

**AUTHORIZATION  
TO SEND TEST REPORTS  
TO EPA**

I HEREBY AUTHORIZE MYREN CONSULTING, INC. TO SEND THE APPROPRIATE COPIES OF THE TEST REPORT(S) FOR THE HEAT TECH HTP 26 BAY PELLET STOVE TO THE U.S. EPA.

Signature: 

Printed Name: TOM BASSETT

Title: OWNER

Date: 1-15-16

PLEASE RETURN TO MYREN CONSULTING VIA EMAIL OR FAX AFTER SIGNING.

FAX: 509 684 3987

EMAIL: <myren.ben@gmail.com>

# Myren Consulting, Inc.

512 Williams Lake Road

Colville, WA 99114

Office: (509) 684-1154

Lab: (509) 685-9458

Fax: (509) 684-3987

email: <myren.ben@gmail.com>

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Date: 10 January 2016

To: Tom Bassett, Heat Tech

From: Ben Myren *Ben*

RE: Heat Tech HTP 26 Bay Pellet Stove Test Report

Please find enclosed your copy of the EPA test report for the HEAT TECH HTP 26 BAY pellet stove. Look over the info that is pertinent to your end, i.e., addresses, phone numbers, blueprints (especially), etc., to make certain that they are correct. If there are any corrections, call me and I will take care of them immediately. As soon as I receive the signed Authorization form, I will send the reports to EPA.

Remember to send in your EPA Wood Heater Certification Application to EPA ASAP. Here I am assuming the old Application still works.

If you have any questions or comments, call.

Regards, Ben

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PE 1.2 Sanchez Letter

10 December 2016

Dr. Rafael Sanchez, PhD.

U.S.EPA

Office of Enforcement and Compliance Assurance

Office of Compliance

William Jefferson Clinton Building, South

Room 7419D

1200 Pennsylvania Ave., N.W.

Washington, DC 20003

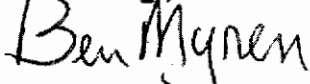
Dear Dr. Sanchez:

Please find enclosed the required two (2) copies of the certification test report for HEAT TECH HTP 26 BAY pellet stove. As the test results indicate, the unit's emissions are well below the EPA standard of 4.5 g/hr.

Report is organized in the same way as the previous pellet stove test reports submitted to EPA. While the report is basically organized like the reports submitted under the old NSPS, some parts of the report have been reorganized/ revised to insure compliance with the rules in the new NSPS. Thus look at the relevant pages, e.g., Individual Test Run Page Index, in the Introduction Section to find the required information.

If you or anyone else has any questions about the information or data in this test report, please contact me immediately.

Sincerely,



Alben T. Myren Jr.

President

ATM/im

# Myren Consulting, Inc.

512 Williams Lake Road

Colville, WA 99114

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---

12 January 2010

EPA CBI Office

Attn: Residential Wood Heater Compliance Program Lead

1200 Pennsylvania Ave. NW

Washington, D.C. 20004

Dear Dr. Sanchez:

RE: CBI INFORMATION FOR THE HEAT TECH HTP 26 BAY PELLETT STOVE

Please find enclosed the required two (2) copies of the CBI for the test report for the HEAT TECH HTP 26 BAY pellet stove. The main test report has been sent under a separate cover to the following address:

Dr. Rafael Sanchez, PhD.

U.S.EPA

Office of Enforcement and Compliance Assurance

Office of Compliance

William Jefferson Clinton Building, South

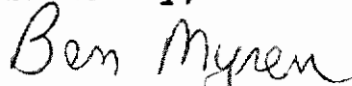
Room 7419D

1200 Pennsylvania Ave., N.W.

Washington, DC 20003

If you or anyone else has any questions about the CBI information in this test report, please contact me or Tom Bassett at HEAT TECH at 530 846 1985 immediately.

Sincerely,



Alben T. Myren Jr.

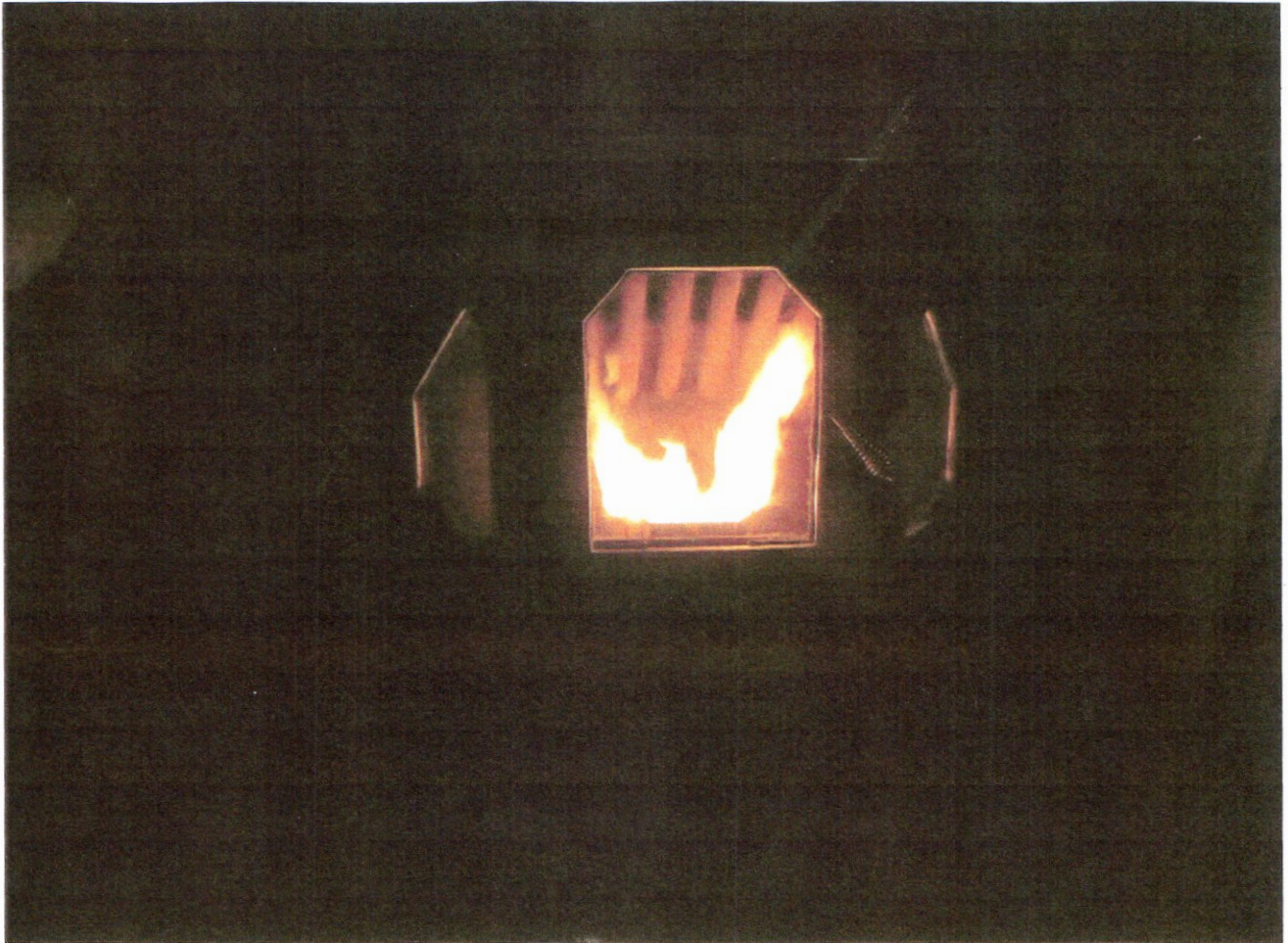
President

ATM/im

**US EPA WOOD HEATER  
CERTIFICATION TEST REPORT**

**HEAT TECH 26 BAY PELLETT STOVE**

**JANUARY 12, 2016**



**MYREN CONSULTING, INC.**

**OFFICE**

512 WILLIAMS LAKE ROAD  
COLVILLE, WA 99114  
PHONE 509-684-1154  
FAX 509-684-3987

**LABORATORY**

501 C WILLIAMS LAKE ROAD  
COLVILLE, WA 99114  
PHONE 509-685-9458  
EMAIL [myren.ben@gmail.com](mailto:myren.ben@gmail.com)

\*\*\*\*\*

**Confidential**

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**The data and information in this test report is confidential, proprietary information and is not to be released to and/or discussed with any party who is not authorized by the manufacturer or the testing laboratory to receive such data.**

\*\*\*\*\*

**Confidential**

\*\*\*\*\*

### Report Certification

The sampling and analysis for the appliance described in this report was carried out under my direction and supervision.

Date: 1/13/2016

Signature: Albert V. Myren Jr  
Title: President

I have reviewed all of the test data and test results found in this report and hereby certify that the test report is authentic and accurate.

Date: 1/13/2016

Signature: Albert V. Myren Jr.  
Title: President

**PELLET STOVE  
TABLE OF CONTENTS**

p 1 of 1  
Rev 0 12.15

<b>Introduction</b>	<b>Section(s)</b>	<b>Page(s)</b>
Title Page	Introduction	i
Confidentiality Statement		ii
Report Certification		iii
Table of Contents		iv
Testing Location and Personnel Information		v
Test Report (Data) Page Number Index		vi-vii
Individual Test Run Page Number Index		viii
Test Series Information and Discussion		ix
 <b>Summary and Discussion of Results</b>		
Integrated Test Results	Data Summary	1
Particulate Sampling Train Performance		1
Test Data Summary		2-4
 <b>Pellet Stove Aging Data</b>		
	Aging	2
 <b>Individual Test Run (Raw Data)</b>		
See Pellet Stove Test Run Page Index in the Introduction Section for a complete, sequential list of the data pages in the integrated test run.	Test Run	vari
 <b>Calibration Data</b>		
See Test Report (Data) Page Number Index, Item 14, for a complete, sequential listing of the data in this section.	Cal Data	vari
 <b>Stove QC</b>		
Pellet Stove Description	Stove QC	1
 <b>Blueprints</b>		
Promotional (Sales) Brochure	Blueprints	vari
Laboratory verified blueprints		vari
 <b>Manual</b>		
Manufacturer's Written Test Instructions	Manual	vari
Manufacturer's Owner's Manual		vari
 <b>Storage</b>		
Storage Location/ Sealing Information	Storage	1
Photo of Sealed Stove		1



**TESTING LOCATION AND PERSONNEL INFORMATION**

**Unit Name: HEAT TECH HTP 26 BAY PELLET STOVE**

**Manufacturer Name: HEAT TECH**

**Manufacturer Address: PO BOX 727  
Biggs, CA 95917**

**Manufacturer Phone: 530 846 1985  
Fax:**

**Observers & Affiliation: None**

**SUPERVISOR: Ben Myren**

**MYREN CONSULTING'S LAB TEAM: Ilse Myren, Ben Myren, Eric Schaefer**

**LAB LOCATION: Myren Consulting's lab in Colville, WA**

**ELEVATION: ~ 1650 FEET**

**MYREN CONSULTING, INC.**

**LABORATORY  
501-C WILLIAMS LAKE ROAD  
COLVILLE, WA 99114  
509 685 9458  
509 684 3987 (Fax)**

**OFFICE  
512 WILLIAMS LAKE ROAD  
COLVILLE, WA 99114  
509 684 1154  
email: <myren.ben@gmail.com>**

**Pellet Stove Page Number Index**

	<u>Section</u>	<u>Location</u>	
1. Integrated Test Results	Data Summary	Integrated Test Results	p. 1
2. Summary Table of Other Data	Data Summary	Data Summary Sheets	p. 2-4
3. Wood Heater Description	Stove QC	Wood Heater Description	p.1 (vari)
4. Manufacturer's Testing Instructions	Operators Manual	P. 1 of Section	vari
5. Test Camber Installation Description	Installation Description	Introduction	p. x
6. Pellet Stove Aging Documentation	Aging		p. 1-2
7. Pretest Burn Procedures	Individual Test Runs	Data Sheets	#9,13
8. Pretest Facility Measurements	Individual Test Runs	Data Sheets	#8, 16
9. Test Fuel Measurements			
A. Fuel Moisture	Individual Test Runs	Data Sheets	#11
10. Heater Operation and Air Supply Settings	Individual Test Run	Data Sheets	#9, 13
11. Calibrations			
A Platform Scale			
1. Semi Annual	Cal Data	P. 1	
2. Pre and Post Test	Individual Test Run	Data Sheet	#16
B. Analytical Balance			
3. Semi Annual	Cal Data	P. 3 (Variable)	
4. Pre Weighing Check	Individual Test Run	Data Sheet	#4-4
C. Temperature			
5. Thermometers	Cal Data	P. 5	
6. Thermocouple Readout(s)			
a. Semi Annual	Cal Data	P. 6	
b. Daily Check	Individual Test Run	Data Sheet	#16
D. Dry Gas Meters			
a. Semi Annual Calibration	Cal Data	P. 7 (Variable # of pp.)	
b. Post Test Audits	Cal Data	(Variable # of pp.)	
c. Transfer Meter Calibration	Cal Data	(Variable # of pp.)	
E. Miscellaneous Test Equipment			
a. Anemometer	Cal Data	P. 11	
b. Barometer	Cal Data	P. 11	
c. Draft/ Static Pressure Gauge	Cal Data	P. 11	

d. Humidity Gauge Calibration ( Sling Psychrometer)	Cal Data	P. 13
F. Combustion Gas (CO <sub>2</sub> , O <sub>2</sub> , CO) Train Response Check	Cal Data	P. 20
G. CO <sub>2</sub> Analyzer		
1. Calibration	Cal Data	P. 22
2. Pre and Post Test Zero/Span	Individual Test Run	Data Sheet #15-3
B. CO Analyzer		
1. Calibration	Cal Data	P. 24
2. Pre and Post Test Zero/Span	Individual Test Run	Data Sheet #15-1
C. Calibration Gas Certificates of Analysis		
15. Quality Checks		
A. Leak Checks		
1. Particulate Sampling Train	Individual Test Runs	P.1 of Data Sheet #2
2. Combustion Gas (CO <sub>2</sub> , O <sub>2</sub> , CO) (CEM) Train	Individual Test Runs	Data Sheet #16
B. Proportional Checks	Individual Test Runs	Table 1
16. Sample Calculations		
A. Dry Burn Rate	Individual Test Runs	Data Sheet # 8; Computer Printout
17. Raw Test Data	Individual Test Runs	Data Sheets #1-16
18. Analytical Data		
A. Filter and Beaker Tares	Individual Test Runs	Data Sheets #4-1, 4-2
B. Solvent Blanks	Individual Test Runs	Data Sheets #4-3, 5
C. Particulate Catches		
1. Gross	Individual Test Runs	Data Sheet #5
2. Blanks	Individual Test Runs	Data Sheet #5
3. Net	Individual Test Runs	Data Sheet #5
D. Constant Weight Weighings		
1. Tares	Individual Test Runs	Data Sheets # 4-1, 4-2
2. Finals	Individual Test Runs	Data Sheet #4-3
3. Analytical Balance QC Checks	Individual Test Runs	Data Sheet #4-4 (Variable pp.)

d. Humidity Gauge Calibration ( Sling Psychrometer)	Cal Data	P. 13	
F. Combustion Gas (CO <sub>2</sub> , O <sub>2</sub> , CO) Train Response Check	Cal Data	P. 20	
G. CO <sub>2</sub> Analyzer			
1. Calibration	Cal Data	P. 22	
2. Pre and Post Test Zero/Span	Individual Test Run	Data Sheet	#15-3
B. CO Analyzer			
1. Calibration	Cal Data	P. 24	
2. Pre and Post Test Zero/Span	Individual Test Run	Data Sheet	#15-1
C. Calibration Gas Certificates of Analysis			
15. Quality Checks			
A. Leak Checks			
1. Particulate Sampling Train	Individual Test Runs	P.1 of Data Sheet #2	
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B. Solvent Blanks	Individual Test Runs	Data Sheets	#4-3, 5
C. Particulate Catches			
1. Gross	Individual Test Runs	Data Sheet	#5
2. Blanks	Individual Test Runs	Data Sheet	#5
3. Net	Individual Test Runs	Data Sheet	#5
D. Constant Weight Weighings			
1. Tares	Individual Test Runs	Data Sheets	# 4-1, 4-2
2. Finals	Individual Test Runs	Data Sheet	#4-3
3. Analytical Balance QC Checks	Individual Test Runs	Data Sheet	#4-4 (Variable pp.)

ASTM E2515/ EPA M5G-1 Individual Test Run Page Index (Pellet Stove)

The data sheets in the individual test runs are organized in the following sequence.

<u>Page Description</u>	<u># of Pages</u>
Filters photo	1
CSA B415.1-10 "Report" computer spreadsheet printout	Variable
CSA B415.1-10 "Data Input" computer spreadsheet printout	Variable
Dilution Tunnel Traverse data	1
Dilution Tunnel Gas Velocity and Volumetric Flow Rate Calculations	1
Train 1 Emission Rate/ Dilution Tunnel Calculations computer spreadsheet printout	Variable
Train 1 0-60 Minute Emission Rate/ Dilution Tunnel Calculations computer spreadsheet printout	Variable
Train 1 0-60 Minute Particulate Sampling data (Meter Box data)	Variable
Train 1 60 Minute Plus Particulate Sampling data (Meter Box data)	Variable
Filter Constant Tare Weight data	Variable
Beaker Constant Tare Weight data	Variable
Acetone Blank Beaker Constant Final Weight data	1
Train 1 0-60 Minute PM Sample Constant Final Weight data	1
Train 1 60 Minute Plus Constant Final Weight data	1
Train 1 Particulate Matter Catch Calculations	Variable
Train 2 Emission Rate/ Dilution Tunnel Calculations computer spreadsheet printout	Variable
Train 2 Particulate Sampling data (Meter Box data)	Variable
Train 2 PM Sample Constant Final Weight data	1
Train 2 Particulate Matter Catch Calculations	1
Train 3 Room Blank Sampling Rate and PM Concentration Calculations computer spreadsheet printout	Variable
Train 3 Particulate Sampling data (Meter Box data)	Variable
Train 3 PM Sample Constant Final Weight data	1
Train 3 Particulate Matter Catch Calculations	1
Analytical Balance QA/ QC data	Variable
Woodstove Data Sheet #8 Miscellaneous data	1
Woodstove Data Sheet #9 Pellet Stove Operating data	1
Woodstove Data Sheet #10 Preburn and Fuel Load Moisture Determination data	1
Woodstove Data Sheet #11 ASTM E2780 Fuel Load Calculations	1
Woodstove Data Sheet #13 Pre Burn Data	Variable
Woodstove Data Sheet #14 Burn Rate, Flue Gas and Temperature Data	Variable
Woodstove Data Sheet #15-1 CO <sub>2</sub> Pre and Post Test Zero/Span Audits	1
Woodstove Data Sheet #15-3 CO Pre and Post Test Zero/Span Audits	1
Woodstove Data Sheet #16 Quality Checks	1

## TEST SERIES INFORMATION AND DISCUSSION

MODEL LINE: HEAT TECH HTP 26 BAY PELLETT STOVE

TEST UNIT: HEAT TECH HTP 26 BAY PELLETT STOVE

Manufacturer: HEAT TECH

Date Received: 6/20/2015

Date(s) Aged: 6/24, 25, 26, 29, 30, 2015. See AGING Section

Test Date(s): 7/30/2015

PM Sampling Method(s): ASTM E2515 using 4" filters (EPA M5G-1)

Operating and Fueling Protocol: EPA M28R, ASTM E2779

Number of Test Runs: 1

The Heat Tech HTP 26 Bay Pellet stove manufactured by Heat Tech located in Biggs, CA was tested by Myren Consulting, Inc. using the Environmental Protection Agency's (EPA) Test Method 28R, "Certification and Auditing of Wood Heaters", ASTM E2515-11, "Standard Test Method for Determination of Particulate Emissions Collected in a Dilution Tunnel" and ASTM E2779-10, "Standard Test Method for Determining Particulate Matter Emissions from Pellet Heaters". (See the Federal Register/ Vol.80, No.50/ Monday, March 16, 2015. [pp.13672-13753]). On March 28, 2015 Myren Consulting, Inc. requested approval from EPA to use four-inch filters when conducting all PM emission certification tests and received the approval to do so on April 7, 2015. Thus the PM sampling and PM sample processing procedures used during the certification tests found in this test report are what are found in EPA M5G-1 in the old NSPS. (See the Federal Register/ Vol.53, No.38/ Friday, February 26, 1988/ pp.5860-54926, especially in Method 5G in Appendix A on pp. 5884-5892.) The particulate matter (PM) emission data was calculated as specified in the Wood Heater New Source Performance Standard (NSPS) dated March 16, 2015. The percent overall efficiency (%OE) for the test run was calculated using the %OE algorithm found in CSA's B415.1-10.

All events and information pertinent to the test data are recorded on the data sheets for the test run, particularly on pp. 9, 13 and 14.

Any deviations made or noted from the promulgated methods other than those that were accepted and certified by EPA during the laboratory accreditation process are listed and discussed below. The Heat Tech HTP 26 Bay pellet stove was tested at Myren Consulting's lab in Colville, WA using Myren Consulting laboratory's lab accreditation. A copy of both Myren Consulting's old Lab Accreditation Certificate (#6) and new Lab Accreditation Certificate (#2) are included in the following pages because at the time the Heat Tech HTP 26 was tested, EPA had not yet been issued the new Lab Accreditation Certificate. (Myren Consulting, Inc. had formally notified EPA on February 15, 2015 that Myren Consulting, Inc. wished to continue as an accredited laboratory after the new NSPS went into effect.)

A brief note about how the four-inch (EPA M5G-1) particulate samples were processed is necessary to help the reviewer understand the net catch values. Experience has shown that the small portions of the filters that are left on the frits in the M5G-1 filter housing apparatus after the filters are removed are full of static electricity. When these small portions are removed to a plastic petri dish, they quickly adhere to the petri dish. Because trying to recapture these small pieces of filter material during weighing causes them to disintegrate into smaller and smaller pieces, which makes obtaining accurate catch weights difficult, it was decided to place this filter material in with the particulate captured with the acetone wash, where it shows up as catch. Some of the filter material was already following this pathway. Thus, there may be negative filter catch weights, particularly for the back half filters, that are used during the particulate emission rate calculation process. However, the filter material lost off the filters is accounted for in the acetone catch. The first page in the TEST RUN Section is a photo of the filters from the test run for this unit and shows this problem.

ASTM E2778-10 Equation 1 calls for a dry moisture content for the test fuel used during testing. There is no way to measure the moisture content of pellets on a dry basis. Instead one can determine the wet basis moisture content by drying a sample. This is what done and the data for this is on Data Sheet 11 in the test run. Once the wet basis moisture content is known, it is then possible to calculate the fuel burnt on a dry basis, which again is what was done. The dry burn rate (DBR) determined is the same. The revised procedures and equations used to determine the actual DBR are to be found on the page after Data Sheet 11.

The following pages contain: (1.) A discussion of test results. (2.) A diagram showing the height of the appliance and chimney used during testing (ICC EXCEL Pellet Pipe) and the location of the sampling ports in the chimney. (3.) A diagram of the EPA 6" diameter dilution tunnel used by Myren Consulting during EPA Certification testing, (4.) Three pages of photographs showing the unit installed on the platform scale. One of these photos is a close up of the flue pipe/ flue collar junction and shows the static probe and the thermocouple used to measure stack temperature at one foot. (5.) A copy of the letter from EPA granting Myren Consulting, Inc accreditation under the new NSPS. (6.) a copy of the old and new EPA Laboratory Accreditation Certificates for Myren Consulting's lab and (7.) a copy of the 30 day advance certification test notification sent to EPA for the week the unit was tested.

#### DISCUSSION:

- (1.) The test series was done at Myren Consulting's lab in Colville, WA.
- (2.) The test series required 1 test run.
- (3.) This is the second pellet stove report Myren Consulting has submitted to EPA since the new NSPS went into effect. Thus, because the whole testing format for pellet stoves has changed, there are several revisions to the report format necessitated by the difference in rules and reporting requirements in the old NSPS versus the rules and reporting requirements in the new NSPS. Specifically the following changes have been made:
  - a. Because the pellet stove test is now an integrated sample test, there are no weighted average calculations because collecting the integrated sample "automatically" generates a "weighted average". Instead of the pages used to calculate a weighted average, there is now a single page titled *Integrated Test Results*, which reports the emission rate and overall efficiency (%OE) for the unit.
  - b. A new page has been added to the Data Summary Section (p. 2) which summarizes the PM Sampling Train Performance information and addresses the *Dual Train Comparison* criteria found in ASTM E2515 Section 11.7. The average emission rate calculated and reported on this new page using the data from the 2 PM sampling trains is then also reported on the page titled *Integrated Test Results*. Also reported on this page are the performance data for



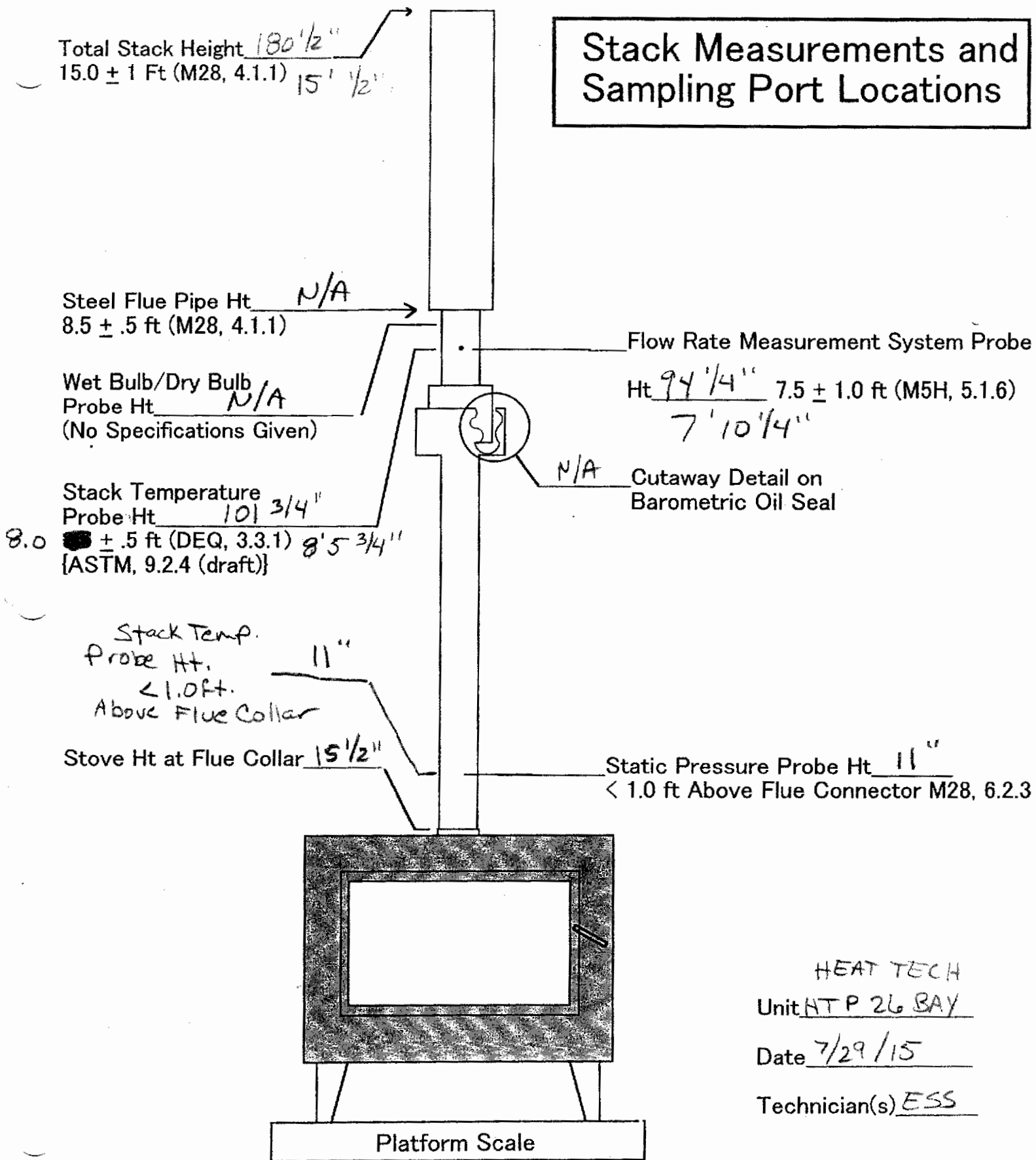
the "Room Blank" train and the PM emission rate (g/h) data for the 0-60 minute filter set from Train 1.

c. Section 60.534(d) requires that filter sets be changed (switched) at 1 h into a test run on one of the PM sampling trains. This was done on Train 1 during the test run. Thus there are additional data sheets in each test run for the 2 filter sets used in Train 1 to accomplish this requirement. There is also a photo of the filters from the test run in the section with the raw data sheets for the test run. As noted above, the PM emission rate for the first hour is reported on the computer spreadsheet for that PM sample and again in the Data Summary section itself.

- d. ASTM E2515 requires 2 PM sampling trains and a third "Room Blank" train. That means there are also additional data sheets for Trains 2 and 3 in the section with the Raw Data sheets for the test run and in the Cal Data Section where the calibration and post test audit data is presented for the equipment used in all 3 of these trains.

Please look at the Table of Contents (p. iv), the Pellet Stove Test Report Page Number Index (pp. vi-vii) and the Individual Test Run Page Index (p. viii) to find any pages of interest. Or call Myren Consulting, Inc. at either 509 685 9458 or 509 684 1154 if further assistance is needed.

# Stack Measurements and Sampling Port Locations



HEAT TECH  
 Unit NTP 26 BAY  
 Date 7/29/15  
 Technician(s) ESS

Stack is all 4" ICC EXCEL PELLET

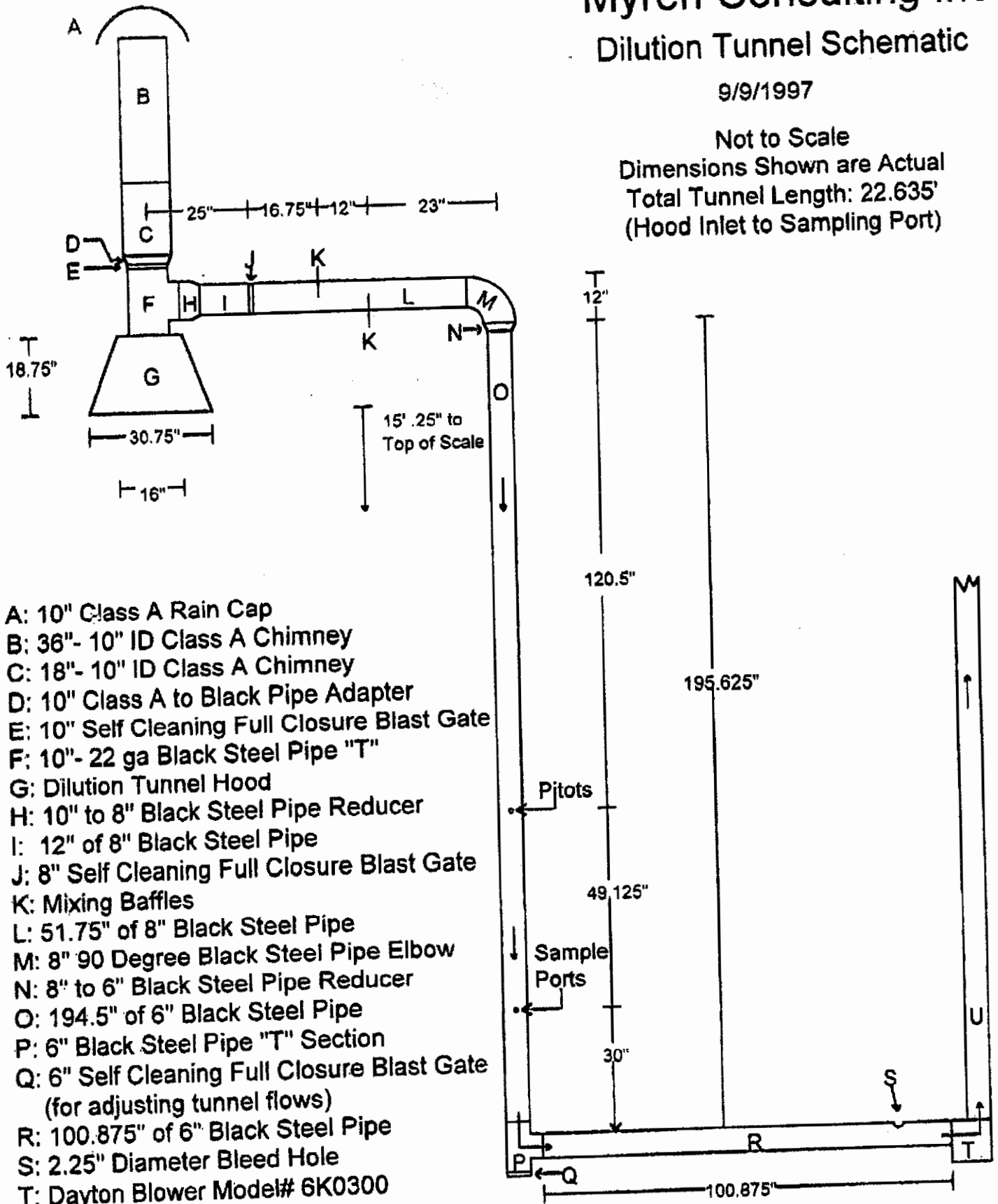
# Myren Consulting Inc

## Dilution Tunnel Schematic

9/9/1997

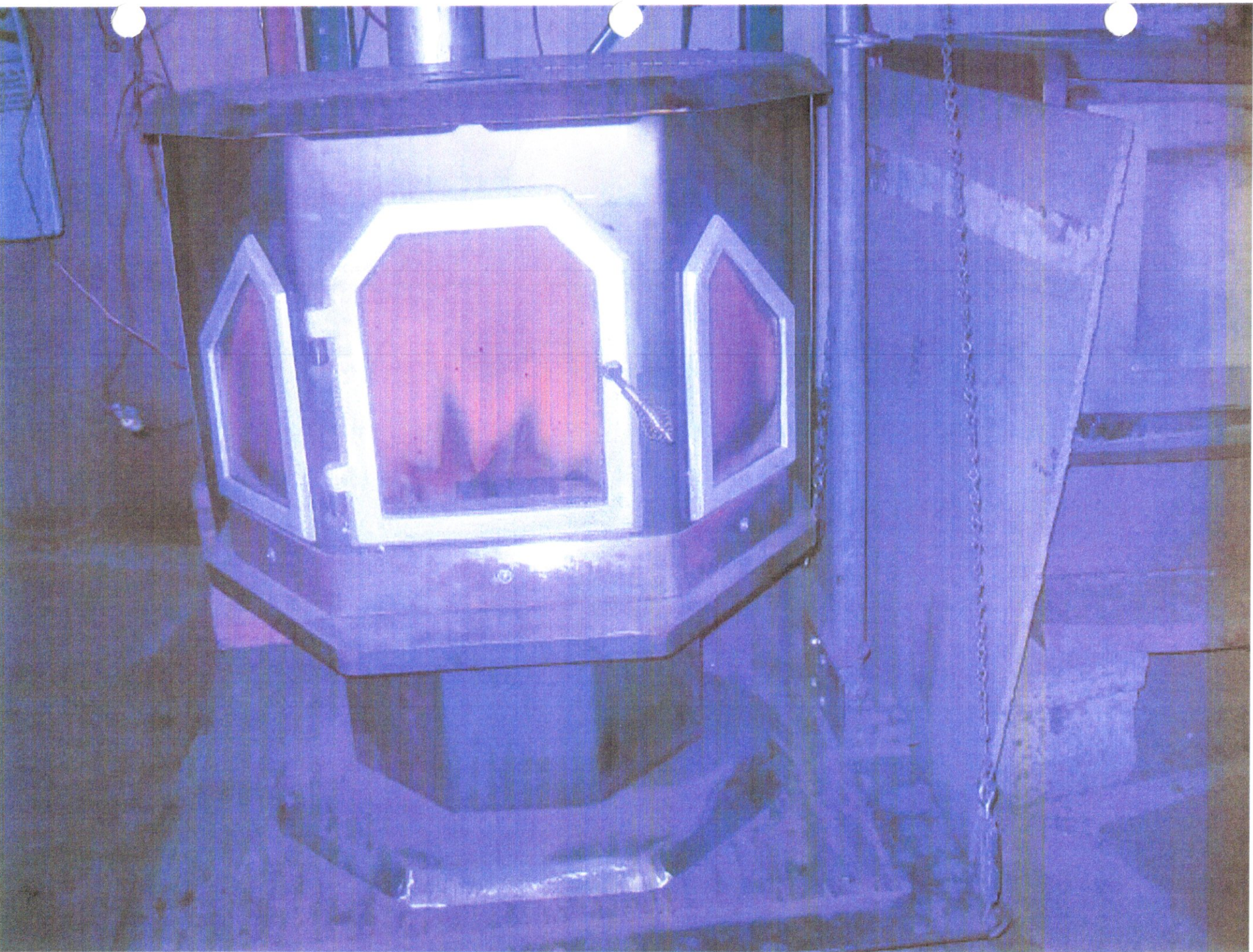
Not to Scale

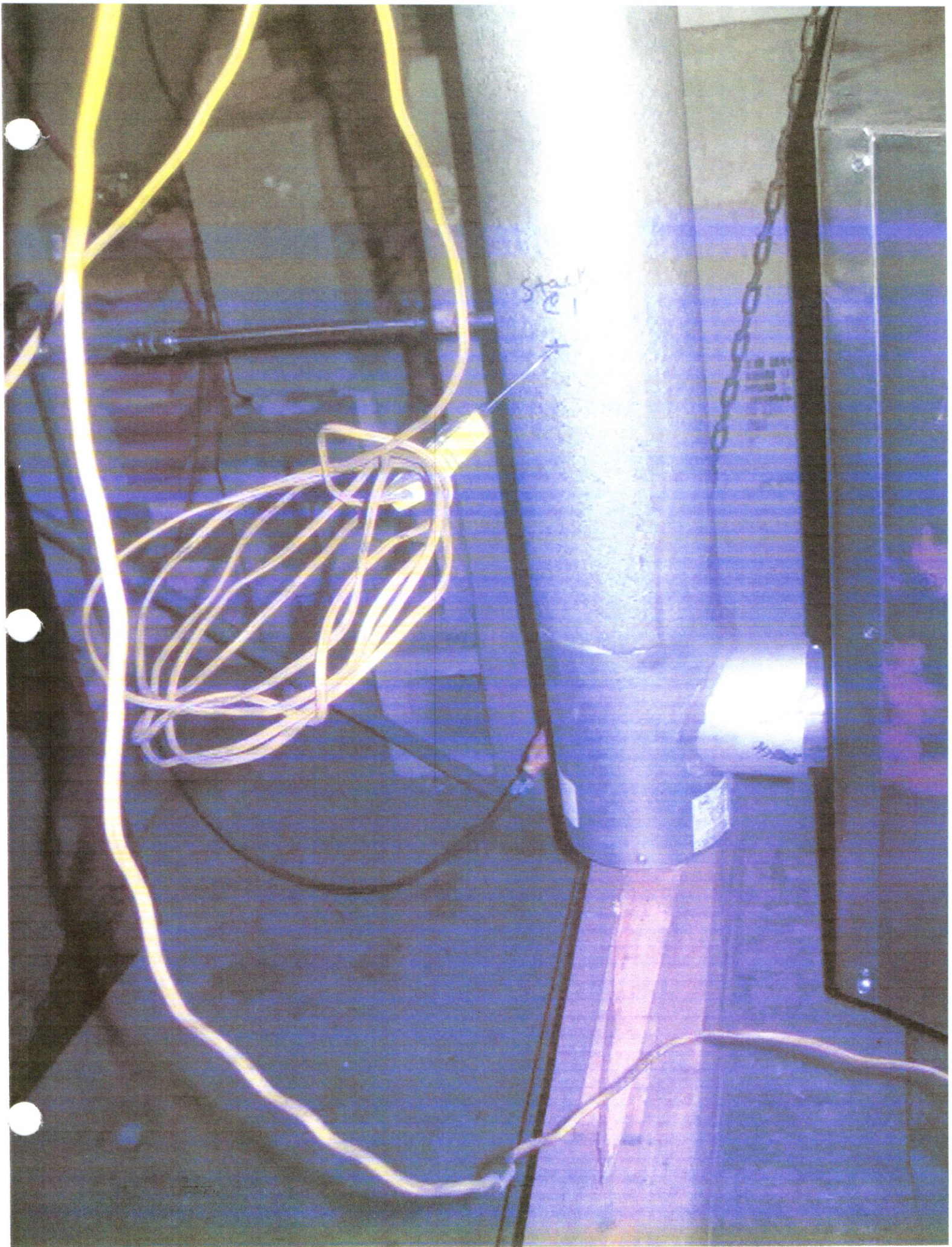
Dimensions Shown are Actual  
 Total Tunnel Length: 22.635'  
 (Hood Inlet to Sampling Port)



- A: 10" Class A Rain Cap
- B: 36"- 10" ID Class A Chimney
- C: 18"- 10" ID Class A Chimney
- D: 10" Class A to Black Pipe Adapter
- E: 10" Self Cleaning Full Closure Blast Gate
- F: 10"- 22 ga Black Steel Pipe "T"
- G: Dilution Tunnel Hood
- H: 10" to 8" Black Steel Pipe Reducer
- I: 12" of 8" Black Steel Pipe
- J: 8" Self Cleaning Full Closure Blast Gate
- K: Mixing Baffles
- L: 51.75" of 8" Black Steel Pipe
- M: 8" 90 Degree Black Steel Pipe Elbow
- N: 8" to 6" Black Steel Pipe Reducer
- O: 194.5" of 6" Black Steel Pipe
- P: 6" Black Steel Pipe "T" Section
- Q: 6" Self Cleaning Full Closure Blast Gate  
(for adjusting tunnel flows)
- R: 100.875" of 6" Black Steel Pipe
- S: 2.25" Diameter Bleed Hole
- T: Dayton Blower Model# 6K0300  
1/3 HP 1725 RPM
- U: 6" black Steel Pipe Exhaust







Stack

+

1000  
1000  
1000

1000

1000



UNITED STATES ENVIRONMENTAL PROTECTION AGENCY  
RESEARCH TRIANGLE PARK, NC 27711

NOV 12 2015

OFFICE OF  
AIR QUALITY PLANNING  
AND STANDARDS

Ben Myren  
Myren Consulting, Inc.  
512 Williams Lake Road  
Coleville, WA 99114

Dear Mr. Myren:

Thank you for your recent inquiry regarding the United States Environmental Protection Agency (EPA) wood heater laboratory accreditation program. The review of your reaccreditation letter that you submitted November 10, 2015 is complete and acceptable. Enclosed is your current certificate of accreditation. Myren Consulting, Inc. is accredited under Subpart AAA 40 CFR Standards of Performance for New Residential Wood Heaters Sections (60.534, 60.535) and Subpart QQQQ 40 CFR Standards of Performance for New Residential Hydronic Heaters and Forced-Air Furnaces Sections (60.5476, 60.5477). Please follow the requirements for EPA Test Method 28R Certification and Auditing of Wood Heaters in Appendix A-8 to Part 60-Test Methods 26 through 30B. This approval expires on March 16, 2018, unless renewed by Myren Consulting, Inc.

