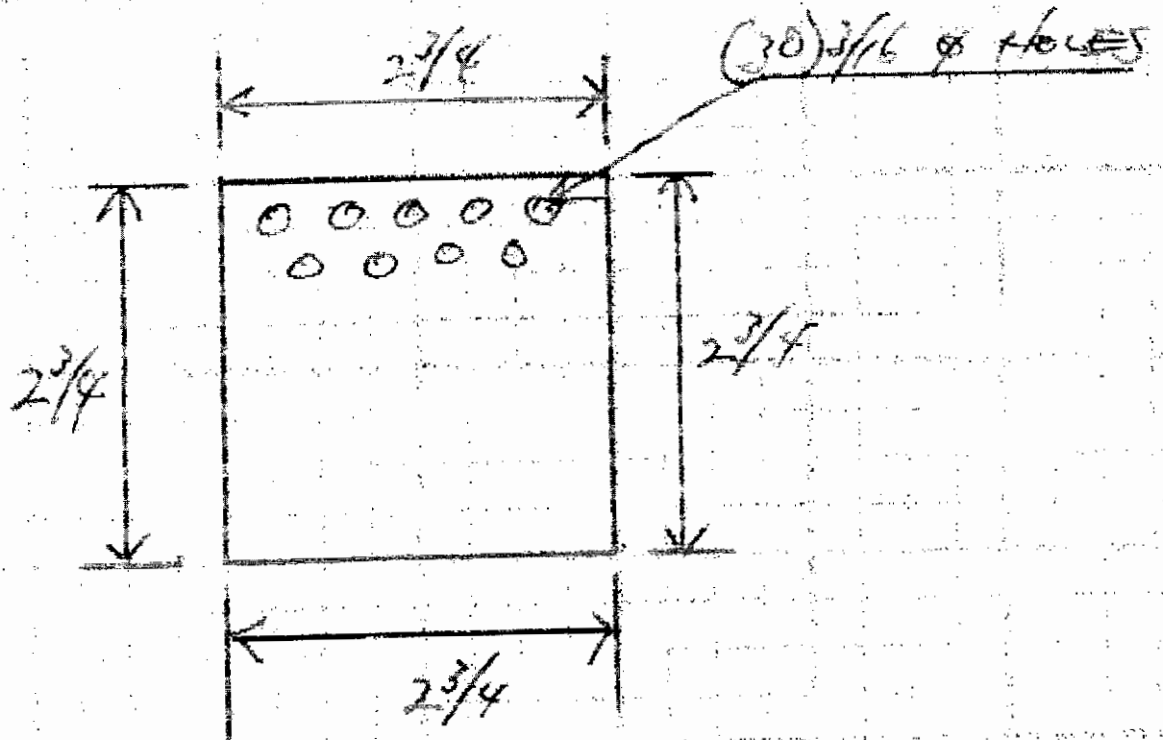
COMP 26 STANDARD PELLET



BURN POT  
 OUTER BOX 4" SS TUBE .065  
 INNER LINER 3" SS TUBE  
 .065

HEAT TECH  
 COMP 5 STANDARD  
 BURN POT  
 10-25-15  
 NOT TO SCALE

COMP 26 STANDARD PLATE



BURN POT BOTTOM PLT.  
 $2\frac{3}{4}$  S.S.  
12 GA.

HEAT TECH  
COMP 26 STANDARD  
BURN POT BOTTOM PLT.  
10-25-15  
NOT TO SCALE

WOODSTOVE DATA SHEET # 30  
STOVE STORAGE

The Heat Tech HTP 26 Standard Pellet stove tested by Myren Consulting, Inc. is being held in custody by:

Heat Tech  
PO Box 727  
Biggs, Ca 95917

Phone 530 846 1985

Contact: Tom Bassett

Heat Tech  
867 Hiway 99  
Gridley, CA 95948

The unit was tested at Myren Consulting's lab in Colville, WA. It was sealed on 7/29/15 after the unit had cooled after testing. The following page contains photos taken after the unit was sealed on 7/29/15.

The unit was sealed with several lengths of metal banding/strapping that were placed around the stove in a manner that prevents the door from being opened. At least two of these straps cross at 90° angles. At one or more of these crossings on the stove a label that clearly identifies the unit as a sealed EPA test stove and/ or a Myren Consulting, Inc. address label is placed over the crossing and taped into place with 2" clear packing tape. The stove was also loaded onto a pallet and strapped to a pallet for transport back to Heat Tech and to its final storage location. A sample stove storage label follows this page.

Once the unit is/ was certified by EPA, the unit will be returned to Heat Tech via common carries;

Carrier: \_\_\_\_\_

Shipped on: \_\_\_\_\_

WST5-Form11

W A R N I N G

SEALED EPA TEST STOVE

DO NOT OPEN OR TAMPER WITH THE SEALS AND PACKAGING ON THIS STOVE.

TO DO SO WILL VOID THE CERTIFICATION ON THIS STOVE.

HEAT TECH HTP 26 Standard

WST5-Form11

W A R N I N G

SEALED EPA TEST STOVE

DO NOT OPEN OR TAMPER WITH THE SEALS AND PACKAGING ON THIS STOVE.

TO DO SO WILL VOID THE CERTIFICATION ON THIS STOVE.

HEAT TECH HTP 26 Standard







**AUTHORIZATION  
TO SEND TEST REPORTS  
TO EPA**

I HEREBY AUTHORIZE MYREN CONSULTING, INC. TO SEND THE APPROPRIATE COPIES OF THE TEST REPORT(S) FOR THE HEAT TECH HTP 26 STANDARD PELLET STOVE TO THE U.S. EPA.

Signature: 

Printed Name: TOM J. J. J. J.

Title: Owner

Date: 1-14-16

PLEASE RETURN TO MYREN CONSULTING VIA EMAIL OR FAX AFTER SIGNING.

FAX: 509 684 3987

EMAIL: <myren.ben@gmail.com>

**HEAT TECH IND. LLC**

867 HWY. 99

Gridley, CA 95948

Office (530) 846-1985 Fax (530) 846-1407

**DATE:** 1-14-15

**TO:** Dean

**FROM:** Tom

**SUBJECT:** BLUEPRINT + <sup>OWNERS</sup> MANUAL

AIR SWITCH SAY TO  
CONNECT WIRES. NEEDS TO  
BE CHANGED TO THE NEW  
PAGE I SENT WITH THE  
SIGNED APPROVAL