As a condition of your lab accreditation, Myren Consulting, Inc. must abide by the following provisions:

- (i) Agree to participate biennially in an independently operated proficiency testing program with no direct ties to the laboratories participating;
- (ii) Agree to allow the EPA, regulatory agencies and certifying bodies access to observe certification testing;
- (iii) Agree to comply with calibration, reporting and recordkeeping requirements that affect testing laboratories; and
- (iv) Agree to perform a compliance audit test at the manufacturer's expense at the testing cost normally charged to such manufacturer if the laboratory is selected by the EPA to conduct a compliance audit test of the manufacturer's model line;
- (v) Have no conflict of interest and receive no financial benefit from the outcome of certification testing conducted pursuant to §60.5475;
- (vi) Agree to not perform initial certification tests on any models manufactured by a manufacturer for which the laboratory has conducted research and development design services within the last 5 years;
- (vii) Agree to seal any wood heater on which it performed certification tests, immediately upon completion or suspension of certification testing, by using a laboratory-specific seal.
- (viii) Agree to immediately notify the EPA of any suspended tests through email and in writing, giving the date suspended, the reason(s) why, and the projected date for restarting.

Emission test reports should be submitted to EPA's Office of Enforcement and Compliance Assurance, at one of the following addresses:

U.S. Postal Service

U.S. EPA  
Office of Enforcement and Compliance  
Assurance, Office of Compliance  
William Jefferson Clinton Building, South  
Mail Code 2227A  
1200 Pennsylvania Ave, NW  
Washington, DC 20003

Attn: Wood heater Certification Lead

Private Courier

U.S. EPA  
Office of Enforcement and Compliance  
Assurance, Office of Compliance  
William Jefferson Clinton Building, South  
Room 7419D  
1200 Pennsylvania Ave, NW  
Washington, DC 20003

Attn: Woodheater Certification Lead

I would like to thank you for your cooperation in the wood heater certification program.

Sincerely,



Steffan Johnson  
Measurement Technology Group

Enclosure (2)

cc.

Julius Banks, OECA (2227A)  
Rafael Sanchez, OECA (2227A)  
Adam Baumgart-Getz, OID (C304-05)  
Amanda Aldridge, OID (C304-05)  
David Cole, OID (C304-05)



# CERTIFICATE OF ACCREDITATION

This certifies that:



Myren Consulting, Inc

Has satisfied the requirements for laboratory accreditation for the certification of wood heaters pursuant to subpart AAA of 40 CFR Part 60, New Source Performance Standards For Residential Wood Heaters

June 5, 2012 - June 5, 2017

**EFFECTIVE DATE**

Connie Oldham  
**MEASUREMENT TECHNOLOGY GROUP  
GROUP LEADER**

Methods 5G, 28, 28A, 5H

**METHODS**

6

**CERTIFICATE NUMBER**

# CERTIFICATE OF ACCREDITATION

This certifies that:

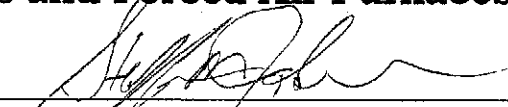


Myren Consulting, Inc

Has satisfied the requirements for laboratory accreditation for the certification of wood heaters pursuant to subpart AAA of 40 CFR Part 60, New Source Performance Standards For Residential Wood Heaters and subpart QQQQ of 40 CFR Part 60, Standards of Performance for New Hydronic Heaters and Forced Air Furnaces.

November 12, 2015 - March 16, 2018

**EFFECTIVE DATE**

  
MEASUREMENT TECHNOLOGY GROUP  
**GROUP LEADER**

Methods 28R, 28 WHH, 28 WHH-PTS,

All Methods listed in Sections 60.534 and 60.5476

**METHODS**

2

**CERTIFICATE NUMBER**

# Myren Consulting, Inc.

512 Williams Lake Road

Colville, WA 99114

Office: (509) 684-1154

Lab: (509) 685-9458

Fax: (509) 684-3987

email:myren.ben@gmail.com

---

DATE: 4 June 2015

TO: Dr. Rafael Sanchez, PhD., EPA

CC: Tom Bassett, Heat Tech

FROM: Ben Myren

RE: Wood Heater 30 Day Advance Certification Test Notification  
for the Heat Tech H.T.P. P 26 Bay

Section 60.534(e)(1) of the Wood Heater NSPS requires that EPA be notified at least 30 days in advance of the start or resumption of EPA Certification Testing for each specific model line. To comply with the above requirement, Myren Consulting, Inc. hereby notifies EPA that Myren Consulting, Inc., 512 Williams Lake Road, Colville, WA 99114 plans to start an EPA Certification Test series on the unit identified below.

UNIT: H.T.P. P 26 Bay pellet stove

Manufactured by:

Heat tech Industries, LLC.

PO Box 727

Biggs, CA 95917

P: 530 846 1985

Email: [sharletasgarden@gmail.com](mailto:sharletasgarden@gmail.com)

Website: [www.heattechstoves.com](http://www.heattechstoves.com)

starting sometime during the period beginning on :

Monday July 27, 2015.

The testing will be conducted at:

Myren Consulting, Inc's lab at 512 Williams Lake Road, Colville, WA 99114

3<sup>rd</sup> Party Certifying Entity (Probable)

PFS, 1507 Matt Pass, Cottage Grove, WI 53527 P: 608 839 1085

If you have any questions about this notification, contact me immediately.

**EPA  
PELLET STOVE  
INTEGRATED TEST RESULTS**

The integrated average particulate matter (PM)  
emission rate for the

**HEAT TECH HTP 26 BAY PELLETT STOVE**

is

**1.3845 g/h.**

The integrated average overall HHV efficiency (%OE)  
for the

**HEAT TECH HTP 26 STANDARD PELLETT STOVE**

is

**69.7%.**

The integrated average overall LHV efficiency (%OE)  
for the

**HEAT TECH HTP 26 STANDARD PELLETT STOVE**

is

**75.2%.**

## SUMMARY OF ASTM E2515 PARTICULATE EMISSIONS SAMPLING TRAIN PERFORMANCE

RUN #	DBR (kg/hr)	T1					T2					Avg. g/h.	% DIFF
		CATCH (mg)	SAMPLE RATE (cfm)	SAMPLE VOL (dscf)	AVG. % PROP	EMISSIONS (g/h)	CATCH (mg)	SAMPLE RATE (cfm)	SAMPLE VOL (dscf)	AVG. % PROP	EMISSIONS (g/h)		
EPA 1	0.998	14.0	.538	189.534	99.904	1.463	12.0	.551	180.125	99.941	1.306	1.3845	5.67

SUMMARY OF ASTM E2515 AMBIENT AIR  
(ROOM BLANK) SAMPLING TRAIN PERFORMANCE

RUN #	CATCH (mg)	SAMPLE RATE (cfm)	SAMPLE VOL. (dscf)	AMBIENT PM CONCENTRATION (mg/dscf)
EPA 1	1.1	.532	175.270	.0.006276

TRAIN 1 0-60 MINUTE  
DBR and PM EMISSIONS

Run #	DBR (kg/h)	EMISSIONS (g/h)
EPA 1	1.797	0.360

HEAT TECH

Unit: HTP 26 Bay

Page 1 of 3

WST2-Form 12 Rev 11/2011

## Woodstove Data Summary

	Run #								
<b><u>Particulate Emissions:</u></b>									
Emission Rate:		<u>1.3845</u>							g/hr
Emission Factor:		<u>1.3875</u>							g/kg
(Dry fuel weight basis)									
<b><u>Efficiency Values: (CSA B415.10-1)</u></b>									
Combustion Efficiency:		<u>99.5</u>							%
Heat Transfer Efficiency: HHV:		<u>70.0</u>							%
Heat Transfer Efficiency: LHV:		<u>75.7</u>							%
Overall Efficiency: HHV:		<u>69.7</u>							%
Overall Efficiency: LHV:		<u>75.4</u>							%
<b><u>Heat Output:</u></b>									
Avg. EPA Btu/hr. for test cycle		<u>14,901</u>							Btu/hr.
Avg. B415 Btu/hr. for test cycle		<u>13,081</u>							Btu/hr.
<b><u>Fuel Burn Rates:</u></b>									
Avg. Dry Burn Rate (Wet Basis)		<u>1.058</u>							kg/hr.
Avg. Dry Burn Rate (Dry Basis)		<u>1.00</u>							kg/hr.
<b><u>PM Sampling Parameters:</u></b>									
Avg. Tunnel Flow(Qsd):		<u>140.291</u>							dscfm
Avg. Tunnel Velocity(Vs):		<u>835.015</u>							ft./min.
Pitot Correction Factor:		<u>.98122</u>		<u>T2</u>					
Total Sample Volume:	<u>T1</u>	<u>189.534</u>		<u>180.125</u>					dscf
Avg. Sampling Flow Rate:		<u>.538</u>		<u>.551</u>					cfm
Avg. % Proportionality:		<u>99904</u>		<u>99941</u>					%
Total Particulate Catch:		<u>14</u>		<u>12</u>					mg

## Woodstove Data Summary

	Run #							
<b><u>Fuel Moisture Content:</u></b>								
Kindling (Wet basis):		—						%
Pre Test Fuel (Wet basis):		5.70						%
Test Fuel (Wet basis):		5.70						%
<b><u>Air/Fuel Ratio:</u></b>								
lbs. air/lbs. fuel:		30.15						
<b><u>Average Stack Gas Composition:</u></b>								
Avg. % CO <sub>2</sub> :		4.02						%
Avg. % O <sub>2</sub> : (stoichiometrically)		16.90						%
Avg. % CO:		.04						%
<b><u>Average Stack Gas Flow Rate:</u></b>								
Stack Flow Rate- EPA CMB		—						dscfm
Draft (static):		-.0458						in. H <sub>2</sub> O
<b><u>Average Stack Gas Emission Factors:</u></b>								
CO:		13.47						g/Kg
		13.45						g/hr.





## **AGING DATA**

**The Heat Tech HTP 26 BAY Pellet Stove was aged by Myren Consulting, Inc. The Aging installation configuration was the same as the installation used during certification testing. During Aging the stove was run on the Medium setting used during certification testing and the temperature and the (wet) burn rate data were collected using a Data Acquisition System (DAS). The Aging data was then transferred from the DAS spreadsheet to the Aging data pages in this section.**

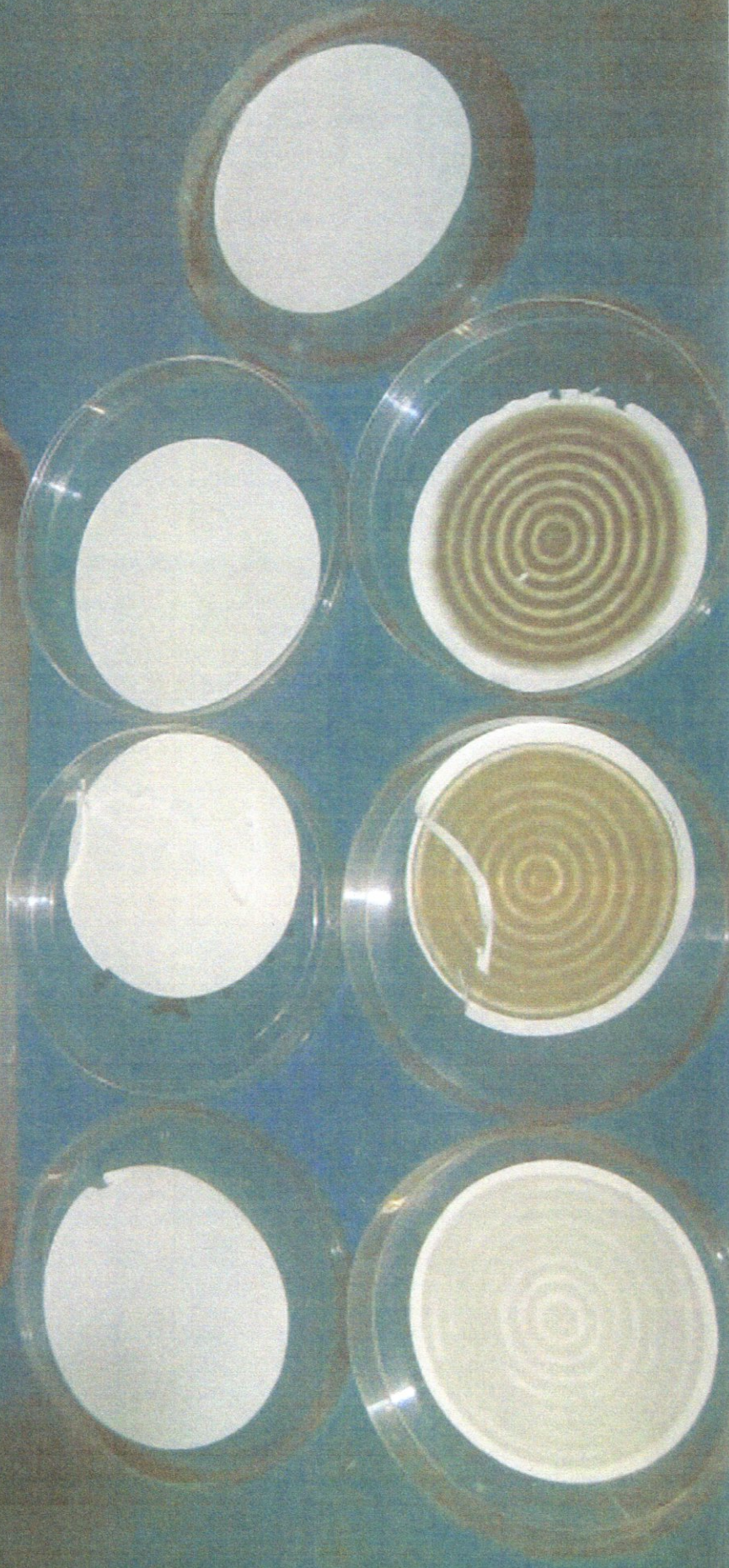
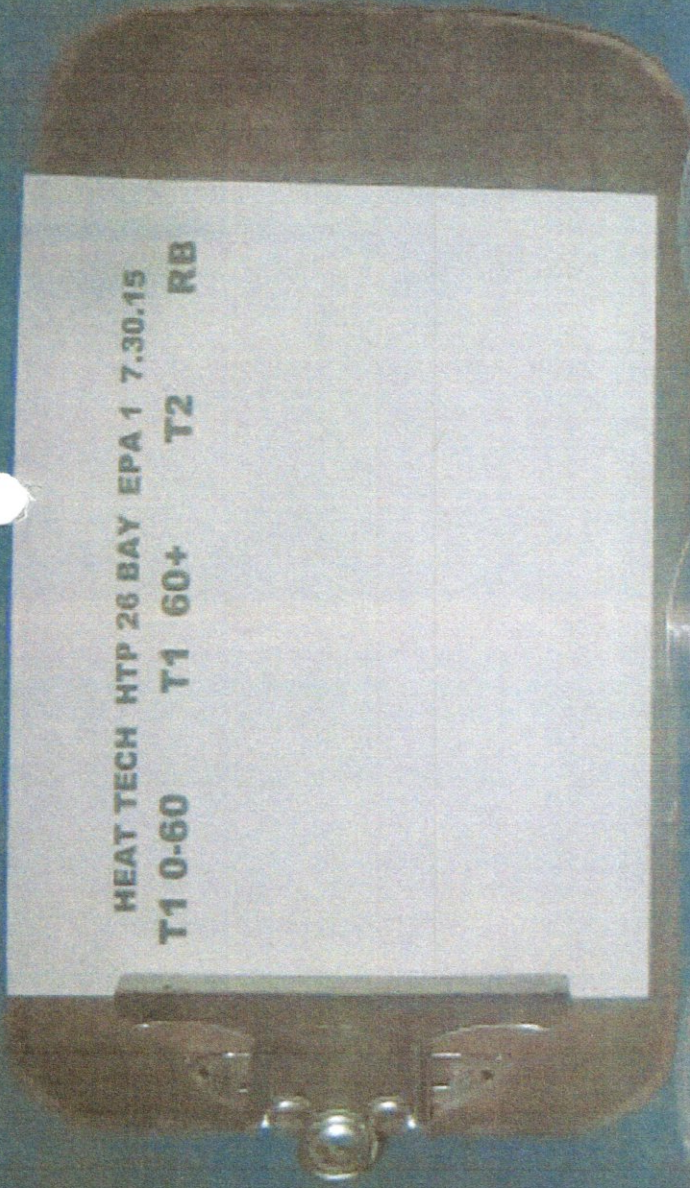
PELLET STOVE AGING DATA  
 Woodstove Test Data Sheet #25P  
 WST5-Form 3A, Rev 12/15

Unit: HEAT TECH HTP 26 Bay  
 Date(s): 6/24, 25, 26, 29, 30, 2015  
 Technicians: ATM ESS  
 Page: 1 of 2

					T/C#	
HOUR #	2015 DATE	TIME	POUNDS BURNT	STACK TEMP		COMMENTS
1	6/24	950	2.5	324		Fire Started @ 8:50
2		1050	2.5	313		
3		1150	2.6	310		
4		1250	2.6	312		
5		1350	2.7	327		
6		1450	2.6	320		
7		1550	2.7	337		
8		1650	2.7	338		
9		1750	2.7	327		
10		1850	2.5	344		
11		1950	2.6	345		
12		2050	2.8	337		
13		2130	2.5	329		
14		2230	2.6	335		
15	✓	2330	2.6	332		
16	6/25	0030	2.5	342		
17		0130	2.6	337		
18		0230	2.4	327		
19	✓	0330	2.0	280		
20	6/25	0945	2.7	326		Fire Started @ 9:45
21		1045	2.9	323		
22		1145	2.6	326		
23		1245	1.0	327		
24		1345	2.5	343		
25		1445	3.0	356		
26		1545	2.6	347		
27		1645	2.9	345		Added fuel @ 1605
28		1745	3.0	343		
29	✓	1845	2.5	347		



HEAT TECH HTP 26 BAY EPA 1 7.30.15  
T1 0-60 T1 60+ T2 RB



# MYREN CONSULTING, INC

**Manufacturer:** HEAT TECH  
**Model:** HTP 26 BAY  
**Date:** 7.30.15  
**Run:** EPA 1  
**Control #:**  
**Test Duration:** 360  
**Output Category:** VARIABLE

**Technicians:** ATMYREN  
 \_\_\_\_\_  
 \_\_\_\_\_

**Test Results in Accordance with CSA B415.1-09**

	HHV Basis	LHV Basis
<b>Overall Efficiency</b>	69.7%	75.4%
<b>Combustion Efficiency</b>	99.5%	99.5%
<b>Heat Transfer Efficiency</b>	70%	75.7%

<b>Output Rate (kJ/h)</b>	13,789	13,081	<b>(Btu/h)</b>
<b>Burn Rate (kg/h)</b>	1.00	2.20	<b>(lb/h)</b>
<b>Input (kJ/h)</b>	19,777	18,761	<b>(Btu/h)</b>

<b>Test Load Weight (dry kg)</b>	5.99	13.20	<b>dry lb</b>
<b>MC wet (%)</b>	5.7		
<b>MC dry (%)</b>	6.04		
<b>Particulate (g)</b>	3.23065		
<b>CO (g)</b>	81		
<b>Test Duration (h)</b>	6.00		

Emissions	Particulate	CO
<b>g/MJ Output</b>	0.04	0.98
<b>g/kg Dry Fuel</b>	0.54	13.47
<b>g/h</b>	0.54	13.45
<b>lb/MM Btu Output</b>	0.09	2.27

<b>Air/Fuel Ratio (A/F)</b>	30.15
-----------------------------	-------

VERSION:

2.2

12/14/2009

VERSION: 2.2

12/14/2009

Manufacturer: HEAT TECH  
 Model: HTP 26 BAY  
 Date: 7.30.15  
 Run: EPA 1

Appliance Type: NON CAT (Cat, Non-Cat, Pellet)

Temp. Units F (F or C)  
 Weight Units lb (kg or lb)

**Default Fuel Values**  
 D. Fir Oak  
 HHV (kJ/kg) 19,810 19,887  
 %C 48.73 50  
 %H 6.87 6.6  
 %O 43.9 42.9  
 %Ash 0.5 0.5

Control #: \_\_\_\_\_  
 Test Duration: 360  
 Output Category: VARIABLE

**Fuel Data**

Wood Moisture (% wet): 5.70  
 Load Weight (lb wet): 14.00  
 Burn Rate (dry kg/h): 1.00  
 Total Particulate Emissions: 3.23065 g

HHV 19,810 kJ/kg  
 %C 48.73  
 %H 6.87  
 %O 43.9  
 %Ash 0.5

Note 1: For other fuels, use the heating value and fuel composition determined by analysis of fuel sample in accordance with Clause 9.2.

Averages 0.04 4.02 16.90 316.43 88.68

Elapsed Time (min)	Fuel Weight Remaining (lb)	Flue Gas Composition (%)			Temp. (°F)	
		CO	CO <sub>2</sub>	O <sub>2</sub>	Flue Gas	Room Temp
0	14.00	0.03	6.28	14.65	422.0	89.0
10	13.20	0.02	6.33	14.60	425.0	88.0
20	12.60	0.02	6.03	14.90	421.0	89.0
30	12.00	0.01	6.55	14.39	428.0	89.0
40	11.30	0.01	5.80	15.14	424.0	89.0
50	10.50	0.02	5.78	15.15	423.0	90.0
60	9.80	0.02	5.03	15.90	422.0	90.0
70	9.40	0.03	3.86	17.27	386.0	90.0
80	8.90	0.03	5.08	15.85	373.0	90.0
90	8.50	0.09	3.13	17.77	363.0	90.0
100	8.10	0.08	3.03	17.87	351.0	84.0
110	7.70	0.05	3.81	17.11	348.0	84.0
120	7.20	0.04	4.56	16.36	349.0	85.0
130	6.80	0.04	3.71	17.21	348.0	89.0
140	6.40	0.02	4.68	16.25	349.0	90.0
150	5.90	0.02	4.93	16.00	359.0	88.0
160	5.40	0.03	4.78	16.15	351.0	88.0
170	5.00	0.04	4.56	16.36	348.0	90.0
180	4.50	0.06	3.26	17.66	347.0	88.0
190	4.10	0.05	2.88	18.04	308.0	89.0
200	3.90	0.04	3.68	17.24	275.0	90.0
210	3.60	0.03	3.26	17.87	256.0	88.0
220	3.40	0.14	1.48	19.39	236.0	88.0
230	3.20	0.03	3.43	17.50	242.0	88.0
240	2.90	0.05	2.81	18.11	246.0	89.0
250	2.70	0.06	2.58	18.33	238.0	88.0
260	2.40	0.01	4.78	16.16	250.0	89.0
270	2.20	0.03	3.58	17.35	243.0	88.0
280	1.90	0.10	2.56	18.31	238.0	89.0
290	1.70	0.06	2.68	18.23	238.0	88.0
300	1.50	0.08	3.06	17.84	246.0	90.0
310	1.20	0.02	5.13	15.80	245.0	89.0
320	1.00	0.04	3.66	17.26	239.0	89.0
330	0.70	0.06	2.41	18.50	234.0	90.0
340	0.50	0.11	2.11	18.78	245.0	90.0
350	0.20	0.05	2.76	18.16	242.0	90.0
360	0.00	0.02	4.83	16.10	250.0	89.0

Note 2: In cases where the "Fuel Weight Remaining" is the same for three or more readings in a row, a "divide by zero error" will occur in the calculation sheet. In such cases, adjust the weight values by interpolation between the first occurrence and the next reading showing a decrease in weight.

# MYREN CONSULTING, INC

**Manufacturer:** HEAT TECH  
**Model:** HTP 26 BAY  
**Date:** 7.30.15  
**Run:** EPA 1  
**Control #:**  
**Test Duration:** 60  
**Output Category:** HIGH

**Technicians:** ATMYREN  
 \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

## Test Results in Accordance with CSA B415.1-09

	HHV Basis	LHV Basis
Overall Efficiency	68.1%	73.6%
Combustion Efficiency	99.5%	99.5%
Heat Transfer Efficiency	68%	74.0%

Output Rate (kJ/h)	24,244	22,998	(Btu/h)
Burn Rate (kg/h)	1.80	3.96	(lb/h)
Input (kJ/h)	35,599	33,769	(Btu/h)

Test Load Weight (dry kg)	1.80	3.96	dry lb
MC wet (%)	5.7		
MC dry (%)	6.04		
Particulate (g)	0.8407		
CO (g)	6		
Test Duration (h)	1.00		

Emissions	Particulate	CO
g/MJ Output	0.03	0.26
g/kg Dry Fuel	0.47	3.52
g/h	0.84	6.33
lb/MM Btu Output	0.08	0.61

Air/Fuel Ratio (A/F)	20.45
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MYREN CONSULTING, INC.

Dilution Tunnel Traverse Data with 8  
Traverse Points Rev: 1.7.12

Unit: HEAT Tech HTP 26 Bay

Run #: EPA 1

Date: 7/30/15

Technicians: ATM ESS

Point	Location	$\Delta p$	$\sqrt{\Delta p_{trav}}$	$\Delta p$	$\sqrt{\Delta p_{cent}}$	$T_{trav}$	$T_{cent}$	$P_g$
W-1	0.5"	<u>.034</u>	<u>.184</u> X			<u>119</u>		
2	1.5	<u>.037</u>	<u>.192</u> X			<u>121</u>		
Center	Center			<u>.039</u>	<u>.197</u> X		<u>121</u>	
3	4.5	<u>.040</u>	<u>.200</u> X			<u>122</u>		
4	5.5	<u>.039</u>	<u>.197</u> X			<u>121</u>		
S-1	0.5	<u>.035</u>	<u>.187</u> X			<u>120</u>		
2	1.5	<u>.038</u>	<u>.195</u> X			<u>121</u>		
Center	Center			<u>.039</u>	<u>.197</u> X		<u>122</u>	
3	4.5	<u>.039</u>	<u>.197</u> X			<u>122</u>		
4	5.5	<u>.038</u>	<u>.195</u> X			<u>121</u>		
	Totals		<u>1.547</u> X		<u>.394</u> X	<u>967</u> X	<u>243</u> X	
	Average		<u>.1934</u> X		<u>.1970</u> X	<u>120.9</u> X	<u>121.5</u> X	
	$^{\circ}R = (^{\circ}F + 460)$					<u>580.9</u> X	<u>581.5</u> X	

BP = 28.60 "Hg    Ps = BP + (-Pg/13.6) = 28.60 + (—/13.6) = 28.60 " Hg

LEAK CHECKS: Manometer Level: OK ✓    Zeroed: OK ✓    Tech: ESS

Pg Leg: Pre Test: Pressure: -.250 " H<sub>2</sub>O Movement: .000 " H<sub>2</sub>O Tech: ESS

Post Test: Pressure: -.250 " H<sub>2</sub>O Movement: .000 " H<sub>2</sub>O Tech: ESS

Velocity Head Leg: Pre Test: Pressure: +.024 " H<sub>2</sub>O Movement: .000 " H<sub>2</sub>O Tech: ESS

Post Test: Pressure: +.009 " H<sub>2</sub>O Movement: .000 " H<sub>2</sub>O Tech: ESS

DILUTION TUNNEL GAS VELOCITY & VOLUMETRIC FLOW RATE CALCULATIONS

Rev 1/7/12

UNIT: HEAT Tech HTP260py DATE: 7/30/15 RUN #: LPA1 TECHNICIAN(S): ATM ESS

Average Gas Velocity in the Dilution Tunnel  $V_{strav}$  (EPA M2 eqn 2-9, ASTM E 2515 EQN 7)

$$(9) V_{strav} = (85.49) \frac{(0.99 \text{ cp})}{(2)} \left( \frac{.1934 \bar{X}}{(2)} \sqrt{\Delta P} \text{ "H}_2\text{O} \right) \sqrt{\frac{\frac{580.9 \text{ Ts } ^\circ\text{A}}{(0)}}{\left( \frac{28.60 \text{ Ps "Hg}}{(2)} \right) \left( \frac{28. \text{ lb./ lb. mole}}{78} \right) (2)}}} = 13.75084 \text{ fps}$$

$$(9A) V_s = \frac{(13.75084 \text{ fps})}{(2)} (60) = \frac{825.050}{(2)} \text{ fpm}$$

EQN. 2-7 Gas Velocity in the Center of the Dilution Tunnel -  $V_{scent}$  (ASTM E 2515-07 EQN 7)

$$(9) V_{scent} = (85.49) \frac{(0.99 \text{ cp})}{(2)} \left( \frac{.1970 \bar{X}}{(2)} \sqrt{\Delta P} \text{ "H}_2\text{O} \right) \sqrt{\frac{\frac{581.5 \text{ Ts } ^\circ\text{A}}{(0)}}{\left( \frac{28.60 \text{ Ps "Hg}}{(2)} \right) \left( \frac{28. \text{ lb./ lb. mole}}{78} \right) (2)}}} = 14.01403 \text{ fps}$$

$$(9A) V_s = \frac{(14.01403 \text{ fps})}{(2)} (60) = \frac{840.842}{(2)} \text{ fpm}$$

ASTM E 2515-07 EQN 1 Adjustment Factor for center of Tunnel Pitot Tube Location

$$F_p = V_{strav} / V_{scent} = \frac{825.050}{840.842} = .98122$$

EQN. 2-8 Average Stack Gas Dry Volumetric Flow Rate  $Q_{std}$  (ASTM E 2515-07 EQN 3)

$$Q_{sd} = 3600 (1 - \frac{0. \overset{02}{Bws}}{(2)}) \frac{(13.75084 \text{ fps})}{(2)} \left( \frac{.1963 \text{ ft}^2}{(3)} \right) \left[ \frac{(528 \text{ } ^\circ\text{A}) \left( \frac{28.60 \text{ Ps "Hg}}{(2)} \right)}{\left( \frac{580.9 \text{ T}_s \text{ } ^\circ\text{A}}{(0)} \right) (29.92 \text{ "Hg})} \right] = 8273.9925 \text{ dscfhr (or dscfh)}$$

$$(10A) \frac{8273.9925 \text{ dscfhr}}{(1)} \div 60 = \frac{137.90}{(1)} \text{ dscfm (or dscfm)}$$

Note: Number in { } under blank lines denotes number of decimals to be used. If a blank calls for an answer already calculated, use the number of decimals previously specified for that answer.







White Round top

T1  
60+

METHOD 5G-1

PARTICULATE SAMPLING DATA

Rev. 10/09

DATE: 7/30/15 PAGE 1 OF 2 UNIT: Heat Tech HTP 26B<sub>2</sub> RUN: EPA 1

METER BOX: 456-P METER Y: 1.066 FILTER #'S: (F) 706 (R) 707

.9005/.9025 FILTER/O-RING ID #:     

PRE TEST LEAK CHECK: .002 CFM @ -15.0 IN HG FILTER SIZE: 110 mm

PROBE ID #:     

POST TEST LEAK CHECK:      CFM @      IN HG PROBE LENGTH      IN

TIME		METER READING (ft <sup>3</sup> )	PITOT		TUNNEL TEMP (°F)	METER TEMP (°F)	GAS METER Δh	VAC (in Hg)
CLOCK	ELAPSED		ΔP	Pg				
1140	00	894.376	.040		127	91	.90	-1.1
50	10	899.726	.040		124	93	.90	-1.1
1200	20	905.078	.040		123	95	.90	-1.1
10	30	910.495	.040		123	96	.90	-1.1
20	40	915.924	.040		121	97	.90	-1.1
30	50	921.351	.040		120	98	.90	-1.1
40	(60)	926.808	.040		120	98	.90	-1.1
50	70	932.249	.040		121	98	.90	-1.1
1300	80	937.698	.040		121	98	.90	-1.1
10	90	943.141	.040		123	98	.90	-1.1
20	100	948.783	.040		124	99	.90	-1.1
30	110	954.009	.040		124	98	.90	-1.1
40	(120)	959.471	.040		123	95	.90	-1.1
50	130	964.918	.040		116	93	.90	-1.1
1400	140	970.336	.040		112	92	.90	-1.1
10	150	975.732	.040		110	91	.90	-1.1
20	160	981.122	.040		109	90	.90	-1.1
30	170	986.510	.040		108	89	.90	-1.1
40	(80)	991.892	.040		110	89	.90	-1.1
50	190	997.275	.040		109	89	.90	-1.1

BP

00	28.60	300	28.52
60	28.59	360	28.51
120	28.58		
180	28.54		
240	28.53	AVG. =	28.553

Pre Test Filter  
Check Weighing  
F .6467  
R .6424

End of Test Weight  
F .6526 R .6252  
.6465 .6423

T1  
60+

METHOD 5G-1

PARTICULATE SAMPLING DATA

Rev. 10/09

DATE: 7/30/15 PAGE 2 OF 2 UNIT: HEAT Tech <sup>HJP</sup> 3<sup>rd</sup> fl RUN: EPA 1

METER BOX: 45G-P METER Y: 1.066 FILTER #'S: (F) 706 (R) 707

FILTER/ O-RING ID #:       

PRE TEST LEAK CHECK:        CFM @        IN HG FILTER SIZE: 110 mm

.188/.191 PROBE ID #:       

POST TEST LEAK CHECK: .003 CFM @ -10.25 IN HG PROBE LENGTH        IN

TIME		METER READING (m <sup>3</sup> ) (ft <sup>3</sup> )	PITOT		TUNNEL TEMP (°F)	METER TEMP (°F)	GAS METER Δh	VAC (in Hg)
CLOCK	ELAPSED		ΔP	Pg				
1500	200	1002.651	.040		110	88	.90	-1.1
10	210	1008.026	.040		110	88	.90	-1.1
20	220	1013.393	.040		110	88	.90	-1.1
30	230	1018.764	.040		110	88	.90	-1.1
40	240	1024.135	.040		111	88	.90	-1.1
50	250	1029.470	.040		110	88	.90	-1.1
1600	260	1034.812	.040		110	89	.90	-1.1
10	270	1040.157	.040		110	89	.90	-1.1
20	280	1045.487	.040		111	89	.90	-1.1
30	290	1050.821	.040		111	89	.90	-1.1
40	300	1056.161	.040		111	89	.90	-1.1
	10							
	20							
	30							
	40							
	50							
	60							
	70							
	80							
	90							

BP

00	<u>28.60</u>	300	<u>28.52</u>
60	<u>28.59</u>	360	<u>28.51</u>
120	<u>28.58</u>		
180	<u>28.54</u>		
240	<u>28.52</u>	AVG. =	<u>28.553</u>

Pre Test Filter  
Check Weighing  
F .6467  
R .6424

End of Test Weight  
F        R         
.6465 .6423

Woodstove Data Sheet #4-1: Initial Filter Weights ( Tare Weights)

Into Dessicator: Date 6/20/15 Time 1245 By ATM Front Half  Back Half

Manufacturer: PALL Size: 110 mm Lot.No.: T41116 Grade: A/E Glass 1.0µm

Balance Used: Sartorius Model: CP224S SN: 24850860

Filter #	First Wt	Date	Time	By	Second Wt	Date	Time	By	Third Wt	Date	Time	By
701	.6445	6/25	1513	ESS	.6442	7/8	11:38	ATM	.6442	7/14	1523	ESS
702	.6466		1512	ESS	.6462		11:35	ATM	.6462		1524	ESS
T3 T2 T2 T160+ T1601 703	.6460		1511	ESS	.6455		11:37	ATM	<del>.6455</del>		1525	ESS
704	.6476		1510	ESS	.6472		11:39	ATM	<del>.6473</del>		1526	ESS
705	.6450		1509	ESS	.6444		11:41	ATM	<del>.6445</del>		1527	ESS
706	.6472		1508	ESS	.6467		11:43	AM	<del>.6465</del>		1528	ESS
707	.6425		1507	ESS	<u>.6423</u>		11:41	ATM				
708	.6470		1506	ESS	.6465		11:46	ATM	.6467		1529	ESS
709	.6503		1506	ESS	.6499		11:47	AM	.6497		1530	ESS
T10-60 T10-60 710	.6509		1505	ESS	.6505	9/10	13:38	AM	<u>.6503</u>		1531	ESS
711	.6514		1504	ESS	.6511		13:39	ATM	<u>.6509</u>		1532	ESS
712	.6515		1503	ESS	.6511		13:40	AM	.6512		1533	ESS
713	.6498		1502	ESS	.6496		13:41	ATM				
714	.6522		1501	ESS	.6520		13:42	ATM				
715	.6494		1500	ESS	.6493		13:43	ATM				
716	.6480		1459	ESS	.6481		13:43	ATM				
717	.6503		1458	ESS	.6502		13:44	ATM				
718	.6539		1457	ESS	.6537		13:45	ATM				
719	.6476		1456	ESS	.6474		13:47	ATM				
720	.6539		1455	ESS	.6534		13:48	ATM	.6536		1534	ESS
721	.6485		1454	ESS	.6485		13:49	ATM				
722	.6588		1453	ESS	.6588		13:50	ATM				
723	.6564		1452	ESS	.6564		13:50	ATM				
724	.6571		1451	ESS	.6569		13:51	ATM				
725	.6601		1450	ESS	.6602		13:52	ATM				

Checked by A.T. Myron

Date: 7/26/15 Time: 1500

QA Reweigh

Balance Room Environmental Conditions

Filter #	WT	Date	Time	By
716	.6481	7.26.15	1525	Jon
711	.6510	7.26.15	1526	Jon
709	.6499	7.26.15	1527	Jon
704	.6475	7.26.15	1528	Jon

WB	DB	%RH	Date	Time	By
56	69	43	6/25	839	ATM
58	72	42	7/10	1315	ATM
57	69	46	7/14	1512	ESS
57	69	47	7.26	1421	ATM

Post	Date	1 <sup>st</sup>	2 <sup>nd</sup>	3 <sup>rd</sup>	4 <sup>th</sup>	5 <sup>th</sup>
Weighing	0.0000g	0.0000	0.0000	0.0000	0.0000	
Scale Check	100.0000g	99.9995	99.9996	99.9996	99.9994	



Woodstove Data Sheet #4-2: Initial Beaker Weights (Tare Weights)

7/23/15 1254 ATM 30-32  
 Into Dessicator: Date 7/21/15 Time 1600 By ATM 20-29  
 Balance Used: Sartorius Model: CP224S SN:24850860

Bkr #	First Wt	Date	Time	By	Second Wt	Date	Time	By	Third Wt	Date	Time	By
00	73.3176	7/23	1243	ATM	73.3173	7/24	1535	ESS	73.3174	7/26	1454	AM
01	71.0016		1244	ATM	71.0019		1534	ESS	71.0019	7/26	1443	AM
02	71.8344		1246	ATM	71.8342		1533	ESS	← T1 60+			
03	70.7389		1247	ATM	70.7384		1532	ESS	70.7385	7/26	1446	AM
04	73.2138		1240	ATM	73.2188		1540	ESS	X T3			
05	72.6525		1241	ATM	72.6524		1539	ESS				
06	71.7871		1242	ATM	71.7870		1538	ESS				
07	72.3306		1243	ATM	72.3306		1537	ESS	72.3306	7/26	1450	AM
08	70.5976		1238	ATM	70.5975		1541	ESS				
09	71.5194	✓	1239	ATM	71.5191	✓	1542	ESS	71.5192	7/26	1448	AM
30	<del>70.7854</del>	<del>7/26</del>	1459	ATM		7/30		↓	↑			
31	<del>69.6666</del>	<del>7/26</del>	1457	AM					↑			
32	<del>53.5997</del>	<del>7/26</del>	1455	ATM					↑			
32												
34												
35												
36												
37												
38												
39												
40												
41												
42												
43												

Checked by \_\_\_\_\_ Date: \_\_\_\_\_ Time: \_\_\_\_\_

QA Reweigh

Beaker #	WT	Date	Time	By

Balance Room Environmental Conditions

WB	DB	%RH	Date <sup>2015</sup>	Time	By
54	65	47	7/23	1205	AM
55	66	48	7/24	1525	ESS
57	69	47	7/26	1421	AM

Date	1 <sup>st</sup>	2 <sup>nd</sup>	3 <sup>rd</sup>	4 <sup>th</sup>	5 <sup>th</sup>
Post Weighing	0.0000g	0.0000	0.0000		
Scale Check	100.0000g	99.9996	99.9996		

Woodstove Data Sheet #4-2: Initial Beaker Weights ( Tare Weights)

Into Dessicator: Date 6/17 Time 1600 By ATM

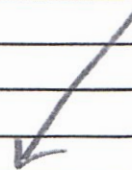
Balance Used: Sartorius

Model: CP224S

SN:24850860

Bkr #	First Wt	Date	Time	By	Second Wt	Date	Time	By	Third Wt	Date	Time	By
20												
21												
22												
23												
24												
25	72.6528	6/23	1315	AM								
26	71.7864	6/20	1443	J	71.7869	6/22	1437	ESS	71.7869	6/23	1321	AM
27												
28	70.5970	6/20	1649	J	70.5972	6/22	1438	ESS				
29												
30												
31												
32												
33	53.1485	6/20	1639	J	53.1490	6/22	1440	ESS	53.1490	6/23	1323	AM
34												
35												
36	53.5737	6/20	1651	J	53.5734	6/22	1442	ESS	53.5743	6/23	1300	AM
37												
38												
39												
40	53.1650	6/23	1317	AM								
41												
42												
43												

Acetone Blank



Checked by \_\_\_\_\_ Date: \_\_\_\_\_ Time: \_\_\_\_\_

QA Reweigh

Beaker #	WT	Date	Time	By

Balance Room Environmental Conditions

WB	DB	%RH	Date	Time	By
56	68	46	6/20	1549	ATM
55	67	45	6/22	1432	ESS
55	68	42	6/23	1213	ATM

Date	1 <sup>st</sup>	2 <sup>nd</sup>	3 <sup>rd</sup>	4 <sup>th</sup>	5 <sup>th</sup>
Post Weighing	0.0000g	0.0000	0.0000	_____	_____
Scale Check	100.0000g	99.9996	99.9996	99.9996	_____

Richard Acetone Blank  
 Lot 271092 50 ml 6/23/15

Woodstove Data Sheet #4-3: Constant Final Weights

Blank  
 Bottle 1 (BD)

Unit HEAT TECH HDP260g  
 Run # EPA 1  
 Date: 7/30/15  
 WST5-Form 9, Pg 1, Rev 10/10

Final Beaker Weights

Beaker	Into	Date	Time	Bv	First	Date	Time	Bv	Second	Date	Time	Bv	Third	Date	Time	Bv
26	71.7863	6/24	1029	ESS	71.7870	6/25	900	ATM	71.7889	6/26	1252	ESS	71.78969	7/1	1331	AM
					71.7869	7/2	1430	J								

Final Filter Weights

Filter #	Into Dessic	Date	Time	By	First	Date	Time	By	Second	Date	Time	By	Third	Date	Time	By

QA Reweigh: Final Weight			
Date	Beaker #	Final Wt	By
Date	Filter #	Final Wt	By

Scale Room Environmental Conditions							Scale Room Environmental Conditions									
Weighing Session	Date	Time	By	WB	DB	%RH	8	9	10	11	12	Comment				
1	6/25	839	ATM	56	69	43	8	9	10	11	12					
2	6/26	1233	ESS	57	69	46	8	9	10	11	12					
3	6/27	2322	AM	58	71	45	8	9	10	11	12					
4	7/2	1354	ATM	58	70	48	8	9	10	11	12					
5							8	9	10	11	12					
6							8	9	10	11	12					
7							8	9	10	11	12					
							✓ Tare wt, 71.7867 6/25 0.0000 6/27 7/2 0.0000 0.0000 71.7869 6/26 0.0000									

MPP  
20  
Bay

Woodstove Data Sheet #4-3: Constant Final Weights

TI  
0-60

Unit HEAT CH  
Run # EPA 1  
Date: 7/30/15  
WST5-Form 9, Pg 1, Rev 10/10

60 ml

Final Beaker Weights

Beaker	Into	Date	Time	Bv	First	Date	Time	Bv	Second	Date	Time	Bv	Third	Date	Time	Bv
27	12.3309	7/31	1143	ATM	72.3347	7/31	1438	ESS	72.3335	8/1	614	AM	72.3334	8/2	1844	AM

Final Filter Weights

Filter #	Into Dessic	Date	Time	By	First	Date	Time	By	Second	Date	Time	By	Third	Date	Time	By
F 711	.6520	7/30	2140	ATM	.6518	7/31	1439	ESS	.6517	8/1	1637	AM				
R 710	.6502	7/30	2140	AM	.6501	7/31	1440	ESS	.6501	8/1	1638	AM				

QA Reweigh: Final Weight

Date	Beaker #	Final Wt	By
Date	Filter #	Final Wt	By

Scale Room Environmental Conditions

Weighing Session	Date	Time	By	WB	DB	%RH					
	2015						8				
							9				
1	7/31	1413	ESS	58	70	47	10				
2	8/1	1547	ATM	54	66	45	11				
3	8/2	1813	ATM	57	69	45	12				
4											
5											
6											
7											

Comment 8/1 8/2  
7/31 0.0000 0.0000  
0.0000 99.9996 99.9996  
99.9995

Woodstove Data Sheet #4-3: Constant Final Weights

T1  
60+

Unit HEAT ECH 26  
Run # EPH 1  
Date: 7/30/15  
WST5-Form 9, Pg 1, Rev 10/10

70 ml

Final Beaker Weights

Beaker	Into	Date	Time	Bv	First	Date	Time	Bv	Second	Date	Time	Bv	Third	Date	Time	Bv
22	71.8522	7/31	1141	ATM	71.8565	7/31	1431	ESS	71.8561	8/1	1615	ATM	71.8561	8/2	1842	ATM

Final Filter Weights

Filter #	Into Dessic	Date	Time	By	First	Date	Time	By	Second	Date	Time	By	Third	Date	Time	By
F 706	.6526	7/30	2210	ATM	.6524	7/31	1435	ESS	.6523	8/1	1628	ATM				
R 707	.6252	7/30	2210	ATM	.6252	7/31	1433	ESS	.6252	8/1	1640	ATM				

QA Reweigh: Final Weight			
Date	Beaker #	Final Wt	By
Date	Filter #	Final Wt	By

Scale Room Environmental Conditions							Scale Room Environmental Conditions			
Weighing Session	2015 Date	Time	By	WB	DB	%RH				
							8			
							9			
1	7/31	1413	ESS	58	70	47	10			
2	8/1	1542	ATM	54	66	45	11			
3	8/2	1813	ATM	57	69	45	12			
4										
5										
6										
7										
							Comment	8/1	8/2	
							7/31	0.0000	0.0000	
							0.0000	99.9996	99.9996	
							99.9995			

Train 1 Woodstove Particulate  
 Catch Processing Sheet  
 Woodstove Data Sheet #5  
 ASTM E 2515/ EPA M5G-1

Unit: HEAT TECH HTP 26 Bay  
 Run: EPA 1 Train 1  
 Date: 7/30/15  
 Technicians: ATM ESS  
 Revised 11/15 - Data Sheet #5

**0-60 Minutes:**

**Filters:**

Filter # (Front): 711 Beaker #: 27 Final Wt.: 72,3334 g  
 Tare Wt.: .6509 g ml 60 Tare Wt.: 73.3306 g  
 Filter # (Rear): 710 Desiccant: Acetone Net Wt.: .0028 g  
 Tare Wt.: .6503 g Beaker Tare Wt. Check: 73,3306 g

0-60 Minute Combined Filter Final Weight: 1,3018 g

0-60 Minute Combined Filter Tare Weight: 1.3012 g

0-60 Minute Combined Net Catch Weight: .0006 g

**60 Minutes Plus:**

Filter # (Front): 706 Beaker #: 22 Final Wt.: 71,8561 g  
 Tare Wt.: .6465 g ml 70 Tare Wt.: 71,8342 g  
 Filter # (Rear): 707 Desiccant: Acetone Net Wt.: .0219 g  
 Tare Wt.: .6423 g Beaker Tare Wt. Check: 71,8340 g

60 Minute Plus Combined Filter Final Weight: 1,2775 g

60 Minute Plus Combined Filter Tare Weight: 1.2888 g

60 Minute Plus Combined Net Catch Weight: -.0113 g

**Acetone Blank Calculation:** Blank Date: 6/23/15 Blank Beaker #: 26 Desiccant: 50 ml Acetone

Final Wt.: 71,7869 g - Tare Wt.: 71,7869 g = Net Catch Wt.: .0000 g

Net Catch Weight: .0000 g / 50 ml Acetone = .0000 g/ml Acetone Blank Residual Value

**0-60 Minute Acetone Residue Value Calculation:**

(.0000 g/ml Acetone)(60 ml Acetone) = .0000 g Residue Value

**60 Minute Plus Acetone Residue Value Calculation:**

(.0000 g/ml Acetone)(70 ml Acetone) = .0000 g Residue Value

**Total Particulate Catch Calculations:**

	<u>0-60 Minute</u>	<u>60 Minute Plus</u>
Combined Filter Net Catch Weight:	<u>.0006</u> g	<u>-.0113</u> g

Acetone Wash Catch Weight:	<u>.0028</u> g	<u>.0219</u> g
----------------------------	----------------	----------------

Less Acetone Residual Value:	<u>-.0000</u> g	<u>-.0000</u> g
------------------------------	-----------------	-----------------

Equals Net Acetone Wash Catch:	<u>.0028</u> g	<u>.0219</u> g
--------------------------------	----------------	----------------

Total Net Catch (Combined Filter + Acetone Catch):	<u>.0034</u> g	<u>.0106</u> g
--	----------------	----------------

	<u>3.4</u> mg	<u>10.6</u> mg
--	---------------	----------------

Total Train 1 Net Catch (0-60 Minute + 60 Minute Plus Catches):		<u>14.0</u> mg
---	--	----------------



Black RoundTOP

T2

METHOD 5G-1 PARTICULATE SAMPLING DATA Rev. 10/09

DATE: 7/30/15 PAGE 1 OF 2 UNIT: HEAT Tech <sup>HTP</sup> <sub>26</sub> <sup>Bray</sup> RUN: EPA1

METER BOX: 511-M METER Y: 0.9685 FILTER #'S: (F) 704 (R) 705

.272/.273 FILTER/ O-RING ID #: \_\_\_\_\_

PRE TEST LEAK CHECK: .001 CFM @ -17.5 IN HG FILTER SIZE: 110 mm

.214/.215 PROBE ID #: \_\_\_\_\_

POST TEST LEAK CHECK: .001 CFM @ -15.5 IN HG PROBE LENGTH 24 IN

541  
944  
9848

TIME		METER READING (m) (ft <sup>3</sup> )	PITOT		TUNNEL TEMP (°F)	METER TEMP (°F)	GAS METER Δh	VAC (in Hg)
CLOCK	ELAPSED		ΔP	Pg				
1040	(00)	355.906	.040		122	64	.75	-0
50	10	361.355	.040		123	66	.75	0
1100	20	366.815	.040		124	70	.75	0
10	30	372.256	.040		124	70.5	.75	0
20	40	377.697	.040		126	72.5	.75	0
30	50	383.238	.040		126	73.5	.75	0
40	(60)	388.783	.040		127	74.5	.75	0
50	70	394.215	.040		124	75.5	.75	0
1200	80	399.647	.040		123	76.5	.75	0
10	90	405.244	.040		123	78	.75	0
20	100	410.774	.040		121	78.5	.75	0
30	110	416.355	.040		120	79	.75	0
40	(120)	421.838	.040		120	80	.75	0
50	130	427.350	.040		121	80	.75	0
1300	140	432.895	.040		121	81	.75	0
10	150	438.397	.040		123	81	.75	0
20	160	443.938	.040		124	81	.75	0
30	170	449.445	.040		124	82	.75	0
40	(180)	454.979	.040		123	81.5	.75	0
50	190	460.507	.040		116	81.5	.75	0

BP

00	28.60	300	28.52
60	28.59	360	28.51
120	28.58		
180	28.54		
240	28.53	AVG. =	28.553

Pre Test Filter  
Check Weighing  
F .6473  
R .6447

End of Test Weight  
F .6560 R .6416  
\_\_\_\_\_  
\_\_\_\_\_  
.6473 .6445

0087



T2

METHOD 5G - 1 PARTICULATE SAMPLING DATA

Rev. 10/09

DATE: 7/30/15 PAGE 2 OF 2 UNIT: HEAT Tech <sup>HJP</sup> <sub>26</sub> <sub>30y</sub> RUN: EPA 1

METER BOX: 511-M METER Y: 0.9685 FILTER #'S: (F) 704 (R) 705

1272/273  
PRE TEST LEAK CHECK: .001 CFM @ -17.5 IN HG FILTER SIZE: 110 mm  
FILTER/ O-RING ID #:     

.214/215  
POST TEST LEAK CHECK: .001 CFM @ -15.5 IN HG PROBE ID #:       
PROBE LENGTH 24 IN

TIME		METER READING (ft <sup>3</sup> )	PITOT		TUNNEL TEMP (°F)	METER TEMP (°F)	GAS METER Δh	VAC (in Hg)
CLOCK	ELAPSED		ΔP	Pg				
1400	200	466.018	.040		112	80.5	.75	0
10	210	471.845	.040		110	80.5	.75	0
20	220	476.064	.040		109	80.5	.75	0
30	230	482.593	.040		108	79.5	.75	0
40	<u>240</u>	488.110	.040		110	79.5	.75	0
50	250	493.641	.040		109	79.5	.75	0
1500	260	499.134	.040		110	79.5	.75	0
10	270	504.645	.040		110	79	.75	0
20	280	510.153	.040		110	79.5	.75	0
30	290	515.668	.040		110	79.5	.75	0
40	<u>300</u>	521.161	.040		111	79.5	.75	0
50	310	526.663	.040		110	79.5	.75	0
1600	320	532.160	.040		110	79.5	.75	0
10	330	537.685	.040		110	80	.75	0
20	340	543.163	.040		111	80	.75	0
30	350	548.653	.040		111	80	.75	0
40	<u>360</u>	554.146	.040		111	80	.75	0
	70							
	80							
	90							

BP

00	<u>28.60</u>	300	<u>28.52</u>
60	<u>28.59</u>	360	<u>28.51</u>
120	<u>28.58</u>		
180	<u>28.54</u>		
240	<u>28.53</u>	AVG. =	<u>28.553</u>

Pre Test Filter  
Check Weighing  
F .6473  
R .6447

End of Test Weight  
F \_\_\_\_\_ R \_\_\_\_\_  
.6473 .6445

Woodstove Data Sheet #4-3: Constant Final Weights

T2

Unit HEAT HTP Co  
 Run # EPA 1 26  
 Date: 7/30/15 Co  
 WST5-Form 9, Pg 1, Rev 10/10

50 ml

Final Beaker Weights

Beaker	Into	Date	Time	Bv	First	Date	Time	Bv	Second	Date	Time	Bv	Third	Date	Time	Bv
29	71.5204	7/30	2130	ATM	71.5204	7/31	1446	ESS	71.5258	8/1	1606	ATM	71.5254	8/2	1845	ATM
					71.5284	8/3	957	ATM								

Final Filter Weights

Filter #	Into Dessic	Date	Time	By	First	Date	Time	By	Second	Date	Time	By	Third	Date	Time	By
F 704	.6560	7/30	1930	ATM	.6563	7/31	1448	ESS	.6561	8/1	1632	ATM				
													1.2976			
R 705	.6416	7/30	1930	ATM	.6416	7/31	1448	ESS	.6415	8/1	1634	ATM				

QA Reweigh: Final Weight			
Date	Beaker #	Final Wt	By
Date	Filter #	Final Wt	By

Scale Room Environmental Conditions							Scale Room Environmental Conditions			
Weighing Session	Date	Time	By	WB	DB	%RH				
	2015						8			
							9			
1	7/31	1413	ESS	58	70	47	10			
2	8/1	1517	ATM	54	66	45	11			
3	8/2	1313	ATM	57	69	45	12			
4	8/3	949	ATM	52	69	45				
5										
6										
7										
							Comment	8/1	8/2	8/3
							7/31	0.0000	0.0000	
							0.0000	99.9996	99.9996	
							99.9995			

Train 2/ Room Blank Woodstove  
Particulate Catch Processing Sheet  
Woodstove Data Sheet #5  
ASTM E 2515/ EPA M5G-1

T2

Unit: HEAT TECH HTP 26 Bay  
Run: EPA 1 Train 2  
Date: 7/30/15  
Technicians: ATM ESS  
Revised 11/15 - Data Sheet #5A

**Filters:**

Filter # (Front): 704 Beaker #: 29 Final Wt.: 71.5254 g  
Tare Wt.: .6473 g ml 50 Tare Wt.: 71.5192 g  
Filter # (Rear): 705 Desiccant: Acetone Net Wt.: .0062 g  
Tare Wt.: .6445 g Beaker Tare Wt., Check: 71.5191 g  
Combined Filter Final Weight: 1.2976 g  
Combined Filter Tare Weight: 1.2918 g  
Combined Net Catch Weight: .0058 g

**Acetone Blank Calculation:** Blank Date: 6/23/15 Blank Beaker #: 26 Desiccant: 50 ml Acetone  
Final Wt.: 71.7869 g - Tare Wt.: 71.7869 g = Net Catch Wt.: .0000 g  
Net Catch Weight: .0000 g / 50 ml Acetone = .0000 g/ml Acetone Blank Residual Value

**Acetone Residue Value Calculation:**

(.0000 g/ml Acetone)(50 ml Acetone) = .0000 g Residue Value

**Total Particulate Catch Calculations:**

Combined Filter Net Catch Weight: .0058 g  
Acetone Wash Catch Weight: .0062 g  
Less Acetone Residual Value: -.0000 g  
Equals Net Acetone Wash Catch: .0062 g  
Total Net Catch (Combined Filter + Acetone Catch): .0120 g  
12.0 mg

ROOM BLANK SAMPLE FLOW PROPORTIONALITY  
5/1/2008

## MYREN CONSULTING CERTIFICATION TEST DATA

	File Name:	EPA 1 T 3	RUN TIME (min)	GAS	INTERVAL	SAMPLING	INTERVAL	DRY GAS	DRY GAS	DRY GAS
				METER	SAMPLE	RATE	SAMPLING	METER	METER	TEMP
				READING (Cu, Ft.)	VOLUME (Cu. Ft.)	% DIFFERENCE	RATE (cfm)	READING (M3)	$\Delta_h$	F
	Manufacturer:	HEAT TECH								
	Model Number:	HTP 26 BAY								
	Lab Name:	MYREN								
	Test Date:	7.30.15	0	4917.2142				139.24000	0.115	66.00
	Run Number:	EPA 1 T 3	10	4922.5573	5.3431	0.0000	0.53431	139.39130	0.115	69.5
Initial Meter Reading (cf):		4917.2142	20	4927.8969	5.3396	-0.0661	0.53396	139.54250	0.115	72.0
Final Meter Reading (cf):		5108.6762	30	4933.2259	5.3290	-0.2644	0.53290	139.69340	0.115	74.0
Test Time (Min):		360.0	40	4938.5584	5.3325	-0.1983	0.53325	139.84440	0.115	75.0
Average Sample Rate (cfm):		0.532	50	4943.8874	5.3290	-0.2644	0.53290	139.99530	0.115	77.5
Preliminary Results:			60	4949.2129	5.3255	-0.3305	0.53255	140.14610	0.115	77.5
Final results:		X	70	4954.5418	5.3290	-0.2644	0.53290	140.29700	0.115	78.5
BP:		28.553	80	4959.8143	5.2725	-1.3219	0.52725	140.44630	0.115	79.5
Average $\Delta_h$ :		0.115	90	4965.1610	5.3466	0.0661	0.53466	140.59770	0.115	81.0
Dry Gas Meter Temp (F):		75.7	100	4970.4793	5.3184	-0.4627	0.53184	140.74830	0.115	81.0
Sample Volume (dscf):		175.270	110	4975.8295	5.3502	0.1322	0.53502	140.8998	0.115	81.5
Dry Gas Meter Y:		0.9734	120	4981.3139	5.4844	2.6438	0.54844	141.0551	0.115	82.0
Room Blank Catch (mg):		1.100	130	4986.4663	5.1524	-3.5691	0.51524	141.2010	0.115	82.5
Room Blank mg/dscf		0.006276	140	4991.7953	5.3290	-0.2644	0.53290	141.3519	0.115	83.0
Avg. Sampling Rate $\Delta_{s(a)}$ :		-0.463	150	4997.1349	5.3396	-0.0661	0.53396	141.5031	0.115	83.5
			160	5002.4638	5.3290	-0.2644	0.53290	141.6540	0.115	83.5
			170	5007.7893	5.3255	-0.3305	0.53255	141.8048	0.115	79.0
			180	5012.7475	4.9582	-7.2042	0.49582	141.9452	0.115	76.5
			190	5018.4119	5.6645	6.0145	0.56645	142.1056	0.115	75.0
			200	5023.7480	5.3360	-0.1322	0.53360	142.2567	0.115	74.0
			210	5029.0593	5.3113	-0.5948	0.53113	142.4071	0.115	73.5
			220	5034.4095	5.3502	0.1322	0.53502	142.5586	0.115	73.5
			230	5039.7032	5.2937	-0.9253	0.52937	142.7085	0.115	73.0
			240	5045.0110	5.3078	-0.6609	0.53078	142.8588	0.115	72.5
			250	5050.3046	5.2937	-0.9253	0.52937	143.0087	0.115	73.0
			260	5055.6089	5.3043	-0.7270	0.53043	143.1589	0.115	73.0
			270	5060.9237	5.3149	-0.5288	0.53149	143.3094	0.115	73.0
			280	5066.2351	5.3113	-0.5948	0.53113	143.4598	0.115	73.0
			290	5071.5252	5.2901	-0.9914	0.52901	143.6096	0.115	73.0
			300	5076.8365	5.3113	-0.5948	0.53113	143.7600	0.115	73.0
			310	5082.1620	5.3255	-0.3305	0.53255	143.9108	0.115	73.0
			320	5087.4592	5.2972	-0.8592	0.52972	144.0608	0.115	73.0
			330	5092.7599	5.3007	-0.7931	0.53007	144.2109	0.115	73.0
			340	5098.0818	5.3219	-0.3966	0.53219	144.3616	0.115	73.0
			350	5103.3967	5.3149	-0.5288	0.53149	144.5121	0.115	74.0
			360	5108.6762	5.2795	-1.1897	0.52795	144.6616	0.115	73.5
			370							
			380							

NOTE: THE SAMPLED VOLUME  
FOR EACH SAMPLING INTERVAL  
MUST BE WITHIN 20% OF THE  
SAMPLE VOLUME FOR THE  
FIRST SAMPLING INTERVAL  
SEE ASTM E2515 SECTION 9.8.1

RB

METHOD 5G-1

PARTICULATE SAMPLING DATA

Rev. 10/09

DATE: 7/30/15 PAGE 1 OF 2 UNIT: Heat Tech <sup>HTP</sup> Bay <sup>26</sup> RUN: EPA 1

METER BOX: RBT METER Y: 0.9734 FILTER #'S: (F) 703 (R) ---  
 ,2290/.2290,0000 CAN  
 PRE TEST LEAK CHECK: .000 CFM @ -180 IN HG FILTER/ O-RING ID #: ---  
 ,6628/.6628  
 POST TEST LEAK CHECK: .000 CFM @ -10.25 IN HG FILTER SIZE: 110 mm  
 PROBE ID #: ---  
 PROBE LENGTH N/A IN

TIME		METER READING (ft <sup>3</sup> )	PITOT		TUNNEL TEMP (°F)	METER TEMP (°F)	GAS METER Δh	VAC (in Hg)
CLOCK	ELAPSED		ΔP	Pg				
1040	(00)	139,2400				66	.115	-1.50
50	10	139,3913				69.5	.115	-1.50
1100	20	139,5425				72	.115	-1.50
10	30	139,6934				74	.115	-1.50
20	40	139,8444				75	.115	-1.50
30	50	139,9953				77.5	.115	-1.50
40	(60)	140,1461				77.5	.115	-1.50
50	70	140,2970				78.5	.115	-1.50
1200	80	140,4463				79.5	.115	-1.50
10	90	140,5977				81	.115	-1.50
20	100	140,7483				81	.115	-1.50
30	110	140,9989				81.5	.115	-1.50
40	(120)	141,0551				82	.115	-1.50
50	130	141,2010				82.5	.115	-1.50
1300	140	141,3519				83	.115	-1.50
10	150	141,5031				83.5	.115	-1.50
20	160	141,6540				83.5	.115	-1.50
30	170	141,8048				79	.115	-1.50
40	(180)	141,9452				76.5	.115	-1.50
50	190	142,1056				75	.	-1.50

BP  
 00 28.60 300 28.52  
 60 28.59 360 28.51  
 120 28.58 \_\_\_\_\_  
 180 28.54 \_\_\_\_\_  
 240 28.53 AVG. = 28.553

Pre Test Filter  
 Check Weighing  
 F .6456  
 R \_\_\_\_\_

End of Test Weight  
 F .6446 R \_\_\_\_\_  
 \_\_\_\_\_  
 .6455  
 -0.9

RB

METHOD 5G -1 PARTICULATE SAMPLING DATA Rev. 10/09

DATE: 7/30/5 PAGE 2 OF 2 UNIT: HEAT Tech HTP 26 Day RUN: EPA 1

METER BOX: RBT METER Y: 0.9734 FILTER #'S: (F) 703 (R) —

PRE TEST LEAK CHECK: 1.000 CFM @ -18.0 IN HG FILTER/ O-RING ID #: —

POST TEST LEAK CHECK: 0.000 CFM @ -10.25 IN HG FILTER SIZE: 110 mm PROBE ID #: —

TIME		METER READING (m³)	PITOT		TUNNEL TEMP (°F)	METER TEMP (°F)	GAS METER Δh	VAC (in Hg)
CLOCK	ELAPSED		ΔP	Pg				
1400	200	142.2567				74	.115	-1.50
10	210	142.4071				73.5	.115	-1.50
20	220	142.5586				73.5	.115	-1.50
30	230	142.7085				73	.115	-1.50
40	(240)	142.8588				72.5	.115	-1.50
50	250	143.0087				73	.115	-1.50
1500	260	143.1589				73	.115	-1.50
10	270	143.3094				73	.115	-1.50
20	280	143.4598				73	.115	-1.50
30	290	143.6096				73	.115	-1.50
40	(300)	143.7600				73	.115	-1.50
50	310	143.9108				73	.115	-1.50
1600	320	144.0608				73	.115	-1.50
10	330	144.2109				73	.115	-1.50
20	340	144.3616				73	.115	-1.50
30	350	144.5121				74	.115	-1.50
40	(360)	144.6616				73.5	.115	-1.50
	70							
	80							
	90							

BP

00	28.60	300	28.52
60	28.59	360	28.51
120	28.58		
180	28.54		
240	28.53		
AVG. =		28.553	

Pre Test Filter  
Check Weighing  
F .6455  
R \_\_\_\_\_

End of Test Weight  
F \_\_\_\_\_ R \_\_\_\_\_  
\_\_\_\_\_ \_\_\_\_\_  
.6455

HTW  
26

RB

Unit HEAT J CH BOY  
Run # EPA 1  
Date: 7/30/15

Woodstove Data Sheet #4-3: Constant Final Weights

40 ml

WST5-Form 9, Pg 1, Rev 10/10

Final Beaker Weights

Beaker	Into	Date	Time	Bv	First	Date	Time	Bv	Second	Date	Time	Bv	Third	Date	Time	Bv
23	70.7370	7/30	2133	ATM	70.7412	7/31	1442	ESS	70.7406	8/1	1613	AM	70.7407	8/2	1843	AM

Final Filter Weights

Filter #	Into Dessic	Date	Time	By	First	Date	Time	By	Second	Date	Time	By	Third	Date	Time	By
F 703	.6446	7/30	1930	ATM	.6446	7/31	1443	ESS	.6444	8/1	1635	AM				

QA Reweigh: Final Weight			
Date	Beaker #	Final Wt	By
Date	Filter #	Final Wt	By

Scale Room Environmental Conditions							Scale Room Environmental Conditions						
Weighing Session	2015 Date	Time	By	WB	DB	%RH							
							8						
							9						
1	7/31	1413	ESS	58	70	47	10						
2	8/1	1547	ATM	54	66	45	11						
3	8/2	1813	ATM	57	69	45	12						
4													
5													
6													
7													
							Comment	8/1	8/2				
							7/31	0.0000	0.0000				
							0.0000	99.9996	99.9996				
							99.9995						

Train 2/ Room Blank Woodstove  
Particulate Catch Processing Sheet  
Woodstove Data Sheet #5  
ASTM E 2515/ EPA M5G-1

RB  
13

Unit: HEAT TECH HTP 26 Bay  
Run: EPA 1 Train 3  
Date: 7/30/15  
Technicians: ATM ESS  
Revised 11/15 - Data Sheet #5A

**Filters:**

Filter # (Front): 703 ✓ Beaker #: 23 Final Wt.: 70.7407 g ✓  
Tare Wt.: .6455 g ✓ ml 40 Tare Wt.: 70.7385 g ✓  
Filter # (Rear): — Desiccant: Acetone Net Wt.: .0022 g ✓  
Tare Wt.: — g Beaker Tare Wt., Check: 70.7385 g  
Combined Filter Final Weight: .6444 g ✓  
Combined Filter Tare Weight: .6455 g ✓  
Combined Net Catch Weight: -.0011 g

**Acetone Blank Calculation:** Blank Date: 6/23/15 Blank Beaker #: 26 Desiccant: 50 ml Acetone  
Final Wt.: 71.7869 g - Tare Wt.: 71.7869 g = Net Catch Wt.: .0000 g  
Net Catch Weight: .0000 g / 50 ml Acetone = .0000 g/ml Acetone Blank Residual Value

**Acetone Residue Value Calculation:**

(.0000 g/ml Acetone)(40 ml Acetone) = .0000 g Residue Value

**Total Particulate Catch Calculations:**

Combined Filter Net Catch Weight: -.0011 g  
Acetone Wash Catch Weight: .0022 g  
Less Acetone Residual Value: -.0000 g  
Equals Net Acetone Wash Catch: .0022 g  
Total Net Catch (Combined Filter + Acetone Catch): .0011 g  
1.1 mg



Woodstove Data Sheet 4-4 Scale QC Record Sheet

Scale 2

Scale: Sartorius

Model: CPA 2245

SN: 24850860

Rev: 5/10

From: 5/8/15

Through: 7/5/15

100+20+10+5

50 2015

Level	Recalibrated	135g Weights	100g Weight	10g Weight	1.0 g Weight	100mg Weight	50 mg Weight	Date	Time	Tech	BP	Wet Bulb	Dry Bulb	% RH	Line Vol/B
Yes	No	134.9997	99.9996	10.0000	1.0000	0.1000	0.0501	5/8/15	1311	ATM	28.48	55	67	45	119
Yes	Yes	134.9995	99.9994	10.0000	0.9999			5/29/15	936	ATM	28.56				119
Yes	No	134.9996	99.9995	9.9999	0.9999	0.1000	0.0501	5/30/15	905	ATM	28.57	65	78	49	118
Yes	No	134.9994	99.9994	10.0000	1.0000	0.1000	0.0501	6/2/15	843	ATM	28.40	62	75	47	119
Yes	No	134.9994	99.9994	9.9999	1.0000	0.1000	0.0502	6/3/15	921	ESS	28.49	57	69	46	118
Yes	No	134.9995	99.9994	9.9999	0.9999	0.0999	0.0500	6/4/15	824	ATM	28.52	59	71	48	116
Yes	No	134.9997	99.9996	9.9999	0.9999	0.0999	0.0500	6/6/15	1028	ATM	28.61	60	72	49	118
Yes	No	134.9996	99.9995	9.9999	0.9999	0.1000	0.0500	6/8/15	1110	ATM	28.42	59	76	40	117
Yes	No	134.9997	99.9996	9.9999	1.0000	0.1000	0.0501	6/10/15	1437	ATM	28.32	56	68	47	116
Yes	No	134.9996	99.9996	9.9999	1.0000	0.1000	0.0500	6/11/15	2245	ATM	28.30	56	68	47	117
Yes	No	134.9996	99.9995	9.9999	1.0000	0.1000	0.0501	6/12/15	2138	ATM	28.50	55	67	46	120
Yes	No	134.9995	99.9995	10.0000	1.0000	0.1000	0.0501	6/13/15	833	ATM	28.52	54	65	48	119
Yes	No	134.9995	99.9994	10.0000	1.0000	0.1000	0.0501	6/14/15	15:14	ATM	28.46	53	64	47	118
Yes	No	134.9996	99.9996	10.0000	1.0000	0.1000	0.0500	6/17/15	13:39	ATM	28.38	57	69	46	116
Yes	No	134.9996	99.9995	10.0000	1.0000	0.0999	0.0501	6/18/15	17:30	ATM	28.42	56	68	46	119
Yes	No	134.9996	99.9995	9.9999	1.0000	0.1000	0.0501	6/20/15	1547	ATM	28.40	56	68	46	119
Yes	No	134.9997	99.9996	9.9999	1.0000	0.1001	0.0501	6/22/15	1432	ESS	28.46	55	67	45	118
Yes	No	134.9996	99.9995	9.9999	0.9999	0.1000	0.0501	6/23/15	12:18	ATM	28.49	55	68	42	117
Yes	No	134.9996	99.9996	9.9999	1.0000	0.1000	0.0501	6/24/15	1434	ESS	28.49	58	70	48	119
Yes	No	134.9996	99.9995	9.9999	1.0000	0.1000	0.0501	6/25	839	ATM	28.60	56	69	43	117
Yes	No	134.9995	99.9996	9.9999	1.0000	0.1001	0.0501	6/26/15	1233	ESS	28.51	57	69	46	114
Yes	No	134.9995	99.9995	10.0000	1.0000	0.1000	0.0501	6/27/15	2222	ATM	28.405	58	71	45	120
Yes	No	134.9995	99.9995	9.9999	1.0000	0.1000	0.0502	6/30/15	1433	ESS	28.47	59	71	48	119
Yes	No	134.9997	99.9996	10.0000	1.0000	0.1000	0.0500	7/1/15	1309	ATM	28.435	57	70	44	116
Yes	No	134.9995	99.9995	9.9999	0.9999	0.0999	0.0500	7/2/15	1354	ATM	28.48	58	70	48	116
Yes	No	134.9996	99.9995	9.9999	1.0000	0.1000	0.0501	7/3/15	1912	ATM	28.38	58	70	48	119

Woodstove Data Sheet 4-4 Scale QC Record Sheet  
Scale 2

From: 7/17/15  
Through: 9/10/15

Scale: Sartorius  
Model: CPA 2245  
SN: 24850860  
Rev: 5/10

Level	Recali- brated	100g Weight	10g Weight	1g Weight	100mg Weight	10mg Weight	DATE	TIME	TECH	BP	LINE VOLTS	WET BULB	DRY BULB	% RH
Yes	No	99.9994	10.0000	1.0000	0.1000	0.0100	7/17/15	1900	ATM	28.40	119	55	67	45
Yes	No	99.9995	10.0000	1.0000	0.1000	0.0100	7/18/15	1957	ATM	28.37	120	57	70	44
Yes	No	99.9994	10.0000	1.0000	0.0999	0.0100	7/19/15	1413	ATM	28.42	121	57	70	44
Yes	NO	99.9994	9.9999	1.0000	0.1000	0.0101	7/20/15	1022	ESS	28.40	118	57	69	46
Yes	No	99.9996	10.0000	1.0000	0.1000	0.0100	7/21/15	1358	ATM	28.28	116	55	66	48
Yes	NO	99.9995	9.9999	0.9999	0.1000	0.0100	7/22/15	1606	ESS	28.27	116	54	65	47
Yes	No	99.9995	9.9999	1.0000	0.1000	0.0100	7/23/15	1205	ATM	28.33	118	54	65	47
Yes	NO	99.9994	10.0000	0.9999	0.1001	0.0101	7/24/15	1525	ESS	28.38	118	55	66	48
Yes	No	99.9996	10.0000	1.0000	0.0999	0.0100	7/26/15	1421	ATM	28.42	118	57	69	47
Yes	No	99.9996	9.9999	0.9999	0.1000	0.0100	7/28/15	1603	ATM	28.58	118	56	67	47
Yes	NO	99.9995	10.0000	1.0000	0.1000	0.0101	7/29/15	1325	ESS	28.57	117	56	68	46
Yes	No	99.9994	9.9999	1.0000	0.1000	0.0100	7/30/15	949	ATM	28.60	119	55	66	48
Yes	NO	99.9995	9.9999	1.0000	0.1000	0.0100	7/30/15	2105	ATM	28.48	118	56	67	48
Yes		99.9995	9.9999	0.9999	0.1000	0.0100	7/31/15	1413	ESS	28.45	116	58	70	48
Yes	No	99.9995	9.9999	1.0000	0.1000	0.0101	8/1/15	1547	ATM	28.33	118	54	66	45
Yes	No	99.9995	9.9999	0.9999	0.0999	0.0100	8/2/15	1813	ATM	28.27	120	57	69	45
Yes	No	99.9995	9.9999	1.0000	0.1000	0.0100	8/3/15	949	ATM	28.30	120	57	69	45
Yes	NO	99.9994	9.9999	1.0000	0.1000	0.0101	8/12/15	1038	ESS	28.43	120	57	69	45
Yes	No	99.9994	9.9999	0.9999	0.1000	0.0100	8/18/15	1530	ATM	28.42	119	58	70	48
Yes	No	99.9996	9.9999	0.9999	0.0999	0.0100	8/19/15	0636	ATM	28.42	119	57	69	45
Yes	No	99.9995	10.0000	1.0000	0.1000	0.0100	8/19/15	2244	ATM	28.20	119	58	70	48
Yes	NO	99.9995	10.0000	0.9999	0.1000	0.0101	8/20/15	1610	ESS	28.20	119	58	70	48
Yes	NO	99.9995	10.0000	1.0000	0.0999	0.0100	8/26/15	1425	ESS	28.40	118	57	70	43
Yes	No	99.9994	10.0000	0.9999	0.1000	0.0100	8/28/15	1200	ESS	28.48	119	58	70	48
Yes	NO	99.9995	9.9999	1.0000	0.1000	0.0100	8/31/15	1547	ESS	28.40	118	57	69	47
Yes	NO	99.9995	10.0000	1.0000	0.1000	0.0100	9/10/15	1047	ATM	28.50	117	56	68	46

**Miscellaneous Test Data  
Woodstove Data Sheet #8**

Unit: HEAT TECH 26  
 Run # EPA 1  
 Date: 7/1/15  
 Technician: ATM ESS  
 WST6-Form1, Rev 6/11

Useable Firebox Dimensions: See QC Section Useable Volume: N/A ft<sup>3</sup>  
 Dilution Tunnel Draft (If Applicable): Start: .000 Stop: .000 Avg: .000 in. H<sub>2</sub>O  
 Test Chamber Air Velocity: Start: 70, 45 Stop: 75, 410 Avg: 5 ft./m.  
 Wet Bulb/ Start: WB: 59 °F DB: 72 °F % Amb Moisture: 1.25 %RH: 45  
 Dry Bulb Stop: WB: 60 °F DB: 78 °F % Amb Moisture: 1.10 %RH: 39  
 $\bar{X}$  Ambient Moisture(%Vol.) = 1.175%  $\bar{X}$  Relative Humidity (%RH) = 42.0%  
 Empty Stove Wt: 185.7 lbs.  
 Empty Stove Wt with Stack (inc oil seal) Wet: N/A lbs. Dry: N/A lbs.  
 Empty Stove Wt with Stack and Ash Ash: — lbs. Total: — lbs.  
 Kindling Wt. Paper: N/A lbs. Wood: N/A lbs. Total: — lbs.  
 Pre Burn Fuel Wt. 4.5 + 4.5 Total: 9.0 lbs.  
 Total Kindling and Pre Burn Fuel Wt. 9.0 lbs.  
 Coal Bed Wt.: Range( N/A - N/A ) lbs. Actual: — lbs.

Allowable Amount of Charcoal That Can Be Removed:  
 Coal Bed Wt. Range  $\left( \begin{array}{c} \text{Upper Wt.} \\ \text{Lower Wt.} \end{array} \right) / 2 \cdot 25 =$  N/A lbs.  
 Test Fuel Wt.: Ideal N/A lbs. Range: N/A lbs. Actual: 14.0 lbs.  
 Test Fuel Size (pcs.) (.75 x 1.5 x 5" Spacers): N/A Pcs. N/A lbs.  
 2 x 4's x N/A " N/A Pcs. N/A lbs. N/A %  
 4 x 4's x N/A " N/A Pcs. N/A lbs. N/A %

Est. Dry Burn Rate(Kg/Hr.)  $\frac{14.0 - (14.0 \times .057)}{2.2046} \times \frac{60}{360} =$  .9981 Dry Burn Rate (Kg/Hr)  
 Est EPA Heat Output (HO<sub>E</sub>)(Avg BTU's/Hr)(19,140) X 78 x .9981 = 14,901  
 100 EPA Heat Output (HO<sub>E</sub>)BTU's/Hr

## STOVE OPERATION

The after cleaning out the stove and stack before the start of the certification, the hopper was filled with pellets and stove was started with the controls set at "Manual". After the stove went thru its "Start" cycle (approximately 10 minutes), the controls were turned to "HIGH" and it ran for about 1 hour as we finished preparing for the test. Then Preburn was started, which lasted another hour. After 60 minutes of preburn, the stove's controls were left on "High" for the first hour of the test. At 60 minutes the stove's controls were set to "Medium". At 180 minutes the stove's controls was turned down to "Low".

Wood Density Determination  
Woodstove Test Data Sheet #11

Unit: HEAT TECH HTP 26 Bag  
Run#: EPA 1  
Date: 7/30/15  
Technician: ATM ESS

Rev 5/10

Wood Piece: Nominal Dimensions: X X  
Depth (D): \_\_\_\_\_ cm  
Width (W): \_\_\_\_\_ cm  
Length(L): \_\_\_\_\_ cm  
\_\_\_\_\_ cm Length  $\bar{X}$  = \_\_\_\_\_ cm  
\_\_\_\_\_ cm  
\_\_\_\_\_ cm Volume: \_\_\_\_\_ cm<sup>3</sup>  
(D x W x L)

Room Temperature: \_\_\_\_\_ °F Correction Factor: \_\_\_\_\_

Meter Readings Corrected for temperature: Yes \_\_\_\_\_ No \_\_\_\_\_

Note: Record Moisture Meter readings to the nearest 0.5% or 0.1%

	Uncor	Cor	Avg % Moisture (Dry) _____ %
Top:		%	
Bottom:		%	Avg % Moisture (Wet) _____ %
Side:		%	Scale: Leveled In _____ Out _____
$\bar{X}$ :		%	Zeroed: In _____ Out _____

Wet Weight: \_\_\_\_\_ g Dry Weight: \_\_\_\_\_ g

% Moisture Dried Basis: \_\_\_\_\_ %

$$([1 - (\text{Dry Wt}/\text{Wet Wt})] \times 100)$$

$$\text{Density} = \frac{\text{_____ g}}{\text{_____ cm}^3} = \text{_____ g/cm}^3$$

(dry wt) (volume)

Into Dryer 7/30/15 1605 216 °F

Out of Dryer 8/6/15 942 218 °F

(Minimum Time in Dryer: 24 hrs.)

NO # (#63)

Pellet Fuel Moisture Content Determination

Tare Beaker Wt. 70.6254 g

Pellet Name: BEAR Mountain

Pellet Manufacturer: BEAR Mountain

Pellet Grade: Premium Plus

Wet Wt: 165.0159 g - 70.6254 g = 94.3905 g

Net Wet Wt.

Gross Wet Wt. Tare Beaker Wt.

Dry Wt: 159.6379 g - 70.6254 g = 89.0125 g

Net Dry Wt.

Gross Dry Wt. Tare Beaker Wt.

% Moisture Wet Basis: 5.6976 % = 5.70%

$$[1 - (\text{Net Dry Wt.}/\text{Net Wet Wt.})] \times 100$$

**ASTM 2779 EQN 1: Pounds of Dry Fuel Burnt, db. (Revised)**

$$M_{Bdb} = ((M_{Swb} - M_{Ewb}) - ((M_{Swb} - M_{Ewb})(FM_{wb}/100)))$$

$FM_{wb}$  = average fuel moisture of test fuel, % wet basis.

$M_{Sdb}$  = Weight of the test fuel in the hopper at the start of the test run, wet basis, kg (lb).

$M_{Ewb}$  = Weight of the test fuel in the hopper at the start of the test run, wet basis, kg (lb), and

$M_{Bdb}$  = Weight of the fuel burnt during the test run, dry basis, kg(lb).

2.2046 = lbs/ kg

$$M_{Bdb} = ((270.1 - 256.1) - ((270.1 - 256.1)(5.700/100))) = 13.202 \text{ lbs.} / 2.2046 = 5.9884 \text{ kg}$$

**ASTM 2779 EQN 2: Pounds of Dry Fuel Burnt During a Test Segment (S<sub>i</sub>), db. (Revised)**

$$M_{Bdb} = ((M_{SSiwb} - M_{ESiwb}) - ((M_{SSiwb} - M_{ESiwb})FM_{wb}))$$

$FM_{wb}$  = average fuel moisture of test fuel, % wet basis.

$M_{SSidb}$  = Weight of the test fuel in the hopper at the start of the test run, wet basis, kg (lb).

$M_{ESiwb}$  = Weight of the test fuel in the hopper at the start of the test run, wet basis, kg (lb), and

$M_{BSidb}$  = Weight of the fuel burnt during the test run, dry basis, kg(lb).

2.2046 = lbs/ kg

$$M_{BSidb} = ((270.1 - 265.9) - ((270.1 - 265.9)(5.70/100))) = 3.9606 \text{ lbs.} / 2.2046 = 1.7965 \text{ kg}$$

**ASTM 2779 EQN 3: Average Dry Burn Rate (DBR)**

$$BR(DBR) = (60 (M_{Bdb}))/\theta = (60(5.9884)) / 360 = 0.9981 \text{ kg/h}$$

BR (DBR) = average dry burn rate over the full integrated test run, kg/h (lb/h), and

$\theta$  = total length of the full integrated test run, min.

**ASTM 2779 EQN 4: Average Dry Burn Rate (DBR) During a Test Run Segment (S<sub>i</sub>)**

$$BR(DBR) = 60 (M_{BSidb})/\theta = (60(1.7965)) / 60 = 1.7965 \text{ kg/h}$$

BR (DBR) = average dry burn rate over the test run segment  $i$ , kg/h (lb/h), and

$\theta$  = total length of test run segment  $i$ , min.



















Pre and Post Test Zero/Span Check

Woodstove Data Sheet # 15-1

Site: Myren Consulting, Colville, WA Date: 7/1/12 Analyte: CO<sub>2</sub>

Source: Hent Tech HTP26 Day Run #: EPA 1

Zero Cyl #: 1TM0803/11 Conc. 00.0 % CO<sub>2</sub> Cyl Press: 220 psi

Certified By: Oxarc Date: 6/11/12

Span Cyl #: EB-0019810 Conc. 12.4 % CO<sub>2</sub> Cyl Press: 220 psi

Certified By: Liquid Technology Corp. Date: 4/25/12

Analyzer: Make: Horiba Model: PIR-2000 SN: 607024

Range: 0 - 25.0% CO<sub>2</sub> Analyzer Output: 0 - 1.0 v.

Flow: 1.5 SCFH Measured By: Rotameter: X Flowmeter: \_\_\_\_\_

EPA Span Values = 25.0% CO<sub>2</sub>

EPA Control Limits = ± 2.5% of 25.0% CO<sub>2</sub> = ± 0.625% CO<sub>2</sub>

Pre Run Audit: By: A.P. Myren Time: 955 Temp: 82 °F

Audit Results								
Point #	Expected Response			Actual Response			± Conc. Difference	Δ %
	Meter	DVM	%	Meter	DVM	%		
Zero	00.0	00.0	00.0	00.0	000	0.03162	+0.03162	+0.13
Span	49.6	49.6	12.4	49.0	49.6	12.4280	+0.0280	+0.23

Comments:

Post Run Audit: By: [Signature] Time: 1723 Temp: 77 °F

Audit Results								
Point #	Expected Response			Actual Response			± Conc. Difference	Δ %
	Meter	DVM	%	Meter	DVM	%		
Zero	00.0	00.0	00.0	00.0	002	0.08160	+0.08160	+0.33
Span	49.6	49.6	12.4	50.0	507	12.70292	+0.30292	+2.44

Comments:

±CONC. Difference = Act % - Exp (Std) %

Zero % Difference (Δ%) =  $\frac{\text{Act \% (ppm)} - \text{Exp \% (ppm)}}{\text{Full Scale Value}} \times 100$

Span % Difference (Δ%) =  $\frac{\text{Act \% (ppm)} - \text{Exp \% (ppm)}}{\text{Exp \% (ppm)}} \times 100$

Pre and Post Test Zero/Span Check

Woodstove Data Sheet # 15-3

Site: Myren Consulting, Colville, WA Date: 7/1/12 Analyte: CO

Source: HEAT Tech HTP 26 Day Run #: EPA 1

Zero Cyl #: 1 TM 9903/11 Conc. 00.0 % CO

Cyl Press: 270 psi

Certified By: Oxarc

Date: 6/11/12

Span Cyl #: EB -0019810 Conc. 2.57 % CO

Cyl Press: 220 psi

Certified By: Liquid Technology Corp

Date: 4/25/12

Analyzer: Make: Horiba Model: Mexa 311 GE SN: GE-30075

Range: 0 - 10.0% CO (0 - 5.0% CO) Analyzer Output: 0 - 1.0 v.

Flow: 1.5 SCFH Measured By: Rotameter: X Flowmeter: \_\_\_\_\_

EPA Span Values= 5.0% CO

EPA Control Limits = ±2.5% of 5.0% CO = ±0.125% CO

Pre Run Audit: By: AT Myren Time: 955 Temp: 82 °F

Point #	Expected Response			Actual Response			± Conc. Difference	Δ %
	Meter	DVM	%	Meter	DVM	%		
Zero	00.0	.000	00.0	—	.000	.02832	+0.02832	+0.57
Span	—	.257	2.57	—	.257	2.54547	-0.02453	-0.95

Comments: meter on front panel is broken

Post Run Audit: By: ES Time: 1723 Temp: 77 °F

Point #	Expected Response			Actual Response			± Conc. Difference	Δ %
	Meter	DVM	%	Meter	DVM	%		
Zero	00.0	.000	00.0	—	.000	.02832	+0.02832	+0.57
Span	—	.257	2.57	—	.271	2.6826	+0.1126	+4.38

Comments:

±CONC. Difference= Act % - Exp (Std) %

Zero % Difference(Δ%) =  $\frac{\text{Act \% (ppm)} - \text{Exp \% (ppm)}}{\text{Full Scale Value}} \times 100$

Span % Difference (Δ%) =  $\frac{\text{Act \% (ppm)} - \text{Exp \% (ppm)}}{\text{Exp \% (ppm)}} \times 100$



**FIREPLACE DATA SHEET #10**  
**Quality Checks (Revised 1/10)**

Unit: HEAT Tech HTP 26 City  
 Run #: EPT 1  
 Date: 7/30/15

Ambient Blank Probe Inlet Location 37 1/4 " from the bottom of the hood (Spec =  $\leq 6.6'$ ) and 32 1/2 " from the chimney centerline (Spec =  $\leq 3.3'$ ).

Dilution Tunnel Draft: Start: .000 Stop: .000 Avg.: .000 "H<sub>2</sub>O

Test Chamber Air Velocity: Start: >0, <5 Stop: >5, <10 Avg.: 5 ft/min

Test Chamber Ambient Moisture (AM) / Relative Humidity (%RH)

Start: Wet Bulb 59 Dry Bulb 72 =%RH 45, %AM (%By Vol) 1.25  
 Stop: Wet Bulb 60 Dry Bulb 78 =%RH 39, %AM (% by Vol) 1.10  
 Avg. %RH 42.0, %AM (% by Vol) 1.175

Minimum Tunnel Flow For 100% Smoke Capture: Pitot Reading (Ap): 0.10  
 ~ Tunnel Flow: 71 dscfm

Fireplace Back Wall Temperature Immediately Prior to Test Start: N/A °F

Scale Check: Pre (Wt., #): 279.7 - 274.7 = 5.0 / 5.0 lbs. OK/598  
 Post (Wt., #): 260.6 - 255.6 = 5.0 / 5.0 lbs. OK/598

Scale Zero Drift: Pre: — lbs. Post: — lbs. Drift: — lbs.

(Note: To avoid having the heat from the bottom of the unit affect the load cells, the fireplace is set on a large steel plate which is supported by 4-2x4's. There also is a piece of insulation directly over the electronics in the scale deck. When the steel plate and fireplace were lifted off the scale deck, the 2X4's and insulation are still on the deck. Thus, the weight shown rather than zero.)

Combustion Gas (CO<sub>2</sub>, O<sub>2</sub> & CO) Train Leak Checks: Pre: OK ✓ 598 Post: OK ✓ 500  
 Draft (Static [P<sub>g</sub>]) Gauge Level and Zero Check: Pre: OK ✓ 598 Post: OK ✓ 598

THERMOCOUPLE CHECK (@ Ambient):				T/C #1:	<u>60</u>	T/C #2:	<u>61</u>
T/C #3:	<u>62</u>	T/C #4:	<u>—</u>	T/C #5:	<u>—</u>	T/C #6:	<u>—</u>
T/C #7:	<u>—</u>	T/C #8:	<u>—</u>	T/C #9:	<u>60</u>	T/C #10:	<u>63</u>
T/C #11:	<u>59</u>	T/C #12:	<u>59</u>	T/C #13:	<u>59</u>	T/C #14:	<u>61</u>
T/C #15:	<u>59</u>	T/C #16:	<u>63</u>	T/C #17:	<u>59</u>	T/C #18:	<u>60</u>
T/C #19:	<u>60</u>	T/C #20:	<u>—</u>	T/C #21:	<u>—</u>	T/C #22:	<u>—</u>

Thermocouple Readout:

Pretest Zero & Span Check and Calibration      Post Test Zero & Span Check  
 Zero (0° F): 0 ° F Adj to: — ° F      0° F | — Δ%: -0.22  
 Span (2000° F): 2000 ° F Adj to: — ° F      Span(2000° F): 2002 Δ%: -0.08

Pretest Thermocouple Readout Linearity Check:

0 °F = 0      200 °F = 202      400 °F = 399      600 °F = 601  
 800 °F = 801      1000 °F = 1000      1200 °F = 1198      1400 °F = 1399  
 1600 °F = 1600      1800 °F = 1800      2000 °F = 2000

Woodstove Data Sheet 4-4 Scale QC Record Sheet  
Scale 2

From: 7/17/15  
Through: 9/10/15

Scale: Sartorius  
Model: CPA 2245  
SN: 24850860  
Rev: 5/10

Level	Recali- brated	100g Weight	10g Weight	1g Weight	100mg Weight	10mg Weight	DATE	TIME	TECH	BP	LINE VOLTS	WET BULB	DRY BULB	% RH
Yes	No	99.9994	10.0000	1.0000	0.1000	0.0100	7/17/15	1900	ATM	28.40	119	55	67	45
Yes	No	99.9995	10.0000	1.0000	0.1000	0.0100	7/18/15	1957	ATM	28.37	120	57	70	44
Yes	No	99.9994	10.0000	1.0000	0.0999	0.0100	7/19/15	1413	ATM	28.42	121	57	70	44
Yes	No	99.9994	9.9999	1.0000	0.1000	0.0101	7/20/15	1022	ESS	28.40	118	57	69	46
Yes	No	99.9996	10.0000	1.0000	0.1000	0.0100	7/21/15	1358	ATM	28.28	116	55	66	48
Yes	No	99.9995	9.9999	0.9999	0.1000	0.0100	7/22/15	1606	ESS	28.27	116	54	65	47
Yes	No	99.9995	9.9999	1.0000	0.1000	0.0100	7/23/15	1205	ATM	28.33	118	54	65	47
Yes	No	99.9994	10.0000	0.9999	0.1001	0.0101	7/24/15	1525	ESS	28.38	118	55	66	48
Yes	No	99.9996	10.0000	1.0000	0.0999	0.0100	7/26/15	1421	ATM	28.42	118	57	69	47
Yes	No	99.9996	9.9999	0.9999	0.1000	0.0100	7/28/15	1603	ATM	28.58	118	56	67	47
Yes	No	99.9995	10.0000	1.0000	0.1000	0.0101	7/29/15	1325	ESS	28.57	117	56	68	46
Yes	No	99.9994	9.9999	1.0000	0.1000	0.0100	7/30/15	949	ATM	28.60	119	55	66	48
Yes	No	99.9995	9.9999	1.0000	0.1000	0.0100	7/30/15	2105	ATM	28.48	118	56	67	48
Yes		99.9995	9.9999	0.9999	0.1000	0.0100	7/31/15	1413	ESS	28.45	116	58	70	48
Yes	No	99.9995	9.9999	1.0000	0.1000	0.0101	8/1/15	1547	ATM	28.33	118	54	66	45
Yes	No	99.9995	9.9999	0.9999	0.0999	0.0100	8/2/15	1813	ATM	28.27	120	57	69	45
Yes	No	99.9995	9.9999	1.0000	0.1000	0.0100	8/3/15	949	ATM	28.30	120	57	69	45
Yes	No	99.9994	9.9999	1.0000	0.1000	0.0101	8/12/15	1038	ESS	28.43	120	57	69	45
Yes	No	99.9994	9.9999	0.9999	0.1000	0.0100	8/18/15	1530	ATM	28.42	119	58	70	48
Yes	No	99.9996	9.9999	0.9999	0.0999	0.0100	8/19/15	0636	ATM	28.42	119	57	69	45
Yes	No	99.9995	10.0000	1.0000	0.1000	0.0100	8/19/15	2244	ATM	28.20	119	58	70	48
Yes	No	99.9995	10.0000	0.9999	0.1000	0.0101	8/20/15	1610	ESS	28.20	119	58	70	48
Yes	No	99.9995	10.0000	1.0000	0.0999	0.0100	8/26/15	1425	ESS	28.40	118	57	70	43
Yes	No	99.9994	10.0000	0.9999	0.1000	0.0100	8/28/15	1200	ESS	28.48	119	58	70	48
Yes	No	99.9995	9.9999	1.0000	0.1000	0.0100	8/31/15	1547	ESS	28.40	118	57	69	47
Yes	No	99.9995	10.0000	1.0000	0.1000	0.0100	9/10/15	1047	ATM	28.50	117	56	68	46

Woodstove Data Sheet 4-4 Scale QC Record Sheet  
Scale 2

Scale: Sartorius  
Model: CPA 2245  
SN: 24850860  
Rev: 5/10

From: 5/8/15  
Through: 7/5/15

100+20+10+S

50 2015

Level	Recalibrated	135g Weights	100g Weight	10g Weight	1.0 g Weight	100mg Weight	mg Weight	Date	Time	Tech	BP	Wet Bulb	Dry Bulb	% RH	Line Vol/b
Yes	No	134.9997	99.9996	10.0000	1.0000	0.1000	0.0501	5/8/15	1311	ATM	28.48	55	67	45	119
Yes	Yes	134.9995	99.9994	10.0000	0.9999			5/29/15	936	ATM	28.56				119
Yes	No	134.9996	99.9995	9.9999	0.9999	0.1000	0.0501	5/30/15	905	ATM	28.57	65	78	49	118
Yes	No	134.9994	99.9994	10.0000	1.0000	0.1000	0.0501	6/2/15	843	ATM	28.40	62	75	47	119
Yes	No	134.9994	99.9994	9.9999	1.0000	0.1000	0.0502	6/3/15	921	ESS	28.49	57	69	46	118
Yes	No	134.9995	99.9994	9.9999	0.9999	0.0999	0.0500	6/4/15	824	ATM	28.52	59	71	48	116
Yes	No	134.9997	99.9996	9.9999	0.9999	0.0999	0.0500	6/6/15	1028	ATM	28.61	60	72	49	118
Yes	No	134.9996	99.9995	9.9999	0.9999	0.1000	0.0500	6/8/15	1110	ATM	28.42	59	76	40	117
Yes	No	134.9997	99.9996	9.9999	1.0000	0.1000	0.0501	6/10/15	1437	ATM	28.32	56	68	47	116
Yes	No	134.9996	99.9996	9.9999	1.0000	0.1000	0.0500	6/11/15	2245	ATM	28.30	56	68	47	117
Yes	No	134.9996	99.9995	9.9999	1.0000	0.1000	0.0501	6/12/15	2138	ATM	28.50	55	67	46	120
Yes	No	134.9995	99.9995	10.0000	1.0000	0.1000	0.0501	6/13/15	833	ATM	28.52	54	65	48	119
Yes	No	134.9995	99.9994	10.0000	1.0000	0.1000	0.0501	6/14/15	15:14	ATM	28.46	53	64	47	118
Yes	No	134.9996	99.9996	10.0000	1.0000	0.1000	0.0500	6/17/15	13:39	ATM	28.38	57	69	46	116
Yes	No	134.9996	99.9995	10.0000	1.0000	0.0999	0.0501	6/18/15	17:30	ATM	28.42	56	68	46	119
Yes	No	134.9996	99.9995	9.9999	1.0000	0.1000	0.0501	6/20/15	1547	ATM	28.40	56	68	46	119
Yes	No	134.9997	99.9996	9.9999	1.0000	0.1001	0.0501	6/22/15	1432	ESS	28.46	55	67	45	118
Yes	No	134.9996	99.9995	9.9999	0.9999	0.1000	0.0501	6/23/15	12:18	ATM	28.49	55	68	42	117
Yes	No	134.9996	99.9996	9.9999	1.0000	0.1000	0.0501	6/24/15	1434	ESS	28.49	58	70	48	119
Yes	No	134.9996	99.9995	9.9999	1.0000	0.1000	0.0501	6/25	839	ATM	28.60	56	69	43	117
Yes	No	134.9995	99.9996	9.9999	1.0000	0.1001	0.0501	6/26/15	1233	ESS	28.51	57	69	46	114
Yes	No	134.9995	99.9995	10.0000	1.0000	0.1000	0.0501	6/27/15	2222	ATM	28.405	58	71	45	120
Yes	No	134.9995	99.9995	9.9999	1.0000	0.1000	0.0502	6/30/15	1433	ESS	28.47	59	71	48	119
Yes	No	134.9997	99.9996	10.0000	1.0000	0.1000	0.0500	7/1/15	1309	ATM	28.435	57	70	44	116
Yes	No	134.9995	99.9995	9.9999	0.9999	0.0999	0.0500	7/2/15	1354	ATM	28.40	58	70	48	116
Yes	No	134.9996	99.9995	9.9999	1.0000	0.1000	0.0501	7/5/15	1912	ATM	28.38	58	70	48	119

Becherini Scale Center, Inc.  
 317 E. Sprague  
 Spokane, WA 99202

# SCALE CALIBRATION RECORD

Customer: MYREN CONSULTING Date: 3/26/15  
 Work Order Number: 48656 PO Number:

Equipment Mfg.	Serial Number	Specifications	Weight used	Initial Readings	Final Readings
1. PANTHER	4466459	1000 x .1	Ø	/	/
	Pass...Fail		50		
Notes: NOT WORKING, TOOK BACK TO SHOP			100		
			300		
			500		
			Ø		

Equipment Mfg.	Serial Number	Specifications	Weight used	Initial Readings	Final Readings
2. PANTHER	00155556K	5K x 1		/	/
	Pass...Fail				
Notes: NOT USING					

Equipment Mfg.	Serial Number	Specifications	Weight used	Initial Readings	Final Readings
3. PANTHER	00025736K5	1000 x .1	Ø	/	Ø
	Pass...Fail		50		50.0
Notes: 1 x SMALL - CALIBRATED			100		100.0
			300		300.0
			500		500.2
			Ø	Ø	Ø

Equipment Mfg.	Serial Number	Specifications	Weight used	Initial Readings	Final Readings
4. PANTHER	00926576K2	1000 x .1	Ø	Ø	Ø
	Pass...Fail		50	50.0	50.0
Notes: 3 x 5 DECK, CALIBRATED			100	100.0	100.0
			300	300.1	300.0
			500	500.2	500.0
			Ø	Ø	Ø

Additional Comments:

Last Checked: 9/14 Next Check Due: 9/15  
 Weights Certified: 10/14 Technician: ICC/BB

## DENSITY STANDARD USED FOR TROEMNER PRECISION WEIGHTS

Troemner Inc. adjusts all new weights and all weights received for recalibration on the basis of apparent mass versus material of density  $8.0\text{g}/\text{cm}^3$  at  $20^\circ\text{C}$ . This action is in accordance with the recommendations of the American Society for Testing and Materials specification ANSI/ASTM E 617 and the International Organization of Legal Metrology (OIML) International Recommendation No. 20.

Previously, all weights had usually been adjusted on the basis of apparent mass versus "brass," a hypothetical material of defined density  $8.4\text{g}/\text{cm}^3$  at  $0^\circ\text{C}$  and  $8.3909\text{g}/\text{cm}^3$  at  $20^\circ\text{C}$ . This practice originated in the early 1800's and was adopted in all of the English speaking countries as well as a number of other countries. Now most mass standards and test weights are made from stainless steel (density ranges from  $7.77\text{g}/\text{cm}^3$  to  $8.0\text{g}/\text{cm}^3$ ). A number of countries have adopted the recommendations of OIML and the foremost balance manufacturers are adjusting the built-in weights in their balances on the basis of apparent mass versus  $8.0\text{g}/\text{cm}^3$ . In order to smooth the transition in this country, the Reports of Calibration of the National Bureau of Standards are reporting the corrections to calibrated mass standards on both bases.

In terms of normal weighing procedures the change is very small. For a given weight, the mass value assigned on the basis of apparent mass versus density  $8.0\text{g}/\text{cm}^3$  material will be 7 parts per million higher than the value assigned on the basis of apparent mass versus "density  $8.4\text{g}/\text{cm}^3$ " material. In many cases the allowed weight adjustment tolerances are so

large that this change is immaterial although closely adjusted weights often have a smaller tolerance than the correction change. For example at the 1 kilogram level the change is 7 mg. For comparison the ANSI/ASTM E 617 Class 6 tolerance for 1 kilogram is 100 mg while the Class 1 tolerance is 2.5 mg. A detailed discussion of mass and mass values is given in Reference 3.

Precision Weights manufactured by Troemner Inc. to ASTM Class 1, 1.1, 2, 3, 4, 5, and 6 tolerances and the equivalent OIML and NBS tolerances are of the following materials:

Designation	Base Material	Density	Weight Range
Stainless Steel	18-8	$7.84\text{g}/\text{cm}^3$ at $20^\circ\text{C}$	1 g & larger
Stainless Steel	18-8	$8.0\text{g}/\text{cm}^3$ at $20^\circ\text{C}$	50 mg to 500 mg
Aluminum	1100	$2.7\text{g}/\text{cm}^3$ at $20^\circ\text{C}$	30 mg & smaller

### References:

1. ANSI/ASTM E 617  
Available from: Troemner Inc. 6825 Greenway Ave., Phila. Pa. 19142  
215-724-0800 or American Society for Testing and Materials, 1916 Race Street, Phila., Pa. 19103
2. OIML INTERNATIONAL RECOMMENDATION No. 20  
Available from: Organisation Internationale De Metrologie Legale  
11 Rue Trugot - 75009 Paris, France
3. NBS MONOGRAPH 133, MASS AND MASS VALUES  
Available from: Superintendent of Documents, U.S. Government  
Printing Office  
Washington, D.C. 20402  
Order by SD Catalog No. C13,44:1331 Stock Number  
0303-01178



**TROEMNER INC.**

Manufacturers of Precision Weights...  
Mass Standards • Balances • Laboratory Apparatus  
6825 Greenway Avenue - Philadelphia, Pa. 19142  
215/724-0800

Wts. USED for Scale QC Checks, P. 4-4.



# QUALITY CONTROL SERVICES

LABORATORY EQUIPMENT • SALES • SERVICE • CALIBRATION • REPAIRS  
 2340 SE 11<sup>TH</sup> Ave. Portland, Oregon 97214 • Box 14831 Portland, Oregon 97293  
 (503) 236-2712 • FAX (503) 235-2535 • www.qc-services.com



Myren Consulting  
 512 Williams Lake Road  
 Colville, WA 99114

Report Number: MYRC0224850860150415

## A2LA ACCREDITED CERTIFICATE OF CALIBRATION WITH DATA

### INSTRUMENT INFORMATION

Item	Make	Model	Serial Number	Customer ID	Location
Balance	Sartorius	CPA224S	24850860	N/A	Lab
Units	Readability	SOP	Cal Date	Last Cal Date	Cal Due Date
g	0.0001	QC012	4/15/15	11/12/14	10/2015

### FUNCTIONAL CHECKS

ECCENTRICITY		LINEARITY		STANDARD DEVIATION			ENVIRONMENTAL CONDITIONS
Test Wt:	Tol:	Test Wt:	Tol:	Test Wt:	Tol:		
100	0.0003	50 x 4	0.0002	100	0.0001		<input type="checkbox"/> <input checked="" type="checkbox"/> <input type="checkbox"/>
As-Found:		As-Found:		1. 100.0000	5. 99.9999	9. 99.9999	Good Fair Poor
Pass: <input checked="" type="checkbox"/>	Fail: <input type="checkbox"/>	Pass: <input checked="" type="checkbox"/>	Fail: <input type="checkbox"/>	2. 100.0000	6. 100.0000	10. 100.0000	
As-Left:		As-Left:		3. 100.0000	7. 100.0000	<b>Result</b>	Temperature: 21.3°C
Pass: <input checked="" type="checkbox"/>	Fail: <input type="checkbox"/>	Pass: <input checked="" type="checkbox"/>	Fail: <input type="checkbox"/>	4. 100.0000	8. 100.0000	0.00004	

### A2LA ACCREDITED SECTION OF REPORT

Standard	As-Found	As-Left	Expanded Uncertainty
200	199.9992	200.0002	0.00014
100	99.9995	100.0000	0.00014
50	49.9997	50.0000	0.00014
10	9.9999	10.0000	0.00014
1	1.0000	1.0000	0.00014
0.1	0.1000	0.1000	0.00014

### CALIBRATION STANDARDS

Item	Make	Model	Serial Number	Cal Date	Cal Due Date	NIST ID
Weight Set	Rice Lake	30 kg-1mg	S751	12/2/14	12/2015	OR-13-314-C

Permanent Information Concerning this Equipment:

Comments/Info Concerning this Calibration:

4/15 Performed internal calibration overwrite.

Report prepared/reviewed by:

Date: 4-15-2015

Technician: R. Hintz

Signature:

THIS CERTIFICATE SHALL NOT BE REPRODUCED WITHOUT THE APPROVAL OF QUALITY CONTROL SERVICES, INC.

The uncertainty is calculated according to the ISO Guide to the Expression of Uncertainty in Measurement and includes the uncertainty of standards used combined with the observed standard deviation and readability of the unit under test. The uncertainty is expanded with a k factor of 2 for an approximate 95% level of confidence. Instruments listed above were calibrated using standards traceable to the National Institute of Standards and Technology (NIST). Calibration data reflect results at the time and location of calibration. Calibration data should be reviewed to insure that the instrument is performing to its required accuracy. Calibrations comply with ISO/IEC 17025 and ANSI/Z540-1-1994 quality standards.

**ALTEK**

**CERTIFICATE OF CALIBRATION**

This is to Certify that your Altek Unit has been calibrated using standards whose accuracies are traceable to the National Institute of Standards and Technology (formerly NBS) within the limits of the NIST Calibration Services. Actual records pertaining to these standards are on file and are available for examination.

Certified by: Altek Industries Corp.  
Recommend Recalibration: Annually

In service date 4/11/96

Model K2100F Serial No. Serial # 177533

T. Kuech  
Calibration Technician

31 AUG 95  
Factory Calibration Date

**ALTEK INDUSTRIES CORP**  
210 Commerce Drive, Rochester, NY 14623 U.S.A.  
(716) 334-3720 FAX: (716) 334-6673  
800-32-ALTEK  
800-322-6835  
Anywhere in USA

MYREN CONSULTING, INC.  
512 Williams Lake Road  
Colville, WA 99114  
Office: 509 684 1154  
Lab: 509 685 9458

Calibration Data Sheet # 65  
Revision 1 3/3/04

THERMOCOUPLE READOUT CALIBRATION

DATE: 5/20/15  
TECHNICIAN: ESS

Thermocouple Readout Manufacturer: OMEGA

Model #: 115 KF Serial #: 00114871KF Type: K Range: 0-1900°F

Location: 45 G-P METER Box

Calibrated with: ALTEK SERIES 22 TC SOURCE

As found: 0° F = -1 Adjusted to: 0  
1900° F = 1901 Adjusted to: 1900

	% Dif		% Dif		% Dif
0 = <u>0</u>	<u>0</u>	800 = <u>799</u>	<u>.0008</u>	1600 = <u>1600</u>	<u>0</u>
100 = <u>95</u>	<u>.0089</u>	900 = <u>896</u>	<u>.0029</u>	1700 = <u>1699</u>	<u>.0005</u>
200 = <u>202</u>	<u>-.0030</u>	1000 = <u>1000</u>	<u>0</u>	1800 = <u>1800</u>	<u>0</u>
300 = <u>299</u>	<u>.0013</u>	1100 = <u>1098</u>	<u>.0013</u>	1900 = <u>1900</u>	<u>0</u>
400 = <u>400</u>	<u>0</u>	1200 = <u>1198</u>	<u>.0012</u>	2000 = <u>—</u>	<u>—</u>
500 = <u>498</u>	<u>.0021</u>	1300 = <u>1296</u>	<u>.0023</u>		
600 = <u>600</u>	<u>0</u>	1400 = <u>1399</u>	<u>.0005</u>		
700 = <u>695</u>	<u>.0043</u>	1500 = <u>1498</u>	<u>.0010</u>		

$$\% \text{ Dif} = \frac{(\text{Reference Temperature } ^\circ\text{F} + 460) - (\text{Readout Temperature } ^\circ\text{F} + 460)}{\text{Reference Temperature } ^\circ\text{F} + 460}$$

Or

$$\% \text{ Dif} = \frac{(\text{Reference Temperature } ^\circ\text{C} + 273) - (\text{Readout Temperature } ^\circ\text{C} + 273)}{\text{Reference Temperature } ^\circ\text{C} + 273}$$



MYREN CONSULTING, INC.  
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 Colville, WA 99114  
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Calibration Data Sheet # 65  
 Revision 1 3/3/04

THERMOCOUPLE READOUT CALIBRATION

DATE: 5/20/15  
 TECHNICIAN: ESS

Thermocouple Readout Manufacturer: JENCO

Model #: 768-KF02 Serial #: 900164 Type: K Range: 0-1999°F

Location: 511-M METER BOX

Calibrated with: ALTEK SERIES 22 TC SOURCE

As found: 0° F = -3 Adjusted to: 0  
 1900° F = 1896 Adjusted to: 1900

Reference Temp (°F)	Readout Temp (°F)	% Dif	Reference Temp (°F)	Readout Temp (°F)	% Dif	Reference Temp (°F)	Readout Temp (°F)	% Dif
0	0	0	800	800	0	1600	1614	-1.0068
100	94	.0107	900	900	0	1700	1710	-1.0046
200	199	.0015	1000	1006	-.0041	1800	1807	-.0031
300	295	.0066	1100	1107	-.0045	1900	1900	0
400	394	.0070	1200	1210	-.0060	2000	-	-
500	490	.0104	1300	1313	-.0074			
600	595	.0047	1400	1415	-.0081			
700	693	.0060	1500	1514	-.0071			

$$\% \text{ Dif} = \frac{(\text{Reference Temperature } ^\circ\text{F} + 460) - (\text{Readout Temperature } ^\circ\text{F} + 460)}{\text{Reference Temperature } ^\circ\text{F} + 460}$$

Or

$$\% \text{ Dif} = \frac{(\text{Reference Temperature } ^\circ\text{C} + 273) - (\text{Readout Temperature } ^\circ\text{C} + 273)}{\text{Reference Temperature } ^\circ\text{C} + 273}$$

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 Colville, WA 99114  
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Calibration Data Sheet # 65  
 Revision 1 3/3/04

THERMOCOUPLE READOUT CALIBRATION

DATE: 5/20/15  
 TECHNICIAN: ESS

Thermocouple Readout Manufacturer: Omega

Model #: 460BK Serial #: 99110582 Type: K Range: 0-2000°F

Location: SOUTH STAND T/C Dial Readout - Dial #1

Calibrated with: ALTEK SERIES 22 TC SOURCE

As found: 0° F = .8 Adjusted to: 0  
 2000° F = 1999.3 Adjusted to: 2000

0	% Dif	800	% Dif	1600	% Dif
0 = <u>0</u>	<u>0</u>	800 = <u>801.1</u>	<u>-.0009</u>	1600 = <u>1599.5</u>	<u>.0002</u>
100 = <u>97.1</u>	<u>.0052</u>	900 = <u>897.6</u>	<u>.0018</u>	1700 = <u>1698.6</u>	<u>.0006</u>
200 = <u>201.4</u>	<u>-.0021</u>	1000 = <u>1000.3</u>	<u>-.0002</u>	1800 = <u>1799.8</u>	<u>.00009</u>
300 = <u>297.0</u>	<u>.0013</u>	1100 = <u>1098.0</u>	<u>.0013</u>	1900 = <u>1898.6</u>	<u>.0006</u>
400 = <u>398.9</u>	<u>.0012</u>	1200 = <u>1198.0</u>	<u>.0012</u>	2000 = <u>2000.0</u>	<u>0</u>
500 = <u>497.0</u>	<u>.0031</u>	1300 = <u>1298.2</u>	<u>.0010</u>	2100 = <u>2098.7</u>	<u>.0005</u>
600 = <u>601.0</u>	<u>-.0009</u>	1400 = <u>1399.0</u>	<u>.0005</u>		
700 = <u>697.4</u>	<u>.0022</u>	1500 = <u>1498.6</u>	<u>.0007</u>		

$$\% \text{ Dif} = \frac{(\text{Reference Temperature } ^\circ\text{F} + 460) - (\text{Readout Temperature } ^\circ\text{F} + 460)}{\text{Reference Temperature } ^\circ\text{F} + 460}$$

Or

$$\% \text{ Dif} = \frac{(\text{Reference Temperature } ^\circ\text{C} + 273) - (\text{Readout Temperature } ^\circ\text{C} + 273)}{\text{Reference Temperature } ^\circ\text{C} + 273}$$

THERMOMETER CALIBRATION

DATE: 6/5/15 TECHNICIAN: A.T. Myren

MANUFACTURER:	<u>ERTCO</u>	<u>ERTCO</u>	<u>Fisher</u>	<u>Taylor</u>	<u>Taylor</u>	<u>Premium</u>
CAT #.	<u>1005-3FC</u>	<u>E17</u>	<u>ASTM 59F</u>	<u>1330 N/A</u>	<u>1330 N/A</u>	<u>—</u>
SERIAL NO.	<u>1697</u>	<u>K35413</u>	<u>AD4544</u>	<u>—</u>	<u>—</u>	<u>—</u>
RANGE:	<u>-1 to 100°C</u>	<u>0-260°C</u>	<u>0-180°F</u>	<u>20-120°F</u>	<u>20-120°F</u>	<u>0-220°F</u>
GRADUATIONS:	<u>0.1°C</u>	<u>1°C</u>	<u>1°F</u>	<u>1°F</u>	<u>1°F</u>	<u>2°F</u>
TYPE:	<u>Tube</u>	<u>Tube</u>	<u>Tube</u>	<u>Tube</u>	<u>Tube</u>	<u>Dial</u>
TEMP. POINT						
1	<u>1.9</u>	<u>1</u>	<u>34</u>	<u>35</u>	<u>35</u>	<u>36</u>
2	<u>8.9</u>	<u>9.0</u>	<u>48</u>	<u>48</u>	<u>49</u>	<u>50</u>
3	<u>20.1</u>	<u>21</u>	<u>69</u>	<u>70</u>	<u>70</u>	<u>72</u>
4	<u>31.5</u>	<u>32</u>	<u>89</u>	<u>90</u>	<u>91</u>	<u>92</u>

COMMENTS:

$^{\circ}\text{F} = (^{\circ}\text{C} \times 9/5) + 32$   
 $^{\circ}\text{C} = (5/9) (^{\circ}\text{F} - 32)$

Note: The 2 Taylor Thermometers are in the Sling Psychrometer

R E P O R T O F C A L I B R A T I O N

L I Q U I D - I N - G L A S S - T H E R M O M E T E R

CALIBRATED BY EVER READY THERMOMETER CO.

MARKED: ERTCO CAT 1005-3FC S/N-1697  
RANGE: -1 TO +101 DEGREES C IN 0.1 DEGREE GRADUATIONS.

THERMOMETER READING	CORRECTION (ITS-90)**
0.00 C	0.00 C
10.00	0.00
20.00	0.00
30.00	0.00
37.00	0.00
40.00	0.00
50.00	0.00
56.00	0.00
60.00	0.02
70.00	0.00
80.00	0.00
90.00	0.00
100.00	0.00

\*\* ALL TEMPERATURES IN THIS REPORT ARE BASED ON THE INTERNATIONAL TEMPERATURE SCALE OF 1990 (ITS-90) PUBLISHED IN THE METROLOGIA 27, NO. 1, 3/10/90.

THIS THERMOMETER WAS CALIBRATED AGAINST A STANDARD CALIBRATED AT THE NATIONAL INSTITUTE OF STANDARDS AND TECHNOLOGY (NIST) FORMERLY THE NATIONAL BUREAU OF STANDARDS (NBS) IN ACCORDANCE WITH ASTM METHOD E 77, AND NBS MONOGRAPH 174.

FOR A DISCUSSION OF ACCURACIES ATTAINABLE WITH SUCH THERMOMETERS SEE NBS MONOGRAPH 250-23.

IF NO SIGN IS GIVEN ON THE CORRECTION, THE TRUE TEMPERATURE IS HIGHER THAN THE INDICATED TEMPERATURE; IF THE SIGN GIVEN IS NEGATIVE, THE TRUE TEMPERATURE IS LOWER THAN THE INDICATED TEMPERATURE. TO USE THE CORRECTIONS PROPERLY, REFERENCE SHOULD BE MADE TO THE NOTES GIVEN BELOW.

CONTINUED

TEST NUMBER: 152439  
DATE: 07/16/96  
STANDARD SERIAL NO. 128239  
NIST IDENTIFICATION NO. 88024

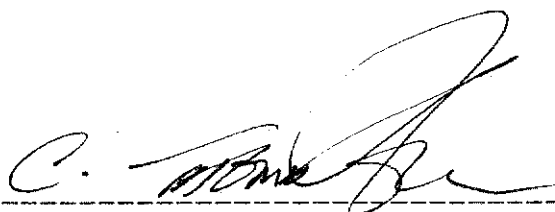
## R E P O R T O F C A L I B R A T I O N

## LIQUID-IN-GLASS-THERMOMETER

THE THERMOMETER WAS TESTED IN A LARGE, CLOSED-TOP, ELECTRICALLY HEATED, LIQUID BATH, BEING "IMMERSED" 76MM. THE TEMPERATURE OF THE ROOM WAS ABOUT 25 DEGREES C (77 DEGREES F). IF THE THERMOMETER IS USED UNDER CONDITIONS WHICH WOULD CAUSE THE AVERAGE TEMPERATURE OF THE EMERGENT LIQUID COLUMN TO DIFFER MARKEDLY FROM THAT PREVAILING IN THE TEST, APPRECIABLE DIFFERENCES IN THE INDICATIONS OF THE THERMOMETER WOULD RESULT.

THE TABULATED CORRECTIONS APPLY PROVIDED THE ICE-POINT READING, TAKEN AFTER EXPOSURE FOR NOT LESS THAN 3 DAYS TO A TEMPERATURE OF ABOUT 20 DEGREES C (70 DEGREES F) IS 0.00 DEGREES C. IF THE ICE-POINT READING IS FOUND TO BE HIGHER (OR LOWER) THAN STATED, ALL OTHER READINGS WILL BE HIGHER (OR LOWER) TO THE SAME EXTENT. IF THE THERMOMETER IS USED AT A GIVEN TEMPERATURE SHORTLY AFTER BEING HEATED TO A HIGHER TEMPERATURE. AN ERROR OF 0.01 DEGREES OR LESS, FOR EACH 10 DEGREE DIFFERENCE BETWEEN THE TWO TEMPERATURES, MAY BE INTRODUCED. THE TABULATED CORRECTIONS APPLY IF THE THERMOMETER IS USED IN THE UPRIGHT POSITION; IF USED IN A HORIZONTAL POSITION, THE INDICATIONS MAY BE A FEW HUNDREDTHS OF A DEGREE HIGHER.

TEST NUMBER: 152439  
DATE: 07/16/96  
STANDARD SERIAL NO. 128239  
NIST IDENTIFICATION NO. 88024



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Charles Tang-Nian  
QUALITY CONTROL MANAGER

Dry Gas Meter Calibration Data

Date: 5/11/15 Technician: A. T. Myrman  
 Calibration Meter Mfr: Rockwell SN: 1052202 Y: 0.9963  
 Meter Box ID 450-P Meter Mfr: Rockwell SN: 3039270  
 Electrical Check OK Pitot Leak Check N/A  
 Leak Check Front Half OK Back Half OK See back of page  
 BP = 28.32 in. Hg

Orifice (Δh) in. H <sub>2</sub> O	Gas Volume			Temperature				Time (Θ), Min.
		Cal. Meter (Vc), (cu.ft.)	Dry Gas Meter (Vm), (m <sup>3</sup> )(ft <sup>3</sup> )		Cal. Meter (Tc), °F	Dry Gas Meter		
						Inlet (Tmi), (°F)(°C)	Outlet (Tmo), (°F)(°C)	
.80	initial	289.827	940.300	initial	72	74	74	14:00.34
	final	296.640	947.060	mid	69.5	77	77	14:00.6
				final	69.5	76	76	0.5
	total	6.813	6.760	avg.	70.3	75.7	75.7	75.7
					530.3	535.7	535.7	535.7
.90	initial	297.291	947.700	initial	69.5	77	77	10:54.75
	final	303.220	953.632	mid	68	79	79	10:59.6
				final	67.5	81	81	0.5
	total	5.929	5.932	avg.	68.3	79	79	79
					528.3	539	539	539
1.00	initial	303.878	954.300	initial	68	80	80	9:54.91
	final	309.613	960.075	mid	67.5	83	83	9:55
				final	67.5	84	84	0.5
	total	5.785	5.775	avg.	67.7	82.3	82.3	82.3
					527.7	542.3	542.3	542.3
	initial			initial				
	final			mid				
				final				
	total			avg.				
	initial			initial				
	final			mid				
				final				
	total			avg.				

$$Y = \frac{(Y)(Vc)(Pb)(Tm + 460)}{(Vm)(Pb + \Delta h/13.6)(Tc + 460)}$$

$$\Delta h @ = \frac{(0.0317)(\Delta h)}{Pb(Tmo + 460)} \left[ \frac{(Tc + 460)(\Theta)}{[(Vc)(Yc)]^2} \right]$$

# Back Half Leak Check

Side 1	mano	"H <sub>2</sub> O
Start	8.35	"H <sub>2</sub> O
Stop	8.35	"H <sub>2</sub> O
	<u>0.00</u>	Leak Rate

Side 2	mano	"H <sub>2</sub> O
Start	5.90	"H <sub>2</sub> O
Stop	5.90	"H <sub>2</sub> O
	<u>0.00</u>	Leak Rate

# Front Half Leak Check

	Vac "Hg	mtr Start	RDG Stop	Leak Rate	
DGM	-18.0	939.123	939.124	.001	cfm
TM	-18.0	288.559	288.560	.001	cfm

Meter Box Calibration Page 2

$$Y = \frac{(Y_c)(V_c)(BP)(T_m + 460)}{(V_m)(BP + \Delta H/13.6)(T_c + 460)} =$$

$$Y = \frac{(.9963)(6.813)(28.32)(703 + 460)}{(6.760)(28.32 + .80/13.6)(75.7 + 460)} = \frac{101,939,710}{102,769,142} = 0.99193$$

530.3  
535.7

$$Y = \frac{(.9963)(5.929)(28.32)(79 + 460)}{(5.932)(28.32 + .90/13.6)(68.3 + 460)} = \frac{90,168,240}{88,958,746} = 1.01360$$

539  
528.3

$$Y = \frac{(.9963)(5.735)(28.32)(82.3 + 460)}{(5.775)(28.32 + 1.00/13.6)(67.7 + 460)} = \frac{87,751,875}{86,528,358} = 1.01414$$

547.3  
527.7

$$Y = \frac{(\quad)(\quad)(\quad)(+460)}{(\quad)(\quad + \quad/13.6)(\quad + 460)} = \quad = \quad$$

$$Y = \frac{(\quad)(\quad)(\quad)(+460)}{(\quad)(\quad + \quad/13.6)(\quad + 460)} = \quad = \quad$$

**Y Factor**                      **Variation**      ( $\pm 0.02$  Allowed From Average Y)

0.99193                      -0.0146

1.01360                      +0.0070

1.01414                      +0.0076

\_\_\_\_\_  
 \_\_\_\_\_

o/k  
 (Am)

Avg Y 1.00656

3.01967



METER BOX 45G-P

DATE 5/11/15

Page 3 of 3

$$\Delta H\theta = \frac{(0.0317)(\Delta H)}{(Pb)(T_{mo} + 460)} \cdot \left[ \frac{(T_w + 460)(\Theta)}{(Y_c)(V_c)} \right]^2 =$$
$$\Delta H\theta = \frac{(0.0317)(.80)}{(28.32)(757 + 460)} \cdot \left[ \frac{(703 + 460)(14.006)}{(.9963)(6.813)} \right]^2 = 2.0015$$
$$\Delta H\theta = \frac{(0.0317)(.90)}{(28.32)(79 + 460)} \cdot \left[ \frac{(683 + 460)(10.996)}{(.9963)(5.929)} \right]^2 = 1.8076$$
$$\Delta H\theta = \frac{(0.0317)(1.00)}{(28.32)(823 + 460)} \cdot \left[ \frac{(677 + 460)(9.915)}{(.9963)(5.735)} \right]^2 = 1.7308$$
$$\Delta H\theta = \frac{(0.0317)( )}{( ) ( + 460)} \cdot \left[ \frac{( + 460)( )}{( ) ( )} \right]^2 = \underline{\hspace{2cm}}$$
$$\Delta H\theta = \frac{(0.0317)( )}{( ) ( + 460)} \cdot \left[ \frac{( + 460)( )}{( ) ( )} \right]^2 = \underline{\hspace{2cm}}$$

<u><math>\Delta H\theta</math></u>	<u>VARIATION (<math>\pm 0.20</math> ALLOWED)</u>
<u>2.0015</u>	<u>+0.1549</u>
<u>1.8076</u>	<u>-0.0390</u>
<u>1.7308</u>	<u>-0.1158</u>
<u>          </u>	<u>          </u>
<u>          </u>	<u>          </u>
<u>AVG <math>\Delta H\theta</math></u>	<u>1.8466</u>

5.5399

OK  
AMU

**Post Test  
Meter Box Audit  
Woodstove Data Sheet #32**

45G-P  
T1

Unit: HEAT TECH HTP26  
Date: 8/3/15  
Technician: ATM ESS  
WST9-Form2, Rev 6/11

**Meter Box Calibration Audit  
Test Data**

Run #	1	2	3	4	5	6	7	8	9	10
Avg. Δh	.90									
Max Vac	-1.1									

Avg. Test Series Δh: .90 in H<sub>2</sub>O. Test Series Max Vac: -1.1 in Hg

Audit Dry Gas Meter Mfr: Rochwell SN: 1052202 Correction Factor (Y): 0.9963  
Test Dry Gas Meter Mfr: Rochwell SN: 3039270 Correction Factor (Y): 1.0066

Audit Data

		Audit #1	Audit #2	Audit #3
BP ("Hg):		<u>28.24</u>	<u>28.25</u>	<u>28.25</u>
Vac ("Hg):		<u>-1.1</u>	<u>-1.1</u>	<u>-1.1</u>
Audit Meter:	Final Vol	<u>483.114</u>	<u>488,562</u>	<u>494,047</u>
	Initial Vol	<u>477,810</u>	<u>483,272</u>	<u>488,797</u>
	Vol (V <sub>e</sub> , Ft <sup>3</sup> )	<u>5.304</u> ✓	<u>5.290</u> ✓	<u>5.250</u> ✓
Audit Meter	Temp (°F) (T <sub>c</sub> )			
	Initial	<u>75</u>	<u>73.5</u>	<u>73</u>
	Mid	<u>74.5</u>	<u>73</u>	<u>72.5</u>
	Final	<u>73.5</u> ✓	<u>73</u> ✓	<u>72.5</u> ✓
	Avg (°F/°A)	<u>74.3 (534.3)</u>	<u>73.2 (533.2)</u>	<u>72.7 (532.7)</u>
Δh ("H <sub>2</sub> O)	Initial	<u>.90</u>	<u>.90</u>	<u>.90</u>
	Mid	<u>.90</u>	<u>.90</u>	<u>.90</u>
	Final	<u>.90</u>	<u>.90</u> ✓	<u>.90</u> ✓
	Avg	<u>.90</u>	<u>.90</u>	<u>.90</u> ✓
Dry Gas Meter:	Final Vol	<u>63.436</u>	<u>68.963</u>	<u>74.580</u>
	Initial Vol	<u>58.100</u>	<u>63.600</u>	<u>69.200</u>
	Vol (V <sub>d</sub> ) (ft <sup>3</sup> ) (m <sup>3</sup> )	<u>5.336</u> ✓	<u>5.363</u> ✓	<u>5.380</u> ✓
Dry Gas Meter	Temp (°F) : Inlet (T <sub>m</sub> )			
	Initial	<u>77</u>	<u>80</u>	<u>84</u>
	Mid	<u>79</u>	<u>82</u>	<u>86</u>
	Final	<u>80</u>	<u>83</u>	<u>86</u>
	Avg (°F/°A)	<u>78.7 (538.7)</u>	<u>81.7 (541.7)</u>	<u>85.3 (545.3)</u>
Dry Gas Meter	Temp (°F) : Outlet (T <sub>m</sub> )			
	Initial	<u>77</u>	<u>80</u>	<u>84</u>
	Mid	<u>79</u>	<u>82</u>	<u>86</u>
	Final	<u>80</u>	<u>83</u>	<u>86</u>
	Avg (°F/°A)	<u>78.7 (538.7)</u>	<u>81.7 (541.7)</u>	<u>85.3 (545.3)</u>
Avg Dry Gas	Meter Temp (T <sub>m</sub> - °F/°A)	<u>78.7 (538.7)</u>	<u>81.7 (541.7)</u>	<u>85.3 (545.3)</u>
	Time (minutes)	<u>10:00.69</u>	<u>10:00.00</u>	<u>10:01.25</u>

Note: If volume is in m<sup>3</sup>, multiply by 35.314667 to obtain ft<sup>3</sup>.  
Note: Add 460° to all temperatures for degrees Absolute.

$$Y = \frac{(V_c)(MCF)(BP)(T_m)}{(V_d)(BP + \Delta h/13.6)(T_c)}$$

$$Y \text{ Factor \% Difference} = \frac{\text{Act} - \text{Exp}}{\text{Exp}} \times 100 \quad 456-P \quad \text{TI}$$

Note: MCF = Meter Correction Factor (Y) for Dry Gas Meter used as a Transfer Standard

**Run 1**

$$Y = \frac{(5.304)(.9963)(28.24)(538.7)}{(5.336)(28.24 + .9/13.6)(534.3)} = \frac{90,390.608}{90,701.611} = 0.99614$$

$$\Delta\% = (.99614 - ) \times 100 = \text{_____} \%$$

**Run 2**

$$Y = \frac{(5.290)(.9963)(28.25)(541.7)}{(5.363)(28.25 + .9/13.6)(533.2)} = \frac{80,653.476}{80,971.568} = 0.99607$$

$$\Delta\% = (.99607 - ) \times 100 = \text{_____} \%$$

**Run 3**

$$Y = \frac{(5.250)(.9963)(28.25)(545.3)}{(5.380)(28.25 + .9/13.6)(532.7)} = \frac{80,575.569}{81,152.066} = 0.99386$$

$$\Delta\% = (.99386 - ) \times 100 = \text{_____} \%$$

Note: The Y Factor % Difference must be < ±5.0% to be acceptable. Avg. Δ% = \_\_\_\_\_

**Determination of Interpolated Y Factor for Average Certification Test Series Δ H from Dry Gas Meter Calibration Data:**

_____ inch H <sub>2</sub> O Δh = _____	Calculated Calibration Y Factor	_____
(A)	(C)	( from Calibration )
_____ inch H <sub>2</sub> O Δh = _____	Calculated Calibration Y Factor	_____
(B)	(D)	( from Calibration )
_____ - _____ = _____ X100 = _____ / _____ = _____		
(B)	(A)	(E) (D) (C) (E) (F)

Avg Δ h \_\_\_\_\_ (A) = \_\_\_\_\_ X 100 = \_\_\_\_\_ (G)

Start + 8.30" H<sub>2</sub>O  
Stop + 8.30" H<sub>2</sub>O  
Δ 0.00

$$\left( \frac{F}{G} \times \frac{C}{D} \right) + \frac{E}{H} = \text{Interpolated Y Factor For Avg. Test Series } \Delta h$$

Dry Gas Meter Back Half Leak Check: \_\_\_\_\_ inch H<sub>2</sub>O in One Minute  
Front Half Leak Check \_\_\_\_\_ Meter Reading Leak Rate

Meter	Vac In. Hg	Start	Stop	cmm	cfm
DGM	-17.0	.415	.415		.000
TM	-17.0	.047	.047		.000



# Back Half Leak Check

Side 1      mano  
 Start      +9.10" H<sub>2</sub>O  
 Stop      +9.10" H<sub>2</sub>O  
0.00 Leak Rate

Side 2      mano  
 Start      +8.00" H<sub>2</sub>O  
 Stop      +8.00" H<sub>2</sub>O  
0.00 Leak Rate

# 2" Manometer System

Side 1      Start      <sup>mano</sup> +0.94" H<sub>2</sub>O  
 Stop      +0.94" H<sub>2</sub>O  
0.00 Leak Rate

Side 2      Start      1.52" H<sub>2</sub>O  
 Stop      1.52" H<sub>2</sub>O  
0.00 Leak Rate

# Front Half Leak Check

	"VAC	MTR BDG		Leak Rate
		Start	Stop	
DGM	-165" Hg	303	303	0.000 cfm
TM	-165" Hg	685	686	0.001 cfm

Had a leak on the pump outlet.  
 Tightened swag fitting, all OK.

Meter Box Calibration Page 2

A.T. Myren

$$Y = \frac{(V_c)(V_e)(BP)(T_m + 460)}{(V_m)(BP + \Delta H/13.6)(T_c + 460)} =$$

$$Y = \frac{(.9963) (8.068) (28.32) (68.8 + 460)}{(8.3045) (28.32 + .80/13.6) (68.8 + 460)} = \frac{120,376.224}{124,623.322} = 0.96592$$

528.8

$$Y = \frac{(.9963) (6.231) (28.32) (69.5 + 460)}{(6.404) (28.32 + .90/13.6) (67.3 + 460)} = \frac{93,090.871}{95,855.270} = 0.97116$$

529.5

$$Y = \frac{(.9963) (5.498) (28.32) (69.5 + 460)}{(5.672) (28.32 + .75/13.6) (67 + 460)} = \frac{82,134.883}{84,817.401} = 0.96843$$

529.5

$$Y = \frac{(\quad)(\quad)(\quad)(+460)}{(\quad)(\quad + \quad/13.6)(\quad + 460)} = \quad = \quad$$

$$Y = \frac{(\quad)(\quad)(\quad)(+460)}{(\quad)(\quad + \quad/13.6)(\quad + 460)} = \quad = \quad$$

Y Factor                      Variation                      (± 0.02 Allowed From Average Y)

0.96592                      -0.0026                      -

0.97116                      +0.0027                      -

0.96843                      -0.0001                      -

ok  
 ATM

Avg Y 0.96850 -

2.90551 -

METER BOX 511-M

DATE 5/11/15

Page 3 of 3

A.T. Myrman

$$\Delta H\theta = \frac{(0.0317)(\Delta H)}{(P_b)(T_{mo} + 460)} \cdot \left[ \frac{(T_w + 460)(\theta)}{(Y_c)(V_c)} \right]^2 =$$

$$\Delta H\theta = \frac{(0.0317)(.80)}{(28.32)(68 + 460)} \cdot \left[ \frac{(68.8 + 460)(16.017)}{(1.9963)(8.068)} \right]^2 = 1.8830$$

$$\Delta H\theta = \frac{(0.0317)(.90)}{(28.32)(68.3 + 460)} \cdot \left[ \frac{(67.3 + 460)(11.616)}{(1.9963)(6.231)} \right]^2 = 1.8595$$

$$\Delta H\theta = \frac{(0.0317)(.75)}{(28.32)(69 + 460)} \cdot \left[ \frac{(67 + 460)(11.143)}{(1.9963)(5.498)} \right]^2 = 1.8734$$

$$\Delta H\theta = \frac{(0.0317)( )}{( ) ( + 460)} \cdot \left[ \frac{( + 460)( )}{( ) ( )} \right]^2 = \underline{\hspace{2cm}}$$

$$\Delta H\theta = \frac{(0.0317)( )}{( ) ( + 460)} \cdot \left[ \frac{( + 460)( )}{( ) ( )} \right]^2 = \underline{\hspace{2cm}}$$

<u>ΔHθ</u>	<u>VARIATION (± 0.20 ALLOWED)</u>
<u>1.8830</u>	<u>+0.0110</u> -
<u>1.8595</u>	<u>-0.0125</u>
<u>1.8734</u>	<u>+0.0143</u> -
<u> </u>	<u> </u>
<u> </u>	<u> </u>
<u>AVG ΔHθ</u>	<u>1.8720</u> -

OK  
ATM

5.6159 -

Post Test  
 Meter Box Audit  
 Woodstove Data Sheet #32

5/11/11  
 Trace 2

Unit: HEAT TECH HTD 26 BA  
 Date: 5/13/11  
 Technician: ATM ESS  
 WST9-Form2, Rev 6/11

Meter Box Calibration Audit  
 Test Data

Run #	1	2	3	4	5	6	7	8	9	10
Avg. Δh	.75									
Max Vac	0									

Avg. Test Series Δh: .75 in H<sub>2</sub>O. Test Series Max Vac: 0 in Hg

Audit Dry Gas Meter Mfr: Rockwell SN: 1052202 Correction Factor (Y): 0.9963  
 Test Dry Gas Meter Mfr: Keimion SN: 5000571 Correction Factor (Y): 0.9734

Audit Data

		Audit #1	Audit #2	Audit #3
BP ("Hg):		<u>28.39</u>	<u>28.385</u>	<u>28.38</u>
Vac ("Hg):		<u>0</u>	<u>0</u>	<u>0</u>
Audit Meter:	Final Vol	<u>502.622</u>	<u>508.078</u>	<u>513.615</u>
	Initial Vol	<u>497.411</u>	<u>502.813</u>	<u>508.411</u>
	Vol (V <sub>c</sub> , Ft <sup>3</sup> )	<u>5.211</u>	<u>5.265</u>	<u>5.204</u>
Audit Meter	Temp (°F) (T <sub>c</sub> )			
	Initial	<u>66.5</u>	<u>65.5</u>	<u>65.5</u>
	Mid	<u>66.5</u>	<u>65.5</u>	<u>65.5</u>
	Final	<u>66</u>	<u>65.5</u>	<u>65.5</u>
	Avg (°F/°A)	<u>66.3 (526.3)</u>	<u>65.5 (525.5)</u>	<u>65.5 (525.5)</u>
Δh ("H <sub>2</sub> O)	Initial	<u>.75</u>	<u>.75</u>	<u>.75</u>
	Mid	<u>.75</u>	<u>.75</u>	<u>.75</u>
	Final	<u>.75</u>	<u>.75</u>	<u>.75</u>
	Avg	<u>.75</u>	<u>.75</u>	<u>.75</u>
Dry Gas Meter:	Final Vol	<u>562.705</u>	<u>568.265</u>	<u>573.887</u>
	Initial Vol	<u>557.400</u>	<u>562.900</u>	<u>568.600</u>
	Vol (V <sub>d</sub> ) (ft <sup>3</sup> ) (m <sup>3</sup> )	<u>5.305</u>	<u>5.365</u>	<u>5.287</u>
Dry Gas Meter	Temp (°F) : Inlet (T <sub>m</sub> )			
	Initial	<u>63</u>	<u>66</u>	<u>67</u>
	Mid	<u>66</u>	<u>68</u>	<u>69</u>
	Final	<u>67</u>	<u>68</u>	<u>70</u>
	Avg (°F/°A)	<u>65.3 (525.3)</u>	<u>67.3 (527.3)</u>	<u>68.6 (528.7)</u>
Dry Gas Meter	Temp (°F) : Outlet (T <sub>m</sub> )			
	Initial	<u>62</u>	<u>64</u>	<u>66</u>
	Mid	<u>63</u>	<u>65</u>	<u>67</u>
	Final	<u>64</u>	<u>65</u>	<u>67</u>
	Avg (°F/°A)	<u>63 (523)</u>	<u>64.7 (524.7)</u>	<u>66.7 (526.7)</u>
Avg Dry Gas	Meter Temp (T <sub>m</sub> - °F/°A)	<u>64.2 (524.2)</u>	<u>66.0 (526)</u>	<u>67.7 (527.7)</u>
	Time (minutes)	<u>10:19.31</u>	<u>10:23.03</u>	<u>10:18.47</u>

Note: If volume is in m<sup>3</sup>, multiply by 35.314667 to obtain ft<sup>3</sup>.  
 Note: Add 460° to all temperatures for degrees Absolute.



$$Y = \frac{(V_c)(MCF)(BP)(T_m)}{(V_d)(BP + \Delta h/13.6)(T_c)}$$

$$Y \text{ Factor \% Difference} = \frac{\text{Act} - \text{Exp}}{\text{Exp}} \times 100 \quad 511-M-72$$

Note: MCF = Meter Correction Factor (Y) for Dry Gas Meter used as a Transfer Standard

Run 1

$$Y = \frac{(0.9963)(5.211)(28.39)(524.2)}{(5.305)(28.39 + .75/13.6)(526.3)} = \frac{77,263.364}{79,419.462} = 0.97285$$

$$\Delta\% = (0.97285 - 1) \times 100 = -2.715\%$$

Run 2

$$Y = \frac{(0.9963)(5.265)(28.385)(526)}{(5.365)(28.385 + .75/13.6)(525.5)} = \frac{78,318.231}{80,131.520} = 0.97676$$

$$\Delta\% = (0.97676 - 1) \times 100 = -2.324\%$$

Run 3

$$Y = \frac{(0.9963)(5.204)(28.38)(527.7)}{(5.287)(28.38 + .75/13.6)(525.5)} = \frac{77,647.397}{79,001.895} = 0.98285$$

$$\Delta\% = (0.98285 - 1) \times 100 = -1.715\%$$

Note: The Y Factor % Difference must be < ±5.0% to be acceptable. Avg. Δ% = \_\_\_\_\_

**Determination of Interpolated Y Factor for Average Certification Test Series Δ H from Dry Gas Meter Calibration Data:**

(A) _____ inch H <sub>2</sub> O Δh =	(C) _____	Calculated Calibration Y Factor (from Calibration)
(B) _____ inch H <sub>2</sub> O Δh =	(D) _____	Calculated Calibration Y Factor (from Calibration)
_____ - _____ = _____ X 100 = _____		_____ / _____ = _____
(B)	(A)	(E) (D) (C) (E) (F)

$$\frac{\text{Avg } \Delta h}{(A)} \times 100 = (G)$$

$$\left[ \frac{(F)}{(G)} \times \frac{(C)}{(D)} \right] + \frac{(E)}{(D)} = \text{Interpolated Y Factor For Avg. Test Series } \Delta h$$

START: + 9.14  
STOP: + 9.14  
Δ 0.00

Dry Gas Meter Back Half Leak Check: 0.00 inch H<sub>2</sub>O in One Minute  
Front Half Leak Check                      Meter Reading                      Leak Rate

Meter	Vac In. Hg	Start	Stop	cmm	cfm
DGM	- 22.25	.992	.998		.006
TM	- 22.25	.925	.935		.010

RB

Dry Gas Meter Calibration Data

Date: 5/12/15 Technician: A.T. Myrman  
 Calibration Meter Mfr: Rockwell SN: 1052202 Y: 0.9963  
 Meter Box ID Room Blank Meter Mfr: Kimmom SN: 8000571  
 Electrical Check ok Pitot Leak Check N/A  
 Leak Check Front Half ok Back Half ok over  
 BP = 28.34 in. Hg

Orifice (Δh) in. H <sub>2</sub> O	Gas Volume			Temperature			Time (Θ), Min.	
		Cal. Meter (Vc), (cu.ft.)	Dry Gas Meter (Vm), (m <sup>3</sup> )(ft <sup>3</sup> )		Cal. Meter (Tc), °F	Dry Gas Meter		
						Inlet (Tmi), (°F)(°C)		Outlet (Tmo), (°F)(°C)
.115	initial	315.769	127.3690	initial	73	70	70	9:58.54
	final	320.996	127.5209	mid	72	73	71	9.976
				final	72	75	72	
	total	5.227	11519	avg.	72.3	72.7	71	71.83
.115			5.3643		532.3	532.7	531	531.8
.100	initial	322.240	127.5570	initial	72	74	72	12:11.75
	final	328.115	127.72755	mid	72	75	73	12.196
				final	72	76	73	
	total	5.875	117055	avg.	72	75	72.7	73.3
.100			6.0229		532	535	532.7	533.8
.130	initial	329.295	127.7600	initial	71.5	75	73	9:19.31
	final	334.505	127.9132	mid	72	77	73	9.322
				final	71.5	77	74	
	total	5.210	11532	avg.	71.7	76.3	73.3	74.8
.133			5.4102		531.7	536.3	533.3	534.8
	initial			initial				
	final			mid				
				final				
	total			avg.				
	initial			initial				
	final			mid				
				final				
	total			avg.				

$$Y = \frac{(Y)(Vc)(Pb)(Tm + 460)}{(Vm)(Pb + \Delta h/13.6)(Tc + 460)} \quad \Delta h @ = \frac{(0.0317)(\Delta h)}{Pb(Tmo + 460)} \quad [(Tc + 460)(\Theta)] / [(Vc)(Yc)]^2$$

# Back Half Leak Check

Start - 7.52" H<sub>2</sub>O

Stop - 7.52" H<sub>2</sub>O

0.00 Leak Rate

# Front Half Leak Check

mtz	Vac "Hg	mtz	Rdg	Leak Rate cmm	cfm
OGM	-20.5	.22635	.22645	.0001	
TM	-20.5	.740	.751	.011	

~~.400~~

.12

Room  
 Meter Box: Blank  
 Date: 5/12/15  
 Page: 2 of 3

Rev 6-10

Meter Box Calibration Page 2

AT Myron

$$Y = \frac{(Y_c)(V_c)(BP)(T_m + 460)}{(V_m)(BP + \Delta H/13.6)(T_c + 460)} =$$

$$Y = \frac{(.9963)(5.227)(28.34)(71.8 + 460)}{(5.3643)(28.34 + .115/13.6)(72.3 + 460)} = \frac{78,485.749}{80,946.660} = 0.96950$$

$$Y = \frac{(.9963)(5.875)(28.34)(73.8 + 460)}{(6.0219)(28.34 + .100/13.6)(72 + 460)} = \frac{88,547.523}{90,830.101} = 0.97487$$

$$Y = \frac{(.9963)(5.270)(28.34)(74.8 + 460)}{(5.4102)(28.34 + .133/13.6)(71.7 + 460)} = \frac{79,577.311}{81,551.070} = 0.97580$$

$$Y = \frac{(\quad)(\quad)(\quad)(\quad + 460)}{(\quad)(\quad + \quad/13.6)(\quad + 460)} = \quad = \quad$$

$$Y = \frac{(\quad)(\quad)(\quad)(\quad + 460)}{(\quad)(\quad + \quad/13.6)(\quad + 460)} = \quad = \quad$$

Y Factor                      Variation      (± 0.02 Allowed From Average Y)

0.96960                      -0.00382

0.97487                      +0.00145

0.97580                      +0.00238

\_\_\_\_\_

\_\_\_\_\_

Avg Y 0.97342

2.92027

$$\Delta H\theta = \frac{(0.0317)(\Delta H)}{(Pb)(T_{mo} + 460)} \cdot \left[ \frac{(T_w + 460)(\theta)}{(Y_c)(V_c)} \right]^2 =$$

$$\Delta H\theta = \frac{(0.0317)(.115)}{(2834)(71 + 460)} \cdot \left[ \frac{(723 + 460)(9.976)}{(1.9963)(5.227)} \right]^2 = .25189$$

$$\Delta H\theta = \frac{(0.0317)(.100)}{(2834)(727 + 460)} \cdot \left[ \frac{(72 + 460)(12196)}{(1.9963)(5.875)} \right]^2 = .25801$$

$$\Delta H\theta = \frac{(0.0317)(.133)}{(2834)(737 + 460)} \cdot \left[ \frac{(717 + 460)(9.322)}{(1.9963)(5.270)} \right]^2 = .24859$$

$$\Delta H\theta = \frac{(0.0317)(\quad)}{(\quad)(\quad + 460)} \cdot \left[ \frac{(\quad + 460)(\quad)}{(\quad)(\quad)} \right]^2 = \underline{\quad}$$

$$\Delta H\theta = \frac{(0.0317)(\quad)}{(\quad)(\quad + 460)} \cdot \left[ \frac{(\quad + 460)(\quad)}{(\quad)(\quad)} \right]^2 = \underline{\quad}$$

<u><math>\Delta H\theta</math></u>	<u>VARIATION (<math>\pm 0.20</math> ALLOWED)</u>
<u>.25189</u>	<u>- .00094</u>
<u>.25801</u>	<u>+ .00518</u>
<u>.24859</u>	<u>- .00424</u>
<u>          </u>	<u>          </u>
<u>          </u>	<u>          </u>
<u>AVG <math>\Delta H\theta</math></u>	<u>.25283</u>

.75849

Post Test  
 Meter Box Audit  
 Woodstove Data Sheet #32

RB  
 T3

Unit: Hwy Tech 111120  
 Date: 013/15  
 Technician: 77M ESS  
 WST9-Form2, Rev 6/11

Meter Box Calibration Audit  
 Test Data

Run #	1	2	3	4	5	6	7	8	9	10
Avg. Δh	.115									
Max Vac	-1.50									

Avg. Test Series Δh: .115 in H<sub>2</sub>O. Test Series Max Vac: -1.50 in Hg

Audit Dry Gas Meter Mfr: Rockwell SN: 1052202 Correction Factor (Y): 0.9963  
 Test Dry Gas Meter Mfr: Rockwell SN: 322914 Correction Factor (Y): 0.9685

Audit Data

		Audit #1	Audit #2	Audit #3
BP ("Hg):		<u>28.375</u>	<u>28.365</u>	<u>28.340</u>
Vac ("Hg):		<u>-1.50</u>	<u>-1.50</u>	<u>-1.50</u>
Audit Meter:	Final Vol	<u>521.7385</u>	<u>527.324</u>	<u>533.062</u>
	Initial Vol	<u>516.0750</u>	<u>521.941</u>	<u>527.802</u>
	Vol (V <sub>c</sub> , Ft <sup>3</sup> )	<u>5.6635</u>	<u>5.383</u>	<u>5.260</u>
Audit Meter	Temp (°F) (T <sub>c</sub> )			
	Initial	<u>66.5</u>	<u>67</u>	<u>67.5</u>
	Mid	<u>66.5</u>	<u>67.5</u>	<u>68.5</u>
	Final	<u>66.5</u>	<u>67.5</u>	<u>68.5</u>
	Avg (°F/°A)	<u>66.5 (526.5)</u>	<u>67.3 (527.3)</u>	<u>68.2 (528.2)</u>
Δh ("H <sub>2</sub> O)	Initial	<u>.115</u>	<u>.115</u>	<u>.115</u>
	Mid	<u>.115</u>	<u>.115</u>	<u>.115</u>
	Final	<u>.115</u>	<u>.115</u>	<u>.115</u>
	Avg	<u>.115</u>	<u>.115</u>	<u>.115</u>
Dry Gas Meter:	Final Vol	<u>144.8939</u>	<u>145.0561</u>	<u>145.2228</u>
	Initial Vol	<u>144.7290</u>	<u>144.9000</u>	<u>145.0700</u>
	Vol (V <sub>d</sub> ) (ft <sup>3</sup> ) (m <sup>3</sup> )	<u>11649.58234</u>	<u>1561.55126</u>	<u>1528.53961</u>
Dry Gas Meter	Temp (°F) : Inlet (T <sub>m</sub> )			
	Initial	<u>68</u>	<u>69</u>	<u>69</u>
	Mid	<u>68</u>	<u>69</u>	<u>70</u>
	Final	<u>68</u>	<u>69</u>	<u>70</u>
	Avg (°F/°A)	<u>68 (528)</u>	<u>69 (529)</u>	<u>69.7 (529.7)</u>
Dry Gas Meter	Temp (°F) : Outlet (T <sub>m</sub> )			
	Initial	<u>68</u>	<u>68</u>	<u>69</u>
	Mid	<u>68</u>	<u>69</u>	<u>69</u>
	Final	<u>68</u>	<u>69</u>	<u>70</u>
	Avg (°F/°A)	<u>68 (528)</u>	<u>68.7 (528.7)</u>	<u>69.3 (529.3)</u>
Avg Dry Gas	Meter Temp (T <sub>m</sub> - °F/°A)	<u>68 (528)</u>	<u>68.8 (528.8)</u>	<u>69.5 (529.5)</u>
	Time (minutes)	<u>11:21.90</u>	<u>10:35.44</u>	<u>10:19.13</u>

Note: If volume is in m<sup>3</sup>, multiply by 35.314667 to obtain ft<sup>3</sup>.  
 Note: Add 460° to all temperatures for degrees Absolute.

$$Y = \frac{(V_c)(MCF)(BP)(T_m)}{(V_d)(BP + \Delta h/13.6)(T_c)}$$

$$Y \text{ Factor \% Difference} = \frac{\text{Act} - \text{Exp}}{\text{Exp}} \times 100$$

RB-73

Note: MCF = Meter Correction Factor (Y) for Dry Gas Meter used as a Transfer Standard

**Run 1**

$$Y = \frac{(0.9963)(5.6635)(28.375)(528)}{(5.8234)(28.375 + .115/13.6)(526.5)} = \frac{84,536.610}{87,024,246} = 0.97141$$

$$\Delta\% = (0.97141 - \text{---}) \times 100 = \text{---}\%$$

**Run 2**

$$Y = \frac{(0.9963)(5.383)(28.365)(528.8)}{(5.8126)(28.365 + .115/13.6)(527.3)} = \frac{80,443.090}{82,475.791} = 0.97535$$

$$\Delta\% = (0.97535 - \text{---}) \times 100 = \text{---}\%$$

**Run 3**

$$Y = \frac{(0.9963)(5.260)(28.340)(529.5)}{(5.8961)(28.340 + .115/13.6)(528.2)} = \frac{78,565.412}{80,799.336} = 0.97235$$

$$\Delta\% = (\text{---} - \text{---}) \times 100 = \text{---}\%$$

Note: The Y Factor % Difference must be < ±5.0% to be acceptable. Avg. Δ% = \_\_\_\_\_

**Determination of Interpolated Y Factor for Average Certification Test Series Δ H from Dry Gas Meter Calibration Data:**

_____ inch H <sub>2</sub> O Δh = _____	Calculated Calibration Y Factor
(A)	(C) (from Calibration)
_____ inch H <sub>2</sub> O Δh = _____	Calculated Calibration Y Factor
(B)	(D) (from Calibration)
_____ - _____ = _____ X 100 = _____	_____ - _____ = _____ / _____ = _____
(B) (A)	(E) (D) (C) (E) (F)

$$\frac{\text{Avg } \Delta h}{(A)} = \text{---} \times 100 = \text{---} (G)$$

Time 1:00 min  
Start 9.190  
Stop 9.190  
Δ .000

$$\left[ \frac{(F) \times (G)}{(A)} \right] + \frac{\text{---}}{(C)} = \text{---} = \text{Interpolated Y Factor For Avg. Test Series } \Delta h$$

Dry Gas Meter Back Half Leak Check: \_\_\_\_\_ inch H<sub>2</sub>O in One Minute  
Front Half Leak Check \_\_\_\_\_ Meter Reading \_\_\_\_\_ Leak Rate

Meter	Vac In. Hg	Start	Stop	cmm	cfm
DGM	-21.0	.9870	.9870	.0000	.000
TM	-21.0	.825	.833		.008

**APEX INSTRUMENTS REFERENCE METER VERIFICATION  
USING WET-TEST METER #11AE6  
2-POINT ENGLISH UNITS**

Calibration Meter Information	
WTM Model #	AL20
WTM Serial #	11AE6
WTM Gamma	0.9999
Original 15Pt Gamma	0.9963

Calibration Conditions			
Date	Time	13-Mar-15	2:00
Barometric Pressure		30.05	in Hg
Calibration Tech		EW	
DGM Serial Number		S-110-1052202	

Factors/Conversions		
Std Temp	528	°R
Std Press	29.92	in Hg
K <sub>1</sub>	17.647	°R/in Hg

Calibration Data											Results			
Run Time	Metering Console				Calibration Meter						Dry Gas Meter			
	DGM Input Pressure	Volume Initial	Volume Final	Volume Sample	Outlet Temp		Volume Initial	Volume Final	Volume Sample	Outlet Temp		Calibration Factor		Flowrate
Elapsed	(P <sub>m</sub> )	(V <sub>ni</sub> )	(V <sub>mf</sub> )	(V <sub>ns</sub> )	Initial	Final	(V <sub>wi</sub> )	(V <sub>wf</sub> )	(V <sub>ns</sub> )	Initial	Final	Previous	Current	Std & Corr
(θ)	(P <sub>m</sub> )	(V <sub>ni</sub> )	(V <sub>mf</sub> )	(V <sub>ns</sub> )	(t <sub>ni</sub> )	(t <sub>mf</sub> )	(V <sub>wi</sub> )	(V <sub>wf</sub> )	(V <sub>ns</sub> )	(t <sub>ni</sub> )	(t <sub>mf</sub> )	(Y)	(Y)	(Q <sub>meas</sub> (corr))
min	in H <sub>2</sub> O	cubic feet	cubic feet	cubic feet	°F	°F	cubic feet	cubic feet	cubic feet	°F	°F			cfm
6.00	-3.7	253.732	259.811	6.079	73.4	73.4	731.750	737.710	5.960	71	71	0.9963	0.9939	0.992
												Variation	0.25%	must be less than 1.5%
10.00	-2.2	259.811	265.431	5.620	73.4	73.4	737.710	743.240	5.530	71	71	0.9964	0.9938	0.552
												Variation	0.26%	must be less than 1.5%

I certify that the above Dry Gas Meter was calibrated in accordance with USEPA Methods, CFR 40 Part 60, App A, Method 5, Paragraph 7.1.2.2, using the Precision Wet Test Meter # 11AE6, which in turn was calibrated using the American Bell Prover # 3785, certificate # F107, which is traceable to the National Bureau of Standards (N.I.S.T.).

Signature



Date

3/13/15



**APEX INSTRUMENTS REFERENCE METER CALIBRATION**  
**USING WET-TEST METER #11AE6**  
**15-POINT ENGLISH UNITS**

Calibration Meter Information	
WTM Model #	AL-20
WTM Serial #	11AE6
WTM Gamma	0.9999

Calibration Conditions			
Date	Time	18-Feb-14	9:15
Barometric Pressure		29.8	in Hg
Calibration Technician		EW	
DGM Serial Number		S-110-1052202	

Factors/Conversions		
Std Temp	528	°R
Std Press	29.92	in Hg
K <sub>1</sub>	17.647	°R/in Hg

Calibration Data													Results		
Run Time	Dry Gas Meter						Calibration Meter						Dry Gas Meter		
	Elapsed	Meter Pressure	Volume Initial	Volume Final	Sample Volume	Outlet Temp	Outlet Temp	Volume Initial	Volume Final	Sample Volume	Outlet Temp	Outlet Temp	Calibration Factor	Variation	Flowrate
(9)	(P <sub>m</sub> )	(V <sub>m</sub> )	(V <sub>m</sub> )	(V <sub>m</sub> )	(T <sub>m</sub> )	(T <sub>m</sub> )	(V <sub>m</sub> )	(V <sub>m</sub> )	(V <sub>m</sub> )	(T <sub>m</sub> )	(T <sub>m</sub> )	(Y)	(ΔY)	(Q <sub>avg</sub> (cm))	
min	in H <sub>2</sub> O	cubic feet	cubic feet	cubic feet	°F	°F	cubic feet	cubic feet	cubic feet	°F	°F			cfm	
5	-5.1	657.117	663.335	6.218	73.4	73.4	677.080	683.140	6.060	68.0	68.0	0.9970	0.00149	1.21	
5	-5.1	663.335	669.550	6.215	73.4	73.4	683.140	689.180	6.040	68.0	68.0	0.9942	-0.00133	1.20	
5	-5.1	669.550	675.768	6.218	73.4	73.4	689.180	695.230	6.050	68.0	68.0	0.9954	-0.00016	1.21	
Passed Calibration Factor												0.9955	Averages	1.21	

6	-3.7	694.023	699.987	5.964	75.2	75.2	713.145	718.970	5.825	68.0	68.0	0.9990	0.00269	0.97
6	-3.7	699.987	705.997	6.010	75.2	75.2	718.970	724.820	5.850	68.0	68.0	0.9956	-0.00071	0.97
6	-3.7	705.997	712.025	6.028	75.2	75.2	724.820	730.680	5.860	68.0	68.0	0.9944	-0.00198	0.97
Passed Calibration Factor												0.9963	Averages	0.97

7	-2.8	712.025	717.674	5.649	75.2	75.2	730.680	736.190	5.510	68.0	68.0	0.9955	0.00082	0.78
7	-2.8	717.674	723.317	5.643	75.2	75.2	736.190	741.690	5.500	68.0	68.0	0.9947	0.00007	0.78
7	-2.8	723.317	728.975	5.658	75.2	77.0	741.690	747.190	5.500	68.0	68.0	0.9938	-0.00090	0.78
Passed Calibration Factor												0.9947	Averages	0.78

10	-2.0	728.975	734.645	5.670	77.0	77.0	747.190	752.730	5.540	68.0	68.0	0.9986	0.00215	0.55
10	-2.0	734.645	740.312	5.667	77.0	77.0	752.730	758.260	5.530	68.0	68.0	0.9973	0.00088	0.55
10	-2.0	740.312	745.991	5.679	77.0	77.0	758.260	763.780	5.520	68.0	68.0	0.9934	-0.00303	0.55
Passed Calibration Factor												0.9964	Averages	0.55

15	-1.9	675.768	681.868	6.100	73.4	75.2	695.230	701.215	5.985	68.0	68.0	0.9974	-0.00135	0.40
15	-1.9	681.868	687.947	6.079	75.2	75.2	701.215	707.180	5.965	68.0	68.0	0.9992	0.00043	0.40
15	-1.9	687.947	694.023	6.076	75.2	75.2	707.180	713.145	5.965	68.0	68.0	0.9997	0.00092	0.40
Passed Calibration Factor												0.9988	Averages	0.40

Overall Average Y **0.9963**

Note: For Calibration Factor Y, the ratio of the reading of the calibration meter to the dry gas meter, acceptable tolerance of individual values from the average is ±0.02.

I certify that the above Dry Gas Meter was calibrated in accordance with USEPA Methods, CFR 40 Part 60, using the Precision Wet Test Meter # 11AE6, which in turn was calibrated using the American Bell Prover # 3785, certificate # F107, which is traceable to the National Bureau of Standards (N.I.S.T.).

Signature

*Eric Webb*

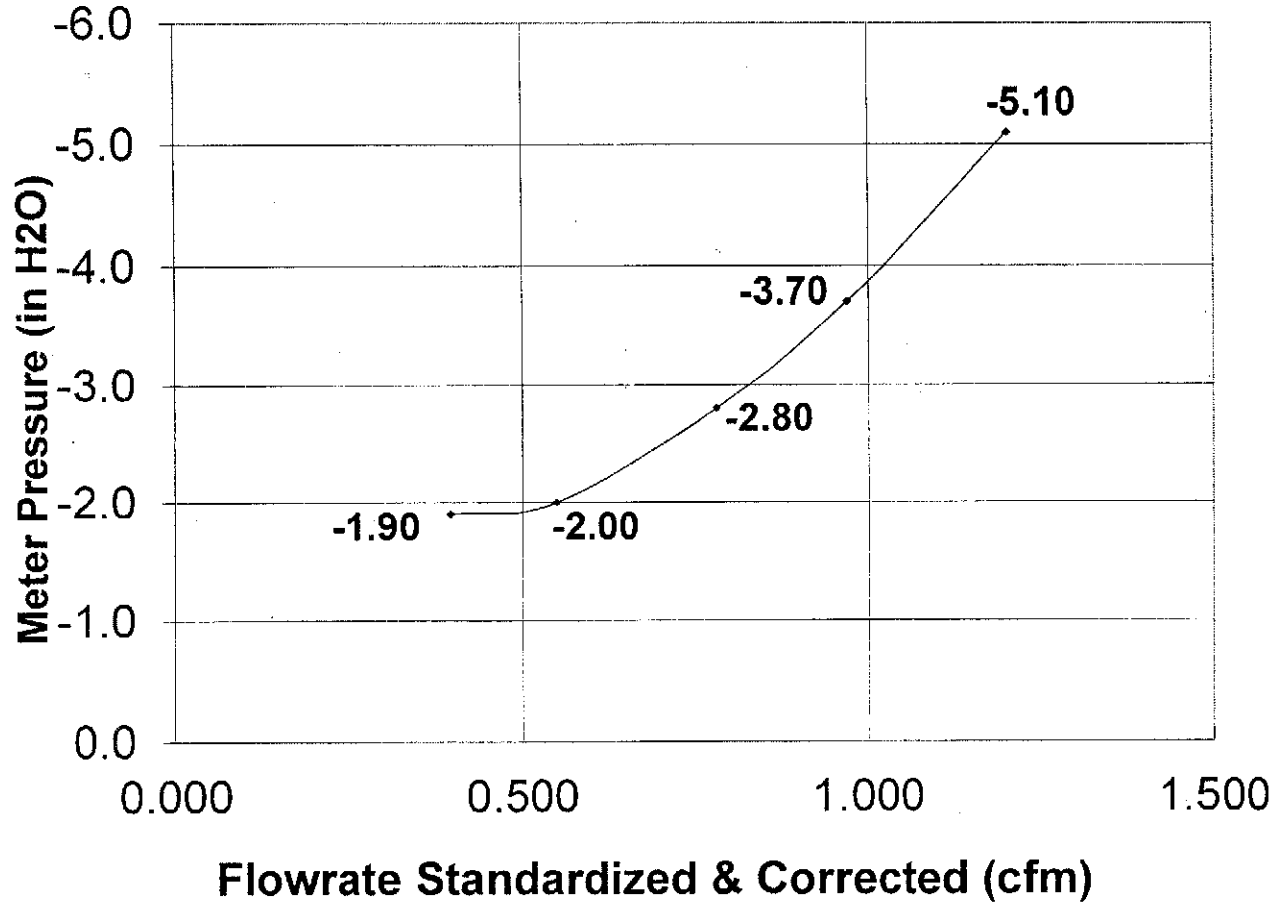
Date

2/18/14

Calibration Date: 2-18-2014

Calibration Technician:

### Meter Pressure vs Flowrate



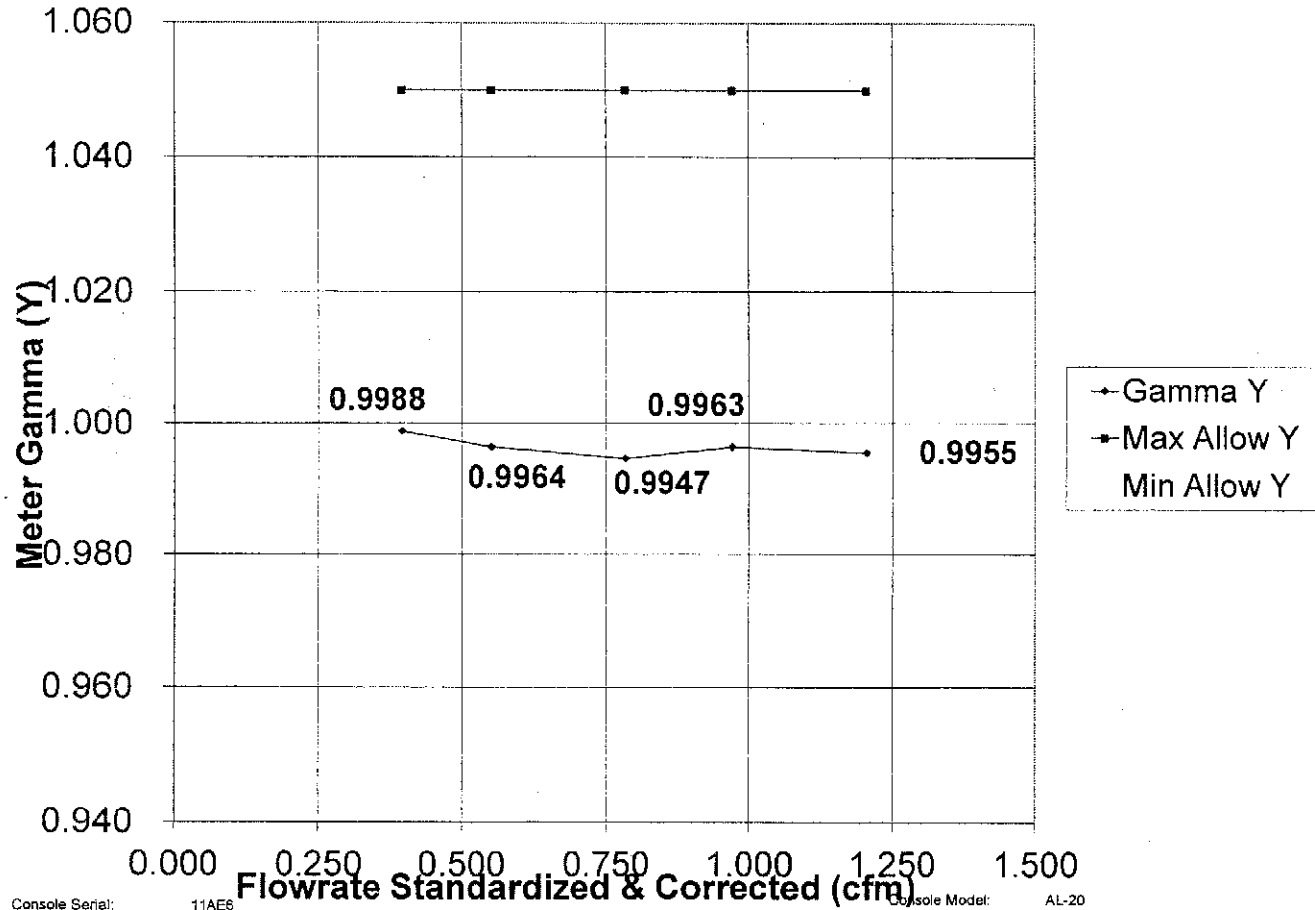
Console Serial: 11AE6

Console Model: AL-20

Calibration Date: 2-18-2014

Calibration Technician: EW

### Meter Gamma vs Flowrate



Console Serial: 11AE6

Console Model: AL-20

## VANEOMETER CALIBRATION

Myren Consulting used a Dwyer Model 3480 Vaneometer to measure test chamber air velocity. The manufacturer's specifications for accuracy are  $\pm 5.0\%$  from 0 to 100 fpm and  $\pm 10\%$  from 100 to the top of the scale. Myren Consulting insures that the instrument is level and clean prior taking each reading. According to EPA personnel (Westlin, RTP) no further calibration is necessary.

## DRAFT GUAGE CALIBRATION

Myren Consulting used a Dwyer Model 115 AV, a -0.05 - 0.0 - 0.25" inclined red oil manometer (readability resolution  $\pm 0.001"$  H<sub>2</sub>O) to measure the static pressure in the stack. Once leveled and zeroed as per the manufacturer's written operating instructions, the Dwyer manometer is a primary standard and needs no further calibration.

The manometer is leveled and zeroed at the start of each test, checked as necessary during a run to verify that the settings have not changed and again at the end of each test run. The results of these checks are recorded on Woodstove Data Sheet #16 in each individual test.

## BAROMETER CALIBRATION

Myren Consulting used a Princo Model 453 SN W14275 Mercury barometer and a Weems and Plath aneroid barometer to measure the barometric pressure (BP). The Weems and Plath barometer was calibrated daily by comparing it to the Princo and adjusting it as necessary. The Princo when calibrated following the manufacturer's instructions is a primary standard and needs no further calibration.

## MOISTURE METER CALIBRATION

Myren Consulting uses a Delmhorst J-2000 which was calibrated daily using the "Check" feature. Then the operation of the moisture meter was checked with a Delmhorst Moisture Content Standard Model MCS-1 at 12.6 and 23.8%. The results of these checks are recorded on Data Sheet #10.

The readings obtained with the moisture meter are then corrected as per the manufacturer's written instructions for temperature. If Delmhorst #496 insulated pins are used, the meter is set at 222 using the Set Pin Calibration instructions. The meter is set at 1 for the Species correction. 1 is the setting for D. Fir

WOODSTOVE DATA SHEET #26-A  
 CEM GAS TRAIN RESPONSE TIME  
 PRE CERTIFICATION TEST SERIES CHECK

Date	5/13/15										
Technicians	ATM										
Elapsed Time	CO <sub>2</sub> Conc.(V)	CO <sub>2</sub> Conc.(V)	CO <sub>2</sub> Conc.(V)	CO Conc.(V)	CO Conc.(V)	CO Conc.(V)	O <sub>2</sub> Conc.(V)	O <sub>2</sub> Conc.(V)	O <sub>2</sub> Conc.(V)	Conc.(V)	Conc.(V)
0 Seconds	.486	.484	.480	.156	.158	.159					
15	.486	.485	.480	.155	.158	.159					
30	.291	.290	.288	.149	.150	.151					
45	.106	.102	.101	.060	.061	.061					
60	.046	.048	.047	.043	.043	.044					
75	.008	.009	.008	.032	.031	.031					
90	.004	.006	.004	.005	.005	.006					
105	.003	.004	.002	.002	.002	.003					
120	.001	.001	.001	.001	.001	.001					
135	.001	.001	.001	.000	.001	.001					
150	.000	.001	.000	.000	.001	.001					
165	.000	.000	.000	.000	.000	.001					
180	.000	.000	.000	.000	.000	.000					
Initial Response Time (Seconds)	N 286	N 295	N 295	> 30, < 45	7 30, < 45	7 30, < 45					
95% Response Time (Seconds)	> 60 < 75	> 60 < 75	7 60 < 75	> 75 < 90	7 75 < 90	7 75 < 90					
Analyzer Flow Rate	1.90 ft <sup>3</sup> /min										

Comments

95% drop  
 .024 .024 .024 .008 .008 .008

Pre Heat Test  
HTP 26 Bay

CO<sub>2</sub> Analyzer

Multipoint Calibration Report Form

Site: Myren Lab, Colville, WA Date: 7/30/15

Analyzer: Make: Horiba Model: PIR 2000 SN: 607204

Calibration by: A.T. Myren

Cal Gas Flow: 1.5 scfh Measured by: Rotameter: X Mass Flowmeter: \_\_\_\_\_

BP: 28.625 "Hg Instrument ID: Princo

Temp: 64 °F Instrument ID: Omega Digicator

Analyzer Last Calibrated: 7/28/15 By: A.T. Myren

Cylinders:  
ITM 0003 / "

1. # \_\_\_\_\_ Concentration: 0.00 %CO<sub>2</sub> Cyl. Press.: 220 psi.

Certified By: Oxarc Date: 6/11/12

2. # FB-0019810 Concentration: 12.4 %CO<sub>2</sub> Cyl. Press.: 220 psi.

Certified by: Liquid Technology Corp Date: 4/25/12

3. # 250-1175 Concentration: 21.0 %CO<sub>2</sub> Cyl. Press.: 680 psi.

Certified by: Oxarc Date: 8/22/97

4. # 5X-40585 Concentration: 6.04 %CO<sub>2</sub> Cyl. Press.: 1320 psi.

Certified by: Matheson Tri Gas Date: 4/12/10

Analyzer: Calibrated Range: 0-25 % Output: 0-1.0 v.

Flow: 1.5 scfh Measured by: Rotameter: X Mass Flowmeter: \_\_\_\_\_

Span Valve = 25.0%  
2% of Span Valve = 0.500%

Calibration Results

Point #	Cyl. #	% CO <sub>2</sub>	Expected		Actual		Adj.		% Dif.	Curve Conc.	Potentiometer	
			Meter	DVM	Meter	DVM	Meter	DVM			Unadj.	Adj.
1	1	0.00	00.0	000	00.0	000	-	-		+0.13	4.90	-
2	2	12.4	49.6	496	48.5	493	48.75	496		+0.23	6.92	6.98
3	3	21.0	84.0	840	82.5	839				+0.002		
4	4	6.04	24.2	242	23.5	238				-1.00		
5	1	0.00	00.0	000	00.0	000				+0.13		

Comments:

0.000 V = 0.0316170 %CO<sub>2</sub> = +0.0316

0.446 V = 12.4280009 = +0.0280

0.839 V = 21.0005002 = +0.0005

0.238 V = 5.9798319 = -0.0601

HJP 26 Bay

### Linear Regression Results

$$Y = MX + B$$

Slope M = 0.0400108

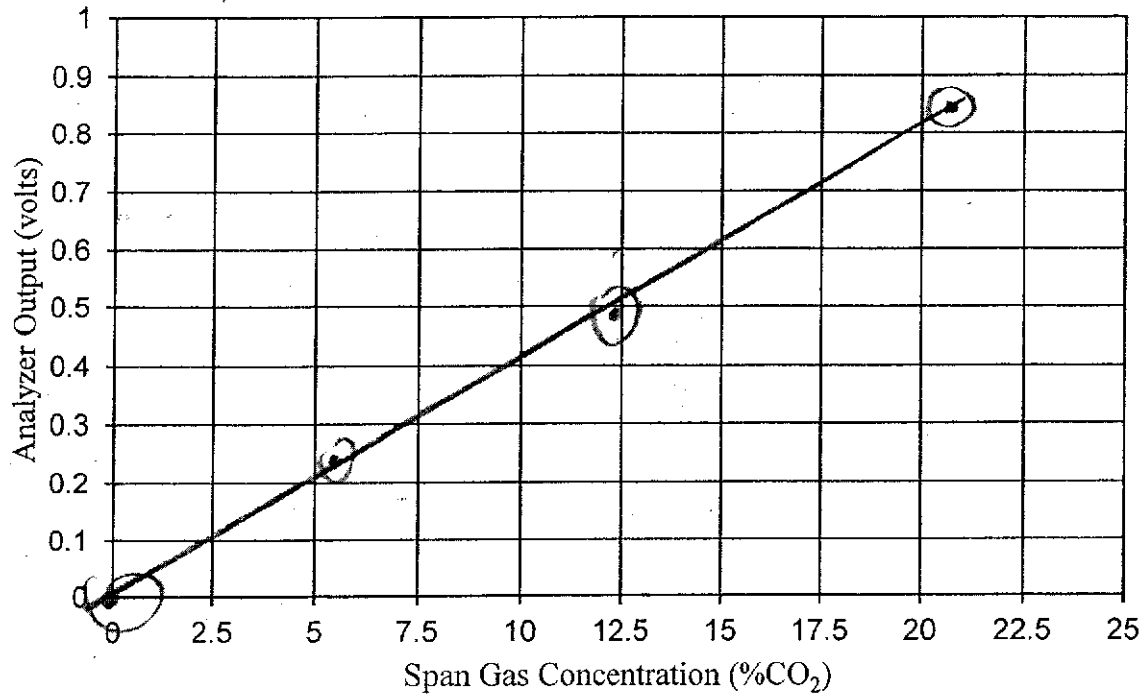
Y Intercept (B) = -0.0012563

Correlation Coefficient (r) 0.9999389

Analyzer: Horiba PIR 2000

SN: 607204

Date: 7/30/15



**Comments:**

Pre HERTech  
HJP 26 Bay

CO Analyzer

Multipoint Calibration Report Form

Site: EPA Lab, Colville, WA

Date: 7/30/15

Analyzer: Make: Horiba

Model: MEXA 311-GE

SN: GE-30075

Calibration by: A.T. Myren

Cal Gas Flow: 1.5scfh Measured by: Rotameter: X Mass Flowmeter: \_\_\_\_\_

BP: 28.625 °Hg Instrument ID: Princo

Temp: 64 °F Instrument ID: Omega Digicator

Analyzer Last Calibrated: 7/28/15 By: A.T. Myren

Cylinders:  
ITM 8803/11

1. # \_\_\_\_\_ Concentration: 0.00 %CO Cyl. Press.: 220 psi.

Certified By: Oxarc Date: 6/11/12

2. # F8-0019810 Concentration: 2.57 %CO Cyl. Press.: 220 psi.

Certified by: Liquid Technology Corp Date: 4/25/12

3. # 250-1175 Concentration: 4.03 %CO Cyl. Press.: 680 psi.

Certified by: Oxarc Date: 8/22/97

4. # 5X-40585 Concentration: 1.29 %CO Cyl. Press.: 1320 psi.

Certified by: Matheson Tri Gas Date: 4/12/10

Analyzer: Calibrated Range: 0-5.0 % Output: 0-1.0 v. For 0-10.00 %

Flow: 1.50 CFH Measured by: Rotameter: X Mass Flowmeter: \_\_\_\_\_

Calibration Results 2% of Span Value = 0.100% CO

Point #	Cyl. #	% CO	Expected		Actual		Adj.		Curve Conc.	% Dif.	Potentiometer	
			Meter	DVM	Meter	DVM	Meter	DVM			Unadj.	Adj.
1	1	0.00	-	1.000	-	1.002	-	-		+0.57	-	-
2	2	2.57	-	2.57	-	2.56	-	2.57		-0.95	-	-
3	3	4.03	-	4.03	-	4.11	-			+0.59		
4	4	1.29	-	1.29	-	1.26	-			-2.13		
5	1	0.00	-	1.000	-	1.000	-			+0.57		

Comments: The meter on the instrument is broken and unreparable. Man ba no longer has the part.

0.000 V = 0.0283233 % CO +.0283  
0.257 V = 2.5454690 % CO -.0245  
0.411 V = 4.0537975 % CO +.0238  
0.126 V = 1.2624108 % CO -.0236

us. 10



Pre Heat Tech HTP 26 Bny

### Linear Regression Results

$$Y = MX + B$$

Slope M = 0.1020686

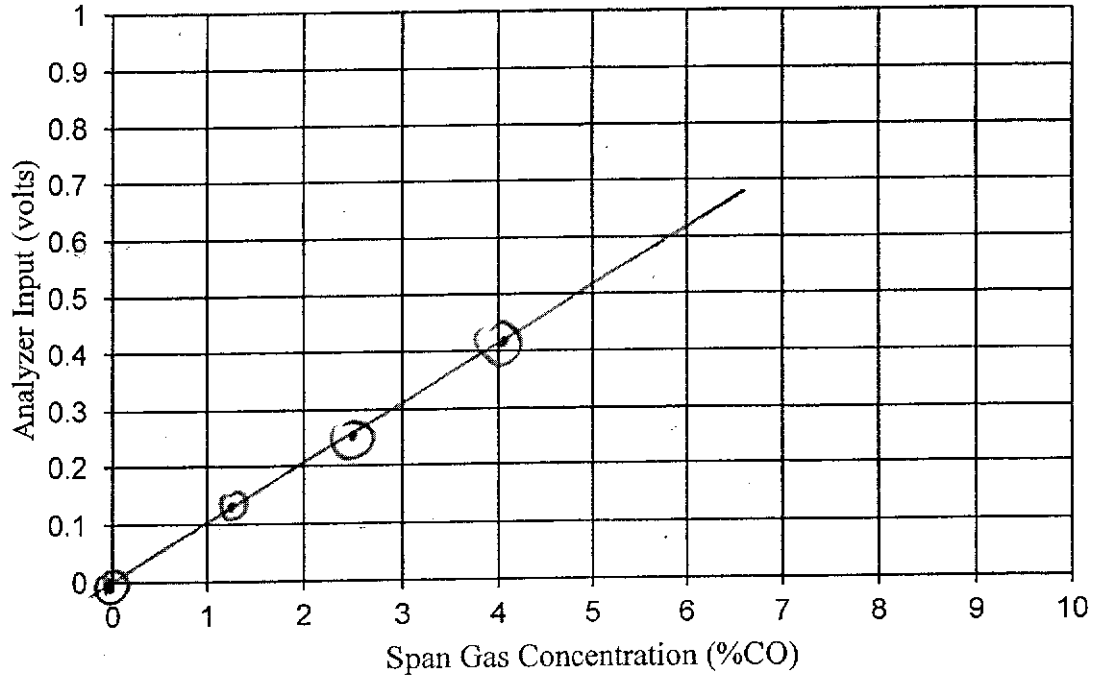
Y Intercept (B) = -0.0028303

Correlation Coefficient (r) 0.9998473

Analyzer: Horiba Mexa 311-GE

SN: GE-30075

Date: 7/30/15



Comments:



# LIQUID TECHNOLOGY CORPORATION

"INDUSTRY LEADER IN SPECIALTY GASES"

## Certificate of Analysis - EPA PROTOCOL GAS -

Customer OXARC (Colville, WA)  
Date April 25, 2012  
Delivery Receipt DR-42051  
Gas Standard 2.50% CO, 12.5% Carbon Dioxide/Nitrogen - EPA PROTOCOL  
Final Analysis Date April 25, 2012  
Expiration Date April 25, 2015

**DO NOT USE BELOW 150 psig**

### Cylinder Data

Cylinder Serial Number: EB-0019810 Cylinder Outlet: CGA 350  
Cylinder Volume: 133 Cubic Feet Cylinder Pressure: 1900 psig, 70°F  
Expiration Date: April 25, 2015

### Analytical Data

EPA Protocol, Section No. 2.2, Procedure G-1

### Replicate Concentrations

**Carbon Monoxide: 2.57% +/- 0.02%**

**Carbon Dioxide: 12.4% +/- 0.12%**

**Nitrogen: Balance**

### Reference Standard(s):

SRM/GMIS:	GMIS	GMIS
Cylinder Number:	CC-166392	CC-125534
Concentration:	2.48% CO/Nitrogen	13.32% CO2/Nitrogen
Expiration Date:	04/18/14	10/14/12

### Certification Instrumentation

Component:	Carbon Monoxide	Carbon Dioxide
Make/Model:	Horiba - VIA 510	Horiba - VIA 510
Serial Number:	4344482008	SN075GSF
Principal of Measurement:	NDIR	NDIR
Last Calibration:	April 06, 2012	April 06, 2012

Analytical uncertainty and NIST Traceability are in compliance with EPA-600/R-97/121.

Certified by:

  
Adam Strickland

PGVP Vendor ID: E12012

"UNMATCHED EXCELLENCE"



# MATHESON TRI-GAS

ask. . . The Gas Professionals™

## Certificate of Analysis - EPA Protocol Mixtures

1650 Enterprise Parkway  
Twinsburg, Ohio 44087  
215-648-4000

Customer: OXARC INC  
Cylinder Number: SX-40586  
Cylinder pressure: 1600 psig  
Last Analysis date: 4/9/2010  
Expiration Date: 3/18/2013

Protocol: Reference # Lot #  
G1 519323 109-96-17643

**DO NOT USE THIS CYLINDER WHEN THE PRESSURE FALLS BELOW 150 PSIG**

### REPLICATE RESPONSES

Component	Certified Conc	Date	Response 1	Response 2	Response 3	Date	Response 1	Response 2	Response 3
Oxygen	5.98% ± 1% REL	3/18/2010	5.98%	5.98%	5.99%				
Carbon Dioxide	6.04% ± 1% REL	3/18/2010	6.03%	6.07%	6.01%				
Carbon Monoxide	1.29% ± 1% REL	4/2/2010	1.30%	1.30%	1.30%	4/9/2010	1.29%	1.28%	1.29%

ANCE GAS: Nitrogen

### REFERENCE STANDARDS

Component	SRM #	Sample #	Cylinder #	Concentration	Component	SRM #	Sample #	Cylinder #	Concentration
Oxygen	NTRM-82658	01110212	SX-20658	10.09%	Carbon Dioxide	SRM-1674b	7-F-05	CAL-014611	6.876 %
					Carbon Monoxide	SRM-2639a	54-D-51	CAL-013889	0.991 %

### CERTIFICATION INSTRUMENTS

Component	Make/Model	Serial Number	Measurement Principle	Last Calibration	Component	Make/Model	Serial Number	Measurement Principle	Last Calibration
Oxygen	Rosemount 755	2002832	Paramagnetic	2/26/2010	Carbon Dioxide	Varian 3800 GC	LR-92489	TC, FID	3/16/2010
					Carbon Monoxide	Varian 3800 GC	LR-92489	TC, FID	4/2/2010

Notes: T134744

This certification was performed according to EPA Traceability Protocol for Assay & Certification of Gaseous Calibration Standards September 1997, using procedure G1 and/or G2.

Analyst Philip D. Monti Date 4/12/2010

WELDING PRODUCTS  
 INDUSTRIAL SUPPLIES  
 INDUSTRIAL GASES  
 MEDICAL GASES



SPECIALTY GASES  
 BEVERAGE SYSTEMS  
 SAFETY PRODUCTS  
 FIRE EQUIPMENT

WWW.OXARC.COM

**MAIN OFFICE**

SPOKANE, WA 99220  
 4003 E. BROADWAY  
 P.O. BOX 2605  
 (509) 535-7794  
 FAX (509) 535-0388

BOISE, ID 83709  
 7615 W. LEMHI ST.  
 (208) 376-0377  
 FAX (208) 376-1133

COEUR D'ALENE, ID 83814  
 3530 RAMSEY RD.  
 (208) 765-3311  
 FAX (208) 667-5874

COLVILLE, WA 99114  
 328 W. 1ST.  
 (509) 684-3776  
 FAX (509) 684-8742

ELLENSBURG, WA 99828  
 704 N. WENAS  
 (509) 925-1518  
 FAX (509) 925-1136

HERMISTON, OR 97838  
 HERMISTON-  
 McNARY HWAY  
 (503) 567-7377  
 FAX (503) 567-2285

KENNEWICK, WA 99336  
 800 W. COLUMBIA DR.  
 (509) 582-4202  
 FAX (509) 586-9859

LEWISTON, ID 83601  
 2513 3RD. AVE., NORTH  
 (208) 743-6571  
 FAX (208) 748-8374

MOSES LAKE, WA 98837  
 1401 WHEELER ROAD  
 (509) 765-9247  
 FAX (509) 768-9958

OKANOGAN, WA 98840  
 2256 ELMWAY  
 (509) 826-3205  
 FAX (509) 826-3905

PASCO, WA 99302  
 716 SOUTH OREGON  
 (509) 547-2494  
 FAX (509) 547-3103

TWIN FALLS, ID 83303  
 729 COMMERCIAL AVE.  
 (208) 734-9711  
 FAX (208) 734-7923

NATCHEE, WA 98801  
 HME GARDENS RD.  
 (509) 662-8417  
 FAX (509) 662-1229

YAKIMA, WA 98903  
 1004 EAST MEAD  
 (509) 248-0827  
 FAX (509) 452-8704

Primary Standard Certificate of Analysis  
 Method of Analysis Micro GC / Gravimetric  
 Customer: Myren Consulting Reference # PM7234-2  
 P.O.# Cylinder # 250-1175

**Results of Investigation**

<u>Component</u>	<u>Requested</u>	<u>Concentration</u>
Air	N/A	N/A
Argon	N/A	N/A
Carbon Dioxide	21.0%	21.0%
Carbon Monoxide	4.00%	4.03%
Helium	N/A	N/A
Hydrogen	N/A	N/A
Methane	N/A	N/A
Nitrogen	Balance	Balance
Oxygen	21.0%	21.0%

Hazard Class UN 1956  
 DOT Shipping Name Compressed Gas NOS  
 Shipping Volume (scf approximate) 160 scf @ ntp  
 Cylinder Pressure 1500 psig  
 CGA Valve Connection 350

Oxarc Primary Standard mixtures are prepared with gravimetric techniques using weights traceable to NIST. Mixture blended to +/- 1% relative to minor component and certified to +/- 1% analytical accuracy.

Authorized Signature Travis Auger Date 8/25/97  
 Travis Auger

Comments:

## STOVE DESCRIPTION/ QC

The HEAT TECH HTP 26 BAY pellet stove has a bay shape. It uses a top feed auger system to drop pellets down a chute into the burn pot. The operating controls are located on the side and are easy to use.

## CBI

The information in this Section of this test report is considered Confidential Business Information (CBI) and has been redacted and sent under a separate cover to the following address:

EPA CBI Office

Attn: Residential Wood Heater Compliance Program Lead

1200 Pennsylvania Ave. NW

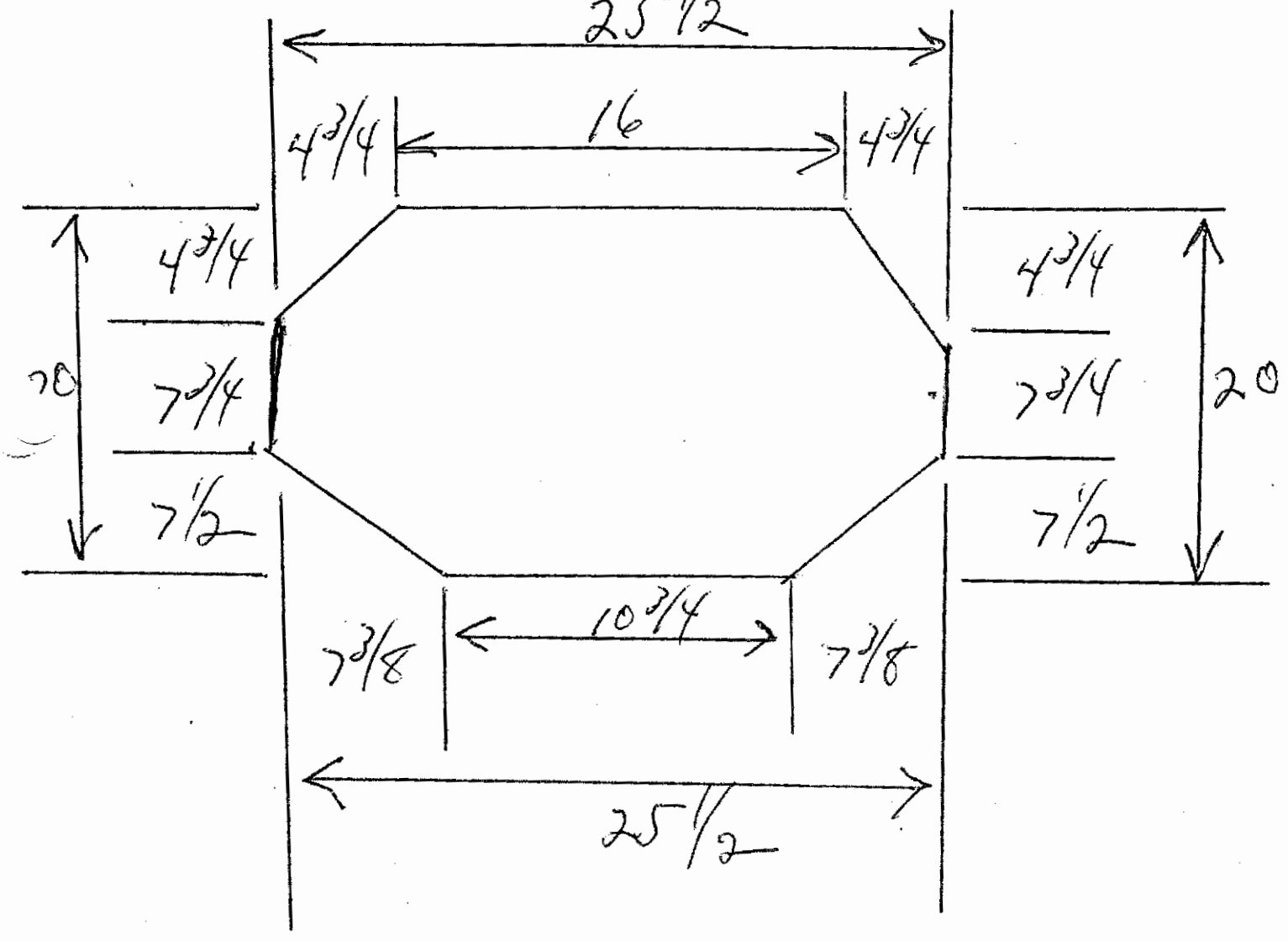
Washington, D.C. 20004

5/06

PELLET BAY

REV. JASE

12 GA.  
25 1/2



NOT TO SCALE

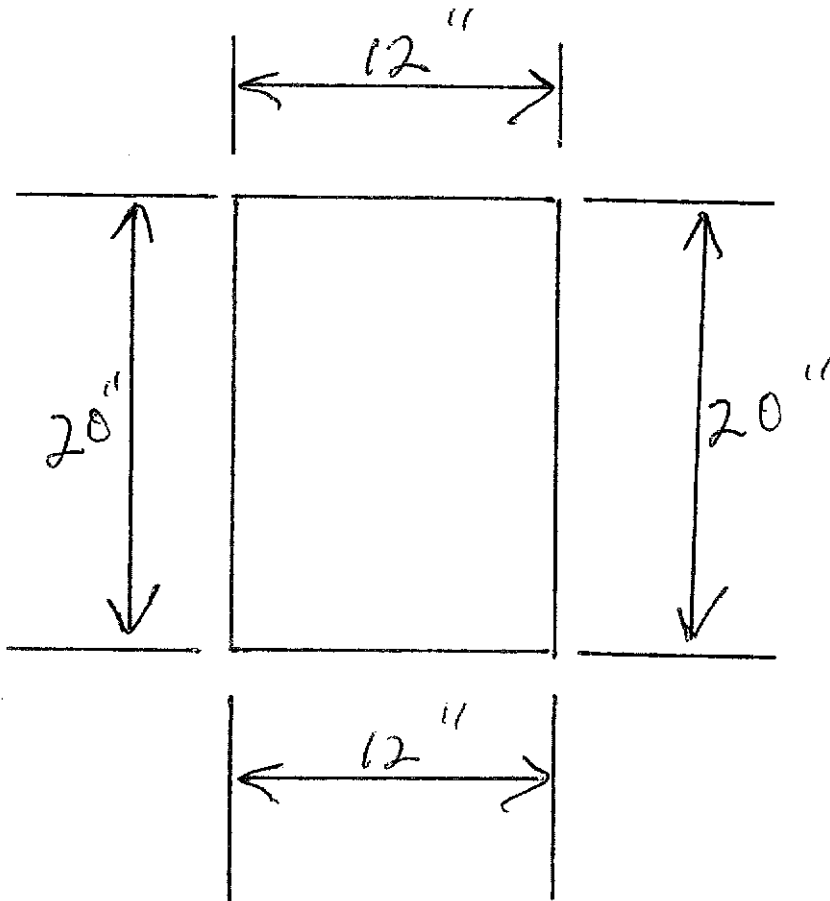
HEAT TECH  
6M 26 BAY  
PELLET

PELLET BAY

5706

PEL. SIDE

16 GA.



NOT TO SCALE

HEAT TECH  
GM 26 BAY  
PELLET

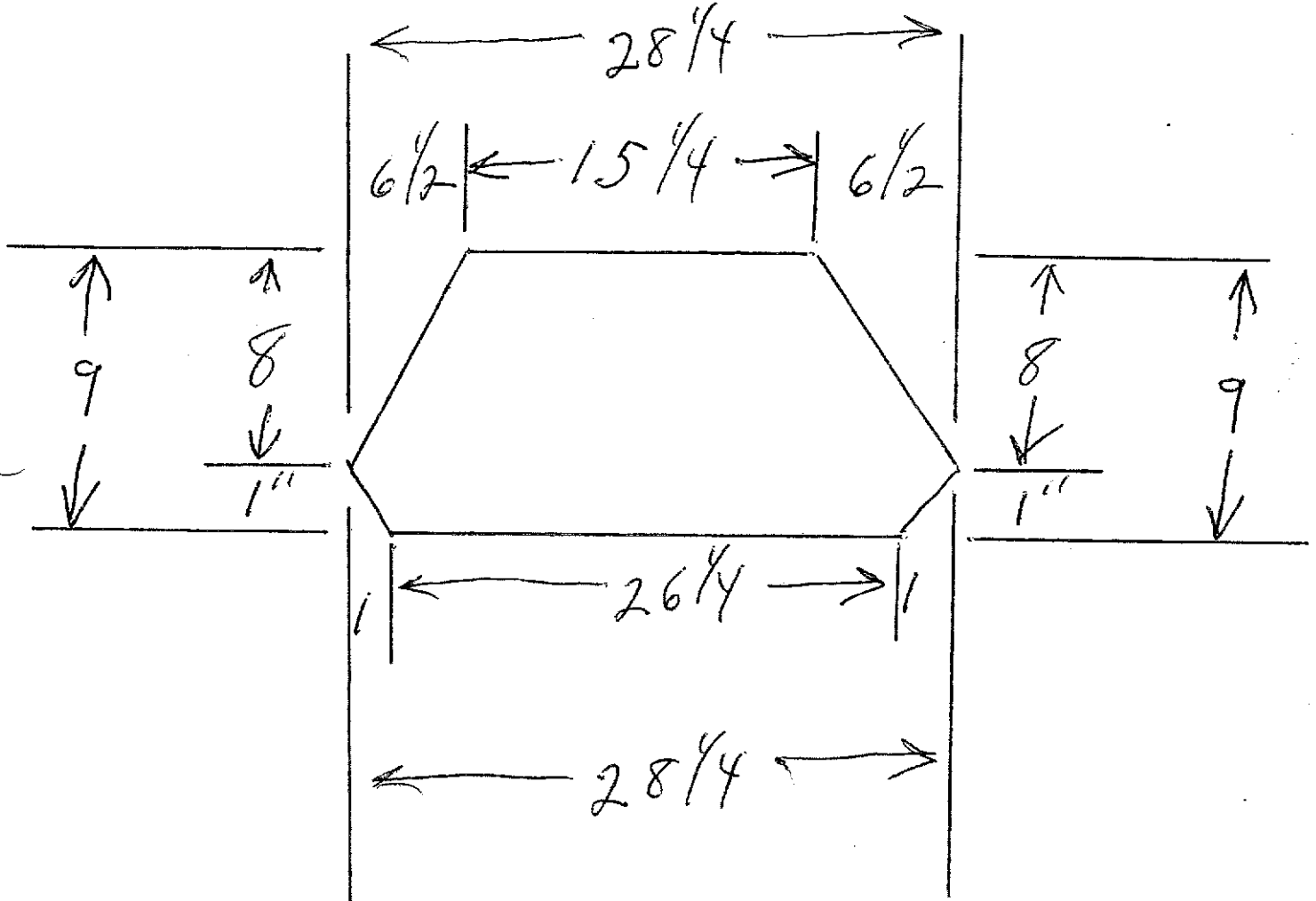


PELLET BAY

5/06

FRONT TOP

12 GA. PLT.



NOT TO SCALE

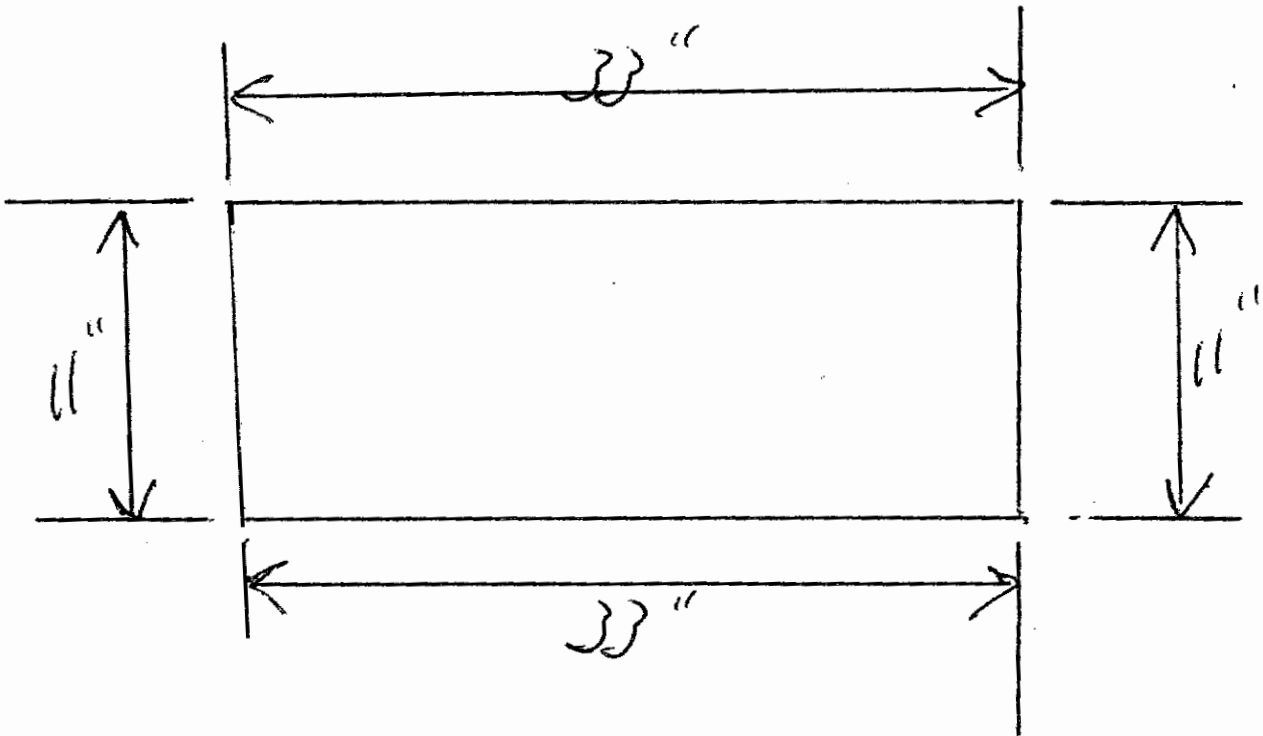
HEAT TECH  
6M 26 BAY  
PELLET

PECKET BAY

5/01

PECKET

16 GA.



NOT TO SCALE

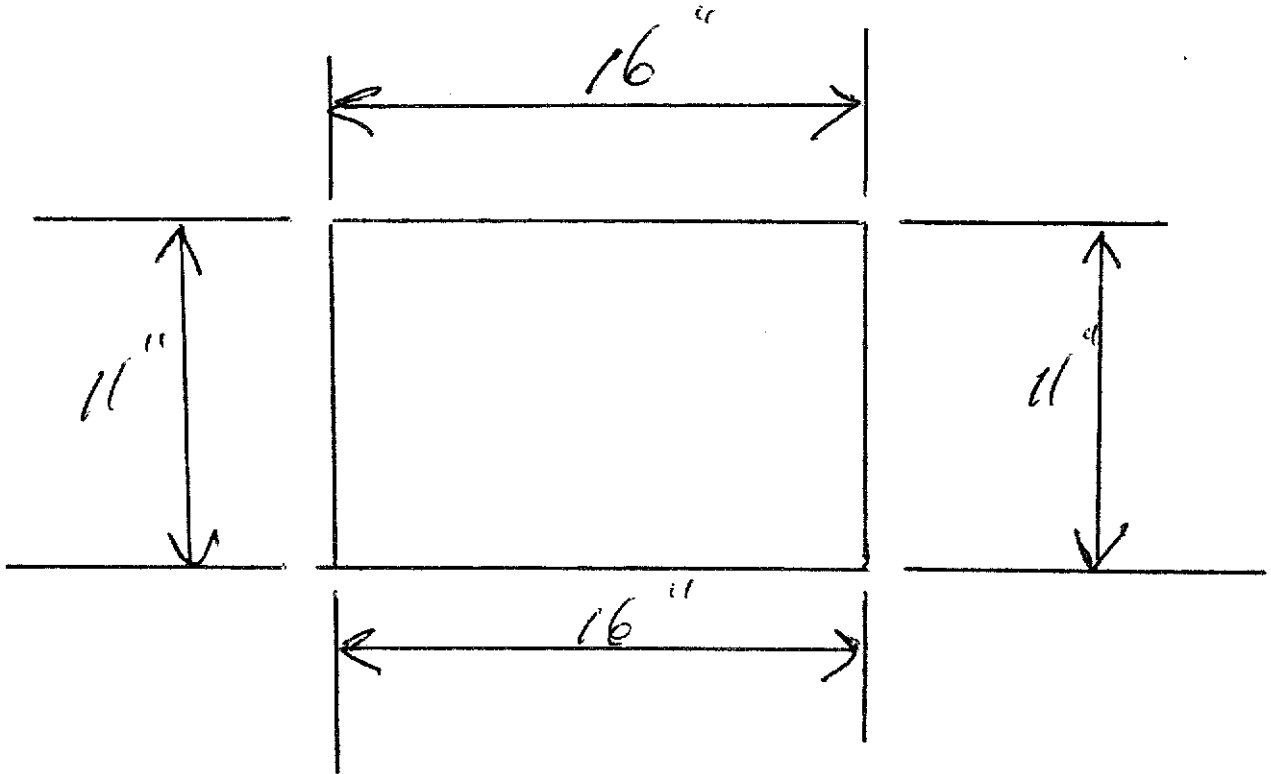
HEAT TECH  
FOR 26 BAY  
PECKET

PERLET BAY

5/06

HOPPER SIDES

16 GA.



NOT TO SCALE

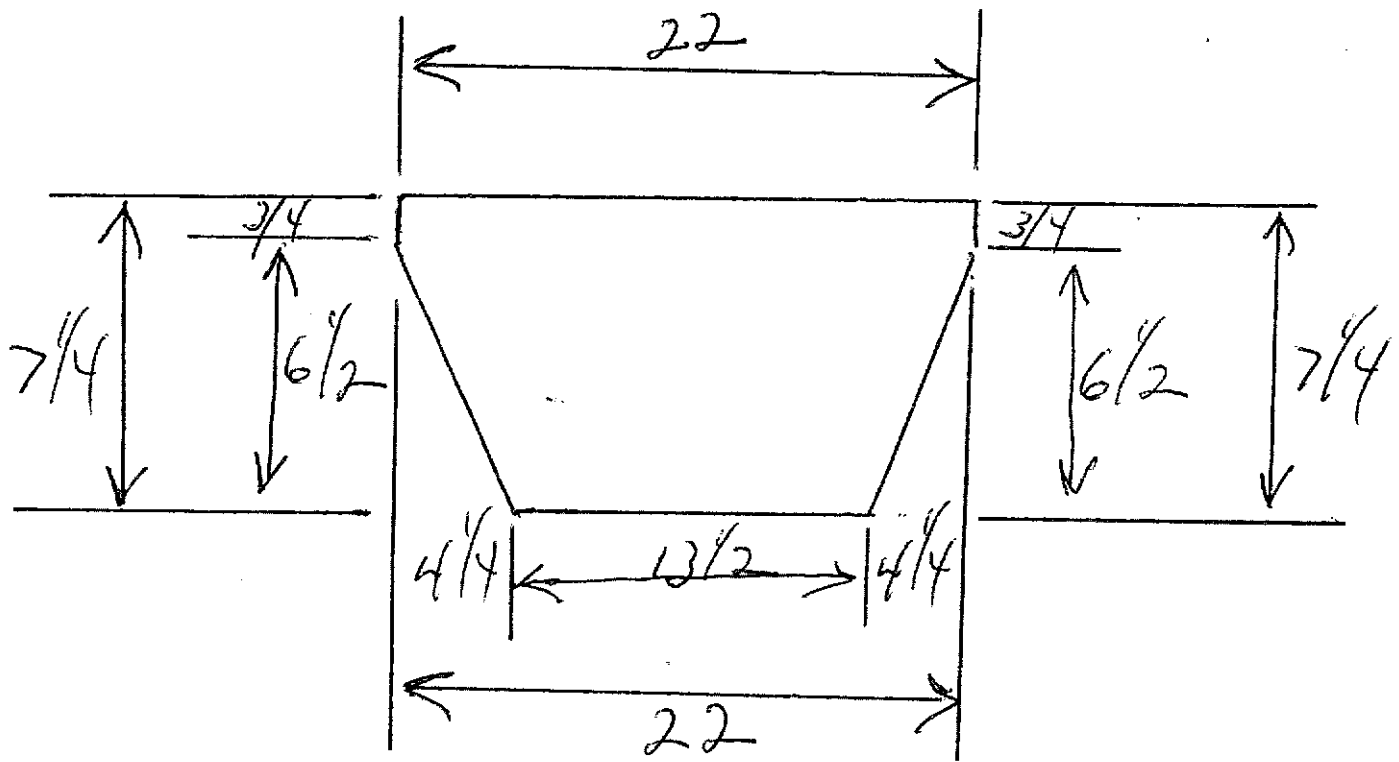
HEAT TREAT  
Q14 26 BAY  
PERLET

PELLET JAY

5/06

HOPPER SHIELD

16 GA.

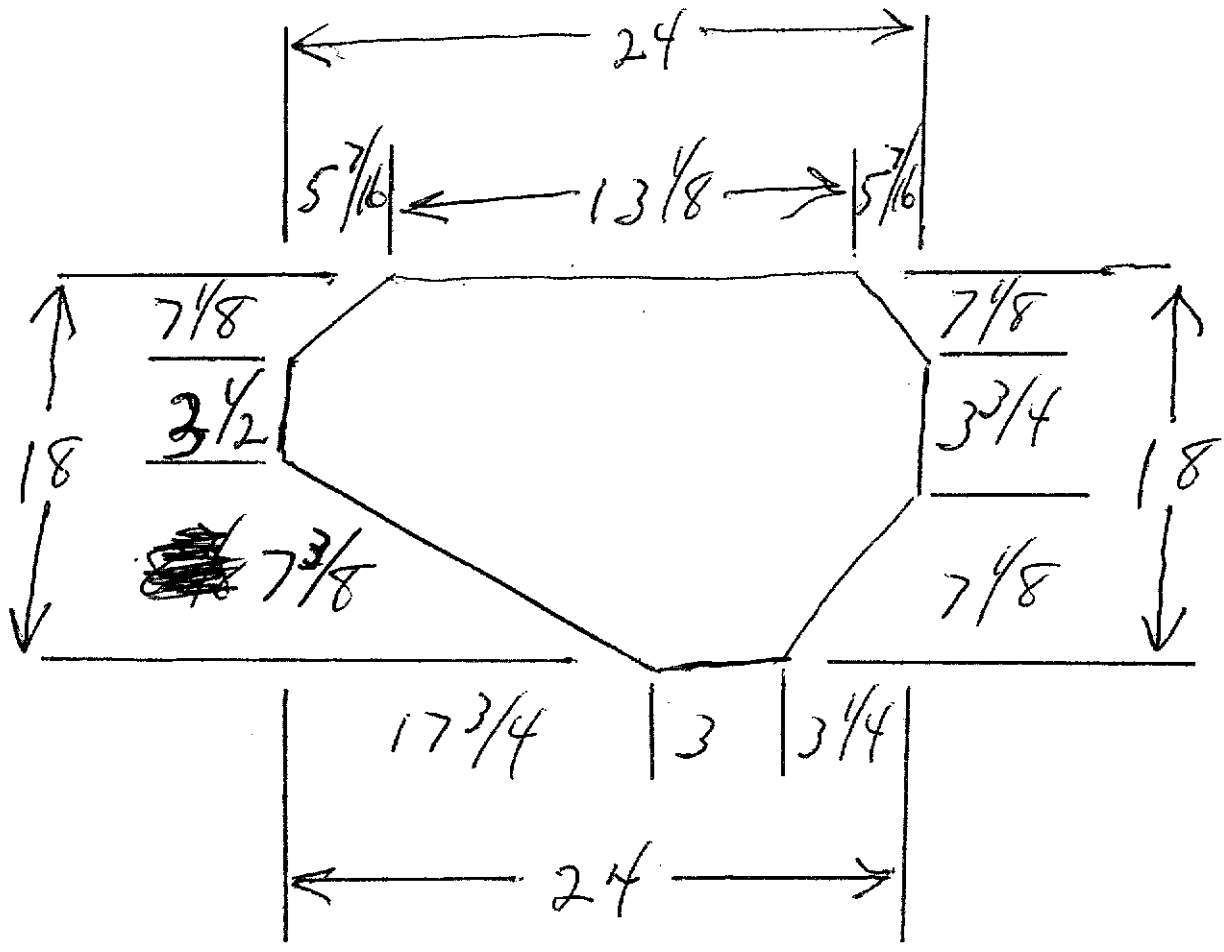


NOT TO SCALE

HEAT BELT  
QM 26 JAY  
PELLET

5/06

PELLET BAY  
FALSE BOTTOM  
12 GA PLT.



NOT TO SCALE

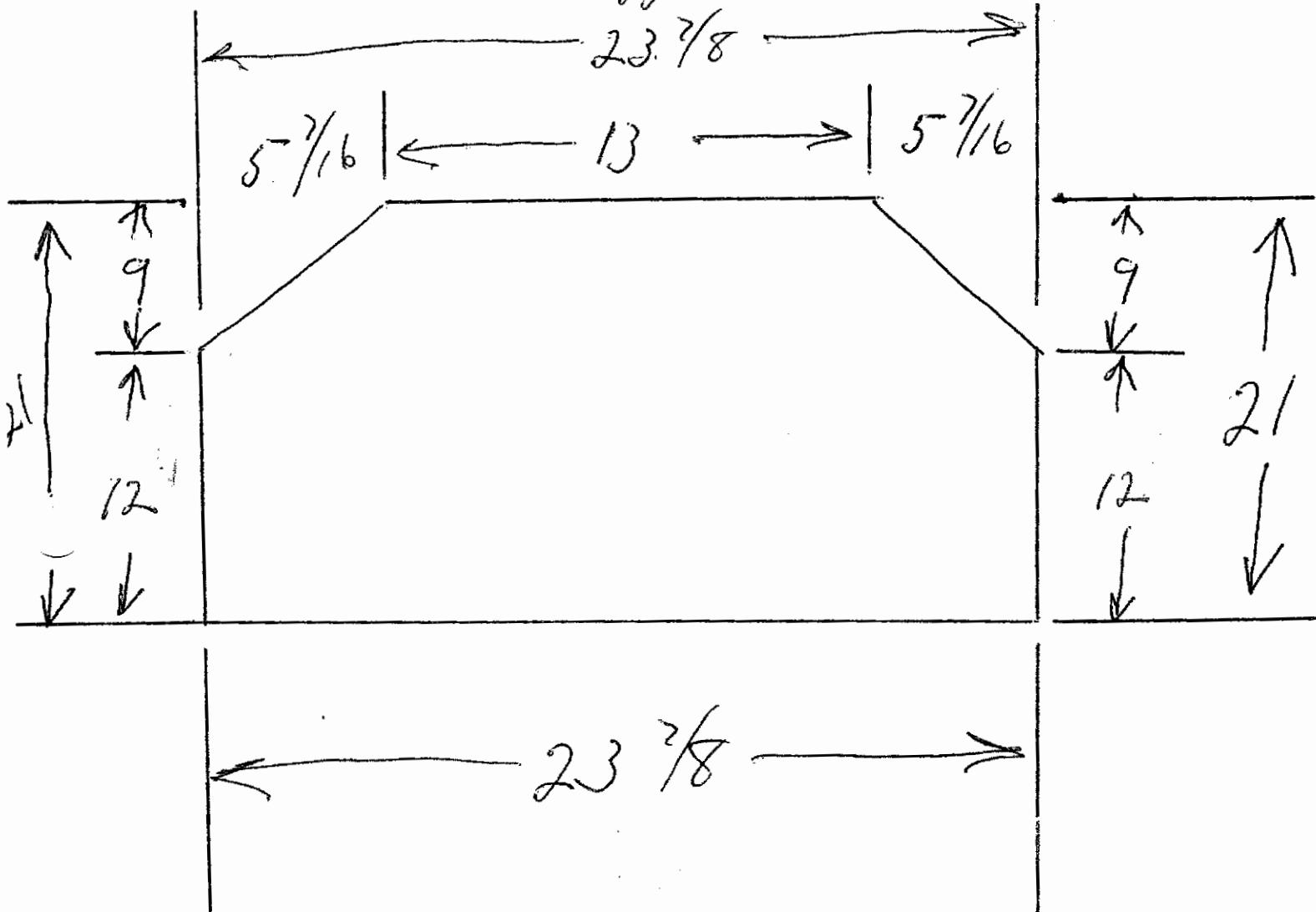
HEAT TECH  
CIR 26 BAY  
PELLET

# PELLET BAY

5/06

AIR CHAMBER

12 GA PLT.



NOT TO SCALE

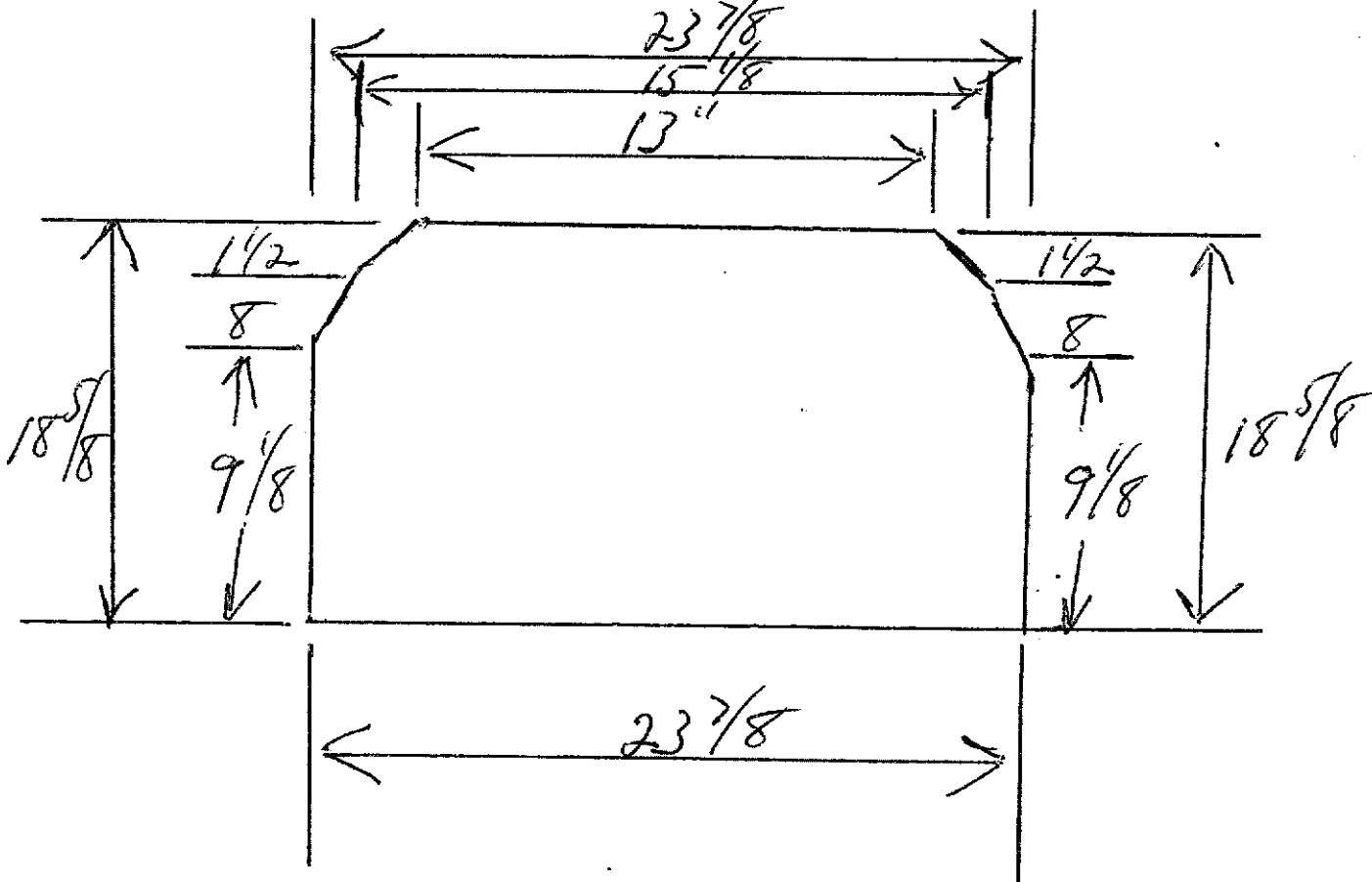
HEAT EXCHANGER  
COM 26 BAY  
PELLET

PELLET JAY

5/06

FIRE BOX

12 GA. PLT

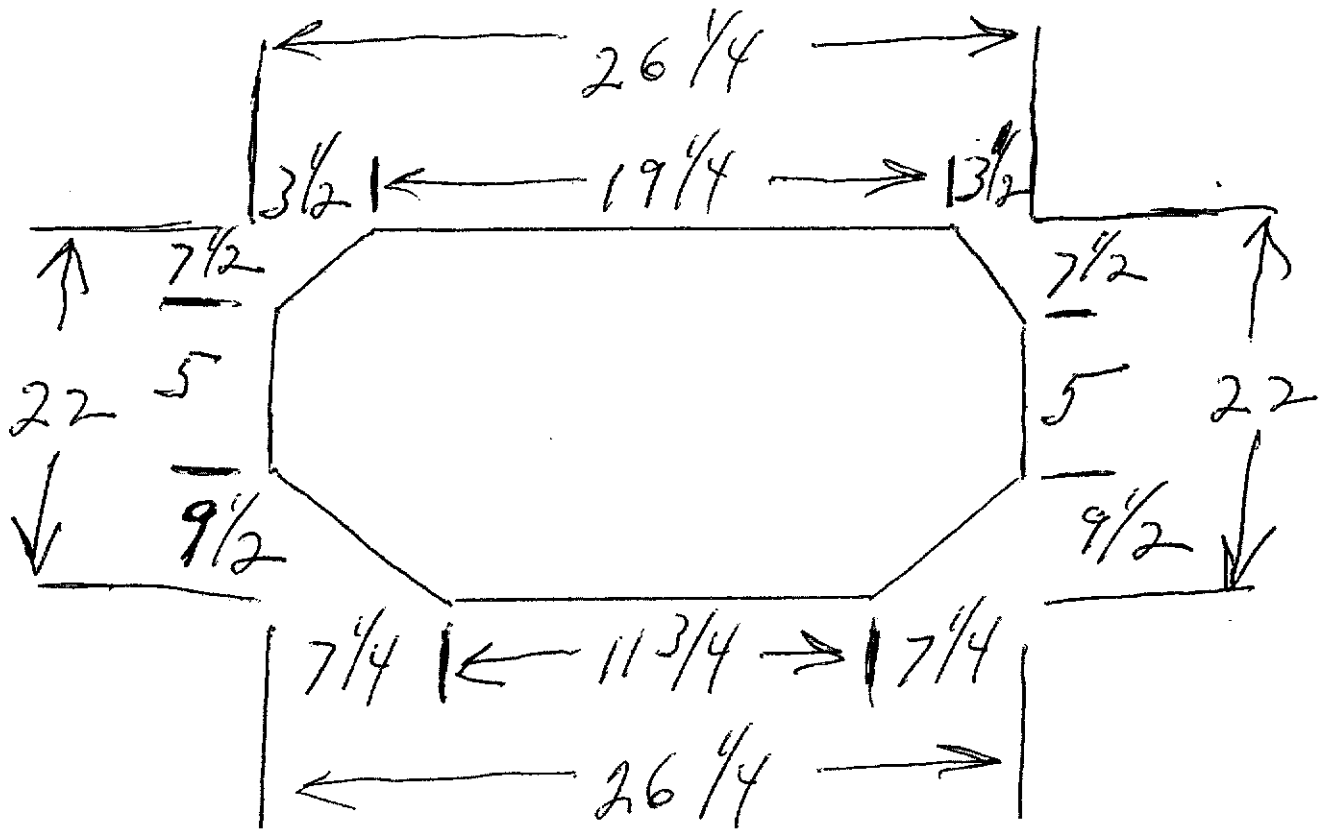


NOT TO SCALE HEATTECH  
GM 26 JAY  
PELLET

# PELLET BAY

Bottom

3/16 PWT



NOT TO SCALE

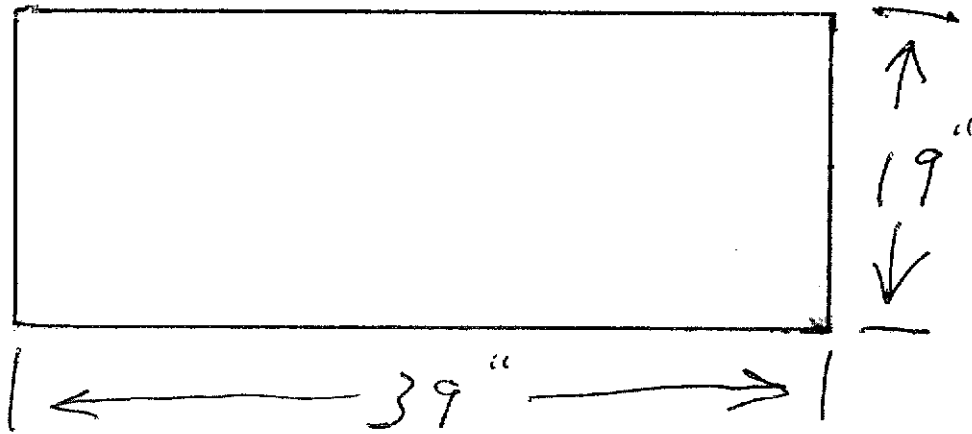
HEAT TECH  
COM 26 BAY  
PELLET



PELLET BAY

Body

10 GA. 19" X 39"



NOT TO SCALE

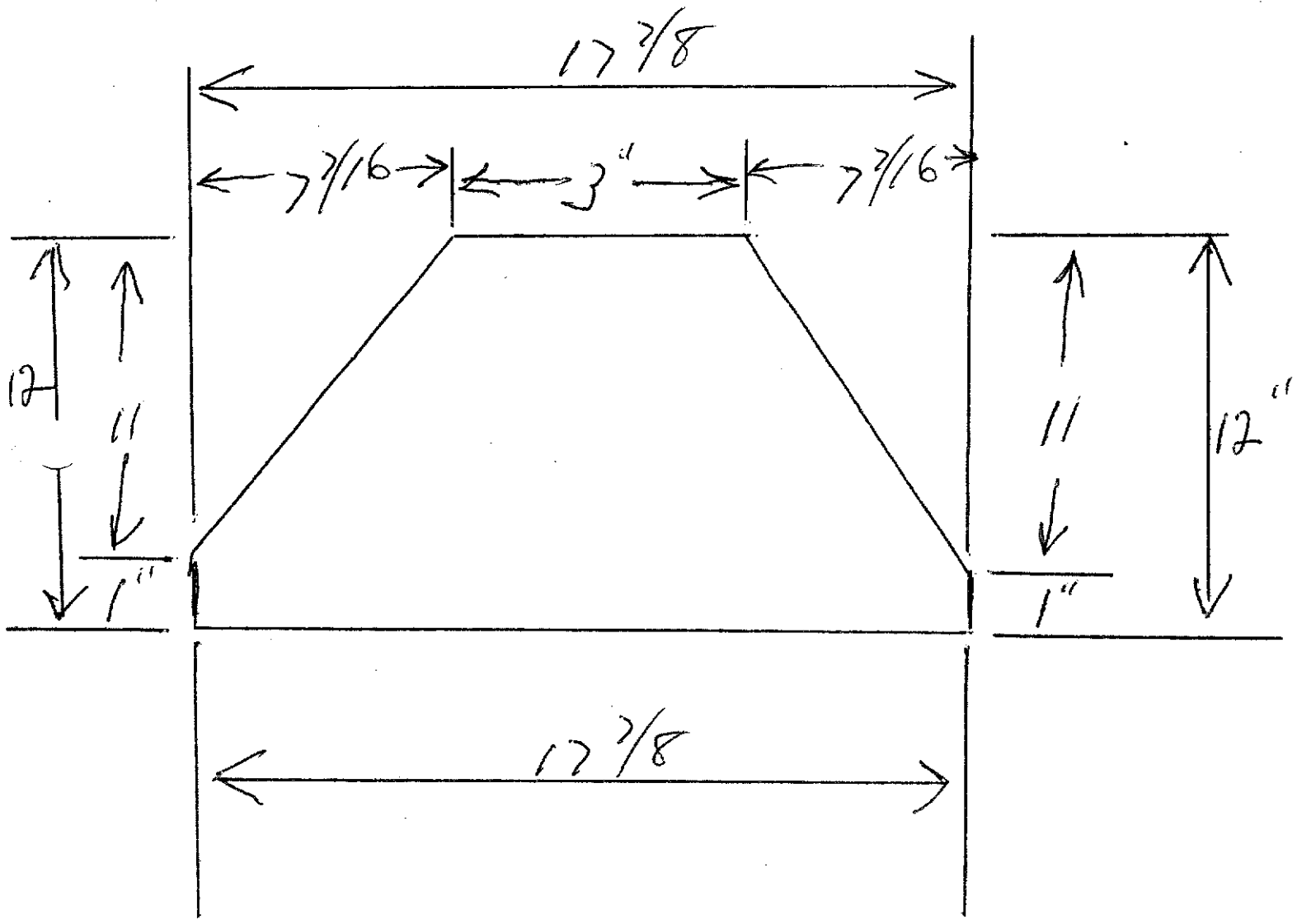
HEAT TREAT  
Q1M 26 BAY  
PELLET

5/06

# PELLET JAY

## HOPPER BACK

16 GA.



NOT TO SCALE

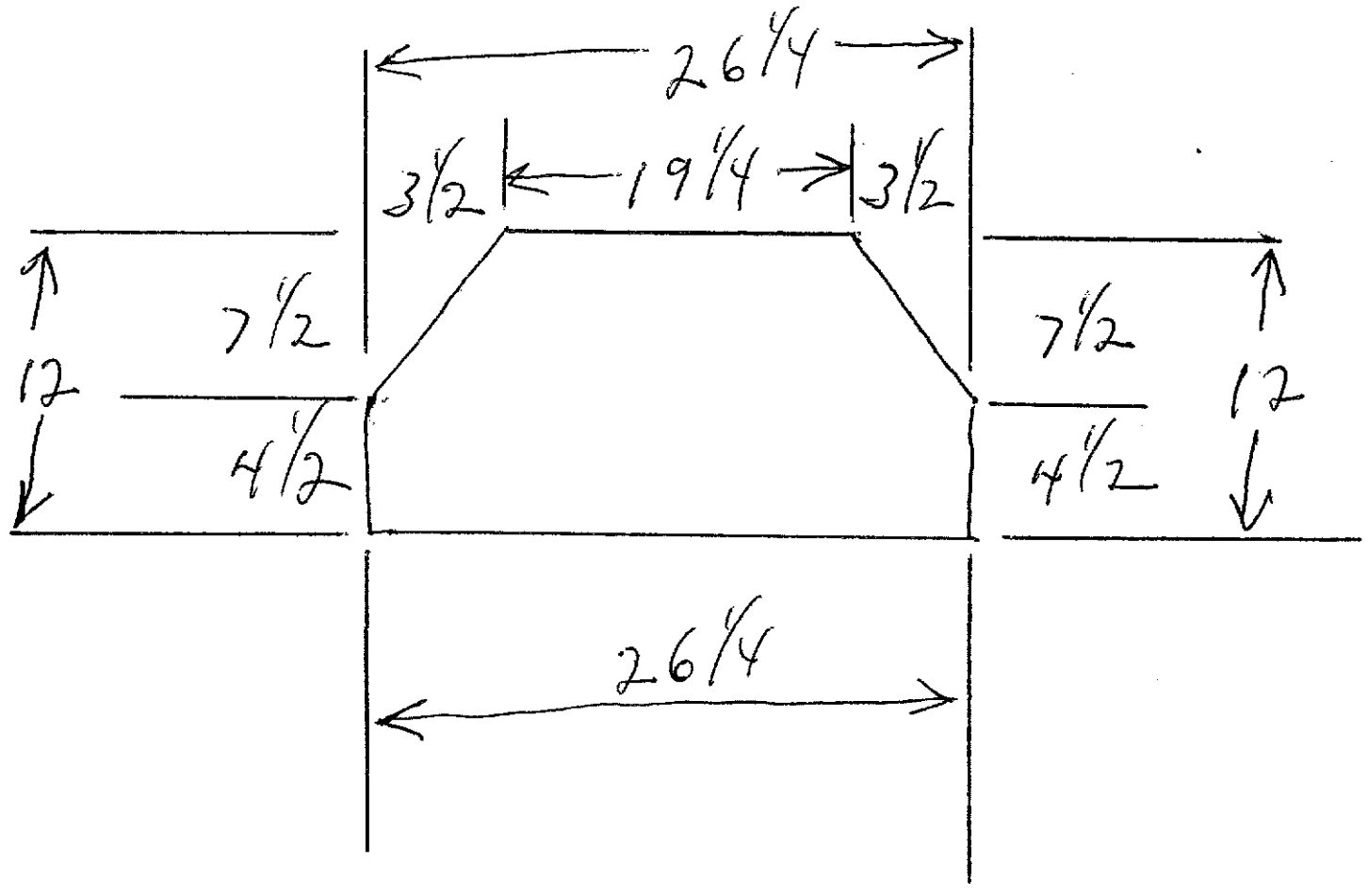
HEAT TREAT  
Q/M 26 JAY  
PELLET

5/06

# PEWEE JAY

REAR TOP

12 GA. PWT



NOT TO SCALE

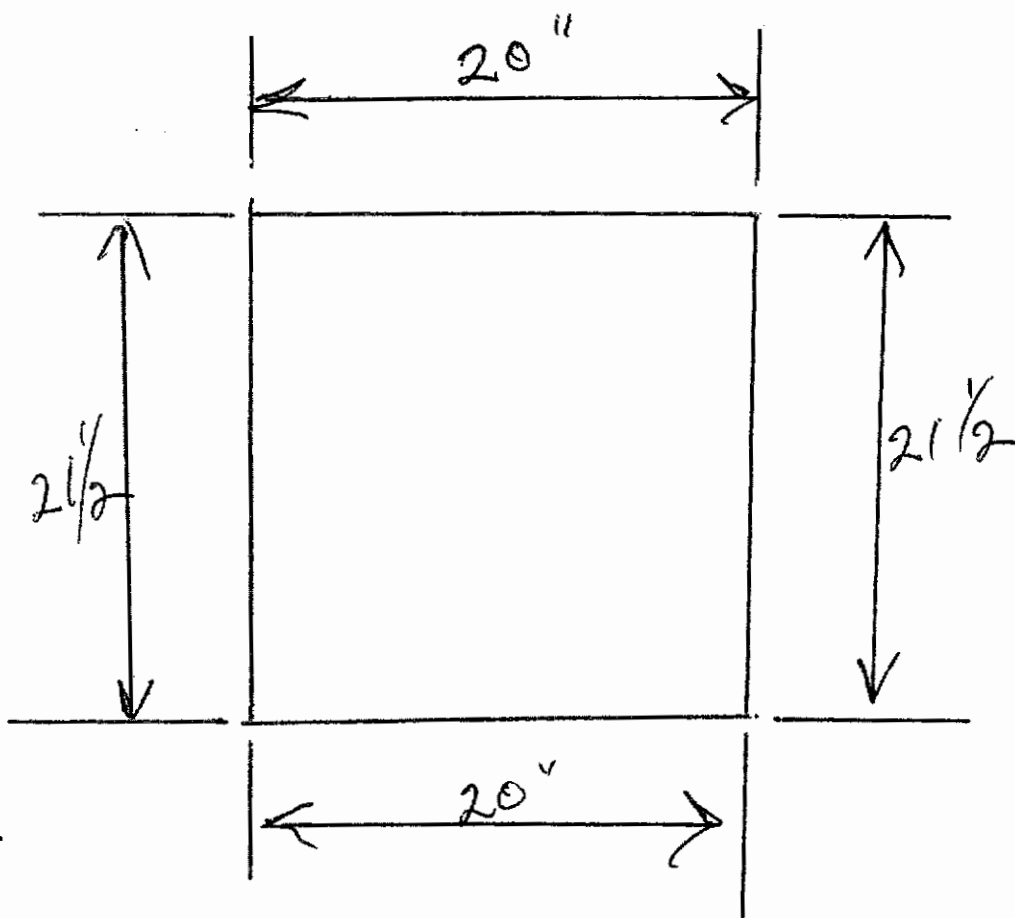
HEAT TECH  
Q/M 26 JAY  
PEWEE

5/06

PELLET BAY

BACK

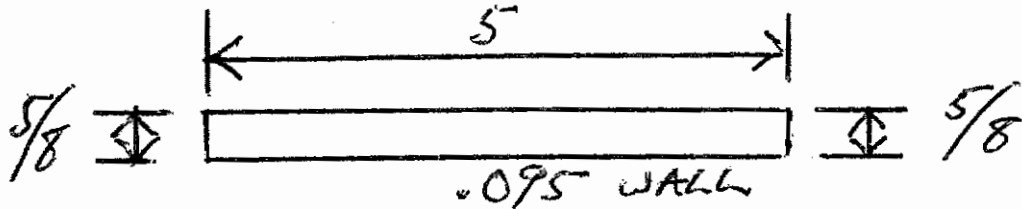
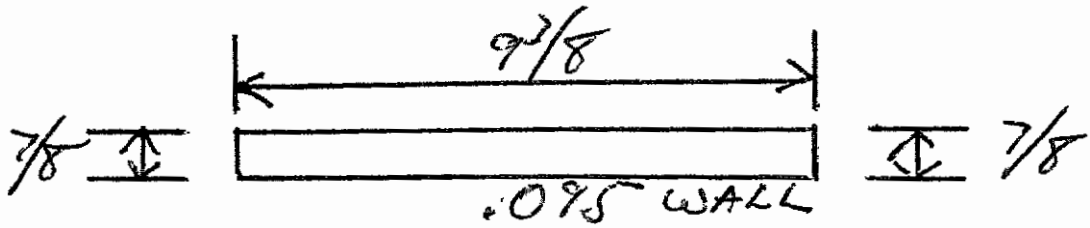
16 GA.



NOT TO SCALE

HEAT TECH  
CM 26 BAY  
PELLET

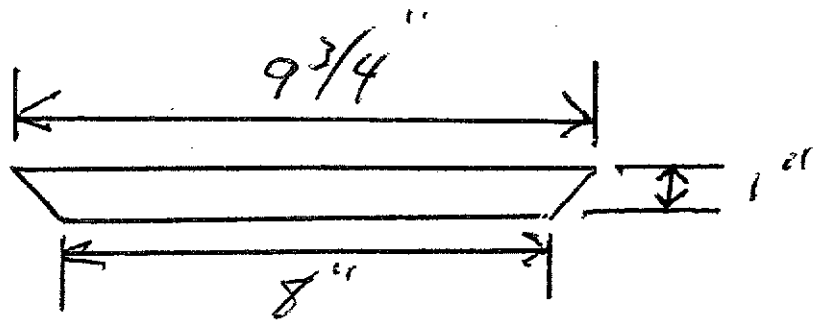
QMP 26 STANDARD PELLET  
BAY



IGNITOR TUBE (OUTER)  
IGNITOR TUBE (INNER)

HEAT TECH  
QMP 26 STANDARD  
IGNITOR TUBE  
10-25-15  
NOT TO SCALE

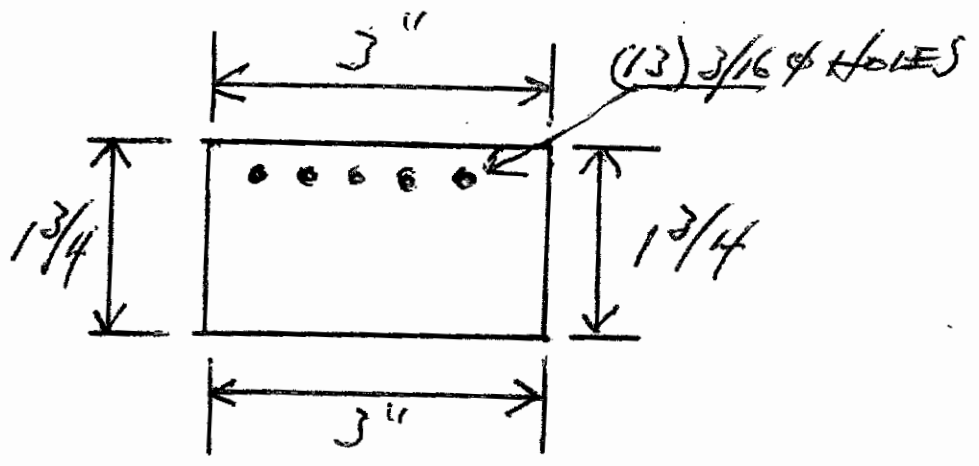
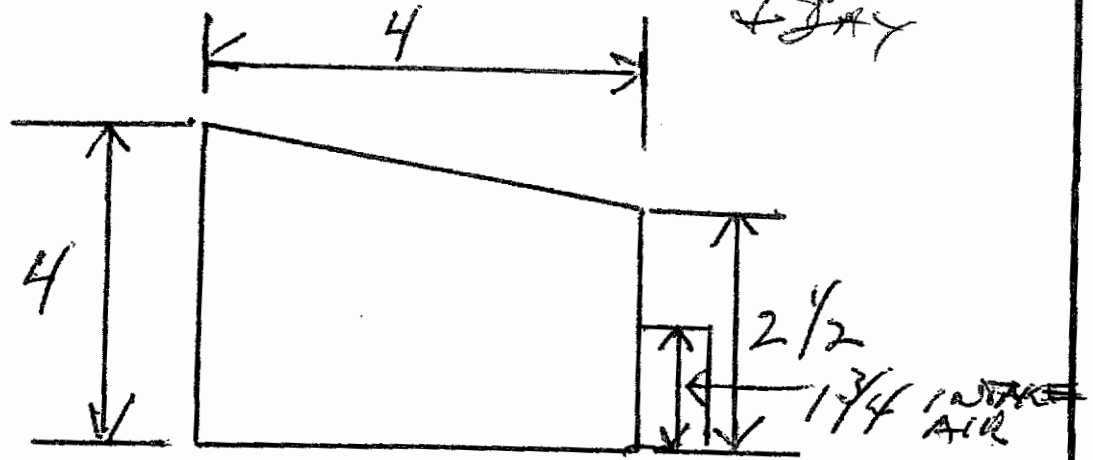
Comp 26 STANDARD PELLET  
+  
RAY



HEAT EXCHANGE TUBE  
1" Ø .065 WALL

10-25-15  
HEAT TECH  
COMP 26 STANDARD  
HEAT EXCHANGE  
TUBE  
NOT TO SCALE

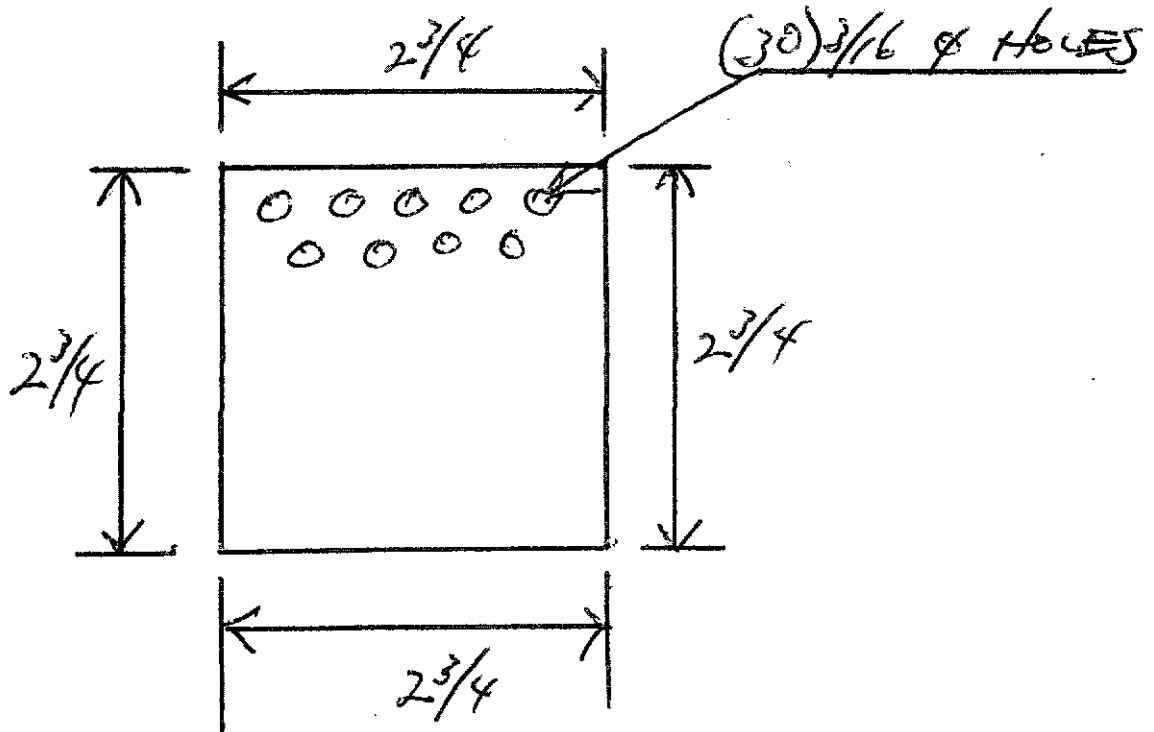
COMP 26 STANDARD RECLET  
 + JAY



BURN POT  
 OUTER BOX 4"  $\phi$  TUBE .065  
 INNER LINER 3" SS.  $\phi$  TUBE  
 .065

HEAT TECH  
 COMP STANDARD  
 BURN POT  
 10-25-15  
 NOT TO SCALE

COMP 26 STANDARD PELLET  
+  
GAY

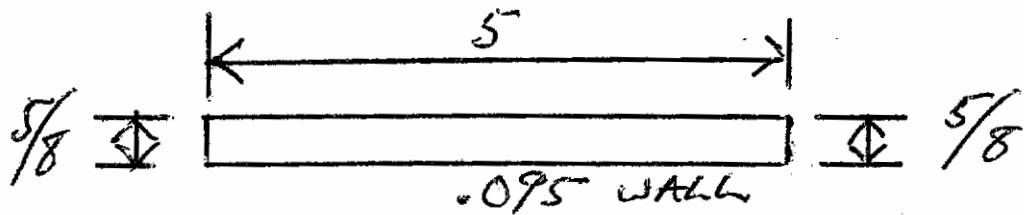
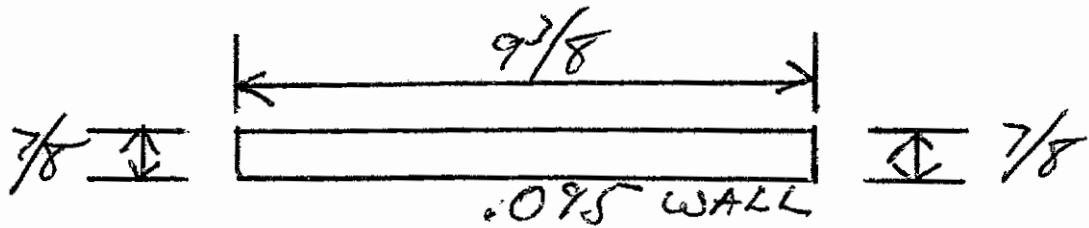


BURN POT BOTTOM PLT.  
 $2\frac{3}{4}$  S.S.  
12 GA.

HEAT TECH  
COMP 26 STANDARD  
BURN POT BOTTOM PLT.  
10-25-15  
NOT TO SCALE



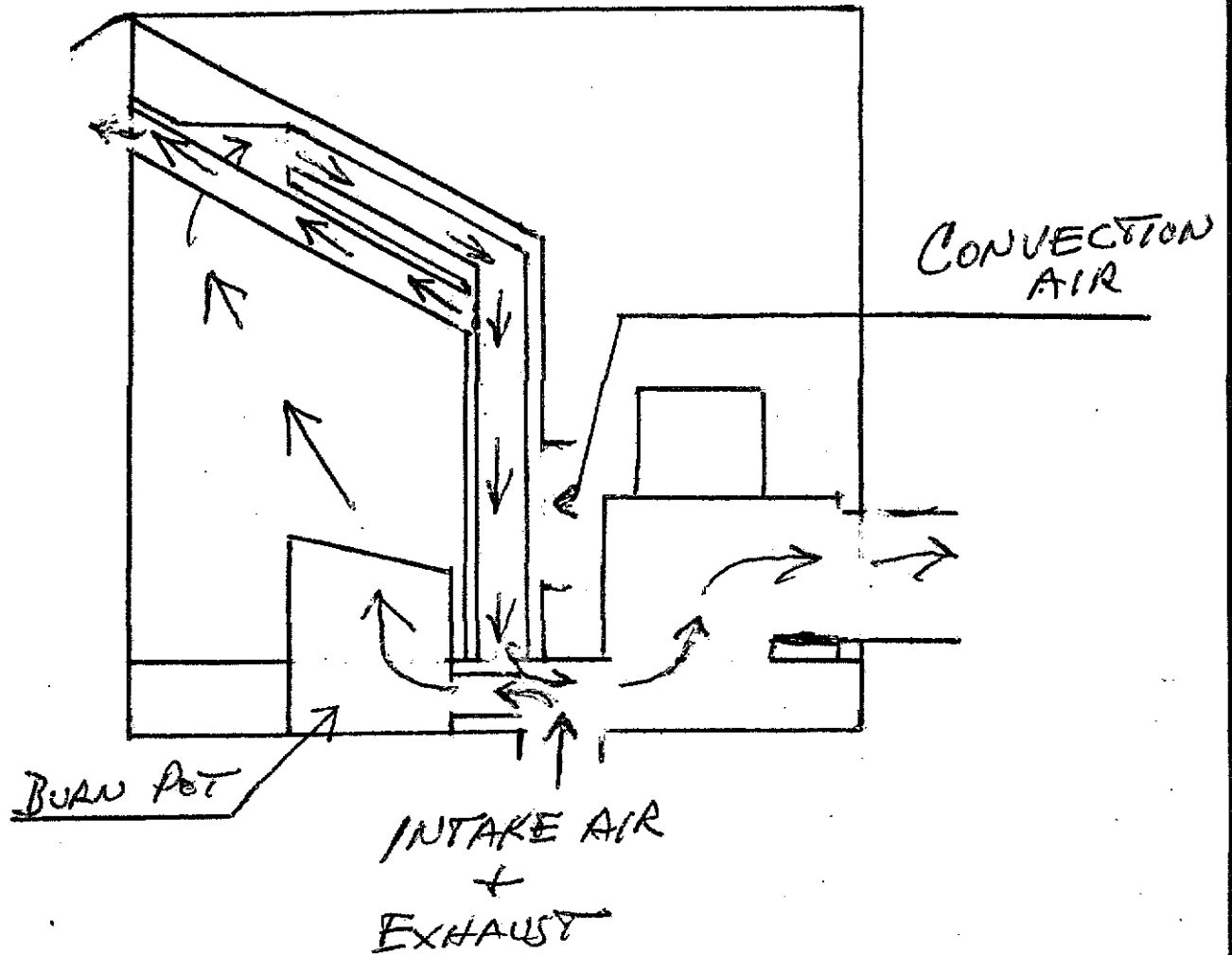
QMP 26 STANDARD PELLET  
BAY



IGNITOR TUBE (OUTER)  
IGNITOR TUBE (INNER)

HEAT TECH  
QMP 26 STANDARD  
IGNITOR TUBE  
10-25-15  
NOT TO SCALE

Comp 26 STANDARD PELLET  
+ JAY



HEAT TECH  
Comp 26 STANDARD  
AIR FLOW (SIDE VIEW)  
10-25-15  
NOT TO SCALE



WOODSTOVE DATA SHEET # 30  
STOVE STORAGE

The Heat Tech HTP 26 Bay Pellet stove tested by Myren Consulting, Inc. is being held in custody by:

Heat Tech  
PO Box 727  
Biggs, Ca 95917

Phone 530 846 1985

Contact: Tom Bassett

Heat Tech  
867 Hiway 99  
Gridley, CA 95948

The unit was tested at Myren Consulting's lab in Colville, WA. It was sealed on 7/29/15 after the unit had cooled after testing. The following page contains photos taken after the unit was sealed on 7/29/15.

The unit was sealed with several lengths of metal banding/strapping that were placed around the stove in a manner that prevents the door from being opened. At least two of these straps cross at 90° angles. At one or more of these crossings on the stove a label that clearly identifies the unit as a sealed EPA test stove and/ or a Myren Consulting, Inc. address label is placed over the crossing and taped into place with 2" clear packing tape. The stove was also loaded onto a pallet and strapped to a pallet for transport back to Heat Tech and to its final storage location. A sample stove storage label follows this page.

Once the unit is/ was certified by EPA, the unit will be returned to Heat Tech via common carries;

Carrier: \_\_\_\_\_

Shipped on: \_\_\_\_\_

WST5-Form11

W A R N I N G

SEALED EPA TEST STOVE

DO NOT OPEN OR TAMPER WITH THE SEALS AND PACKAGING ON THIS STOVE.

TO DO SO WILL VOID THE CERTIFICATION ON THIS STOVE.

HEAT TECH HTP 26 BAY

WST5-Form11

W A R N I N G

SEALED EPA TEST STOVE

DO NOT OPEN OR TAMPER WITH THE SEALS AND PACKAGING ON THIS STOVE.

TO DO SO WILL VOID THE CERTIFICATION ON THIS STOVE.

HEAT TECH HTP 26 BAY

